

Relationship between the energy dissipation function and the skin friction law in a turbulent channel flow

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Integrals of the mean and turbulent energy dissipation rates are examined using direct numerical simulation (DNS) databases in a turbulent channel flow. Four values of the Kármán number ($h^+ = 180, 395, 640$ and 1020 ; h is the channel half-width) are used. Particular attention is given to the functional h^+ dependence by comparing existing DNS and experimental data up to $h^+ = 10^4$. The logarithmic h^+ dependence of the integrated turbulent energy dissipation rate is established for $300 \leq h^+ \leq 10^4$, and is intimately linked to the logarithmic skin friction law, *viz.* $U_b^+ = 2.54 \ln(h^+) + 2.41$ (U_b is the bulk mean velocity). This latter relationship is established on the basis of energy balances for both the mean and turbulent kinetic energy. When h^+ is smaller than 300, viscosity affects the integrals of both the mean and turbulent energy dissipation rates significantly due to the lack of distinct separation between inner and outer regions. The logarithmic h^+ dependence of U_b^+ is clarified through the scaling behaviour of the turbulent energy dissipation rate $\bar{\epsilon}$ in different parts of the flow. The overlap between inner and outer regions is readily established in the region $30/h^+ \leq y/h \leq 0.2$ for $h^+ \geq 300$. At large h^+ (≥ 5000) when the finite Reynolds number effect disappears, the magnitude of $\bar{\epsilon}y/U_\tau^3$ approaches 2.54 near the lower bound of the overlap region. This value is identical between the channel, pipe and boundary layer as a result of similarity in the constant stress region. As h^+ becomes large, the overlap region tends to contribute exclusively to the $2.54 \ln(h^+)$ dependence of the integrated turbulent energy dissipation rate. The present logarithmic h^+ dependence of U_b^+ is essentially linked to the overlap region, even at small h^+ .

Key words: turbulence simulation, turbulent boundary layers, turbulent flows

1. Introduction

Since the earlier experimental studies by Laufer (1951) and Comte-Bellot (1963), the fully developed turbulent channel flow has received a great deal of attention, both experimentally and numerically, due mainly to the simplicity of the flow geometry and consequent simplifications that can be made to the governing equations of motion. A major stimulus for unravelling various aspects of the physics of turbulence,

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especially close to the wall, was provided by the direct numerical simulation (DNS) of Kim, Moin & Moser (1987) in which the governing equations were solved directly so that all the essential scales of the motion were resolved. In their DNS, the data were obtained at a relatively small value ($=180$) of the Kármán number h^+ ($\equiv U_\tau h/\nu$), which represents the ratio of the half-width of the channel h and the viscous length scale ν/U_τ ($U_\tau \equiv (\tau_w/\rho)^{1/2}$) is the friction velocity, where τ_w is the wall shear stress and ρ is the density of the fluid; the superscript $+$ will subsequently denote normalization by ν/U_τ and U_τ). Since then, many DNSs (e.g. Moser, Kim & Mansour 1999; Abe, Kawamura & Matsuo 2001, 2004a; Iwamoto, Suzuki & Kasagi 2002; Abe, Kawamura & Choi 2004b; del Álamo *et al.* 2004; Tanahashi *et al.* 2004; Hu, Morfey & Sandham 2006; Laadhari 2007; Hoyas & Jiménez 2008; Abe, Antonia & Kawamura 2009; Bernardini, Pirozzoli & Orlandi 2014; Lozano-Durán & Jiménez 2014; Vreman & Kuerten 2014; Lee & Moser 2015) have been performed at increasingly larger values of h^+ in the same flow. To date, the maximum value for h^+ reached in the DNS of the present flow is 5000 (Lee & Moser 2015) without compromising spatial resolution requirements. This is about a factor of 2 smaller than the maximum value achieved in the laboratory by Comte-Bellot (1963) by using a large physical value of h ($= 0.09$ m).

A major difficulty in experiments is the accurate determination of the wall shear stress τ_w . In this context, significant attention has been given to the streamwise length (L) and the aspect ratio (AR) of the channel. To achieve a fully developed flow with $d\bar{P}/dx = \text{const.}$, a relatively long channel is required (Monty (2005) suggests $L = 260h$). The AR also needs to be as large as possible to avoid possible side wall effects and hence ensure two-dimensionality (Monty (2005) suggests that the AR should be at least 12). When these requirements are met, the momentum balance over a control volume which extends across the whole section of the channel and includes the two walls yields

$$\tau_w = -h \frac{d\bar{P}}{dx}. \quad (1.1)$$

However, in order to check that momentum is conserved on an integral basis, an independent, preferably direct estimate of τ_w is needed. Zanoun, Durst & Nagib (2003) have estimated τ_w using both the measured pressure gradient and the oil film interferometry technique in a fully developed channel flow. Good agreement between the two estimates was obtained for values of h^+ extending up to $h^+ \approx 5000$. The corresponding data for the skin friction coefficient defined as

$$C_f \equiv \tau_w / \frac{1}{2} \rho U_b^2 = 2 / U_b^{+2} \quad (1.2)$$

(U_b is the bulk mean velocity defined in the channel as $U_b \equiv (1/h) \int_0^h \bar{U} dy$) were consistent with Dean's (1978) well-known power-law formulation as a function of Re_b ($\equiv U_b 2h/\nu$), viz.

$$C_f = 0.073 Re_b^{-1/4}. \quad (1.3)$$

Recently, Zanoun, Nagib & Durst (2009) observed that the logarithmic skin friction relation

$$U_b^+ = \frac{1}{\kappa} \ln(h^+) - \frac{1}{\kappa} + A \quad (1.4)$$

or, equivalently,

$$\sqrt{\frac{2}{C_f}} = \frac{1}{\kappa} \ln \left(Re_b \sqrt{C_f} / 2\sqrt{2} \right) - \frac{1}{\kappa} + A \quad (1.5)$$

obtained from the logarithmic law of the wall

$$U^+ = \frac{1}{\kappa} \ln(y^+) + A \quad (1.6)$$

(κ and A denote the Kármán constant and the additive constant, respectively), with $\kappa = 0.37$ and $A = 3.7$, as obtained by Zanoun *et al.* (2003), represents more accurately the experimental skin friction data than Dean's (1978) formula (1.3), in particular, for $h^+ > 2000$ (see figure 5 of their paper). Relation (1.4) is obtained by integrating (1.6) across the channel. Although this may be valid strictly when $h^+ \rightarrow \infty$, the mean velocity profiles of Zanoun *et al.* (2003) do not deviate significantly from the log law over a wide cross-section of the flow (this was also confirmed by Monty *et al.* (2007)). More recently, Schultz & Flack (2013) made laser Doppler velocimetry measurements in the range $h^+ = 1000$ – 6000 and employed (1.1) to determine τ_w . They reported that the logarithmic friction relation (1.4) with $\kappa = 0.40$ and $A = 5.0$ provides a good fit to their experimental data.

