

Slip flow past a gas–liquid interface with embedded solid particles

A. Vidal¹ and L. Botto^{1,†}

¹School of Engineering and Materials Science, Queen Mary University of London,
Mile End Road, London E1 4NS, UK

(Received 23 June 2016; revised 6 December 2016; accepted 6 December 2016;
first published online 17 January 2017)

We simulate shear flow past a stationary monolayer of spherical particles embedded in a flat gas–liquid interface. This problem is relevant to the understanding of the microhydrodynamics of particle-laden interfacial structures, including particle-laden drops, bubbles and foams. The combination of the free-shear condition at the gas–liquid interface and the no-slip condition at the particle surfaces gives rise to a velocity slip at the particle-laden interface. We study the characteristics of the flow near the monolayer, focusing on slip velocity, slip length and interfacial shear stress. Two microstructures are compared: a square array, and a reticulated array mimicking a percolating network of aggregated particles. We demonstrate that the scaling laws for the dependence of the slip length on solid area fraction developed for flow past superhydrophobic microstructured surfaces apply to the case of interfacial particles. The calculated slip lengths are in general smaller than those reported for microstructured superhydrophobic surfaces. This difference, which is due to the significant protrusion of the spherical particles in the liquid, can be accounted for in the case of the square array by an approximate argument. For a given area fraction, the reticulated array yields a larger slip length than the square array. We analyse the hydrodynamic forces acting on the particles, and the corresponding tangential stress exerted by the bulk ‘subphase’.

Key words: colloids, drops, multiphase flow

1. Introduction

In applications and natural settings, gas–liquid interfaces are often found covered with particulate material. Fouling of gas–liquid interfaces can occur in unsaturated porous media or environmental bubbly flows, owing to the presence of fine grains and biocolloids that adhere to the fluid interface (Weber, Blanchard & Syzdek 1983; Shang, Flury & Deng 2009). In applications, rigid particles or globular proteins are often added as surface-active agents to change the mechanical properties of the interface or induce stabilisation against coalescence (Tambe & Sharma 1994; Binks 2002; Stancik, Kouhkan & Fuller 2004).

As for molecular surfactants, the presence of the embedded solid particles alters the boundary conditions at a fluid interface; for experimental evidence, see e.g. Hunter

† Email address for correspondence: l.botto@qmul.ac.uk

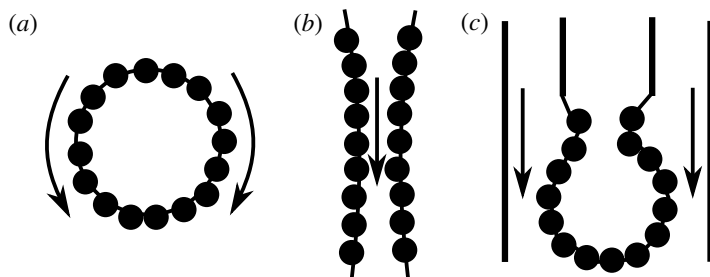


FIGURE 1. Examples of flow problems involving gas–liquid particle-laden interfaces where significant particle–fluid velocity slip is expected: (a) a rising particle-coated bubble (Weber *et al.* 1983); (b) liquid drainage in particle-laden thin films (Stancik *et al.* 2004; Hunter *et al.* 2008; Bournival, Ata & Wanless 2015); and (c) formation of particle-coated bubbles in a microfluidic device (Subramaniam, Abkarian & Stone 2005; Kotula & Anna 2012).

et al. (2008) and Kotula & Anna (2012); for a theoretical analysis, see Deemer & Slattery (1978). These boundary conditions for the bulk fluid are to be applied to the particle-laden fluid interface, i.e. the composite interface formed by the particles and the fluid interface in which the particles are embedded. In the absence of mass transfer effects, the no-penetration condition at the particle-laden interface is expected to hold with good accuracy. However, the boundary condition for the velocity tangential to the particle-laden fluid interface must be modified to account for the additional resistance caused by the presence of the particles to the motion of the adjacent fluid layers. This additional resistance is expected to be particularly significant when a significant velocity difference occurs between the particle-laden fluid interface and the adjacent fluid (figure 1).

In this paper we simulate shear flow past a gas–liquid interface containing a monolayer of spherical particles, for the case in which the particle-laden fluid interface is flat and the monolayer is stationary (or moving with constant velocity if a change of reference frame is accounted for). All the simulations are carried out in the Stokes flow limit. The simulation results allow one to gain insights into the dependence of the slip length parameter appearing in a partial slip boundary condition for the particle-laden interface on the macroscopic flow variables and particle distribution. Such a boundary condition could be applied to problems related to froth flotation (Subrahmanyam & Forssberg 1988), solid stabilised foams and emulsions (Horozov 2008; Martinez *et al.* 2008) and spray drying (Tsapis *et al.* 2005).

Recently, the statics and dynamics of particles embedded in fluid interfaces has been subject to increasing interest. Singh & Joseph (2005) studied the equilibrium condition for particles supported by surface tension at a horizontal fluid interface, as a function of particle weight and contact angle. Under the effect of gravity, particles induce a distortion of the fluid interface whose amplitude is proportional to the magnitude of the particle weight. For particles in the size range of typical colloids ($a < 10\ \mu\text{m}$), the particle weight is orders of magnitude smaller than the capillary force on the particle. As a consequence, the interface around the particle can be considered locally flat and unaffected by the gravitational force acting on the particle. This notion can be generalised to non-horizontal particle-laden interfaces. For curved particle-laden fluid interfaces, the composite interface can be considered locally flat if the particle radius is small in comparison to the radius of curvature of the particle-laden interface. For a

locally flat interface, the degree of protrusion of a solid particle in the liquid phase is a function of only the contact angle θ_c and the particle radius (Rapacchietta & Neumann 1977).

The drag forces on single spheres embedded in fluid–fluid interfaces has been studied by several authors. For gas–liquid interfaces, the drag force is a monotonic function of the degree of protrusion of the particle in the liquid phase (Petkov *et al.* 1995; Danov, Dimova & Pouligny 2000; Fischer, Dhar & Heinig 2006). When $\theta_c = 90^\circ$, owing to symmetry, the drag on an isolated sphere in a uniform flow is exactly half the Stokes drag for a fully immersed sphere. A particle embedded in a gas–liquid interface and subject to a shear flow will also experience a hydrodynamic torque and may rotate (Pozrikidis 2007). However, effects due to rotation, which depend on the shear rate, are expected to be subdominant with respect to those due to relative translation between the particle and the surrounding fluid; for small particles contact line pinning may prevent rotation completely, and this is a situation often found in practice (Dörr *et al.* 2016). Only a few studies have investigated the hydrodynamics of multiple interfacial particles. These studies are typically concerned with the dynamics of small clusters of particles (Singh & Joseph 2005; Dani *et al.* 2015), or the macroscopic effect of the collective motion of many particles on the dynamics of liquid–liquid interfacial structures (Frijters, Günther & Harting 2012). To the best of our knowledge, the interfacial drag on multiple particles subject to shear flow and the characteristics of the slip flow for this flow configuration have not been considered in the literature.

The flow past a stationary monolayer of spheres embedded in a gas–liquid interface bears obvious similarities to flow past a microstructured superhydrophobic surface. In both cases one can define a composite surface composed of free-slip and no-slip ‘patches’. From the point of view of continuum modelling, i.e. considering flow variables on a scale much larger than the particles, the boundary condition at such a composite surface is expected to be a linear combination of the boundary conditions that are appropriate for the solid and fluid regions. Composite free-slip/no-slip interfaces indeed have been successfully modelled through a Navier slip boundary condition

$$\lambda \langle \dot{\gamma} \rangle_s = \langle u \rangle_s, \quad (1.1)$$

where $\langle \dot{\gamma} \rangle_s$ is the bulk shear rate at the interface, $\langle u \rangle_s$ is the interfacial slip velocity and λ is the slip length. For superhydrophobic surfaces, the dependence of λ on the geometry of the microstructure has been studied extensively (Rothstein 2010): λ is a function of the size of the microstructural elements, the area fraction covered by the solid and the arrangement of the microstructural elements in the slip plane (Lauga & Stone 2003; Sbragaglia & Prosperetti 2007; Ybert *et al.* 2007; Ng & Wang 2009). In this paper we investigate the suitability of boundary condition (1.1) for flat particle-laden gas–liquid interfaces; results for flat interfaces are relevant to flow situations in which the radius of curvature of the interface is much larger than the characteristic particle radius. We characterise the slip flow past a monolayer of stationary spherical particles for a specific contact angle, $\theta_c = 90^\circ$, and investigate the dependence of λ on relevant parameters for two cases: a square array, and a reticulated array in which the particles are distributed according to a mesh-like arrangement. These two cases are idealisations of two limiting cases found in practice (Aveyard *et al.* 2000) of monolayers constituted by particles well dispersed in the interface due to interparticle repulsion, and monolayers constituted by particles forming two-dimensional percolating networks due to particle–particle attraction, respectively.

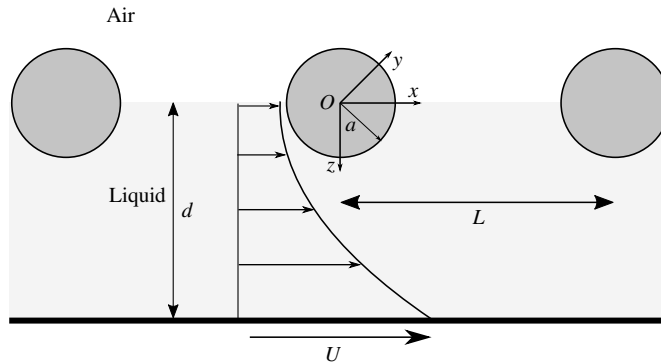


FIGURE 2. We simulate a stationary monolayer of particles half-immersed in a flat gas–liquid interface. The fluid is sheared by a moving wall located at a distance d from the monolayer and moving with constant velocity U . For large values of d our results converge to the asymptotic limit in which the flow near the monolayer depends on the macroscopic shear rate induced by the moving wall, but not on d directly.

