

Pressure-driven flow across a hyperelastic porous membrane

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We report an experimental investigation of pressure-driven flow of a viscous liquid across thin polydimethylsiloxane (PDMS) membranes. Our experiments revealed a nonlinear relation between the flow rate Q and the applied pressure drop Δp , in apparent disagreement with Darcy's law, which dictates a linear relationship between flow rate, or average velocity, and pressure drop. These observations suggest that the effective permeability of the membrane decreases with pressure due to deformation of the nanochannels in the PDMS polymeric network. We propose a model that incorporates the effects of pressure-induced deformation of the hyperelastic porous membrane at three distinct scales: the membrane surface area, which increases with pressure, the membrane thickness, which decreases with pressure, and the structure of the porous material, which is deformed at the nanoscale. With this model, we are able to rationalize the deviation between Darcy's law and the data. Our result represents a novel case in which macroscopic deformations can impact the microstructure and transport properties of soft materials.

Key words: microfluidics, porous media

1. Introduction

Selective polymer membranes are much used in gas separation (Koresh & Sofer 1983), as gas sensors (Rego & Mendes 2004), for drug delivery (Pernaut & Reynolds 2000) and as filters (Dhopeswarkar *et al.* 2008). A popular material for these applications is polydimethylsiloxane (PDMS), which exhibits hydrophobicity and organophilicity. This property has contributed to the extensive usage of this material for the dehydration of alcohol solutions (Vankelecom *et al.* 1997). Moreover, PDMS is soft, biocompatible, permeable to gases or vapour and relatively inexpensive, and can also be used, for example, in micropumps (Jeong & Konishi 2007), microvalves (Jo *et al.* 2000) and microfluidics (Duffy *et al.* 1998), for pervaporation (Peng *et al.* 2006) and in nanofiltration (Stafie, Stamatalis & Wessling 2005).

In the aforementioned technological applications, it is important to know the transport characteristics based on the structure of the material, such as the permeability

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and the diffusion coefficient, because these properties determine the end use of the material. While these attributes can be measured (e.g. Tsuru *et al.* 2000; Geens, Van der Bruggen & Vandecasteele 2004; Ebert *et al.* 2006), the experiments are often cumbersome and/or too costly to perform in an industrial setting. In such cases, theoretical models or computational approaches are effective tools to inform designers (e.g. Vankelecom *et al.* 2004; Makrodimitri & Economou 2008; Chang *et al.* 2012; Sanaei & Cummings 2017, 2018), and it is most common to assume that the properties, once measured, are constants independent of the details of the application.

To understand the transport properties of PDMS, a number of studies have been conducted using a combination of experiments, theory and simulations (e.g. Vankelecom *et al.* 2004; Makrodimitri & Economou 2008; Ismail *et al.* 2009; Firpo *et al.* 2015). It is, however, difficult to derive the transport properties and flux equation of a thin PDMS membrane, because it is unclear which mode of transport, diffusive or convective, dominates. If the PDMS is an ideal dense membrane, the mass transfer through the membrane is described as diffusive transport with the familiar solution–diffusion model. Bhanushali *et al.* (2001) provided a standard flux equation based on the solution–diffusion model as $J_D \approx A_D(\Delta p - \Delta\pi)$, where J_D is the flux, Δp and $\Delta\pi$ are the pressure drop and the osmotic pressure drop across the membrane, respectively, and A_D is the pure solvent permeability coefficient consisting of diffusivity and solubility terms. This model shows good agreement for hydrophobic membranes in various alcohols and alkanes. Chang *et al.* (2012) adopted molecular dynamics simulations to analyse the membrane structure and transport processes. The diffusion coefficient calculated from simulations is in accord with experiments where the PDMS membrane is assumed to be a dense material with a pore diameter of approximately 0.8 nm.

On the other hand, a number of studies have reported that the transport characteristics of PDMS membranes can be rationalized by a convective flow model, which treats PDMS as a porous material. The typical description of convective flow through a porous membrane is Darcy's law, $J_{conv} \sim d_p^2 \phi \Delta p / L \eta$, assuming that the internal pore structure is a cylindrical tube bundle or packed bed of spheres, where J_{conv} , ϕ , d_p , L and η are, respectively, the flux, porosity, pore size, membrane thickness and viscosity of fluid (see Priske *et al.* 2016). Robinson *et al.* (2005) showed that the pore flow model could be applied to a broad range of swelling of PDMS membranes whereas the solution–diffusion model did not adequately describe the higher degrees of swelling. Darvishmanesh *et al.* (2009) presented a model combining the pore flow model and solution–diffusion model. The membrane is considered as a parallel connected matrix having the solution–diffusion mechanism of solvent transport and of pores where the solvent is convectively transported without change of concentration. Soltane, Roizard & Favre (2013) reported that the flux and pressure drop showed a linear relationship when the flux was measured by varying the pressure drop, which is consistent with the convective flow approach, whereas the flux data were also consistent with Fick's law related to the solution–diffusion model, when it was measured while changing the solvent concentration. Therefore, Priske *et al.* (2016) concluded that this phenomenon occurs because the pore size of PDMS is not small or large enough to be described only by the solution–diffusion model or only by the pore flow model, respectively, and thus the mass transfer through the PDMS membrane is a combination of the two transport mechanisms.

To understand liquid transport in PDMS, and other polymer membranes, diffusive and convective processes should be evaluated separately (Phillip *et al.* 2009; Soltane

et al. 2013). Previous studies of PDMS permeability have focused on relatively thick membranes, which retain their shape when subjected to mechanical stress. However, such experiments are not representative of thin permeable PDMS membranes, where relatively large deformations of the membrane can occur.