An interesting question which arises from the above observations is why a skin friction relation, based on log-law constants which can only be defined, with some degree of confidence, for $h^+ > 2000$, represents adequately data at values of h^+ that are smaller by almost one order of magnitude. For example, for the $h^+ = 180$ DNS channel data of Kim *et al.* (1987), C_f is approximately 8% smaller than the prediction by the logarithmic skin friction law (1.5). It is also only approximately 3% smaller than the value given by Dean's (1978) relation (1.3) (see also figure 1 of Abe *et al.* (2001)). We explore this theme by focusing almost exclusively on the behaviour of the turbulent dissipation rate; this approach provides an answer to the question raised above. Particular attention is given to the energy dissipation function E (Rotta 1962) since E/U_τ^3 is equal to U_b^+ . This latter relation is obtained readily by considering that the total energy dissipated in the channel is equal to the energy input via the mean pressure gradient, *viz.*

$$E = -\frac{1}{\rho} \frac{d\bar{P}}{dx} U_b h = U_\tau^2 U_b \quad \text{or equivalently,} \quad U_b^+ = E/U_\tau^3. \quad (1.7)$$

Possible relations for U_b^+ are therefore obtained on the basis of not only the velocity log law (*viz.* (1.4)), but also via E (*viz.* (1.7)). This approach provides an interesting insight into the logarithmic skin friction law since the logarithmic h^+ dependence of U_b^+ appears to be established at lower Reynolds numbers than the velocity log law. In this context, Laadhari (2007) examined the relative contributions of the turbulent strain rate $\bar{\epsilon}$ and that which arises from the mean strain rate $\bar{\epsilon}_{mean}$, *viz.*

$$E \equiv \underbrace{\nu \overline{u_{i,j}(u_{i,j} + u_{j,i})}}_{\bar{\epsilon}} + \nu \overline{U_{i,j}(\overline{U}_{i,j} + \overline{U}_{j,i})}. \quad (1.8)$$

Note that u_1, u_2, u_3 denote the streamwise, wall-normal and spanwise velocity fluctuations, respectively; u, v, w are used interchangeably with u_1, u_2, u_3 ; ν denotes the kinematic viscosity and the overbar denotes averaging with respect to x, z (x, y, z are the streamwise, wall-normal and spanwise directions, respectively) and t (time); upper cases denote instantaneous quantities. He noted that the logarithmic friction relation is obtained from E , with $\kappa = 0.38$ and $A = 4.65$, and the resulting relation agrees well with his DNS data for $h^+ > 500$ as well as the higher h^+ data of Zanoun *et al.* (2003). In the present paper, we extend Laadhari's (2007) work and assess how

E varies over a wider range of h^+ than covered by Laadhari (2007). In particular, we try to clarify how the logarithmic dependence of U_b^+ is established by focusing on how the turbulent energy dissipation rate $\bar{\epsilon}$ scales in different regions of the channel. We also give significant attention to the overlap scaling of $\bar{\epsilon}$ by applying a matching argument to elucidate the outer layer similarity we observe for $\bar{\epsilon}$.

This paper is organized as follows. In § 2, E is explained in the context of a turbulent channel flow. A brief description is given in § 3 of the present DNS databases for the channel flow. The effect of the streamwise domain on E is addressed in § 4.1. Results for the dependence of E on h^+ are presented in § 4.2 together with available DNS and experimental data. Section 4.3 extends the U_b^+ relation established in § 4.2 to a pipe flow since (1.7) holds in internal flows. The relationship between the resulting $\ln(h^+)$ dependence of U_b^+ and the scaling law of the turbulent energy dissipation rate is also discussed in some detail in §§ 4.4 and 4.5 where comparisons are made with available DNS data of $\bar{\epsilon}$ for the pipe and the zero-pressure-gradient turbulent boundary layer. Conclusions are given in § 5.

2. Relation for the energy dissipation function E in a channel flow

Rotta (1962) discussed the energy dissipation function E in some detail in the context of the boundary layer. By integrating the transport equations of the mean and turbulent kinetic energy between the wall and the freestream, he obtained

$$\begin{aligned}
 E &= \int_0^\infty \bar{\epsilon} \, dy + \int_0^\infty \nu \left(\frac{\partial \bar{U}}{\partial y} \right)^2 \, dy \\
 &= \int_0^\infty \frac{\tau}{\rho} \left(\frac{\partial \bar{U}}{\partial y} \right) \, dy - \int_0^\infty (\bar{u}^2 - \bar{v}^2) \frac{\partial \bar{U}}{\partial x} \, dy - \frac{d}{dx} \int_0^\infty \bar{U} k \, dy, \tag{2.1}
 \end{aligned}$$

where τ is the total shear stress and k the turbulent kinetic energy. Rotta (1962) underlined that the last two terms on the right of (2.1) are merely corrections and that the main contribution to E comes from the work done by the shear stress.

In a channel flow, a relation for E is obtained readily using the total shear stress relation, *viz.*

$$\frac{\tau}{\rho} \equiv -\bar{u}\bar{v} + \nu \frac{d\bar{U}}{dy} = \frac{1}{\rho} \left(\tau_w - y \frac{d\bar{P}}{dx} \right), \tag{2.2}$$

where the mean-pressure-gradient term appears. By multiplying (2.2) by $d\bar{U}/dy$, we obtain the energy balance for the mean flow, *viz.*

$$-\bar{u}\bar{v} \frac{d\bar{U}}{dy} + \nu \left(\frac{d\bar{U}}{dy} \right)^2 = \frac{1}{\rho} \left(\tau_w \frac{d\bar{U}}{dy} - y \frac{d\bar{P}}{dx} \frac{d\bar{U}}{dy} \right). \tag{2.3}$$

$(\tau_w/\rho)(d\bar{U}/dy)$ represents the rate of energy transfer from the outer part of the boundary layer to the inner region (see also DeGraaff & Eaton 2000; Morrison *et al.* 2004); the term which includes $d\bar{P}/dx$ is the energy input from the mean pressure gradient. The energy is partly dissipated directly by viscosity (the second term on the left-hand side of (2.3)) and partly extracted to turbulence via the work done by the Reynolds shear stress (the first term on the left-hand side of (2.3)).

By assuming the symmetry with respect to the centreline, the integral of (2.3) from $y = 0$ to h then leads to

$$\int_0^h -\bar{u}\bar{v} \frac{d\bar{U}}{dy} \, dy + \int_0^h \nu \left(\frac{d\bar{U}}{dy} \right)^2 \, dy = -\frac{1}{\rho} \frac{d\bar{P}}{dx} \int_0^h \bar{U} \, dy, \tag{2.4}$$

or equivalently,

$$\langle \bar{\varepsilon} \rangle + \left\langle v \left(\frac{d\bar{U}}{dy} \right)^2 \right\rangle = U_\tau^2 U_b, \quad (2.5)$$

where the angular brackets denote integration with respect to y across the channel half-width. Note that in (2.5) we also consider the energy balance for the turbulent kinetic energy so that $\langle P_k \rangle$ is replaced by $\langle \bar{\varepsilon} \rangle$ where $P_k \equiv -\overline{uv}(d\bar{U}/dy)$ since the relation

$$\langle P_k \rangle = \langle \bar{\varepsilon} \rangle, \quad (2.6)$$

which expresses equality between the net turbulent energy production and the total turbulent energy dissipation rate, holds in a channel flow. Relation (2.5) can then be arranged as follows

$$\frac{U_b}{U_\tau} = \frac{\langle \bar{\varepsilon} \rangle}{U_\tau^3} + \left\langle v \left(\frac{d\bar{U}}{dy} \right)^2 \right\rangle / U_\tau^3 = \frac{E}{U_\tau^3}. \quad (2.7)$$

Equation (2.7) is equivalent to the relationship between E/U_τ^3 and U_b/U_τ , (1.7). The viscous contribution is expected to dominate near the wall while the contribution from the turbulent energy dissipation rate should dominate elsewhere. It is also expected that the viscous term will be dominant at small h^+ whereas $\langle \bar{\varepsilon} \rangle$ should become increasingly important as h^+ becomes very large so that the h^+ dependence of U_b/U_τ , which is related to the skin friction coefficient $C_f \equiv 2(U_\tau/U_b)^2$ (1.2), should essentially reflect that of the normalized integrated energy dissipation rates across the channel.