The neutrally wetting case $\theta_c = 90^\circ$ studied here has practical relevance. In applications it is indeed desirable to have a contact angle close to 90° , as this limiting angle gives the strongest adhesion of the particle to the interface against desorption in either of the two adjacent fluids (Binks & Horozov 2006).

2. Problem formulation

We model shear flow past a stationary monolayer of spherical particles of radius a embedded in a flat air–liquid interface for a contact angle of 90° (figure 2). The fluid is set in motion by a flat wall located at a distance d from the monolayer and translating with velocity U with respect to the spheres. For large values of d , the liquid can be considered to be bounded by the particle-laden interface only. In this limit we obtain asymptotic results that depend on the macroscopic bulk shear rate, and not on d directly.

To simulate the flow configuration described above, we employ an expedient that allows us to use a fast solver for finite size particles in bulk flows to simulate a particle-laden gas–liquid interface. We simulate the flow past a monolayer of spherical particles completely embedded in the liquid and placed at the centre of a two-dimensional channel. The channel walls translate parallel to the monolayer with velocity U . Because the air–water free-shear interface is a plane of symmetry for the flow, the flow below the monolayer with the fully immersed particles is identical to the flow in which the particles are half-immersed in a liquid domain bounded from the top by the air–water interface (Dörr & Hardt 2015). The use of this expedient enables us to use a fast and accurate fixed-grid method for fully resolved particles, Physalis (Zhang & Prosperetti 2005; Sierakowski 2016), to simulate at a reasonable computational cost many particles embedded in a gas–liquid interface.

Following recent work on particles at interfaces (Dörr & Hardt 2015; Dörr *et al.* 2016), we neglect the rotation of the particles. This assumption holds when the viscous dissipation due to the rotation of the particles is negligible in comparison to the dissipation due to the particle–fluid velocity difference (Dörr *et al.* 2016) or when the motion of the contact line is hindered due to pinning of the contact line

at roughness elements or chemical heterogeneities (Dörr & Hardt 2015; Dörr *et al.* 2016). The maximum pinning force per unit length of contact line is approximately equal to $\sigma\Delta$, where σ is the surface tension of the air–liquid interface and Δ is the difference between the cosines of the advancing and receding contact angles (De Gennes 1985). The parameter Δ is often not negligible (the difference between the advancing and receding contact angles is often larger than 10° ; see e.g. Lewandowski *et al.* (2010)) and this translates to finite torque due to pinning that scales as σa^2 . The hydrodynamic torque on each particle is $O(\mu\dot{\gamma}a^3)$, where μ is the liquid viscosity and $\dot{\gamma}$ is the characteristic value of the shear rate near the particle monolayer. The ratio of the torque due to pinning to the hydrodynamic torque is thus proportional to the capillary number $Ca = \mu\dot{\gamma}a/\sigma$. Our results are valid in the limit $Ca \ll 1$, in which the particle does not rotate and hydrodynamic stresses are too small to appreciably deform the interface. Small capillary numbers are often found in practice: for example, for a particle-covered bubble of radius $R = 100 \mu\text{m}$ translating with a velocity $U_\infty = 1 \text{ cm s}^{-1}$, $\dot{\gamma} \sim U_\infty/R = 100 \text{ s}^{-1}$ and $Ca \sim 10^{-6}$. The capillary number for the entire drop based on the velocity scale U_∞ is a factor R/a larger than Ca (which is based on the velocity scale $\dot{\gamma}a$), but is still very small.

We consider plane monolayers of particle arrangements in a biperiodic configuration for two situations: a square array, and a reticulated mesh-like array formed by orthogonal chains of particles with one of the chains oriented parallel to the flow.

The problem is governed by two non-dimensional parameters: the non-dimensional gap size d/a and the solid area fraction $\phi_s = N_p\pi a^2/L^2$, where N_p is the number of particles in the periodic cell of side L . For the simulation of the square array, we simulate a single sphere and vary the area fraction by changing the lateral size of the computational domain. For the reticulated array case, examined in §3.4, N_p varies from 5 to 25.

A Cartesian coordinate system (x, y, z) is set at the centre of the computational domain, with x parallel to the flow direction and z in the direction normal to the monolayer. In the following, u will denote the flow velocity component in the x direction.

The numerical method employed for the simulation, Physalis, couples a finite-difference solution of the incompressible Navier–Stokes equation to a spectral solution of the Stokes equation for the velocity, vorticity and pressure disturbances induced by the sphere. The spectral solution is used only in the immediate neighbourhood of the particle surfaces. The pressure and vorticity are expressed in terms of spherical harmonics. To enforce the no-slip condition at the particle surfaces, an iterative procedure is used to match the coefficients of the spherical harmonics expansion to the finite-difference Navier–Stokes solution at a cage of computational points surrounding the particle surface. For the simulations in the current paper, we use the Navier–Stokes solver with the nonlinear convective term set to zero (i.e. all the simulations are carried out in the Stokes flow limit). The results we report are for steady-state conditions. Physalis has been extensively validated in laminar flows (Zhang & Prosperetti 2005; Bluemink *et al.* 2008, 2010). It has been applied to a shear flow over a porous medium surface composed of several layers of spheres (Liu & Prosperetti 2011), a situation that bears some similarities with the flow simulated in the current work.

The accuracy of the simulation was assessed through comparison with Faxén’s power-series analytical solution for the drag force on a single sphere translating with constant velocity between two parallel walls (Happel & Brenner 2012). Terms up to $O(d^5/a^5)$ were retained in the power series. Our numerical results for the drag force

on a fully immersed sphere in a periodic domain converged to Faxén’s solution in the limit $\phi_s \rightarrow 0$. The relative error between the numerical solution – for small but finite values of ϕ_s – and the analytical solution was found to be always less than 5%, and typically around 2.5%. For example, for $\phi_s = 0.349\%$ the relative error between the numerical solution and Faxén’s solution is 3.89% and 2.57% for $d/a = 3$ and $d/a = 15$, respectively.

Owing to the use of a spectral solution close to the particle surface, the Physalis method demonstrates good accuracy even in simulations in which a relatively small number of nodes per particle diameter is used (Zhang & Prosperetti 2005; Bluemink *et al.* 2008; Botto & Prosperetti 2012). For the simulations in this paper we used either eight or 16 nodes per particle diameter. The smaller resolution was used for relatively large gaps, $d/a > 5$, and small area fractions, $\phi_s < 0.15$, for which the flow velocity gradients are small. These values of the parameters correspond to large domains for which computational cost and memory requirements were found to be limiting factors. The simulations are carried out on a desktop PC equipped with an NVIDIA GTX 970 graphic card (the version of Physalis used here, BlueBottle, has the ability to exploit the GPU card of the PC).

Unless explicitly stated, all the quantities reported in this paper are normalised using the particle size a and the wall velocity U as the characteristic length and velocity scales, respectively.

3. Results and discussion

3.1. Square array: general features

We begin our analysis by examining the square array case. The periodic computational domain of side L contains in this case a single sphere, and the area fraction can be simply calculated as $\phi_s = \pi a^2/L^2$. We are particularly interested in the area-averaged streamwise velocity $\langle u \rangle$, defined as

$$\langle u \rangle = \frac{1}{L^2} \int u \, dx \, dy, \tag{3.1}$$

and how this quantity changes in the direction normal to the monolayer. In (3.1) the integral is extended over the region $-L/2 \leq x \leq L/2$, $-L/2 \leq y \leq L/2$.

In figure 3(a), the area-averaged velocity is plotted as a function of the coordinate z normal to the monolayer for a fixed gap size, $d = 3a$. The velocity profile is approximately linear in two limits: when $\phi_s \ll 1$ and when ϕ_s is close to the maximum packing fraction $\phi_{s,max} = \pi/4 \simeq 0.78$. For intermediate values of ϕ_s , the curvature of the velocity profile has a maximum. This trend can be understood by applying the averaging operator defined in (3.1) to the streamwise component of the fluid momentum equation in the Stokes flow limit. The resulting averaged equation reads

$$\frac{d^2 \langle u \rangle}{dz^2} = \frac{\Delta \bar{p}}{\mu L}, \tag{3.2}$$

where $\Delta \bar{p}(z)$ is the difference between the pressure at the plane $x = -L/2$, averaged over the line $-L/2 \leq y \leq L/2$, and the corresponding average pressure at the plane $x = L/2$. Expression (3.2) shows that the curvature of the average velocity profile can be neglected when the streamwise pressure drop occurring over a distance L is negligible.

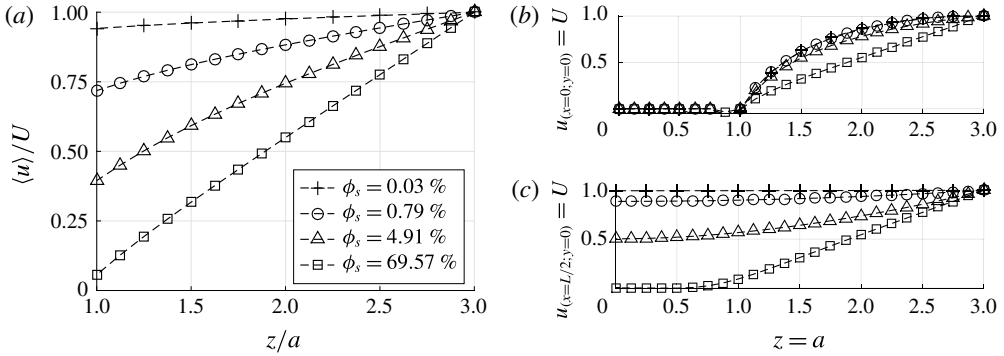


FIGURE 3. (a) Normalised area-averaged streamwise velocity versus coordinate normal to the monolayer for $d=3a$. (b,c) Normalised area-averaged streamwise velocity along lines passing through the centre of each sphere (b) or through the midpoint between adjacent spheres (c).