Accordingly, in this paper, we investigate the permeability of a thin PDMS membrane in convective flow conditions. Our starting point is the general relation between flow rate Q and applied pressure drop Δp , also known as Darcy's law:

$$Q = \frac{A\kappa}{d} \frac{\Delta p}{\eta}. \quad (1.1)$$

Here, κ is the permeability of the membrane, $A = Lw$ is the cross-sectional area of the membrane of length L , width w and thickness d , and η is the viscosity of the liquid. Because thin PDMS membranes are flexible, the parameters in the first factor of (1.1), i.e. the area A , thickness d and pore-level permeability κ , are functions of the applied pressure drop Δp . This potentially leads to a nonlinear relationship between the flow rate Q and pressure drop Δp , which we seek to elucidate.

The following sections describe our set-up (§ 2.1), deformation and flow experiments (§§ 2.2 and 2.3) and a model to describe the relation between permeability and membrane deformation (§ 3.1), which compares favourably to our data (§ 3.2). Finally, we conclude by summarizing our results (§ 4).

2. Experiments

Our experiments were designed to elucidate the relationship between liquid flow rate Q and applied pressure drop Δp across a soft porous membrane. We begin by describing the experimental set-up and the methods used to quantify flow and deformation.

2.1. Experimental set-up

The experimental device was fabricated by first milling a shallow rectangular channel into a glass slide. The channel was then covered by a thin PDMS membrane, thus forming a closed chamber. Vertical channels were drilled through the glass slide, so as to provide access to the chamber. The chamber was filled by a viscous liquid (ethanol), and the chamber was pressurized (figure 1). The deflection of the membrane (figure 2) and the flow rate were quantified as a function of the applied pressure drop.

The micro-milled channel and access ports were fabricated from a 1 mm thick glass slide with a milling machine utilizing a cylinder-shaped diamond grinding wheel. The fabricated channel was 5 mm wide (w_0), 0.5 mm deep and 45 mm long (L) (see figure 1*a*). A 60–200 μm thick PDMS membrane was prepared by mixing the monomer and curing agent (Sylgard 184, Dow Corning, USA) in a 10:1 weight ratio. The PDMS mixture was placed in vacuum desiccator for 30 min for degassing. The membrane was produced by spin coating on a glass substrate for 30 s with selection of the rotation speed to achieve the target membrane thickness d_0 . The glass substrate was coated by silane ((tridecafluoro-1,1,2,2-tetrahydrooctyl)triethoxysilane, Gelest) in a vacuum desiccator prior to the spin coating in order to ease the handling of the thin and fragile PDMS films.

The PDMS membranes were separated from the substrate and bonded, using an oxygen plasma treatment, onto the aforementioned glass slide, thus forming a closed channel. The access ports were connected by rigid tubing (PEEK, Upchurch)

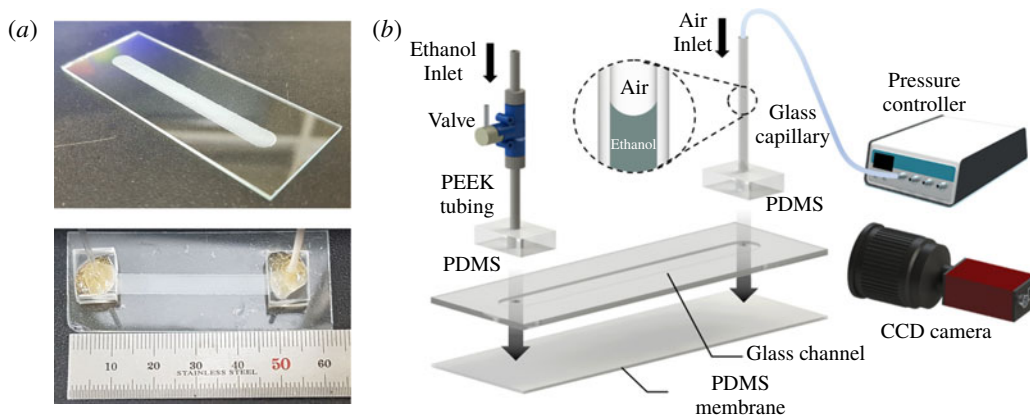


FIGURE 1. (Colour online) Experimental set-up. (a) Fabricated glass channel (top) and assembled membrane channel (bottom). The glass channel has width $w_0 = 5$ mm and length $L = 45$ mm. (b) Schematic diagram of the experimental set-up and assembly of the chip. The thin PDMS membrane is bonded at the bottom of the glass chip. The interface of ethanol and air is located in the glass capillary and its position is recorded by a charge coupled device (CCD) camera as pressurized air is supplied by a controller. The change of position of the interface enables measurement of the flow rate across the membrane and of the permeability of the membrane.

to a valve and a glass capillary tube. Both tubes were held in place by thick PDMS blocks. The flow valve enabled us to fill and seal the chamber. The open end of the glass capillary tube was connected with a pressure-controlled pump (MFCSTM-EZ, Fluigent) that allowed us to regulate the pressure inside the channel. The pressure drops used in our experiments were in the range $1 \text{ kPa} < \Delta p < 15 \text{ kPa}$, significantly above the gravitational pressure head due to the vertical liquid columns ($\sim 0.3\text{--}0.4 \text{ kPa}$). The device was immersed in an ethanol bath for 6 h prior to starting an experiment. During each experiment, the entire device remained immersed in the ethanol bath to prevent evaporation or air infiltration within the membrane and microchannel. To quantify the flow rate Q across the membrane, a charge coupled device camera (Manta G-282, Allied Vision) recorded the movement of the air–liquid interface inside the glass capillary tube. The position of the meniscus as a function of time was obtained using ImageJ (US National Institutes of Health) and MATLAB software based on the analysis of sequential images. The volumetric flow rate Q was calculated from the slope of the meniscus position versus time. The same recording set-up was used to quantify the deflection of the PDMS membrane. Images of the membrane deformed by air pressure were analysed with ImageJ.