3. DNS databases

The present numerical databases have been obtained from DNSs in a turbulent channel flow with passive scalar transport by Abe *et al.* (2004a, 2009). In the present study, we exclusively use flow field data for a fully developed turbulent channel flow driven by a constant streamwise mean pressure gradient. Four values of h^+ ($= 180, 395, 640$ and 1020) are used. We also consider other DNS data available in the literature up to $h^+ = 5200$ (Moser *et al.* 1999; Iwamoto *et al.* 2002; del Álamo *et al.* 2004; Tanahashi *et al.* 2004; Tsukahara *et al.* 2005; Hu *et al.* 2006; Laadhari 2007; Hoyas & Jiménez 2008; Bernardini *et al.* 2014; Lozano-Durán & Jiménez 2014; Vreman & Kuerten 2014; Lee & Moser 2015).

The numerical methodology for the DNSs is briefly as follows. A fractional step method is used with semi-implicit time advancement. The third-order Runge–Kutta method is used for the viscous terms in the y direction and the Crank–Nicolson method is used for the other terms. A finite difference method is adopted for the spatial discretization. A fourth-order central scheme is used in the x and z directions, whilst a second-order central scheme is used in the y direction. The periodic boundary condition is employed in the x and z directions, whereas the no-slip condition applies in the y direction. Further details of the simulations are given in Abe *et al.* (2001, 2004a,b, 2009) and Antonia, Abe & Kawamura (2009), and the reader may refer to these papers for information on basic turbulence statistics.

The computational domain size ($L_x \times L_y \times L_z$), number of grid points ($N_x \times N_y \times N_z$) and spatial resolution ($\Delta x, \Delta y, \Delta z$) are given in table 1, the superscript * representing normalization by either v_K ($\equiv (v\bar{\varepsilon})^{1/4}$; the Kolmogorov velocity scale) or η ($\equiv (v^3/\bar{\varepsilon})^{1/4}$; the Kolmogorov length scale); the subscripts w and c referring to

| h^+ | 180 | 395 | 640 | 1020 |
|--|-------------------------------|-------------------------------|--------------------------------|---------------------------------|
| $L_x \times L_y \times L_z$ | | | $12.8h \times 2h \times 6.4h$ | |
| $L_x^+ \times L_y^+ \times L_z^+$ | $2304 \times 360 \times 1152$ | $5056 \times 790 \times 2528$ | $8192 \times 1280 \times 4096$ | $13056 \times 2040 \times 6528$ |
| $N_x \times N_y \times N_z$ | $768 \times 128 \times 384$ | $1536 \times 192 \times 768$ | $2048 \times 256 \times 1024$ | $2048 \times 448 \times 1536$ |
| $\Delta x^+, \Delta y^+, \Delta z^+$ | $3.00, 0.20-5.90, 3.00$ | $3.29, 0.15-6.52, 3.29$ | $4.00, 0.15-8.02, 4.00$ | $6.38, 0.15-7.32, 4.25$ |
| $\Delta x_w^*, \Delta y_w^*, \Delta z_w^*$ | $1.94, 0.13, 1.94$ | $2.24, 0.10, 2.24$ | $2.77, 0.11, 2.77$ | $4.46, 0.11, 2.97$ |
| $\Delta x_c^*, \Delta y_c^*, \Delta z_c^*$ | $0.82, 1.62, 0.82$ | $0.74, 1.47, 0.74$ | $0.82, 1.64, 0.82$ | $1.16, 1.33, 0.77$ |

TABLE 1. Domain size, grid points and spatial resolution of the DNS databases.

| h^+ | 395 | 1020 |
|--------------|----------------|---|
| L_x | $(h, 12.8h)$ | $(0.4h, 0.8h, 1.6h, 3.2h, 6.4h, 12.8h)$ |
| L_x^+ | $(395, 5056)$ | $(408, 816, 1632, 3264, 6528, 13056)$ |
| N_x | $(40, 1536)$ | $(64, 128, 256, 512, 1024, 2048)$ |
| Δx^+ | $(9.88, 3.29)$ | 6.38 |
| Δz^+ | $(4.94, 3.29)$ | 4.25 |

TABLE 2. Information on streamwise domain size, grid points and spatial resolution need for testing the effect of L_x on the quantities plotted in figures 1 and 2.

the wall and centreline, respectively. The effect of the domain size was examined by Abe *et al.* (2004b) ($h^+ = 640$) who compared two cases: $(L_x \times L_z) = (6.4h \times 2h)$ and $(12.8h \times 6.4h)$. They found that the effect on the mean flow variables and second-order moments was negligible. They also examined one-dimensional energy spectra and noted that their streamwise domain size was not large enough to include all the large-scale contributions, whereas their spanwise domain size was quite sufficient. Abe *et al.* (2004b) also reported that the most energetic spanwise wavelength of u is approximately 1.3–1.6 h in the outer region. The identical behaviour was also observed for $h^+ = 1020$ (see figure 4b of Antonia *et al.* (2009)) and for $h^+ = 2022$ and 4079 (see figure 13a of Bernardini *et al.* (2014)), which supports the finding of Flores & Jiménez (2010) and Lozano-Durán & Jiménez (2014) that $L_z = \pi h$ is sufficient to obtain good one-point statistics up to the centre of the channel.

In §4.1, we further examine the effect of L_x on the main quantities of interest, *viz.* those which contribute most significantly to E . This will be done for $h^+ = 395$ and 1020 by varying the streamwise domain size, while keeping the spanwise domain constant (Abe *et al.* 2007). The domain size, number of grid points and spatial resolutions are listed in table 2. The smallest streamwise domain for $h^+ = 395$ and 1020 is $L_x^+ \approx 400$, which is the minimal unit of near-wall turbulence (Jiménez & Moin 1991). We also compare our results with other DNS data obtained with different domain sizes (Lozano-Durán & Jiménez 2014; Lee & Moser 2015).