According to the Stokes equation, the pressure disturbance induced by the particle determines the curvature of the velocity profile. When $\phi_s \ll 1$, $\Delta\bar{p} \simeq 0$ because the pressure disturbance set up by each sphere evaluated at the boundaries of the computational domain is small. Indeed, we will shortly see that in the dilute limit the pressure disturbance induced by a particle looks like a pressure dipole, and in the dilute limit we therefore expect $\Delta\bar{p} = O(\mu a U / L^2)$ (Batchelor 2000), as for a single sphere in uniform flow. The pressure disturbance $\Delta\bar{p}$ decreases linearly with ϕ_s as $\phi_s \rightarrow 0$, since $\phi_s \propto 1/L^2$. On the other hand, when the monolayer is near maximum packing, the monolayer behaves almost as a flat wall. In this case, $\Delta\bar{p} \simeq 0$. For intermediate values of ϕ_s , the inter-particle distance is simultaneously sufficiently small for the pressure disturbance produced by each particle on the boundaries of the computational domain to be significant, and sufficiently large for each particle not to block significantly the flow velocity incident on the other particles. As a consequence, the curvature has a maximum for intermediate values of ϕ_s .

To characterise how the velocity profile changes in the plane of the monolayer, we show in figure 3(b,c) the profiles of u along lines perpendicular to the plane of the monolayer and passing through the sphere centre, ($x=0, y=0$), and through the midpoint between two spheres, ($x=L/2, y=0$), respectively. Because of the fore–aft symmetry of the Stokes equation, the velocity disturbances generated by two adjacent spheres cancel out at the midpoint ($x=L/2, y=0$). As a consequence, the velocity profiles corresponding to the midpoint are linear for any value of ϕ_s . As ϕ_s is reduced, the slope of the velocity profiles decreases. This trend gives a larger slip velocity. The velocity profiles that correspond to the sphere centres (figure 3b) display significant curvature for any ϕ_s , except perhaps at the highest value of the area fraction.

The error induced by approximating a liquid interface covered by a packed monolayer of particles as a no-slip surface is due to two sources. First of all, a packed monolayer contains free-slip surfaces even at maximum packing. Secondly, owing to the convexity of the spheres, the packed monolayer is not flat. A more accurate interpretation is considering the monolayer as a collection of bluff solid protuberances over the no-shear plane $z=0$. Each protuberance will locally block the flow and therefore produce a significant pressure disturbance.

To illustrate the spatial extent and magnitude of the pressure disturbance set up by each sphere in the monolayer, we show in figure 4(a,c) isocontours of the normalised

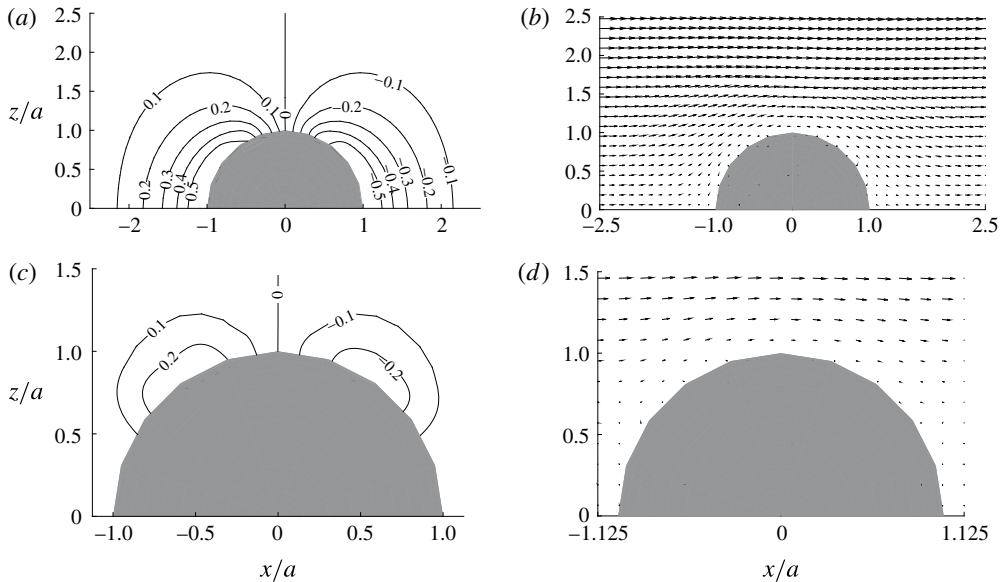


FIGURE 4. Normalised pressure (*a,c*) and velocity (*b,d*) in the plane $y=0$ for $\phi_s = 12.57\%$ (*a,b*) and $\phi_s = 62.05\%$ (*c,d*). The gap size is $d = 4a$.

pressure in the plane parallel to the mean flow and perpendicular to the monolayer, for two selected values of the area fraction, $\phi_s = 12.57\%$ and $\phi_s = 62.05\%$. For $\phi_s = 12.57\%$, the pressure distribution bears a signature of the fore–aft symmetric pressure dipole characteristic of uniform flow past a sphere (Batchelor 2000). As the area fraction increases (figure 4*b*), the two pressure ‘lobes’ seen in figure 4(*a*) move upwards, and occupy a smaller region near the top apex of the sphere. The streamwise pressure drop caused by the sphere is smaller for $\phi_s = 62.05\%$ than for $\phi_s = 12.57\%$. This observation supports our suggestion that $\Delta\bar{p}$ decreases as ϕ_s approaches the maximum packing fraction.

Figure 4(*b,d*) shows the velocity fields corresponding to figure 4(*a,c*), respectively. Flow recirculation regions do not seem to occur between the spheres. Flow recirculation between the spheres was evidenced in a simulation of pressure-driven slip flow over a porous medium interface, where the simulations were carried out using the same numerical method as used here (Liu & Prosperetti 2011). Flow recirculation is instead not apparent in the simulation results reported by Danov *et al.* (1995), who examined a single sphere straddling a fluid interface for a range of contact angles. One could expect that, owing to the presence of a re-entrant ‘wedge region’ between the particle surface and the free interface, recirculation would occur for contact angles for which the sphere is mostly immersed in the liquid.

The slip velocity is plotted as a function of ϕ_s for different values of the gap size d in figure 5(*a*), and as a function of d for different values of ϕ_s in figure 5(*b*). Following other authors (Ybert *et al.* 2007; Ng & Wang 2009; Liu & Prosperetti 2011), we define the slip velocity $\langle u \rangle_s$ as the value of $\langle u \rangle$ at $z = a$. As expected $\langle u \rangle$ tends to a uniform velocity of magnitude U as $\phi_s \rightarrow 0$. The rate at which this limit is approached as ϕ_s changes depends on the gap size. As a consequence, the value ϕ_s for which $\langle u \rangle$ is a significant fraction of U becomes smaller as d increases. For instance, when $d/a = 20$, $\langle u \rangle/U \simeq 0.5$ when $\phi_s \simeq 1.5\%$. When $d/a = 1.5$, $\langle u \rangle/U \simeq 0.5$

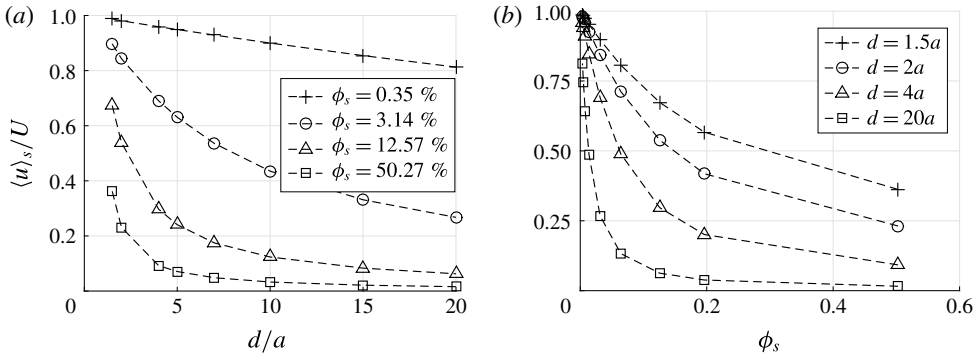


FIGURE 5. Normalised slip velocity versus (a) area fraction and (b) gap size.

when $\phi_s \simeq 30\%$. Since smaller gaps are associated with larger velocity gradients, this dependence on d indicates a dependence of $\langle u \rangle_s$ on the shear rate.

The dependence of $\langle u \rangle_s$ on d is nonlinear, but approximates a linear relation in the limit $\phi_s \rightarrow 0$ (figure 5b). The following argument shows that in the dilute limit the slope of the $\langle u \rangle_s$ versus d curve is proportional to the gap size and inversely proportional to the slip length. Approximating the flow past the monolayer as a Couette flow past a flat partial slip surface, the macroscopic shear rate is $\langle \dot{\gamma} \rangle_s \simeq (U - \langle u \rangle_s)/d$. Using this value in the Navier slip boundary condition (1.1) gives $\langle u \rangle_s/U \simeq 1/[d/\lambda + 1]$. For $\phi_s \ll 1$, λ becomes much larger than d and therefore $\langle u \rangle_s/U \simeq 1 - (d/\lambda)$ with a small $O(d/\lambda)$ error.

3.2. Scaling of slip length for square array

Figure 6 shows the slip length λ as calculated from the definition (1.1). Consistently with the calculation of the slip velocity, the bulk shear rate at the interface $\langle \dot{\gamma} \rangle_s = d\langle u \rangle/dz$ is evaluated at $z = a$. In the surface plot of figure 6(a), λ is plotted as a function of both ϕ_s and d/a . Projections of figure 6 onto the λ - d and λ - ϕ_s planes are shown in linear-linear plots in figure 6(b,c), respectively. The inset of figure 6(c) shows the λ - ϕ_s relation in log-log scale.

The slip length is seen to increase for increasing gap sizes, eventually saturating to an asymptotic value. A gap size $d = 10a$ already gives a value of λ close to the asymptotic limit.