2.2. Results: membrane deflection

To quantify the deformation of the membrane, the pressure in the channel was increased to a level Δp above atmospheric using the pressure controller (figure 2a). The deflection of the PDMS membrane can be described by the vertical displacement $u(x, \Delta p)$ from the initial position $u(x, \Delta p = 0) = 0$ (figure 2b). Here, x is the distance from the centre of the channel of total width w_0 . We pressurized one inlet of the membrane channel through the glass capillary, but the pressure drop and the variation of membrane displacement along the length direction were negligible because the

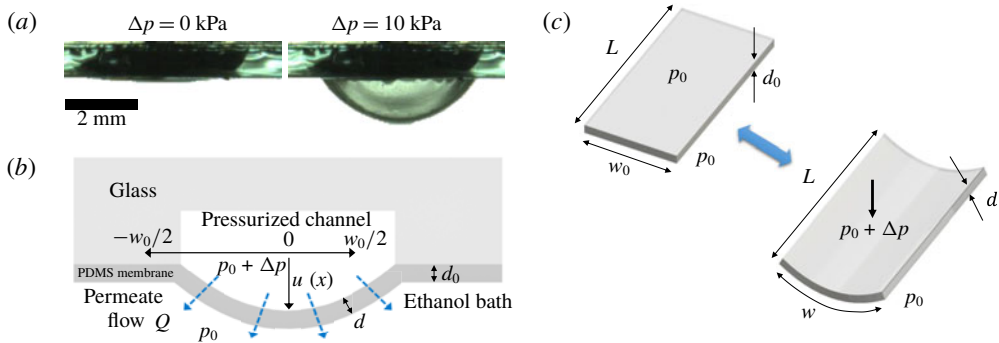


FIGURE 2. (Colour online) Deformation and flow across a soft porous membrane. (a) Photographs of a PDMS membrane of thickness $d_0 = 100 \mu\text{m}$ in the flat equilibrium state ($\Delta p = 0 \text{ kPa}$) and when subjected to a pressure drop $\Delta p = 10 \text{ kPa}$. (b) Schematic of the PDMS membrane covering one side of a rectangular glass channel. The pressure drop Δp drives the flow rate Q across the membrane, and also elastically deforms the PDMS membrane. The amplitude of the deformation $u(x)$ is approximately quadratic (see details in the text). (c) Schematic of an undeformed PDMS membrane of initial width w_0 and thickness d_0 , and the deformed membrane of pressure-dependent stretched width $w(\Delta p)$ and thickness $d(\Delta p)$. The length L of the membrane remains constant in our experiments.

flow rate Q through the membrane is very low and the membrane was sufficiently deformed over its entire area. Figure 3(a) shows the measured maximum displacement u_{max} as a function of pressure drop Δp for each d_0 . At low to moderate pressures, we observed an inverse relationship between thickness and deformation, and an approximate square-root dependence of the maximum displacement on pressure drop, i.e. $u_{\text{max}} \sim \beta' d (\Delta p w_0^2 L^2 / E_0 d^4)^{1/2}$, where the constant $\beta' = 5.8 \times 10^{-3}$ (figure 3a,b) and the elastic modulus of the PDMS $E_0 = 1.89 \text{ MPa}$ (see Johnston *et al.* 2014). The observed deformation along the long axis of the channel was negligible. The membranes failed at a critical pressure drop $\Delta p_c > 10 \text{ kPa}$, which gradually increased with the membrane thickness d_0 (figure 3a).

We note two well-established mathematical models that can be used to estimate the deflection of a thin plate subjected to loads: Kirchhoff–Love (KL) plate theory and the Föppl–von Kármán (FK) equations. Deformations described by KL theory are characterized by a linear relationship between the maximum displacement of the membrane u_{max} and the applied load Δp . This prediction is consistent with our experiments (figure 3a,b) for relatively small deformations ($u_{\text{max}} < d$). However, the data deviate from KL theory when the deformation exceeds the plate thickness. In this limit, the deformation of the membrane can be described by the FK equations generally, where $u_{\text{max}}/d \sim (\Delta p w_0^4 / E_0 d^4)^{1/3}$ (see Bouremel *et al.* 2017). In our experiments, the deformation scales as $u_{\text{max}}/d \sim (\Delta p w_0^2 L^2 / E_0 d^4)^{1/2}$, due to the hyperelastic properties of PDMS (see Nunes 2011). Unfortunately, few analytical solutions are known in this case, and numerical simulations would therefore be required to predict the exact relationship between u_{max} and Δp for elastic materials (see Wang & El-Sheikh 2005; Razdolsky 2015) and hyperelastic materials (see Selvadurai & Shi 2012; Amabili *et al.* 2016).