4. Results for the energy dissipation function E

4.1. Effect of the streamwise domain

We first clarify the effect of L_x on the total energy dissipation E . Distributions of $\langle \nu(d\bar{U}/dy)^2 \rangle$ and $\langle \bar{\epsilon} \rangle$ normalized by U_τ^3 are shown in figure 1 as a function of L_x/h for both $h^+ = 395$ and 1020. Also included in figure 1(a) are the data of Lozano-Durán & Jiménez (2014) at $h^+ = 4179$ with $L_x = 2\pi h$ and Lee & Moser (2015) at $h^+ = 1000$ and 5186 with $L_x = 8\pi h$ since $\langle \nu(d\bar{U}/dy)^2 \rangle/U_\tau^3$ is constant for $h^+ \geq 300$ (see figure 3a) and the departure from constancy corresponds to the L_x effect. It is shown that the viscous energy dissipation rate $\langle \nu(d\bar{U}/dy)^2 \rangle/U_\tau^3$ increases with decreasing L_x when $L_x < 2h$. This is caused by the thickened buffer region as L_x decreases (see figure 2a where the distributions of $(d\bar{U}^+/dy^+)^2$ are shown). $\langle \bar{\epsilon} \rangle/U_\tau^3$ is however essentially unaffected by L_x/h , whereas $\langle \bar{\epsilon}_{11} \rangle/U_\tau^3$ (the streamwise component of the dissipation) is affected in a similar manner to $\langle \nu(d\bar{U}/dy)^2 \rangle/U_\tau^3$. This is closely associated with the energy redistribution where the pressure strain rate and pressure diffusion terms, *viz.*

$$\phi_{ij}^+ = p^+ \overline{\left(\frac{\partial u_i^+}{\partial x_j^+} + \frac{\partial u_j^+}{\partial x_i^+} \right)} \quad (4.1)$$

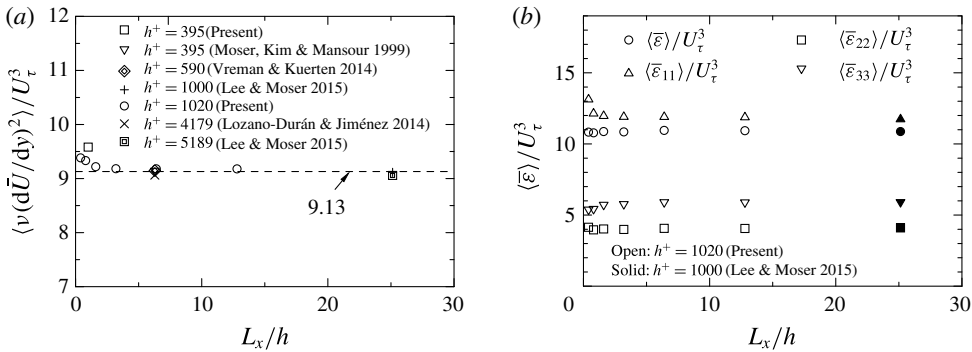


FIGURE 1. Distributions of $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$ and $\langle \bar{\epsilon} \rangle / U_\tau^3$ in a channel flow as a function of L_x/h : (a) $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$; (b) $\langle \bar{\epsilon} \rangle / U_\tau^3$.

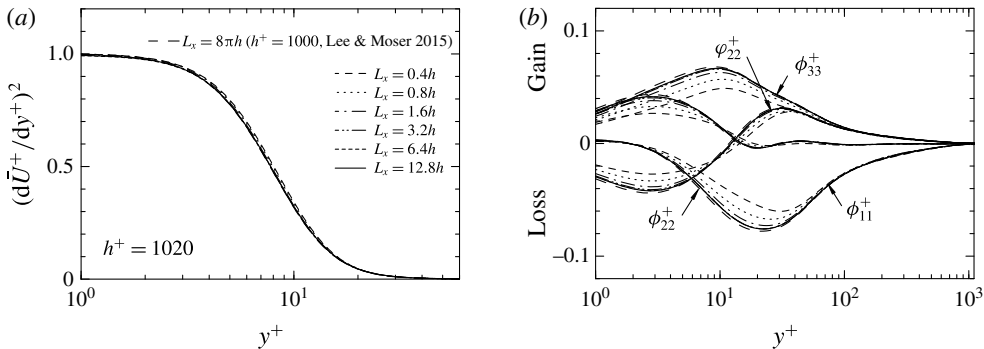


FIGURE 2. Distributions of $(d\bar{U}^+/dy^+)^2$, ϕ_{ij}^+ and ϕ_{22}^+ in a channel flow for $h^+ = 1020$: (a) $(d\bar{U}^+/dy^+)^2$; (b) ϕ_{ij}^+ and ϕ_{22}^+ .

and

$$\phi_{ij}^+ = - \left(\frac{\partial}{\partial x_i^+} \overline{u_j^+ p^+} + \frac{\partial}{\partial x_j^+} \overline{u_i^+ p^+} \right), \tag{4.2}$$

play an important role. Distributions of ϕ_{ij}^+ and ϕ_{ij}^+ are shown in figure 2(b) for $h^+ = 1020$. The data of Lee & Moser (2015) for $h^+ = 1000$ with $L_x = 8\pi h$ are also plotted. For $L_x < 6.4h$, the magnitudes of ϕ_{11}^+ , ϕ_{22}^+ and ϕ_{33}^+ are attenuated significantly due to the impaired global nature of the pressure, i.e. the turbulent kinetic energy is not redistributed properly to $\overline{v^+v^+}$ and $\overline{w^+w^+}$. In particular, the rate of decrease in ϕ_{11}^+ and ϕ_{33}^+ with decreasing L_x/h is large, which makes $\overline{u^+u^+}$ and $\overline{w^+w^+}$ more and less energetic, respectively. This result implies that the inactive motion is affected more significantly by L_x than the active motion. Note that the inactive motion refers to the large-scale motion (or structure) and the irrotational pressure fluctuations of the outer region (Townsend 1961; Bradshaw 1967) which contribute to the Reynolds normal stress (mostly to the low-wavenumber components of $\overline{u^+u^+}$ and $\overline{w^+w^+}$ as described by Townsend’s (1976) attached eddy model) in the inner region, while the active motion contributes almost exclusively to the Reynolds shear stress (see also §6 of Antonia *et al.* (1992)) in this region. $\bar{\epsilon}_{11}$ (the streamwise component of the dissipation) and $\bar{\epsilon}_{33}$ (the spanwise component of the dissipation) become therefore larger and smaller with decreasing L_x/h . This leads to an increase in $\langle \bar{\epsilon}_{11} \rangle / U_\tau^3$ and decrease in $\langle \bar{\epsilon}_{33} \rangle / U_\tau^3$ (figure 1b), and hence a small dependence on L_x/h of

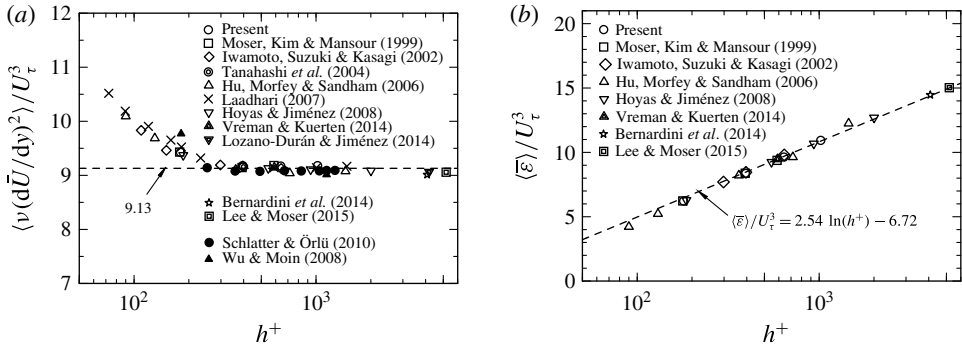


FIGURE 3. Distributions of $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$ and $\langle \bar{\epsilon} \rangle / U_\tau^3$ in a channel flow as a function of h^+ : (a) $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$; (b) $\langle \bar{\epsilon} \rangle / U_\tau^3$.