In figure 6(c), the values of λ for different values of d are seen to lie practically on the same curve, suggesting similar scaling laws for different gap sizes. The inset shows that the relation λ - ϕ_s follows approximately a power law. To guess possible scaling exponents, we have examined the literature on flows over microstructured superhydrophobic surfaces. Ybert *et al.* (2007) developed a comprehensive theory for the dependence of the slip length on the area fraction for superhydrophobic surfaces. The theory was compared against literature data. Data for unconfined shear flow past a superhydrophobic surface composed of vertical pillars of circular or square cross-section could be fitted with good accuracy by a correlation of the form $\lambda/L = (A_1/\sqrt{\phi_s}) - B_1$, where L is the distance between the pillars, and A_1 and B_1 are constants. Ybert *et al.* (2007) proposed $A_1 = 0.325$ and $B_1 = 0.44$ (the analytical expressions proposed by Davis & Lauga (2010) give coefficient values very close to those indicated by Ybert *et al.* (2007)). In the dilute limit, i.e. in our case for

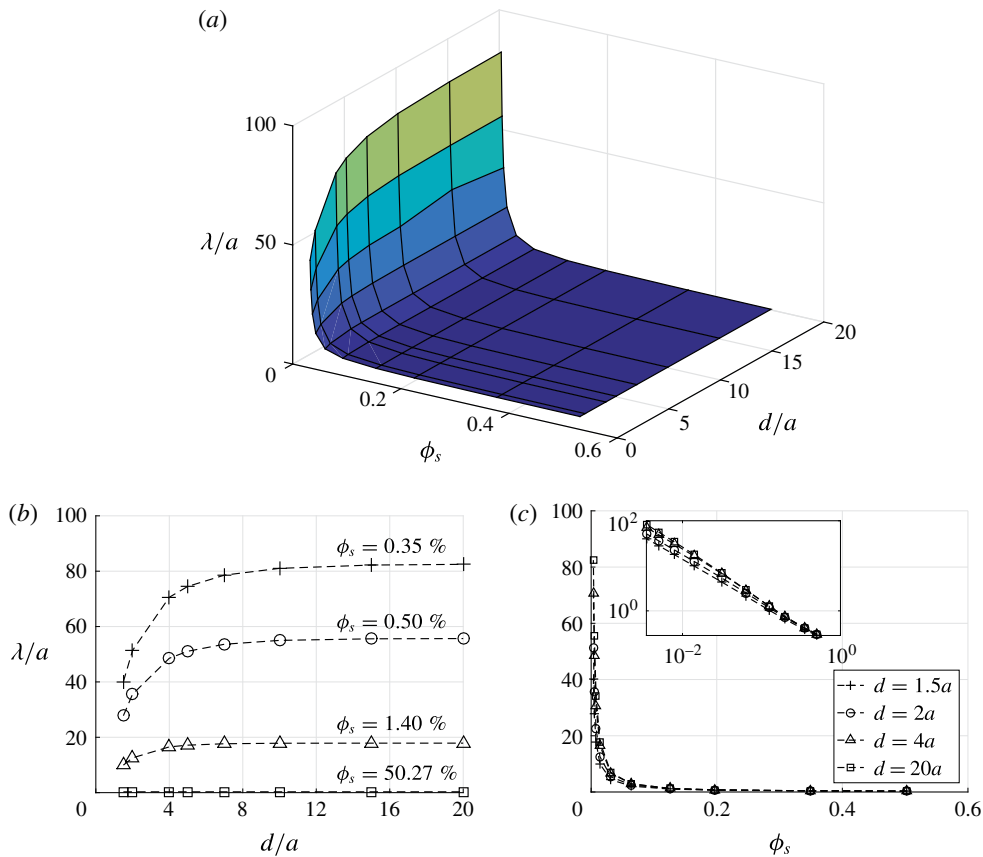


FIGURE 6. (Colour online) (a) Normalised slip length versus area fraction and normalised gap size. The plots in panels (b) and (c) are projections of the surface plot of panel (a) onto the λ – d and λ – ϕ_s planes, respectively. The inset in panel (c) shows the λ – ϕ_s relationship in log–log scale.

$\phi_s \ll (A_1/B_1)^2 \simeq 0.54$, the correlation above reduces to $\lambda/L \sim 1/\sqrt{\phi_s}$, which is equivalent to $\lambda/a \sim 1/\phi_s$. This scaling can be understood from the fact that in the dilute limit the ratio of the hydrodynamic force on each pillar to the slip velocity is expected to be practically independent of ϕ_s . The tangential stress on the monolayer due to the bulk flow is proportional to the ratio of the hydrodynamic force and L^2 . Since the tangential stress for a Newtonian fluid is proportional to the macroscopic shear rate, then (1.1) yields $\lambda \propto a/\phi_s$ for $\phi_s \ll 1$.

The argument above is expected to hold independently of the specific geometry of the solid object in contact with the fluid interface. Therefore, it should be possible to apply the scaling proposed by Ybert *et al.* (2007) to our case. This expectation is confirmed in figure 7(a), where λ/a is plotted as a function of $1/\phi_s$ for values of ϕ_s corresponding to a relatively dilute monolayer. A linear correlation fits the data remarkably well. From figure 7(a) it appears that a linear scaling holds for any value of d . The log–log plot in the inset of figure 6(b) shows that the power-law exponent has a small dependence on d for $d \leq 4a$. However, differences between the exponents corresponding to different values of d are approximately 10% of the $d = 20a$ case, and therefore not noticeable if the data are plotted as in figure 7(a).

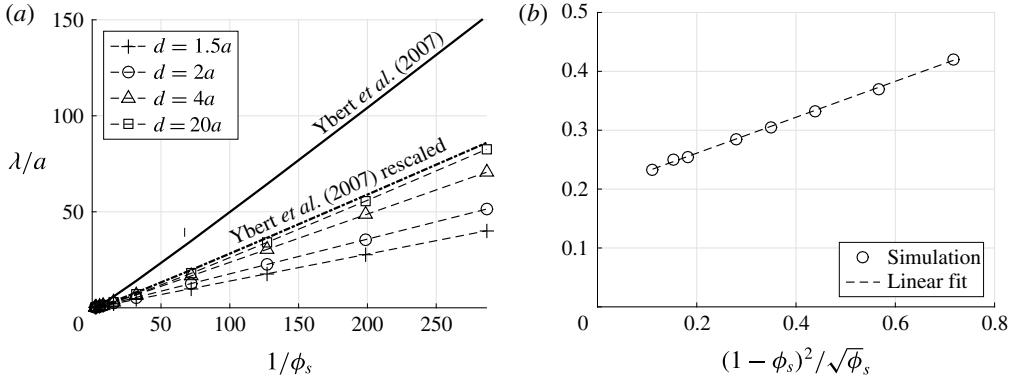


FIGURE 7. (a) Normalised slip length versus ϕ_s^{-1} . The continuous line is (3.2), developed by Ybert *et al.* (2007) for flow past a superhydrophobic surface. The dashed line is (3.3), where (3.2) has been rescaled by the ratio of the Stokes drag coefficient for a sphere to that for a thin disk. (b) Normalised slip length versus $(1 - \phi_s)^2 / \sqrt{\phi_s}$ showing the dense limit $\phi_s = 35\% - 70\%$ for $d = 4a$.

While the functional form proposed by Ybert *et al.* (2007) does fit our data well, the prefactors are different. The function $\lambda/a = (A_1\sqrt{\pi}/\phi_s) - (B_1\sqrt{\pi}/\phi_s^{1/2})$, obtained using the definition $\phi_s = \pi a^2/L^2$, is plotted as a continuous line in figure 7(a), using the coefficient values for A_1 and B_1 suggested by Ybert *et al.* This function is seen to overpredict the magnitude of the slip length computed in our simulation.

There is a simple explanation for the difference between our result and that of Ybert *et al.* (2007). The flow configuration considered by those authors can be interpreted as shear flow past a monolayer of infinitely thin disks (representing the top surfaces of the pillars composing the superhydrophobic surface). In our case the spheres protrude significantly into the liquid. Several studies in the context of superhydrophobic surfaces have shown that a larger protrusion produces smaller slip lengths (Sbragaglia & Prosperetti 2007; Ng & Wang 2009; Kumar, Datta & Kalyanasundaram 2016; Shelley *et al.* 2016). Therefore, a smaller slip length in the current case of a sphere monolayer is not unexpected.

We can attempt a simple correction to (3.2) to account for the finite protrusion of the spheres into the flow. For a given free-stream velocity, the hydrodynamic drag on an infinitely thin disk in a uniform flow is $9\pi/16$ times smaller than the drag on a sphere having the same radius. Assuming that tangential stress due to the bulk flow is approximately proportional to the slip velocity (we will confirm this hypothesis in §3.3), it should be expected that, for sufficiently dilute systems, the slip length for flow past a monolayer of spheres embedded in a gas–liquid interface is a factor of $9\pi/16$ smaller than that predicted by (3.2). To verify this approximation, we plot the function

$$\frac{\lambda}{a} = \frac{A_2}{\phi_s} - \frac{B_2}{\phi_s^{1/2}} \tag{3.3}$$

as a thick dashed line in figure 7(a). Here $A_2 = (16\pi\sqrt{\pi}/9)A_1$ and $B_2 = (16\pi\sqrt{\pi}/9)B_1$. The values given by this corrected expression are remarkably close to our data, suggesting that the difference between the data of Ybert *et al.* (2007) and ours can be mainly attributed to the larger drag produced by the protruding spheres on the flowing liquid as opposed to the flat top surfaces of the pillars.

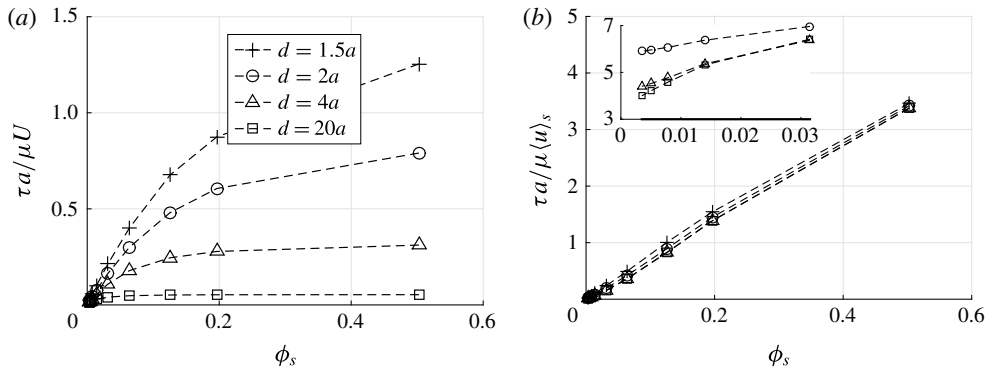


FIGURE 8. Tangential stress due to the bulk flow normalised by (a) the wall velocity U or (b) the slip velocity $\langle u \rangle_s$ as a function of the solid area fraction. The inset in panel (b) shows a zoom for small values of ϕ_s of the effective friction coefficient $\tau a / (\mu \langle u \rangle_s \phi_s)$.