To simplify the subsequent analysis, we base the discussion on the observed robust scalings of membrane deflection and effective width with pressure drop (figure 3). We observed that the shape of the inflated membrane was well approximated by a

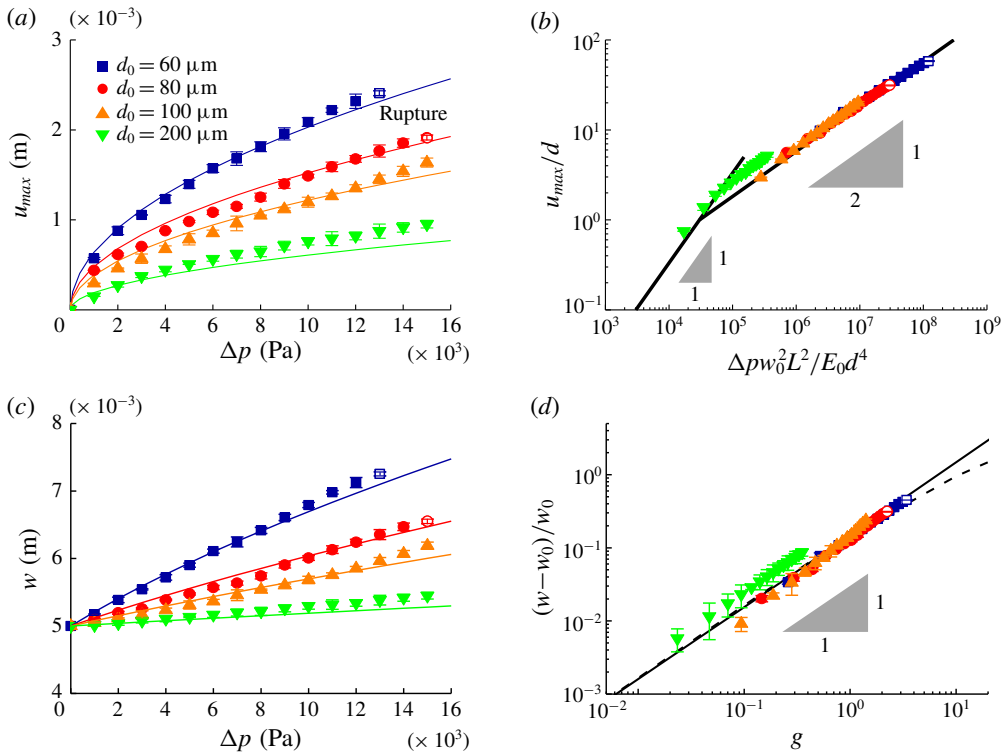


FIGURE 3. (Colour online) Experimental data. (a) Maximum displacement of the membrane u_{max} as a function of the pressure drop Δp . Solid lines show the function $u_{max} = \beta'd(\Delta pw_0^2L^2/E_0d^4)^{1/2}$, where we fit $\beta' = 5.8 \times 10^{-3}$. (b) Rescaled maximum dimensionless displacement plotted as a function of dimensionless applied pressure drop, illustrating the data collapse (solid line). (c) Measured membrane width w as a function of the pressure drop Δp . Solid lines show the function $w = w_0\lambda$, where λ is the deformation ratio of the membrane represented in (2.2). (d) Rescaled dimensionless membrane width plotted as a function of $g = 16\beta^2L^2\Delta p/E_0d_0^2$, illustrating the data collapse (solid line is a linear fit and dashed line is (2.2)). The membranes start to rupture at $\Delta p_c > 10$ kPa (open symbols).

quadratic curve whose x -intercepts are fixed by the width of the channel $x = \pm w_0/2$. Hence, the displacement of the membrane can be expressed as

$$u(x) = \frac{4u_{max}}{w_0^2} \left(\frac{w_0}{2} + x \right) \left(\frac{w_0}{2} - x \right), \tag{2.1}$$

where from our observations $u_{max} \sim \beta'd(\Delta pw_0^2L^2/E_0d^4)^{1/2}$ is a function of the applied pressure drop and membrane thickness. This u_{max} can be approximated using the undeformed dimensions as $u_{max} = \beta d_0(\Delta pw_0^2L^2/E_0d_0^4)^{1/2}$, where $\beta = 7.4 \times 10^{-3}$. The stretched width of the deformed membrane, w , was calculated from the arc length of the quadratic curve as $\int \sqrt{1 + (du/dx)^2} dx$. We expressed this as a deformation ratio of the membrane, λ , as

$$w = \frac{w_0}{2} \left(\sqrt{1 + g} + \frac{\sinh^{-1} \sqrt{g}}{\sqrt{g}} \right) = w_0\lambda, \tag{2.2}$$

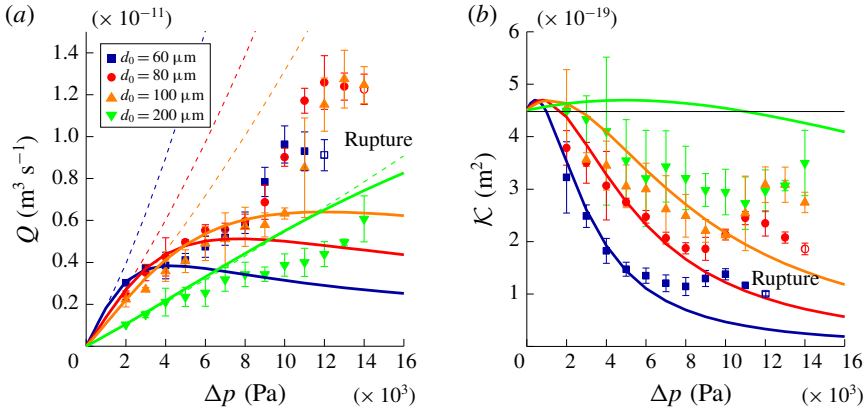


FIGURE 4. (Colour online) Experimental data and comparison to theory. (a) Flow rate Q plotted as a function of pressure drop Δp (symbols). (b) Membrane permeability κ plotted as a function of pressure drop Δp (symbols). The open symbols in (a,b) mean the rupture threshold value Δp_c . The dashed lines in (a) illustrate Darcy's law with a simple geometric correction and constant permeability $\kappa_0 = 0.45 \text{ nm}^2$ (2.3). The solid lines in (a,b) show our full model, where the microscopic pore structure is altered by the macroscopic deformation of the membrane (3.7).

where $g = (4u_{max}/w_0)^2 = 16\beta^2 L^2 \Delta p / E_0 d_0^2$. This model of the membrane width w is in accord with experimental data (figure 3c) and the experimental data collapse to one line after scaling (figure 3d).