$\langle \bar{\epsilon} \rangle / U_\tau^3$ since the sum of $\langle \bar{\epsilon}_{11} \rangle / U_\tau^3$, $\langle \bar{\epsilon}_{22} \rangle / U_\tau^3$, $\langle \bar{\epsilon}_{33} \rangle / U_\tau^3$ is equal to $2\langle \bar{\epsilon} \rangle / U_\tau^3$. This is the reason why the L_x effect does not appear in $\langle \bar{\epsilon} \rangle / U_\tau^3$ explicitly. The present criterion of $L_x = 6.4h$ is identical with the finding of Lozano-Durán & Jiménez (2014) that correct one-point statistics are obtained when L_x is larger than $2\pi h$. This criterion is most likely associated with the streamwise extent of the large-scale structures (Balakumar & Adrian (2007) reported $2-3\delta$), but not very large-scale structures (Monty *et al.* (2007) reported long meandering features up to 25δ long in the channel and pipe) since the latter are very long structures and exhibit a shallow angle to the wall so that they may be thought of as the wall-parallel mode (i.e. the zero mode in the energy spectra). The required L_x in the DNS is obviously shorter than that in the experiment since the DNS is started with the fully developed turbulent state. In the DNS, once the velocity field reaches the statistically steady state (*viz.* a linear profile of the total shear stress), the Navier–Stokes equations are integrated further in time to obtain various turbulence statistics.

4.2. Reynolds number dependence

We now quantify the h^+ dependence of the total energy dissipation rate by considering the DNS data in which $L_x \geq 2\pi h$. The normalized values of $\langle \bar{\epsilon} \rangle$ and $\langle \nu(d\bar{U}/dy)^2 \rangle$ are plotted in figure 3 (on linear–log scales) in terms of h^+ using the present and existing DNS data. The viscous energy dissipation rate $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$ (figure 3a) is essentially constant for $h^+ \geq 300$; the value of the constant ($=9.13$) is the same as that reported by Laadhari (2007), who noted that this constancy applies for $h^+ \geq 500$, when $\langle \bar{\epsilon} \rangle / U_\tau^3$ exceeds $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$. The value of $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$ seems to be identical with the values obtained in either a pipe or a boundary layer (see figure 3a where the data of Wu & Moin (2008) in a pipe flow and Schlatter & Örlü (2010) in a zero-pressure-gradient boundary layer are included in terms of R^+ (R is the pipe radius) and δ_{99}^+ (δ_{99} is the 99% boundary layer thickness), respectively). This is consistent with the good collapse in the near-wall distribution of \bar{U}^+ in terms of y^+ for these three flows; the inner layer similarity of \bar{U}^+ leads to the constancy of $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$. Klebanoff (1954) also noted that the viscous energy dissipation rate is negligible above $y^+ \approx 30$ for the three flows (see also figure 2a where the distribution of $(d\bar{U}^+/dy^+)^2$ is shown at $h^+ = 1020$). On the other hand, $\langle \bar{\epsilon} \rangle / U_\tau^3$ (figure 3b) increases logarithmically with increasing h^+ over the same range of h^+ (*viz.* $h^+ \geq 300$). This increase is well described by

$$\langle \bar{\epsilon} \rangle / U_\tau^3 = 2.54 \ln(h^+) - 6.72, \tag{4.3}$$

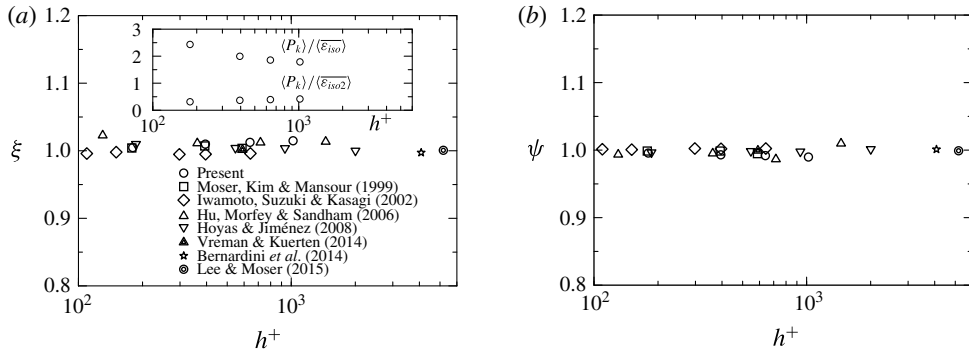


FIGURE 4. Distributions of ξ and ψ in a channel flow as a function of h^+ : (a) ξ ; (b) ψ .

which is obtained by substituting the relation for U_b^+ (4.6) and the constant value ($=9.13$) for $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$ into (2.7). Viscosity affects $\langle \bar{\epsilon} \rangle$ and $\langle \nu(d\bar{U}/dy)^2 \rangle$ significantly below $h^+ = 300$ since there is no clear separation between the inner and outer regions.

To ensure the accuracy of $\langle \bar{\epsilon} \rangle$ and $\langle \nu(d\bar{U}/dy)^2 \rangle$, the ratios

$$\xi = \langle P_k \rangle / \langle \bar{\epsilon} \rangle \tag{4.4}$$

and

$$\psi = (\langle \bar{\epsilon} \rangle + \langle \nu(d\bar{U}/dy)^2 \rangle) / U_\tau^2 U_b \tag{4.5}$$

should be equal to 1 (see also (2.6) and (2.7)). Several DNS data, including the present data, indicate that the departure from 1 of the ratios ξ and ψ is almost negligible (figure 4), thus confirming the accuracy of these simulations. From a historical perspective, it is of interest to note that the earliest attempt to test $\bar{\epsilon}_{iso2}$, measured in a turbulent channel flow, was made in Taylor’s (1935) seminal paper where the isotropic expressions $\bar{\epsilon}_{iso} = 15\nu(\partial u/\partial x)^2$ and $\bar{\epsilon}_{iso2} = 7.5\nu(\partial u/\partial y)^2$ were first derived. In essence, Taylor (1935) was testing (2.6), except that his integration was started at the centre of the channel and the upper limit of the integration did not quite go to the wall (the measurement location closest to the wall was $y/h \approx 0.08$). By extrapolating the data to the wall, we estimate that $\langle P_k \rangle / \langle \bar{\epsilon}_{iso2} \rangle$ could be somewhat greater than 2. This is, perhaps surprisingly, not an implausible outcome since the contribution from $\langle \nu(d\bar{U}/dy)^2 \rangle$ is likely to be comparable to that of $\langle \bar{\epsilon} \rangle$ at this Reynolds number ($h^+ \approx 450$), $\langle \bar{\epsilon}_{iso2} \rangle$ is likely to overestimate $\langle \bar{\epsilon} \rangle$ (inset of figure 4a) and the aspect ratio of the channel was only 4. In experiments, data for $\langle \bar{\epsilon} \rangle / U_\tau^3$ and $\langle \nu(d\bar{U}/dy)^2 \rangle / U_\tau^3$ are not usually available. A possible formula for U_b^+ can however be established from the experimental data.