The scaling law discussed above holds for a relatively dilute limit (the data points clearly discernible in figure 7(a) correspond to $\phi_s \leq 4\%$, while these corresponding to the dense limits are clustered near the origin and are barely visible). In the dense limit, the slip velocity results from a fraction $1 - \phi_s$ of the plane $z = a$ occupied by the gas–liquid interfaces. Since the slip velocity in these regions is of the order of $\langle \dot{\gamma} \rangle_s L (1 - \phi_s)$ (Ybert *et al.* 2007) and $L \propto \phi_s^{-1/2}$, we expect $\lambda \sim a(1 - \phi_s)^2 / \sqrt{\phi_s}$. Figure 7(b) shows that the simulation data follow this scaling law with very good accuracy.

3.3. Tangential stress due to the bulk flow: square array

In many situations of practical interest it would be useful to estimate the drag per unit area on the particles due to the motion of the bulk fluid (or ‘subphase’, as it is often called in the surfactants literature). We call the hydrodynamic drag on the particles per unit area the tangential stress due to the bulk flow, and denote this quantity by τ . In the current paper, τ for a square array is calculated as $\tau = F_x / L^2$, where F_x is the x component of the hydrodynamic force acting on each sphere in the monolayer.

In figure 8(a), τ is normalised by using U as velocity scale. With this normalisation, the normalised value of τ has a relatively strong dependence on both ϕ_s and d . However, we note that the wall velocity is characteristic of the fluid velocity ‘seen’ by the particles only in the extremely dilute limit for which the velocity profile is almost a plug flow. An improved parametrisation of the shear stress and pressure exerted on each particle by the bulk flow is expected to be given by the slip velocity $\langle u \rangle_s$. In figure 8(b), τ is normalised by $\langle u \rangle_s$. Using the slip velocity in the normalisation causes the data to collapse onto a single curve for any value of d .

The fact that τ is practically proportional to the slip velocity suggests the introduction of a non-dimensional friction coefficient $\tau a / (\mu \langle u \rangle_s \phi_s)$ having only a marginal dependence on d and ϕ_s . A linear fit to the data in figure 8(b) suggests a non-dimensional friction coefficient of approximately 7. For small values of ϕ_s the friction coefficient is smaller than 7 and non-constant (see inset), suggesting that the relation between $\tau / \langle u \rangle_s$ and ϕ_s is linear only in an approximate sense.

In the limit $\phi_s \rightarrow 0$ and $d \rightarrow \infty$, we expect $F_x \simeq 3\pi\mu a U$ (i.e. half the Stokes drag on a fully immersed sphere). Since $\langle u \rangle_s$ tends to U as $\phi_s \rightarrow 0$ (figure 5a), and

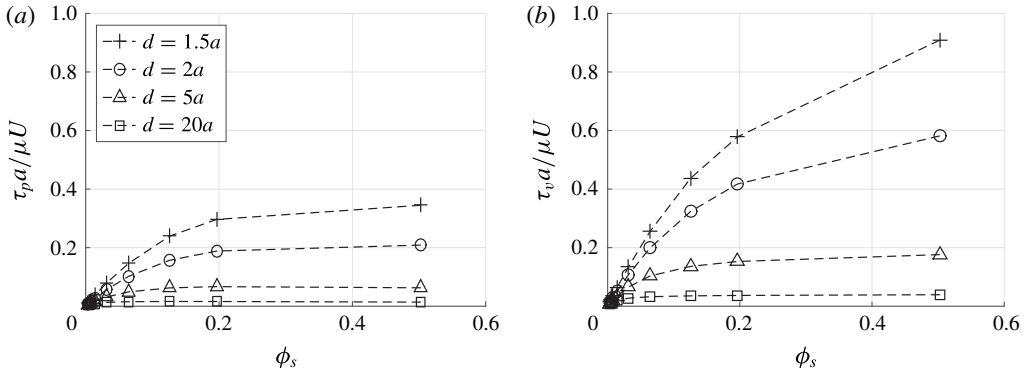


FIGURE 9. Normalised pressure (a) and viscous (b) contributions to τ .

by definition $\tau = F/L^2 = F\phi_s/(\pi a^2)$ for a square array, one might expect a friction coefficient of approximately 3 in the limits $\phi_s \rightarrow 0$ and $d \rightarrow \infty$. For small values of ϕ_s the data do appear to converge to a friction coefficient of 3 as d increases (see inset of figure 8b). However, the convergence is slow and for the values that we simulated the friction coefficient is significantly larger than 3 even for the smallest values of ϕ_s we considered. This fact may be due to the strong dependence of $\langle u \rangle_s$ on the surface fraction (figure 5a). One would need to simulate truly negligible values of ϕ_s , and therefore use extremely large computational domains, to recover the expected asymptotic limit.

The expansion in spherical harmonics in Physalis enables one to easily compute the pressure and viscous components of the hydrodynamic force on each sphere with excellent accuracy (Zhang & Prosperetti 2005; Bluemink *et al.* 2010; Botto & Prosperetti 2012). Upon normalisation, these force components yield τ_p and τ_v , namely the pressure and viscous contributions to τ , respectively. Figure 9(a,b) shows τ_p and τ_v as a function of ϕ_s for different values of d . As expected from the analytical solution for Stokes flow past a sphere, which suggests that pressure and viscous contributions to the drag are comparable, for $\phi_s \ll 1$ the viscous and pressure contributions to τ are comparable in magnitude. For intermediate and relatively large values of ϕ_s , viscous stresses produce the dominant contribution to τ . For instance, for $d = 7a$ and $\phi_s > 0.5$, τ_v is approximately one order of magnitude larger than τ_p . The contribution τ_p is only significant for small gap sizes, particularly at the highest values of the area fraction. This result confirms the intuitive notion that the largest contribution to τ for a moderately dense monolayer originates from the shear forces exerted by the fluid on the portion of the sphere surfaces where the streamwise fluid velocity is larger.

For completeness, we also report in figure 10 the hydrodynamic force on each particle in the square monolayer as a function of d for different values of ϕ_s . In contrast to the previous figures in which the tangential stress due to the bulk flow was reported, in figure 10 the force is not normalised by L^2 , and therefore the dependence on ϕ_s is perhaps more clear. This graph could be useful to quantify how the drag on a surface-active particle embedded at the boundary of a thin film between a particle-laden interface and a wall changes as a function of the thickness of the film.

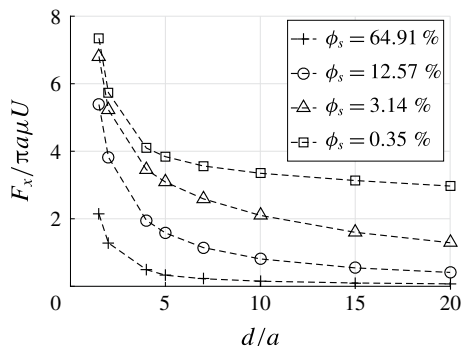


FIGURE 10. Hydrodynamic force on each sphere in the square array as a function of the gap size.

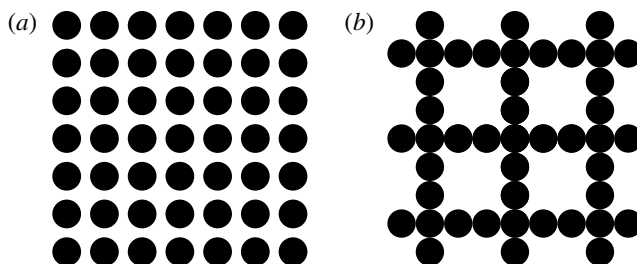


FIGURE 11. Schematic of a square array (a) and a reticulated array (b) for the same value of the solid area fraction, $\phi_s = 43.63\%$.

3.4. Reticulated array

The slip length depends on the specific microstructure of the monolayer. Two categories of microstructures are particularly relevant to particle-laden interfaces: well-dispersed systems, in which the particles are not in contact when ϕ_s is smaller than the maximum packing fraction; and percolating networks, where the particles form connected chains that span the boundaries of the interface (see e.g. Aveyard *et al.* 2000). The square array case examined in the previous section belongs to the first category. The percolating network case is examined in the current section. To get initial insights into more realistic situations, in which the percolating networks are disordered and are characterised by a variety of scales, in this section we simulate a periodic mesh-like reticulated arrangement. One example of such an arrangement is illustrated in figure 11(b).

The simulations for the reticulated array case are carried out by including in the doubly periodic simulation box a variable number of spheres. The spheres form two orthogonal rectilinear chains that intersect each other in the centre of the domain. One of the chains is oriented along the flow direction.

Because of the need to consider several particles, simulating reticulated arrays requires a significantly larger domain than for a square array, for a given area fraction. To limit the number of simulations while allowing the exploration of the relevant parameter space, the majority of the simulations presented in this section are carried out for a fixed gap size, $d = 7a$. Preliminary tests confirm that this gap

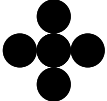
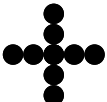
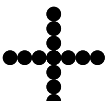
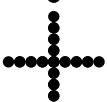
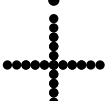
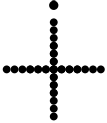
Structure	ϕ_s (%)	L/a	λ/a	$\tau a/\mu U$	λ_{sq}/a	$\tau_{sq}a/\mu U$
	43.63	6	0.3941	0.1617	0.3294	0.1598
	28.27	10	0.7656	0.1536	0.5249	0.1559
	20.8	14	1.2591	0.1435	0.7016	0.1519
	16.48	18	1.8106	0.1349	0.9228	0.1471
	13.63	22	2.3812	0.1258	1.1202	0.1459
	11.62	26	2.9633	0.1177	1.4267	0.1402

TABLE 1. Normalised slip length, λ/a , and normalised tangential stress due to the bulk flow, $\tau a/\mu U$, for reticulated arrays characterised by different values of the area fraction ϕ_s and mesh size L , for $d/a=7$. The last two columns report the values of λ and τ for a square array having the same solid area fraction as the corresponding reticulated array.

size is sufficiently large for the results to reasonably approximate the unbounded case $d = \infty$.