Having established the relationship between applied pressure drop and membrane area, the remaining essential parameter in Darcy's law (1.1) is the thickness of the deformed membrane d . We can estimate the value of d by noting that Poisson's ratio for PDMS is approximately $\nu \simeq 0.5$ (Johnston *et al.* 2014). Volume conservation then dictates that $V_0 = Lwd$ is constant, i.e. the thickness can be expressed as $d = d_0 w_0 / w$.

With these observed variations in membrane dimensions (2.2), we can now express Darcy's law (1.1) as

$$Q = \kappa \frac{Lw_0}{\eta d_0} \Delta p \lambda^2. \quad (2.3)$$

However, it remains unclear whether the permeability κ is also affected by the deformation of the membrane.

2.3. Results: membrane permeability

To quantify the permeability κ of the PDMS membrane, we measured the liquid flow rate Q between the enclosed channel and the surrounding reservoir driven by the applied pressure drop Δp . At relatively low pressures, our experiments show a linear relationship between flow rate Q and applied pressure drop Δp (figure 4a), in accord with (1.1) and (2.3) with constant permeability $\kappa_0 = 0.45 \text{ nm}^2$ (figure 4b). At moderate pressures, however, the data deviate from this trend; the flow rate Q scales sub-linearly with the applied pressure drop Δp . Finally, the flow rate increases sharply as the pressure approaches the rupture threshold value Δp_c .

Comparing our data to the modified Darcy equation (2.3), in figure 4(a), we observe reasonable agreement at low pressures. However, this model, which assumes

a constant permeability $\kappa = \kappa_0$, is clearly unable to account for the sub-linear scaling of flow with pressure drop at moderate to high pressures (figure 4a). To further elucidate the link between permeability and applied pressure drop, we can determine the effective permeability directly from the observed data by solving for κ in (2.3):

$$\kappa = \frac{Q\eta d_0}{Lw_0\Delta p}\lambda^{-2}, \quad (2.4)$$

shown in figure 4(b) as symbols. According to our data, the effective permeability decreases with pressure. In the following, we proceed and attempt to rationalize the observed decrease in permeability due to changes in the membrane microstructure.

3. Theory

3.1. Effects of pore deformation on membrane permeability

We consider flow through a PDMS membrane to elucidate the impact of macroscopic deformations on the membrane permeability κ . We model PDMS as a porous medium containing numerous interconnected channels. To understand how the deformation of the internal nano-dimension channels caused by membrane deformation affects the permeability, we introduce a simplified geometric model (figure 5a). In our model, the pore structure in a cube with sides of length ℓ are cylindrical channels consisting of vertical and horizontal tubes of equal hydraulic resistance that connect the inlet and outlet at random positions on the top and bottom of the cube (figure 5b). The total length of vertical channels is the same as the height of the cube, i.e. ℓ . The inlet and outlet are located at random positions (x, y) and $(x + \Delta x, y + \Delta y)$ representing values of horizontal distance, $b\ell = \sqrt{(\Delta x)^2 + (\Delta y)^2}$, where b is a constant. The horizontal length between the inlet and outlet was calculated from the probability of positions. We assume that all locations for the inlet/outlet on the top/bottom of cube are randomly distributed with same probability. Within the various combinations, the horizontal channel length was decided as 0.52ℓ , which gave the maximum probability among inlet and outlet locations.

When the pressure is applied, the cube is deformed in the same proportion as the membrane as follows: $\ell \rightarrow \ell\lambda$, $\ell \rightarrow \ell/\lambda$ and $\ell \rightarrow \ell$ in width, thickness and length, respectively. As shown in figure 5(c), the nanochannel is also deformed along with the cube so that the cross-section of a channel is transformed from circular to elliptic, and its length is also changed. The hydraulic resistance of a vertical channel decreases due to the increasing cross-sectional area and the reduction in length, whereas the hydraulic resistance of a horizontal channel increases.

The relation between pressure drop and flow rate for elliptic cylinders of semi-axes r_1 and r_2 is given by (see Bruus 2007)

$$Q_p = \frac{\pi}{4} \frac{1}{\eta\ell_c} \frac{r_1^3 r_2^3}{r_1^2 + r_2^2} \Delta p = \frac{\Delta p}{R}, \quad (3.1)$$

where Q_p is the Poiseuille flow rate, Δp is the applied pressure drop, R is the hydraulic resistance and ℓ_c is the channel length. In a circular channel, $r_1 = r_2 = r_0$, where r_0 is the radius of the circular channel without deformation. When the cube of PDMS is deformed (figure 5c), the inner channel is significantly deformed. This can be represented by an effective elastic modulus of the channel $E_c = E_0(\Delta\ell/\ell)/(\Delta r/r) = (1/c)E_0$, where $\ell + \Delta\ell = \ell\lambda$, since the liquid inside the