Distributions of U_b^+ in a channel flow for all available DNS data and several sets of experimental data are shown in figures 5(a) and (b), respectively. A least squares fit to the DNS data in figure 5(a) over the range $h^+ \geq 300$ yields

$$U_b^+ (\equiv U_b / U_\tau) = 2.54 \ln(h^+) + 2.41, \tag{4.6}$$

or, equivalently,

$$\frac{1}{\sqrt{C_f}} = 1.80 \ln \left(Re_b \sqrt{C_f} \right) - 0.163. \tag{4.7}$$

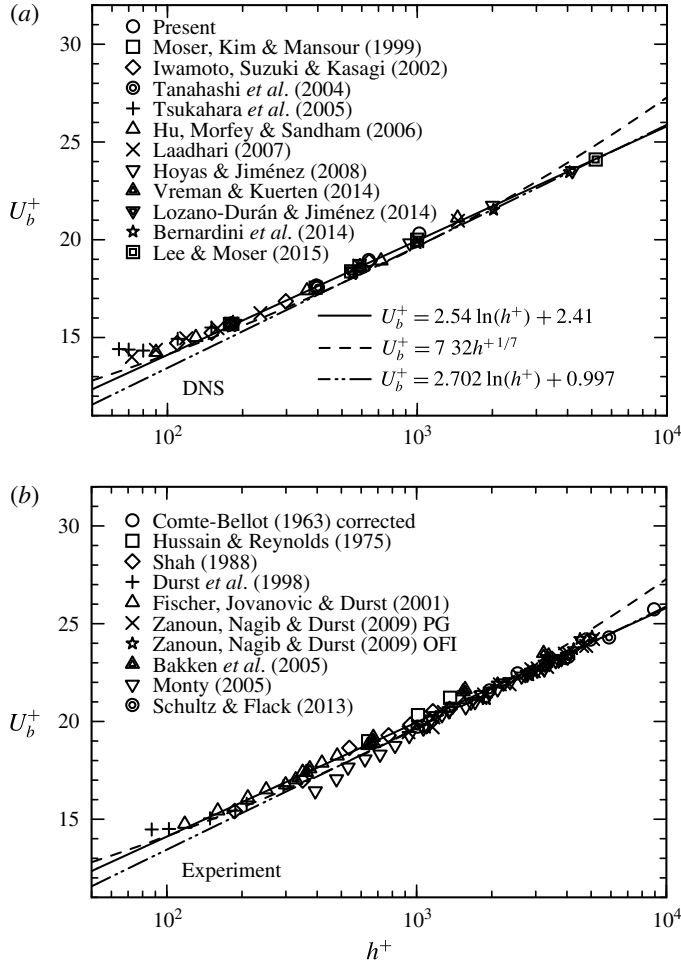


FIGURE 5. Distributions of U_b^+ in a channel flow as a function of h^+ : (a) DNS; (b) experiment.

This relation represents a good fit to nearly all the experimental data for U_b^+ over more than one decade of h^+ (see figure 5b). Also included in figure 5 are relations for U_b^+ , originally established for the skin friction coefficient C_f by Dean (1978) and Zanoun *et al.* (2009), which can be written as

$$U_b^+ = 7.32 h^{1/7} \tag{4.8}$$

and

$$U_b^+ = 2.702 \ln(h^+) + 0.997, \tag{4.9}$$

respectively. Dean's (1978) relation (4.8) appears to represent the data adequately over almost the complete range of h^+ . However, the concave curvature exhibited by (4.8) is not discernible in the overall trend of the data and implies that the difference between the logarithmic dependence (4.6) and the power-law relation (4.8) will become more perceptible as h^+ extends beyond 10^4 .

Note that among the experimental data included in figure 5(b), U_τ was most likely underestimated by Comte-Bellot (1963) ($AR = 13.3$, $L = 133h$) (see also Abe & Antonia 2011). For the latter data, correction was hence made for U_τ using (4.7); the resulting values of U_b^+ lie much closer to relation (4.6) than the original values (see figure 5b). For more recent experiments, special care was taken in determining U_τ . Zanon *et al.* (2003) (also Zanon *et al.* 2009) obtained close agreement between τ_w determined from the static pressure distribution along the fully developed part of the channel (aspect ratio $AR = 12$ and length $L = 260h$) and that estimated using oil film interferometry. Their hot-wire data covered the range $1167 < h^+ < 4783$. Fischer, Jovanović & Durst (2001) determined U_τ from a polynomial fit to the mean velocity in the viscous sublayer and the lower part of the buffer region. Their LDA measurements in a water channel ($AR = 18$, $L = 200h$), acquired with good spatial and temporal resolution, extended up to $h^+ \approx 480$. Earlier, Durst *et al.* (1998) reported results in the same channel over the range $87 < h^+ < 293$. Shah (1988) ($AR = 18.1$, $L = 349h$) and Hussain & Reynolds (1975) ($AR = 16.4$, $L = 460h$) conducted measurements with long channels for $h^+ = 187$ – 1357 and 637 – 1383 , respectively, to ensure $d\bar{P}/dx = \text{const.}$ and hence accuracy of U_τ . Bakken *et al.* (2005) made measurements in both smooth and rough walls ($AR = 14$, $L = 100h$). In their smooth wall case, h^+ ranges from 360 to 3300; U_τ was determined from both the mean pressure gradient and the Reynolds shear stress using the total shear stress relation. Monty (2005) obtained U_τ using the mean pressure gradient in a channel ($AR = 11.7$, $L = 205h$) for $h^+ \approx 380$ – 4000 . Monty's data for U_b^+ are in reasonable agreement with those of Zanon *et al.* (2003) (also Zanon *et al.* 2009) when h^+ exceeds approximately 2000. Schultz & Flack (2013) also obtained U_τ using (1.1) in their LDV measurements ($AR = 8$, $L = 248h$) for $h^+ = 1010$ – 5900 . These experimental data indeed provide strong support for relation (4.6) in figure 5(b). The logarithmic variation of U_b^+ , established from DNS data up to $h^+ = 5000$, can be extrapolated to values of h^+ that extend to approximately 10^4 .

It should also be noted that the logarithmic relation (4.6) is a better fit to both the DNS and experimental data than (4.9) for $h^+ < 2000$, possibly because the present U_b^+ relation (4.6) is based on (2.7), whereas Zanon *et al.* (2009) obtained the U_b^+ relation (4.9) from the velocity log law (1.4). This difference cannot be dismissed given that, unlike the velocity log law, the skin friction law (4.6) is established unambiguously for $h^+ > 300$.

4.3. Extension to a pipe flow

Given that the sum of the integrals of the mean and turbulent energy dissipation rates is equal to the non-dimensional energy input from the mean pressure gradient (U_b^+) in internal flows (i.e. (2.7)) and that as in a channel (i.e. (4.3)), $\langle \bar{\epsilon} \rangle / U_\tau^3$ exhibits the $2.54 \ln(R^+)$ dependence in a pipe (see § 4.5), it would be straightforward to check if the slope of U_b^+ (*viz.* $\ln(h^+)$ versus h^+) obtained in the channel (*viz.* the slope of (4.6)) also applies to the pipe. In the latter flow, Prandtl (see Schlichting 1979) established the well-known law for the friction factor $\lambda (= 4C_f)$ based on Nikuradse's (1932) data, *viz.*

$$1/\sqrt{\lambda} = 2.0 \log \left(Re_b \sqrt{\lambda} \right) - 0.8. \quad (4.10)$$

This equation can be rewritten as

$$U_b^+ = 2.46 \ln(R^+) + 2.0. \quad (4.11)$$

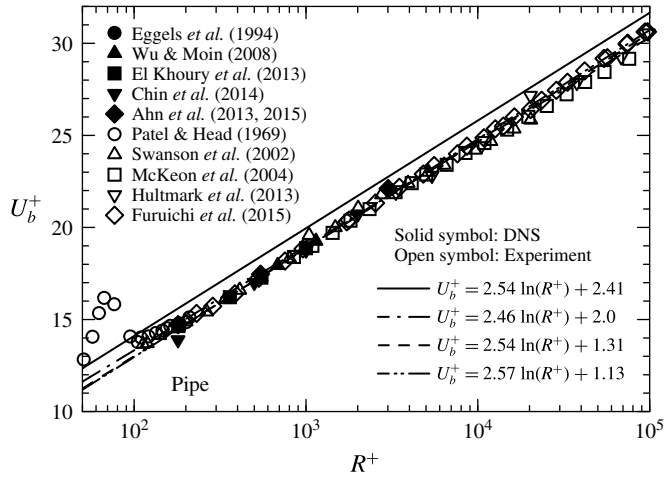


FIGURE 6. Distributions of U_b^+ in a pipe flow as a function of R^+ .