Table 1 summarises values of the slip length λ and tangential stress τ due to the bulk flow for different values of L (and therefore of ϕ_s). The last two columns in table 1 report the values of λ and τ for a square array having the same area fraction as the corresponding reticulated array. These two quantities are denoted by the symbols λ_{sq} and τ_{sq} , respectively.

Comparison of λ with λ_{sq} shows that, for a given surface coverage and particle size, the reticulated array gives a significantly larger value of the slip length. The effect of the specific microstructure (square array versus reticulated array) on λ becomes more and more significant as ϕ_s decreases. The difference between τ and τ_{sq} is comparatively small.

Why does the reticulated array give a larger slip length? The slip length is defined as the ratio of $\langle u \rangle_s$ to $\langle \dot{\gamma} \rangle_s$. A difference in slip length can therefore be attributed to: (i) differences in $\langle u \rangle_s$; (ii) differences in $\langle \dot{\gamma} \rangle_s$; or (iii) the combined effect of both quantities. Figure 12(a) compares values of $\langle u \rangle_s$ obtained with the reticulated array to those obtained with the square array. The corresponding values of $\langle \dot{\gamma} \rangle_s$ are shown in figure 12(b).

It can be seen that the values of $\langle u \rangle_s$ given by the two microstructures are comparable only for relatively large values of ϕ_s . For moderate and small values

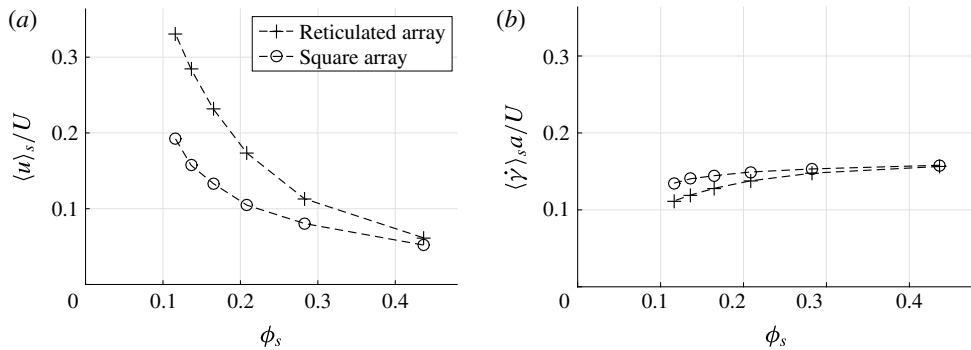


FIGURE 12. (a) Normalised slip velocity and (b) normalised bulk shear rate at the interface as a function of solid area fraction for $d/a=7$, comparing square and reticulated arrays.

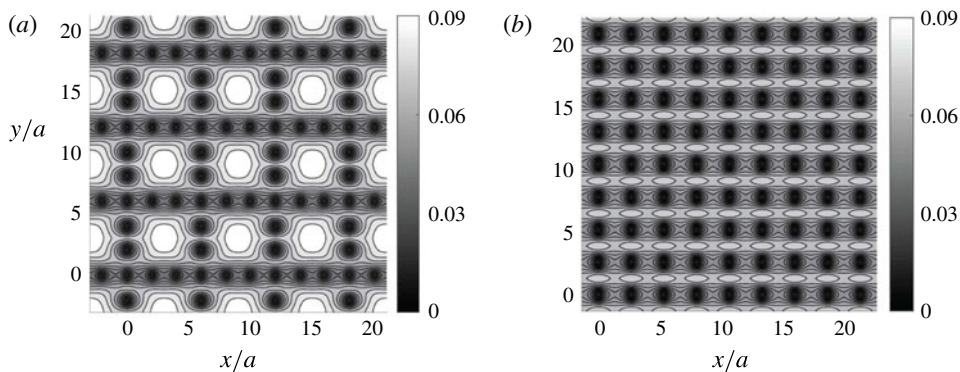


FIGURE 13. Contours of normalised streamwise velocity, u/U , in the plane $z=a$ for (a) square array and (b) reticulated array. The solid area fraction in (a) and (b) is $\phi_s = 43.63\%$ and $d/a=7$.

of ϕ_s , the reticulated array gives a significantly larger value of $\langle u \rangle_s$ than the square array. Over a similar range of values of ϕ_s , the differences in the values of $\langle \dot{\gamma} \rangle_s$ corresponding to the two microstructures are relatively small (figure 12b). The observed dependence of the slip length on the microstructure is thus mainly due to changes in the slip velocity, while changes in the bulk shear rate at the interface play a relatively marginal role.

A question arises as to why the slip velocity is larger in the case of the reticulated array. Comparison of figure 11(a) with figure 11(b) shows that, for a given area fraction, the reticulated array is characterised by larger connected regions not occupied by particles. Because the flow in these regions is relatively unobstructed by the particles, the slip velocity in these regions could be substantially larger than the slip velocity in the interstices between the particles in the square array case. To verify this hypothesis, we plotted isocontours of u in the plane $z=a$, comparing the reticulated and square arrays (figure 13). The characteristic velocities in the open areas bounded by chains in the reticulated array case are at least 50% larger than those in the interstices between particles in the square array case. These relatively large velocities are spread over regions of linear size comparable to the mesh size L . In contrast, in

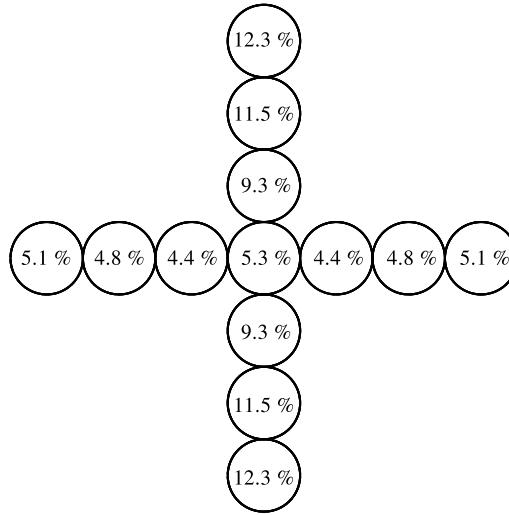


FIGURE 14. Percentage contribution to the tangential stress due to the bulk flow τ for each particle in a reticulated array, $\phi_s = 20.8\%$ and $d = 7a$. The horizontal chain in the diagram is parallel to the flow direction.

the square array the smaller slip velocities are spread over regions of characteristic linear dimension $\ell \ll L$, where ℓ is the average inter-particle separation. We have $\phi_s = (L/a - 1)\pi a^2/L^2$ for the reticulated array and $\phi_s = \pi a^2/\ell^2$ for the square array. Therefore, the ratio L^2/ℓ^2 of the interfacial areas occupied by high-velocity fluid (reticulated array) to that occupied by low-velocity fluid increases with decreasing ϕ_s . Since the slip velocity is an area-averaged quantity, larger local velocities spread over larger areas will give a larger value of the slip velocity.

We also note that, despite significant differences in slip length between the reticulated array and the square array, the interfacial shear stresses are comparable in the two cases (cf. table 1).

Comparing the values of τ , we note that, despite significant differences in slip length between the reticulated array and the square array, the values of the tangential stress due to the bulk flow are comparable in the two cases (cf. table 1). A significant difference between the square and reticulated arrays is that, while in the square array each particle will contribute equally to τ , in the reticulated array different particles can be subject to different hydrodynamic forces, and therefore the local tangential stress will in general be non-uniform. To characterise the degree of non-uniformity in τ , we show in figure 14 the fraction of the total value of τ contributed by each particle. This fraction is calculated as the ratio of the hydrodynamic force on each particle to the sum of the hydrodynamic forces exerted by all the particles within the computational domain.

The chains of particles arranged perpendicular to the flow direction, or transverse chains, carry the largest contribution to τ . In the case considered in figure 14, the transverse chain contributes more than 66 % of the total value of τ . The hydrodynamic force acting on the transverse chain is strongly non-uniform: the largest contribution, 12 %, is associated with the particles located near the midpoint of the transverse chain (farthest away from the intersection point). The central particle, located at the intersection between the longitudinal and transverse chains, contributes only 5.3 %

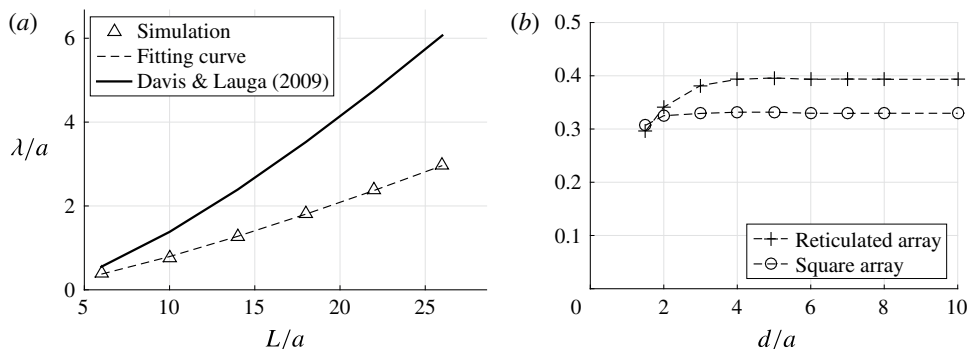


FIGURE 15. Normalised slip length versus (a) normalised mesh size and (b) normalised gap size; reticulated array, $d = 7a$. The area fraction in panel (b) is 43.63 %. The dashed line in panel (a) is (3.4) for $A = -0.039$ and $B = 0.03$.

of the total value of τ . In comparison, particles belonging to the longitudinal chain, oriented along the flow direction, are subject to a relatively uniform bulk tangential stress.