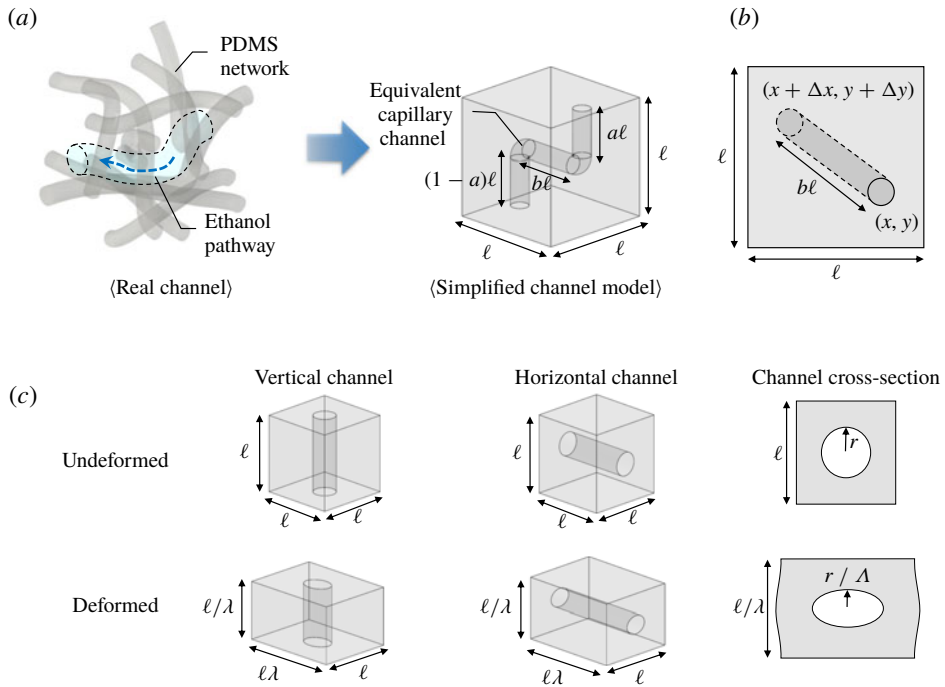


FIGURE 5. (Colour online) (a) In a real PDMS membrane, the fluid flows within small and complex shape pores and channels surrounded by the PDMS network. A representative complex channel is simplified as an equivalent capillary channel assuming that it has the same hydraulic resistance as the real channel. (b) The top view of the simplified channel model shows the length of horizontal channel, which can be estimated using statistical methods. (c) Schematics of the deformation of simplified (nano)channels in a PDMS network. The vertical/horizontal channels are deformed into wide/narrow and long/short shapes. Since the wall and the interior of the channel have different physical properties, channels deform more than bulk PDMS ($r/\Lambda = r/[1 + c(\lambda - 1)]$).

channel is also affected (see Gangi 1978; Zhang *et al.* 2007). A correction factor $c = 7$, the value of which was selected by comparison with the experiments, was introduced to apply the effective elastic modulus of the channel and allowed for r_1 , r_2 and ℓ_c to be expressed as a function of pressure drop according to

$$\left. \begin{array}{l} \text{Horizontal: } r_1 = r_0, \quad r_2 = r_0/\Lambda, \quad \ell_c = b\ell\lambda, \\ \text{Vertical: } r_1 = r_0\Lambda, \quad r_2 = r_0, \quad \ell_c = \ell/\lambda, \end{array} \right\} \quad (3.2)$$

where the deformation ratio of the channel Λ is

$$\Lambda = (r + \Delta r)/r = 1 + c(\lambda - 1). \quad (3.3)$$

In this notation, the hydraulic resistances of the horizontal channel R_H and vertical channel R_V can be written as

$$\left. \begin{array}{l} R_H = b(R_0/2)\lambda(\Lambda^3 + \Lambda), \\ R_V = (R_0/2)(1/\lambda)(1/\Lambda^3 + 1/\Lambda), \end{array} \right\} \quad (3.4)$$

where the hydraulic resistance of a circular channel is $R_0 = 8\eta\ell/\pi r_0^4$. The total resistance of the deformed channel is $R_{tot} = R_H + R_V$, since the nanochannels are connected in series. The initial total resistance is $R_i = (1 + b)R_0$.

To determine the effective permeability, we note that Darcy's law represents the total flow rate through a porous medium, which is composed of individual channels. Assuming that the PDMS membrane consists of n parallel channels, the total flow is

$$Q = nQ_p. \quad (3.5)$$

Finally, from the general relations between flow and applied pressure drop ($Q \approx \kappa \Delta p \approx \Delta p/R$), it is clear that hydraulic resistance R and permeability κ , as defined here, are inversely related. From these considerations, we can express the pressure-dependent permeability κ as a function of the deformation ratio of the membrane λ and the channel Λ by

$$\kappa = \kappa_0 \frac{R_i}{R_{tot}} = \kappa_0 \frac{2(1+b)\lambda\Lambda^3}{(1+\Lambda^2)(1+b\lambda^2\Lambda^4)}, \quad (3.6)$$

where κ_0 is the permeability of the undeformed PDMS membrane, Λ is $1 + c(\lambda - 1)$ and the constants b and c are 0.52 and 7, respectively.

3.2. Comparison between theory and experiments

With the expression for the pressure-dependent permeability κ (3.6), we are now in a position to reformulate Darcy's law (2.3) for the deformable material:

$$Q = \frac{\kappa_0 L w_0}{\eta d_0} \Delta p \frac{2(1+b)\lambda^3 \Lambda^3}{(1+\Lambda^2)(1+b\lambda^2\Lambda^4)}. \quad (3.7)$$

Comparing our data to the modified permeability (3.6) and Darcy equation (3.7), we observe good agreement at both low and moderate pressures (figure 4). In the case of $d_0 = 200 \mu\text{m}$ where deformation is small, the flow rate does not agree well because the model equation (2.2) underestimates the actual experiment (figure 3). Data near the rupture pressure drop Δp_c deviate from our model in that the permeability increases with the deformation, presumably due to the formation of microscopic ruptures in the membrane, or violations of the no-slip boundary condition at sufficiently small length scales (e.g. Choi *et al.* 2003; Priezjev 2007; Ramos-Alvarado, Kumar & Peterson 2016; Hu *et al.* 2017).