The present relation, based on the Reynolds number dependence of $\langle \bar{\varepsilon} \rangle / U_\tau^3$, is written as

$$U_b^+ = 2.54 \ln(R^+) + 1.31, \tag{4.12}$$

which is close to Prandtl’s relation. Clearly, (4.12) gives a reasonable fit to the DNS and experimental data in the range $R^+ = 300\text{--}10^4$ (see figure 6). The magnitude of U_b^+ is approximately 5% larger in the channel than in the pipe. On the other hand, while there is reasonable inner layer similarity in the distributions of \bar{U}^+ , the magnitude of \bar{U}^+ is larger in the pipe than in the channel in the outer region (see Monty *et al.* 2009; see also figure 12 where $\bar{\varepsilon}\delta/U_\tau^3$ (δ denotes either h , R or δ_{99}) shows the same trend as \bar{U}^+). The difference in U_b^+ is thus most likely due to a difference in geometry between these two flows.

It is worthwhile mentioning that the present skin friction relation for the pipe (4.12) is quite close to that obtained by Furuichi *et al.* (2015) using LDV measurements in the range $4 \times 10^2 < R^+ < 2.7 \times 10^5$, *viz.*

$$1/\sqrt{\lambda} = 2.090 \log \left(Re_b \sqrt{\lambda} \right) - 1.172. \tag{4.13}$$

The corresponding expression for U_b^+ is

$$U_b^+ = 2.57 \ln(R^+) + 1.13. \tag{4.14}$$

Both (4.12) and (4.14) give a reasonable fit to the data for lower Reynolds numbers than those at which the velocity log law is established.

4.4. Scaling laws of $\bar{\varepsilon}$ and matching argument

Here, we focus on the scaling of $\bar{\varepsilon}$ in different regions of the channel. There have been a number of observations indicating that the classical inner scaling,

$$\bar{\varepsilon}^+ \equiv \bar{\varepsilon} \nu / U_\tau^4 = f(y^+), \tag{4.15}$$

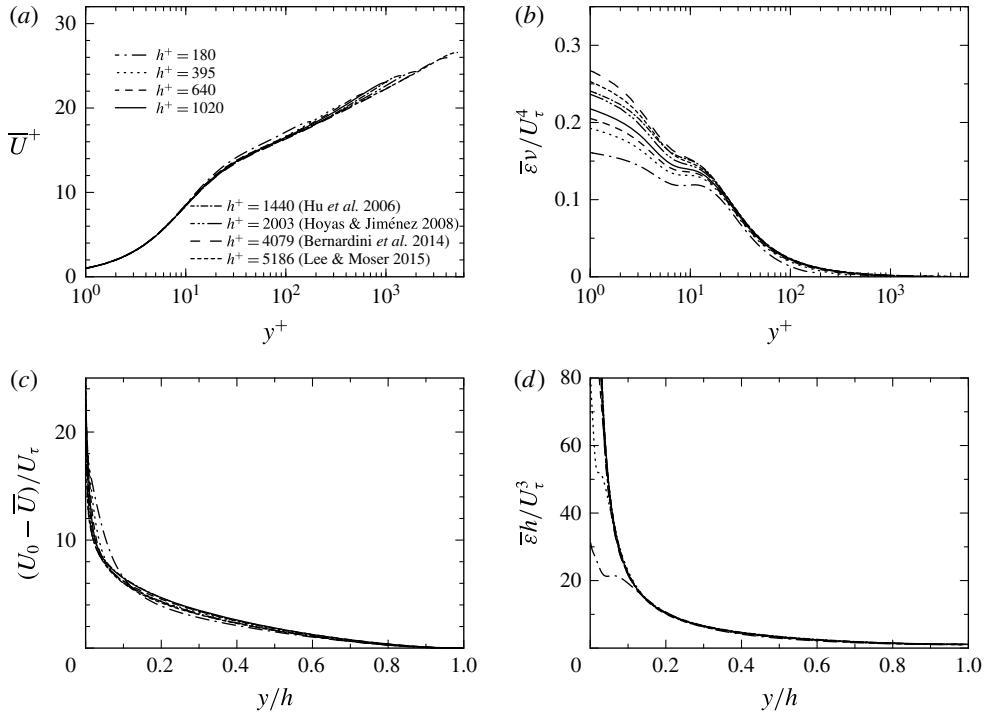


FIGURE 7. Distributions of \bar{U} and $\bar{\varepsilon}$ with the inner and outer scalings: (a) \bar{U}^+ ; (b) $\bar{\varepsilon}v/U_\tau^4$; (c) $(U_0 - \bar{U})/U_\tau$; (d) $\bar{\varepsilon}h/U_\tau^3$. Note that U_0 denotes the centreline mean velocity.

does not hold, the normalized distributions of $\bar{\varepsilon}^+$ in the wall region exhibiting a non-negligible dependence on h^+ (Antonia, Kim & Browne 1991; Hoyas & Jiménez 2008). On the other hand, there is adequate evidence that the outer scaling,

$$\bar{\varepsilon}h/U_\tau^3 = g(y/h), \quad (4.16)$$

is satisfied closely in the outer region of the channel (see Hoyas & Jiménez 2008; Abe & Antonia 2011). Distributions of $\bar{\varepsilon}$ with inner and outer scalings are shown in figure 7 together with those of \bar{U} . The magnitude of $\bar{\varepsilon}^+$ increases with h^+ close to the wall due to the effect of the inactive motion (see Hoyas & Jiménez 2008), while $\bar{\varepsilon}^+$ seems to collapse for $y^+ \geq 20$ provided $h^+ \geq 300$ (figure 7b). In contrast to the mean velocity, viscous effects are unlikely to affect the energy dissipation rate significantly for $y^+ > 20$. This is associated with Bradshaw's (1967) observation that the only noticeable effect of the inactive motion is an increased dissipation of kinetic energy into heat in the viscous sublayer. For $y^+ > 20$, $-\overline{uv} = \text{const.}$ is also satisfied reasonably well when h^+ is large enough (see figure 10b). On the other hand, unlike \bar{U} , $\bar{\varepsilon}$ collapses almost perfectly on U_τ^3 and h in the region $20/h^+ < y/h < 1$ (figure 7d; see also figure 9b where the location $20/h^+$ is identified by the dashed vertical lines). In this context, McKeon & Morrison (2007) indicated that the similarity in $\bar{\varepsilon}$ is obtained for $R^+ > 5000$ in a pipe by analysing the superpipe data, in which estimates for $\bar{\varepsilon}$ are made by invoking $P_k = \bar{\varepsilon}$. The present results indicate that the outer layer similarity for $\bar{\varepsilon}$ is more convincing than that for \bar{U} even at small h^+ ($h^+ \geq 300$) (see figure 7c,d).