The natural choice of length scale to characterise the flow past the reticulated array is the mesh size L . It is therefore expected that the slip length will scale as $\lambda = Lf(\phi_s)$, where $f(\phi_s)$ is a function having relatively weak dependence on ϕ_s (and therefore on L). In figure 15(a), the values of λ for the reticulated array are plotted as a function of L . Over the range of values simulated, the slip length is seen to increase only slightly faster than linearly with L , confirming a scaling of the type $\lambda \sim Lf(\phi_s)$. Davis & Lauga (2009) carried out an analysis of the slip length for a flat partial slip surface composed of a mesh-like distribution of thin solid regions, obtaining a semi-empirical relation of the form

$$\frac{\lambda}{L} = A \ln(\phi_s) + B, \quad (3.4)$$

where A and B are constants. The values obtained by Davis & Lauga (2009) were $A = -0.107$ and $B = 0.003$. Fitting the simulation data (dashed line in figure 15a), we obtain $A = -0.039$ and $B = 0.03$. As for the square array, the effect of the protuberance of the no-slip region in the liquid gives a larger value of λ for a given value of ϕ_s as compared to a flat partial slip surface. We have attempted a simple rescaling by a factor of $9\pi/16$ as done for a square array (see § 3.2) to account for the difference between the results of Davis & Lauga (2009) and ours, but the results have not been as satisfying as for the square array case. This is due to the fact that, for a percolating network, hydrodynamic interactions between the particles are important even in the dilute limit. Therefore, the ratio of the hydrodynamic force on a single sphere to that of a single disk cannot represent a good rescaling factor.

The results above suggest that – in analogy with the case of superhydrophobic surfaces – different scalings for the slip length hold depending on whether the solid or the liquid are the continuous phase in the plane of the particle-laden interface. In the reticulated network, the solid is the continuous phase, and the free-slip interface is the dispersed phase. On the contrary, in the case of the square array, the solid is the dispersed phase. When the solid is the dispersed phase and the fluid is the continuous phase in the particle-laden interface, the particle radius is the characteristic length scale, and the slip length scales as $\lambda \propto a/\phi_s$ (for sufficiently small ϕ_s). When

the solid is the continuous phase, the mesh size L is the characteristic length, and the influence of the particle radius enters only into a weak – potentially logarithmic – dependence on the solid fraction.

4. Conclusions

We have presented numerical simulations for shear flow past a monolayer of neutrally wetting spheres embedded in a liquid–gas interface. In our simulations the shear flow is produced by a flat wall translating parallel to the monolayer. The results are also applicable to situations in which the monolayer translates with respect to a neighbouring wall, a situation that occurs for example in certain evaporating droplets problems (Yunker *et al.* 2011).

To extract effective parameters for the particle-laden interface, we fitted the simulation data to the predictions of a Navier slip boundary condition. The simulations provide accurate values for the slip length as a function of the area fraction, the gap size between the monolayer and the wall, and the microstructure of the monolayer.

The dependence of λ on ϕ_s follows scaling laws similar to those developed for shear flow past superhydrophobic microstructured surfaces: $\lambda \sim a/\phi_s$ for a dilute square array, and $\lambda \sim Lf(\phi_s)$ for a reticulated array, where $f(\phi_s)$ is a weak function of ϕ_s . The slip length is smaller than for flow past superhydrophobic surfaces for the same area fraction and microstructure. This feature can be explained by accounting for the fact that most semi-empirical correlations for superhydrophobic surfaces are developed for flat slip/no-slip surfaces, while in our case the spheres protrude significantly into the flow. For a square array, a simple prefactor rescaling based on the ratio of Stokes drag on a sphere to drag on a disk yields good agreement with the simulation data.

For a given area fraction, the slip length for a reticulated array is larger than for a square array. This feature is associated with the presence in a reticulated array of relatively large connected areas unoccupied by particles: the absence of particles ‘blocking’ the flow apparently leads to a larger slip velocity, and consequently to a larger slip length.

The numerical method we employed enabled us to accurately compute the tangential stress on the monolayer due to the bulk flow, i.e. the drag force per unit area due to the ‘subphase’ and, for the case of the reticulated array, the contribution of each sphere to this quantity. Values for the tangential stress could be useful, for instance, to estimate whether chains of particles would break under the effect of strong hydrodynamic forces. We calculate the tangential stress due to the bulk flow directly from the hydrodynamic force acting on each particle and not from the macroscopic shear rate, as usually done in studies on superhydrophobic surfaces.

In addition to providing insights into the flow in the neighbourhood of a sheared monolayer of interfacial colloids, the results of this paper can be useful to estimate effective resistance coefficients for particle-laden interfaces. For instance, the Stokes drag on a spherical particle having a partial slip surface with slip length λ is given by $F = 6\pi\mu RV(1 + 2\lambda/R)/(1 + 3\lambda/R)$, where R and V are the sphere radius and velocity, respectively (Luo & Pozrikidis 2008). Assuming that partial slip is produced by surface-active particles, this expression can be combined with the appropriate expressions for λ developed in this paper to calculate the rise velocity of a bubble covered by colloids given the surface coverage by particles or, conversely, the time-dependent surface coverage from the measured bubble velocity.

The slip length is not easily linked to the surface viscosity of the particle-laden interface, as the two parameters model different physical aspects. However, a

conceptual link between the two quantities exists. The tangential stress boundary condition (Brenner 2013) states that the tangential stress exerted by the bulk subphase on the particles balances the divergence of the surface stress tensor (the tangential stress on the gas–liquid regions of the particle-laden interface is zero due to the no-shear condition). The Navier slip (1.1) can be interpreted as a linear closure for the tangential stress $\simeq \mu \langle \dot{\gamma} \rangle$ on the monolayer in terms of the particle–fluid velocity difference $\langle u \rangle_s$. The surface viscosity and surface elasticity coefficients are instead parameters for the Newtonian closures of the surface stress tensor in terms of the surface deformation rate and surface deformation tensors. The surface viscosity, the surface elasticity and the slip length therefore enter as parameters in the same differential equation (the tangential stress boundary conditions). However, a simple algebraic relation between these effective parameters cannot be found in general. The description in terms of slip length complements, rather than replaces, the description in terms of surface viscosity and surface elasticity.

The slip length approach is expected to be particularly useful when the relation between the surface stress tensor and the interfacial deformation/deformation-rate tensor is not known *a priori*. For instance, in the analysis of interfacial rheology experiments (see e.g. Buttinoni *et al.* 2015) it is often assumed that the drag due to the subphase is negligible. However, estimates for this potentially important quantity are rarely reported. Equation (1.1) can be used to estimate the drag on the monolayer due to the subphase as a function of the average area fraction covered by the particles. The same equation provides a boundary condition for the bulk ‘subphase’ fluid velocity field.

We emphasise that the slip length and the surface viscosity model different micromechanical aspects, and are related to different moments of the hydrodynamic stress on each particle. The surface viscosity is an effective macroscopic property of the particle–liquid ‘mixture’ that models the resistance to dilation and shearing of an element of the composite interface (Brenner 2013); whereas the slip length is associated with the locally uniform relative velocity between the particles and the surrounding fluid. The surface viscosity is related to the hydrodynamic torque and stresslet on each particle in the monolayer (Edwards & Wasan 1991; Lishchuk & Halliday 2009); whereas the slip length is associated with the hydrodynamic drag on the particles.

The current work, which focuses on a rather idealised situation, can be extended in several directions. In our simulation the relative position between the particles does not change as a result of the flow. This approximation is realistic when the tangential stress due to the bulk flow is much smaller than the gradient in surface pressure (i.e. the two-dimensional pressure due to interparticle forces of non-hydrodynamic origin; see discussion in Gu & Botto (2016)). Large tangential stresses could lead, after a transient, to a non-uniform particle concentration in the interface. An expected effect, for example, is the compaction of the monolayer in the rear stagnation point of a rising particle-covered bubble. Flow-induced compaction effects on flat interfaces could be simulated with minor modifications of the computational set-up used in the current study.

The simulation results presented here are limited to a 90° contact angle. They are expected to hold as first approximations for contact angles not too different from 90°. Single-particle studies offer some insights into expected trends as a function of the contact angle. Previous work (Danov *et al.* 2000) has shown that the hydrodynamic drag is larger when the contact angle is such that the particle has a larger protrusion into the liquid phase. For an isolated particle, the drag force on a particle for a

flat interface can be expressed as $F = 3\pi\mu aUK(\theta_c)$, where $K(\theta_c)$ is a function of the contact angle for which tables are available (Fischer *et al.* 2006). According to the scaling laws developed in the current paper, one might expect that λ will be approximately proportional to $1/K$ (at least in the relatively dilute limit): for variations in the contact angle such that the particles will protrude more and more into the liquid phase, we expect a reduction in the slip length. This expected behaviour assumes that the fluid interface between the particles is perfectly flat; fluctuations in the interface due to thermal motion could change this picture quite substantially, as discussed by Boniello *et al.* (2015). For contact angles close to 0° or 180° , one needs to consider that the area fraction as defined in the current paper is not representative of the surface coverage by the particles, as in these limiting cases the particles barely touch the fluid interface.

While we have started to show evidence for some effects of the microstructure on the slip length by comparing square arrays and mesh-like particle networks, more realistic microstructures should be investigated. These include the regular hexagonal structure of colloidal crystals at fluid interfaces (Irvine, Vitelli & Chaikin 2010) and the fractal structure of percolating networks of aggregated interfacial colloids (Aveyard *et al.* 2000; Poulichet & Garbin 2015).

Acknowledgements

We acknowledge financial support from the European Community through grant no. 618335 ‘FlowMat: Flow and Capillarity in Materials Science’.