4. Conclusion

In this study, we investigated the permeability of deformed hyperelastic thin PDMS membranes in pressure-driven flow. Our experimental results were inconsistent with Darcy's law (1.1) with constant permeability κ_0 , and revealed that the flow rate Q depends nonlinearly on the applied pressure drop Δp (figure 4). These observations suggest that the effective permeability κ decreases until a moderate pressure drop and then increases before rupture. To rationalize our data, we developed a model that incorporates the effects of pressure-induced deformation at distinct scales: at macroscopic scale, the membrane surface area increases while the membrane thickness decreases with pressure; whereas at the nanoscale, the structure of the porous material, modelled as nanochannels, is deformed. With these corrections to the permeability (3.6) and Darcy's equation (3.7), we observe a good agreement between theory and

experiments (figure 4) at low to moderate pressures. Data near the rupture pressure deviate from our model, presumably due to the formation of microscopic ruptures in the membrane, or violations of the no-slip boundary conditions at sufficiently small length scales. Our results represent a novel case in which macroscopic deformations can have an impact on the microstructure and transport properties of soft materials. It would be beneficial to apply the results to design or understand other mass transport processes through soft, deformed porous membranes.

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REFERENCES

- AMABILI, M., BALASUBRAMANIAN, P., BRESLAVSKY, I. D., FERRARI, G., GARZIERA, R. & RIABOVA, K. 2016 Experimental and numerical study on vibrations and static deflection of a thin hyperelastic plate. *J. Sound Vib.* **385**, 81–92.
- BHANUSHALI, D., KLOOS, S., KURTH, C. & BHATTACHARYYA, D. 2001 Performance of solvent-resistant membranes for non-aqueous systems: solvent permeation results and modeling. *J. Membr. Sci.* **189** (1), 1–21.
- BOUREMEL, Y., MADAAN, S., LEE, R. M. H., EAMES, I., WOJCIK, A. & KHAW, P. T. 2017 Pursing of planar elastic pockets. *J. Fluids Struct.* **70**, 261–275.
- BRUUS, H. 2007 *Theoretical Microfluidics*. Oxford University Press.
- CHANG, K. S., CHUNG, Y. C., YANG, T. H., LUE, S. J., TUNG, K. L. & LIN, Y. F. 2012 Free volume and alcohol transport properties of PDMS membranes: insights of nano-structure and interfacial affinity from molecular modeling. *J. Membr. Sci.* **417**, 119–130.
- CHOI, C. H., WESTIN, K., JOHAN, A. & BREUER, K. 2003 Apparent slip flows in hydrophilic and hydrophobic microchannels. *Phys. Fluids* **15** (10), 2897–2902.
- DARVISHMANESH, S., BUEKENHOUDT, A., DEGRÈVE, J. & VAN DER BRUGGEN, B. 2009 General model for prediction of solvent permeation through organic and inorganic solvent resistant nanofiltration membranes. *J. Membr. Sci.* **334** (1), 43–49.
- DHOPESHWARKAR, R., CROOKS, R., HLUSHKOU, D. & TALLAREK, U. 2008 Transient effects on microchannel electrokinetic filtering with an ion-permselective membrane. *Anal. Chem.* **80** (4), 1039–1048.
- DUFFY, D. C., McDONALD, J. C., SCHUELLER, O. J. A. & WHITESIDES, G. M. 1998 Rapid prototyping of microfluidic systems in poly(dimethylsiloxane). *Anal. Chem.* **70** (23), 4974–4984.
- EBERT, K., KOLL, J., DIJKSTRA, M. F. J. & EGGERS, M. 2006 Fundamental studies on the performance of a hydrophobic solvent stable membrane in non-aqueous solutions. *J. Membr. Sci.* **285** (1), 75–80.
- FIRPO, G., ANGELI, E., REPETTO, L. & VALBUSA, U. 2015 Permeability thickness dependence of polydimethylsiloxane (PDMS) membranes. *J. Membr. Sci.* **481**, 1–8.
- GANGI, A. F. 1978 Variation of whole and fractured porous rock permeability with confining pressure. *Intl J. Rock Mech. Min Sci. Geomech. Abstr.* **15** (5), 249–257.
- GEENS, J., VAN DER BRUGGEN, B. & VANDECASTEELE, C. 2004 Characterisation of the solvent stability of polymeric nanofiltration membranes by measurement of contact angles and swelling. *Chem. Engng Sci.* **59** (5), 1161–1164.
- HU, H., BAO, L., PRIEZJEV, N. V. & LUO, K. 2017 Identifying two regimes of slip of simple fluids over smooth surfaces with weak and strong wall–fluid interaction energies. *J. Chem. Phys.* **146** (3), 034701.

- ISMAIL, A. E., GREST, G. S., HEINE, D. R., STEVENS, M. J. & TSIGE, M. 2009 Interfacial structure and dynamics of siloxane systems: PDMS-vapor and PDMS-water. *Macromolecules* **42** (8), 3186–3194.
- JEONG, O. C. & KONISHI, S. 2007 Fabrication and drive test of pneumatic PDMS micro pump. *Sensors Actuators A* **135** (2), 849–856.
- JO, B. H., VAN LERBERGHE, L. M., MOTSEGOOD, K. M. & BEEBE, D. J. 2000 Three-dimensional micro-channel fabrication in polydimethylsiloxane (PDMS) elastomer. *J. Microelectromech. Syst.* **9** (1), 76–81.
- JOHNSTON, I. D., MCCLUSKEY, D. K., TAN, C. K. L. & TRACEY, M. C. 2014 Mechanical characterization of bulk Sylgard 184 for microfluidics and microengineering. *J. Micromech. Microengng* **24** (3), 035017.
- KORESH, J. E. & SOFER, A. 1983 Molecular sieve carbon permselective membrane. Part I. Presentation of a new device for gas mixture separation. *Sep. Sci. Technol.* **18** (8), 723–734.
- MAKRODIMITRI, Z. A. & ECONOMOU, I. G. 2008 Atomistic simulation of poly(dimethylsiloxane) permeability properties to gases and n-alkanes. *Macromolecules* **41** (15), 5899–5907.
- NUNES, L. C. S. 2011 Mechanical characterization of hyperelastic polydimethylsiloxane by simple shear test. *Mater. Sci. Engng A* **528** (3), 1799–1804.
- PENG, F., JIANG, Z., HU, C., WANG, Y., XU, H. & LIU, J. 2006 Removing benzene from aqueous solution using CMS-filled PDMS pervaporation membranes. *Sep. Purif. Technol.* **48** (3), 229–234.
- PERNAUT, J. M. & REYNOLDS, J. R. 2000 Use of conducting electroactive polymers for drug delivery and sensing of bioactive molecules. A redox chemistry approach. *J. Phys. Chem. B* **104** (17), 4080–4090.
- PHILLIP, W. A., AMENDT, M., O'NEILL, B., CHEN, L., HILLMYER, M. A. & CUSSLER, E. L. 2009 Diffusion and flow across nanoporous polydicyclopentadiene-based membranes. *ACS Appl. Mater. Interfaces* **1** (2), 472–480.
- PRIEZJEV, N. V. 2007 Effect of surface roughness on rate-dependent slip in simple fluids. *J. Chem. Phys.* **127** (14), 144708.
- PRISKE, M., LAZAR, M., SCHNITZER, C. & BAUMGARTEN, G. 2016 Recent applications of organic solvent nanofiltration. *Chem. Ing. Tech.* **88** (1–2), 39–49.
- RAMOS-ALVARADO, B., KUMAR, S. & PETERSON, G. P. 2016 Wettability transparency and the quasiuniversal relationship between hydrodynamic slip and contact angle. *Appl. Phys. Lett.* **108** (7), 074105.
- RAZDOLSKY, A. G. 2015 Large deflections of elastic rectangular plates. *Intl J. Comput. Meth. Engng Sci. Mech.* **16** (6), 354–361.
- REGO, R. & MENDES, A. 2004 Carbon dioxide/methane gas sensor based on the permselectivity of polymeric membranes for biogas monitoring. *Sensors Actuators B* **103** (1), 2–6.
- ROBINSON, J. P., TARLETON, E. S., EBERT, K., MILLINGTON, C. R. & NIJMEIJER, A. 2005 Influence of cross-linking and process parameters on the separation performance of poly(dimethylsiloxane) nanofiltration membranes. *Ind. Engng Chem. Res.* **44** (9), 3238–3248.
- SANAEI, P. & CUMMINGS, L. J. 2017 Flow and fouling in membrane filters: effects of membrane morphology. *J. Fluid Mech.* **818**, 744–771.
- SANAEI, P. & CUMMINGS, L. J. 2018 Membrane filtration with complex branching pore morphology. *Phys. Rev. Fluids* **3**, 094305.
- SELVADURAI, A. P. S. & SHI, M. 2012 Fluid pressure loading of a hyperelastic membrane. *Intl J. Non-Linear Mech.* **47** (2), 228–239.
- SOLTANE, H. B., ROIZARD, D. & FAVRE, E. 2013 Effect of pressure on the swelling and fluxes of dense PDMS membranes in nanofiltration: an experimental study. *J. Membr. Sci.* **435**, 110–119.
- STAFIE, N., STAMATIALIS, D. F. & WESSLING, M. 2005 Effect of PDMS cross-linking degree on the permeation performance of PAN/PDMS composite nanofiltration membranes. *Sep. Purif. Technol.* **45** (3), 220–231.
- TSURU, T., SUDOU, T., KAWAHARA, S., YOSHIOKA, T. & ASAEDA, M. 2000 Permeation of liquids through inorganic nanofiltration membranes. *J. Colloid Interface Sci.* **228** (2), 292–296.

- VANKELECOM, I. F. J., DE SMET, K., GEVERS, L. E. M., LIVINGSTON, A., NAIR, D., AERTS, S., KUYPERS, S. & JACOBS, P. A. 2004 Physico-chemical interpretation of the SRNF transport mechanism for solvents through dense silicone membranes. *J. Membr. Sci.* **231** (1), 99–108.
- VANKELECOM, I. F. J., DOTREMONT, C., MOROBE, M., UYTTERHOEVEN, J. B. & VANDECASTEELE, C. 1997 Zeolite-filled PDMS membranes. 1. Sorption of halogenated hydrocarbons. *J. Phys. Chem. B* **101** (12), 2154–2159.
- WANG, D. & EL-SHEIKH, A. I. 2005 Large-deflection mathematical analysis of rectangular plates. *J. Engng Mech. ASCE* **131** (8), 809–821.
- ZHANG, J., STANDIFIRD, W. B., ROEGIERS, J. C. & ZHANG, Y. 2007 Stress-dependent fluid flow and permeability in fractured media: from lab experiments to engineering applications. *Rock Mech. Rock Engng* **40** (1), 3–21.