REFERENCES

- AVEYARD, R., CLINT, J. H., NEES, D. & PAUNOV, V. N. 2000 Compression and structure of monolayers of charged latex particles at air/water and octane/water interfaces. *Langmuir* **16** (4), 1969–1979.
- BATCHELOR, G. K. 2000 *An Introduction to Fluid Dynamics*. Cambridge University Press.
- BINKS, B. P. 2002 Particles as surfactants: similarities and differences. *Curr. Opin. Colloid Interface Sci.* **7** (1), 21–41.
- BINKS, B. P. & HOROZOV, T. S. 2006 *Colloidal Particles at Liquid Interfaces*. Cambridge University Press.
- BLUEMINK, J. J., LOHSE, D., PROSPERETTI, A. & VAN WIJNGAARDEN, L. 2008 A sphere in a uniformly rotating or shearing flow. *J. Fluid Mech.* **600**, 201–233.
- BLUEMINK, J. J., LOHSE, D., PROSPERETTI, A. & VAN WIJNGAARDEN, L. 2010 Drag and lift forces on particles in a rotating flow. *J. Fluid Mech.* **643**, 1–31.
- BONIELLO, G., BLANC, C., FEDORENKO, D., MEDFAI, M., MBAREK, N. B., IN, M., GROSS, M., STOCO, A. & NOBILI, M. 2015 Brownian diffusion of a partially wetted colloid. *Nat. Mater.* **14**, 908–911.
- BOTTO, L. & PROSPERETTI, A. 2012 A fully resolved numerical simulation of turbulent flow past one or several spherical particles. *Phys. Fluids* **24** (1), 013303.
- BOURNIVAL, G., ATA, S. & WANLESS, E. J. 2015 The roles of particles in multiphase processes: particles on bubble surfaces. *Adv. Colloid Interface Sci.* **225**, 114–133.
- BRENNER, H. 2013 *Interfacial Transport Processes and Rheology*. Elsevier.
- BUTTINONI, I., ZELL, Z. A., SQUIRES, T. M. & ISA, L. 2015 Colloidal binary mixtures at fluid–fluid interfaces under steady shear: structural, dynamical and mechanical response. *Soft Matt.* **11** (42), 8313–8321.
- DANI, A., KEISER, G., YEGANEH, M. S. & MALDARELLI, C. 2015 Hydrodynamics of particles at an oil–water interface. *Langmuir* **31** (49), 13290–13302.

- DANOV, K., AUST, R., DURST, F. & LANGE, U. 1995 Influence of the surface viscosity on the hydrodynamic resistance and surface diffusivity of a large Brownian particle. *J. Colloid Interface Sci.* **175** (1), 36–45.
- DANOV, K. D., DIMOVA, R. & POULIGNY, B. 2000 Viscous drag of a solid sphere straddling a spherical or flat surface. *Phys. Fluids* **12** (11), 2711–2722.
- DAVIS, A. M. J. & LAUGA, E. 2009 The friction of a mesh-like super-hydrophobic surface. *Phys. Fluids* **21** (11), 113101.
- DAVIS, A. M. J. & LAUGA, E. 2010 Hydrodynamic friction of fakir-like superhydrophobic surfaces. *J. Fluid Mech.* **661**, 402–411.
- DE GENNES, P.-G. 1985 Wetting: statics and dynamics. *Rev. Mod. Phys.* **57** (3), 827–863.
- DEEMER, A. R. & SLATTERY, J. C. 1978 Balance equations and structural models for phase interfaces. *Intl J. Multiphase Flow* **4** (2), 171–192.
- DÖRR, A. & HARDT, S. 2015 Driven particles at fluid interfaces acting as capillary dipoles. *J. Fluid Mech.* **770**, 5–26.
- DÖRR, A., HARDT, S., MASOUD, H. & STONE, H. A. 2016 Drag and diffusion coefficients of a spherical particle attached to a fluid–fluid interface. *J. Fluid Mech.* **790**, 607–618.
- EDWARDS, D. A. & WASAN, D. T. 1991 A micromechanical model of linear surface rheological behavior. *Chem. Engng Sci.* **46** (5), 1247–1257.
- FISCHER, TH. M., DHAR, P. & HEINIG, P. 2006 The viscous drag of spheres and filaments moving in membranes or monolayers. *J. Fluid Mech.* **558**, 451–475.
- FRIJTERS, S., GÜNTHER, F. & HARTING, J. 2012 Effects of nanoparticles and surfactant on droplets in shear flow. *Soft Matt.* **8** (24), 6542–6556.
- GU, C. & BOTTO, L. 2016 Direct calculation of anisotropic surface stresses during deformation of a particle-covered drop. *Soft Matt.* **12** (3), 705–716.
- HAPPEL, J. & BRENNER, H. 2012 *Low Reynolds Number Hydrodynamics: with Special Applications to Particulate Media*, vol. 1. Springer Science and Business Media.
- HOROZOV, T. S. 2008 Foams and foam films stabilised by solid particles. *Curr. Opin. Colloid Interface Sci.* **13** (3), 134–140.
- HUNTER, T. N., PUGH, R. J., FRANKS, G. V. & JAMESON, G. J. 2008 The role of particles in stabilising foams and emulsions. *Adv. Colloid Interface Sci.* **137** (2), 57–81.
- IRVINE, W. T. M., VITELLI, V. & CHAIKIN, P. M. 2010 Pleats in crystals on curved surfaces. *Nature* **468** (7326), 947–951.
- KOTULA, A. P. & ANNA, S. L. 2012 Probing timescales for colloidal particle adsorption using slug bubbles in rectangular microchannels. *Soft Matt.* **8** (41), 10759–10772.
- KUMAR, A., DATTA, S. & KALYANASUNDARAM, D. 2016 Permeability and effective slip in confined flows transverse to wall slippage patterns. *Phys. Fluids* **28** (8), 082002.
- LAUGA, E. & STONE, H. A. 2003 Effective slip in pressure-driven Stokes flow. *J. Fluid Mech.* **489**, 55–77.
- LEWANDOWSKI, E. P., CAVALLARO, M. JR, BOTTO, L., BERNATE, J. C., GARBIN, V. & STEBE, K. J. 2010 Orientation and self-assembly of cylindrical particles by anisotropic capillary interactions. *Langmuir* **26** (19), 15142–15154.
- LISHCHUK, S. V. & HALLIDAY, I. 2009 Effective surface viscosities of a particle-laden fluid interface. *Phys. Rev. E* **80** (1), 016306.
- LIU, Q. & PROSPERETTI, A. 2011 Pressure-driven flow in a channel with porous walls. *J. Fluid Mech.* **679**, 77–100.
- LUO, H. & POZRIKIDIS, C. 2008 Effect of surface slip on Stokes flow past a spherical particle in infinite fluid and near a plane wall. *J. Engng Maths* **62** (1), 1–21.
- MARTINEZ, A. C., RIO, E., DELON, G., SAINT-JALMES, A., LANGEVIN, D. & BINKS, B. P. 2008 On the origin of the remarkable stability of aqueous foams stabilised by nanoparticles: link with microscopic surface properties. *Soft Matt.* **4** (7), 1531–1535.
- NG, C.-O. & WANG, C. Y. 2009 Stokes shear flow over a grating: implications for superhydrophobic slip. *Phys. Fluids* **21** (1), 013602.

- PETKOV, J. T., DENKOV, N. D., DANOV, K. D., VELEV, O. D., AUST, R. & DURST, F. 1995 Measurement of the drag coefficient of spherical particles attached to fluid interfaces. *J. Colloid Interface Sci.* **172** (1), 147–154.
- POULICHET, V. & GARBIN, V. 2015 Ultrafast desorption of colloidal particles from fluid interfaces. *Proc. Natl Acad. Sci. USA* **112** (19), 5932–5937.
- POZRIKIDIS, C. 2007 Particle motion near and inside an interface. *J. Fluid Mech.* **575**, 333–357.
- RAPACCHIETTA, A. V. & NEUMANN, A. W. 1977 Force and free-energy analyses of small particles at fluid interfaces: II. Spheres. *J. Colloid Interface Sci.* **59** (3), 555–567.
- ROTHSTEIN, J. P. 2010 Slip on superhydrophobic surfaces. *Annu. Rev. Fluid Mech.* **42**, 89–109.
- SBRAGAGLIA, M. & PROSPERETTI, A. 2007 A note on the effective slip properties for microchannel flows with ultrahydrophobic surfaces. *Phys. Fluids* **19** (4), 043603.
- SHANG, J., FLURY, M. & DENG, Y. 2009 Force measurements between particles and the air–water interface: implications for particle mobilization in unsaturated porous media. *Water Resour. Res.* **45**, W06420.
- SHELLEY, S. R., SMITH, J. D., HIBBINS, A. P., SAMBLES, J. R. & HORSLEY, S. A. R. 2016 Fluid mobility over corrugated surfaces in the Stokes regime. *Phys. Fluids* **28** (8), 083101.
- SIERAKOWSKI, A. J. 2016 GPU-centric resolved-particle disperse two-phase flow simulation using the Physalis method. *Comput. Phys. Commun.* **207**, 24–34.
- SINGH, P. & JOSEPH, D. D. 2005 Fluid dynamics of floating particles. *J. Fluid Mech.* **530**, 31–80.
- STANCIK, E. J., KOUHKAN, M. & FULLER, G. G. 2004 Coalescence of particle-laden fluid interfaces. *Langmuir* **20** (1), 90–94.
- SUBRAMANIAM, A. B., ABKARIAN, M. & STONE, H. A. 2005 Controlled assembly of jammed colloidal shells on fluid droplets. *Nat. Mater.* **4** (7), 553–556.
- SUBRAHMANYAM, T. V. & FORSSBERG, E. 1988 Froth stability, particle entrainment and drainage in flotation – a review. *Intl J. Miner. Process.* **23** (1), 33–53.
- TAMBE, D. E. & SHARMA, M. M. 1994 The effect of colloidal particles on fluid–fluid interfacial properties and emulsion stability. *Adv. Colloid Interface Sci.* **52**, 1–63.
- TSAPIS, N., DUFRESNE, E. R., SINHA, S. S., RIERA, C. S., HUTCHINSON, J. W., MAHADEVAN, L. & WEITZ, D. A. 2005 Onset of buckling in drying droplets of colloidal suspensions. *Phys. Rev. Lett.* **94** (1), 018302.
- WEBER, M. E., BLANCHARD, D. C. & SYZDEK, L. D. 1983 The mechanism of scavenging of waterborne bacteria by a rising bubble. *Limnol. Oceanogr.* **28** (1), 101–105.
- YBERT, C., BARENTIN, C., COTTIN-BIZONNE, C., JOSEPH, P. & BOCQUET, L. 2007 Achieving large slip with superhydrophobic surfaces: scaling laws for generic geometries. *Phys. Fluids* **19** (12), 123601.
- YUNKER, P. J., STILL, T., LOHR, M. A. & YODH, A. G. 2011 Suppression of the coffee-ring effect by shape-dependent capillary interactions. *Nature* **476** (7360), 308–311.
- ZHANG, Z. & PROSPERETTI, A. 2005 A second-order method for three-dimensional particle simulation. *J. Comput. Phys.* **210** (1), 292–324.