We now apply a matching argument to $\bar{\varepsilon}$. Here, we assume that h^+ is large enough to have a clear distinction between inner and outer regions, and that there is a region where relations (4.15) and (4.16) overlap so that the gradient of $\bar{\varepsilon}$ should coincide, viz.

$$\frac{d\bar{\varepsilon}}{dy} = \frac{U_\tau^5}{v^2} \frac{df}{dy^+} = \frac{U_\tau^3}{h^2} \frac{dg}{dy^*}, \quad (4.17)$$

where $y^* \equiv y/h$. After multiplying by y^2 , the equality between the second and third members of (4.17) becomes

$$y^{+2} \frac{df}{dy^+} = y^{*2} \frac{dg}{dy^*}. \quad (4.18)$$

This is satisfied if

$$\frac{df}{dy^+} = \frac{D}{y^{+2}} \quad \text{or} \quad \frac{dg}{dy^*} = \frac{D}{y^{*2}}. \quad (4.19a,b)$$

Equation (4.18) indicates that $\bar{\varepsilon}$ should indeed scale with U_τ^3 and y in the overlap region. After integrating (4.19a,b), we obtain

$$f = -\frac{D}{y^+} + D_1 \quad \text{or} \quad g = -\frac{D}{y^*} + D_2. \quad (4.20a,b)$$

Here, we adopt a small parameter $\gamma = 1/h^+$ and an outer variable $y^* = \gamma y^+$ as was done by Afzal (1976) for the mean velocity gradient and obtain $D_1 = -\gamma c$ and $D_2 = -c$. Equation (4.20a,b) is then rewritten as

$$f = -\frac{D}{y^+} - \gamma c \quad \text{or} \quad \gamma g = -\gamma \frac{D}{y^*} - \gamma c, \quad (4.21a,b)$$

where c is a constant. After the normalization, it follows from (4.21a,b) that the overlap scaling may be written as

$$\bar{\varepsilon}y/U_\tau^3 = 1/\kappa_\varepsilon - c(y^+/h^+) \quad (4.22)$$

and

$$\bar{\varepsilon}y/U_\tau^3 = 1/\kappa_\varepsilon - c(y/h) \quad (4.23)$$

in inner and outer coordinates, respectively, where $D = -1/\kappa_\varepsilon$ and κ_ε is a constant. The matching argument highlights that the overlap scaling of $\bar{\varepsilon}$ requires neither the existence of a velocity log law nor energy equilibrium ($P_k = \bar{\varepsilon}$). It does however require the Reynolds number to be large enough ($h^+ \approx 300$) to allow the overlap region, where the relevant length scale is the distance from the wall, y to be distinguished unambiguously. In the overlap region, when $-\overline{uv} \simeq \text{const.}$ (this constancy is plausible only when h^+ is large enough) (see figure 10b), $P_k y/U_\tau^3 \approx y d\bar{U}^+/dy$ (see figures 10c and 11a) and $P_k/\bar{\varepsilon} \approx 1$ (see figure 10a). Equations (4.22) and (4.23) are analogous to the generalized velocity log law for the channel flow proposed by Jiménez & Moser (2007) using the asymptotic matching of the mean velocity gradient,

$$y \frac{d\bar{U}^+}{dy} = \frac{1}{\kappa} + \alpha \frac{y^+}{h^+} + \frac{\beta}{h^+} \quad (4.24)$$

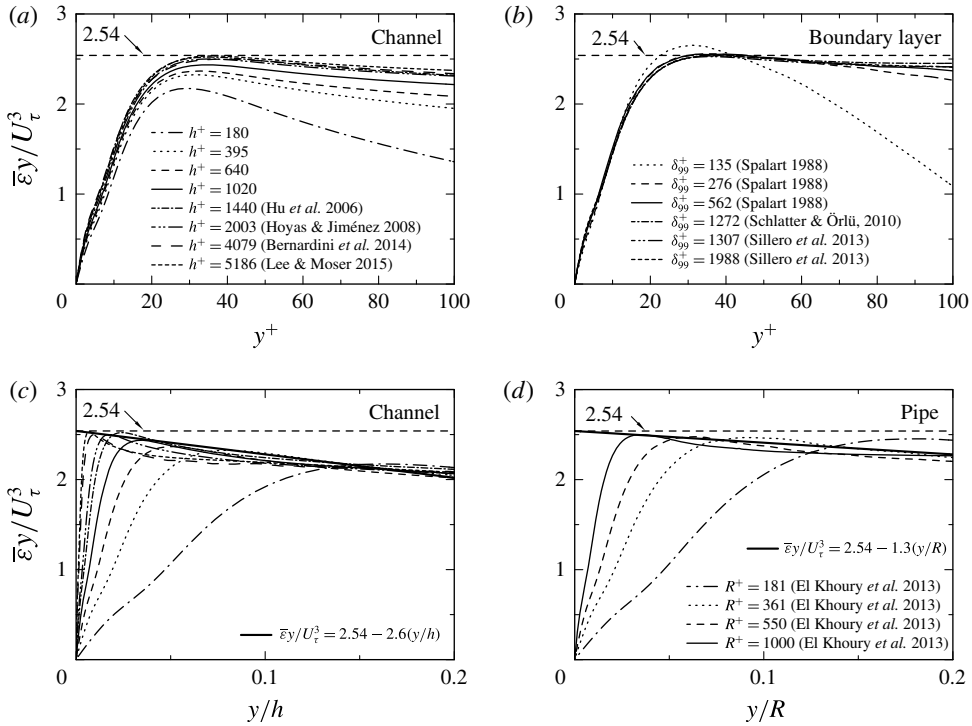


FIGURE 8. Distributions of $\bar{\epsilon}y/U_\tau^3$ in a channel, pipe and boundary layer: (a) channel (in terms of y^+); (b) boundary layer (in terms of y^+); (c) channel (in terms of y/h); (d) pipe (in terms of y/R). In (c), line patterns are the same as in (a).

and

$$y \frac{d\bar{U}^+}{dy} = \frac{1}{\kappa} + \alpha \frac{y}{h} + \frac{\beta}{h^+} \tag{4.25}$$

in inner and outer coordinates, respectively, with $1/\kappa = 2.49$, $\alpha = 1.0$ and $\beta = 150$. While both the present study and that of Jiménez & Moser (2007) use a matching argument, there are discernible differences between (4.22) and (4.23) and (4.24) and (4.25) in terms of the constants (i.e. κ_ϵ and κ) and in the limits of applicability of the overlap expressions (i.e. $30/h^+ \leq y/h \leq 0.2$ in (4.22) and (4.23) (this is discussed below) and $300/h^+ < y/h < 0.45$ in (4.24) and (4.25)).

In (4.22) and (4.23), the second terms on the right-hand sides are responsible for the finite Reynolds number effect, i.e. $-c(y^+/h^+)$ (the second term of (4.22)) goes to zero as $h^+ \rightarrow \infty$, while $-c(y/h)$ (the second term of (4.23)) does not depend on h^+ but may enhance the outer limit of the overlap scaling. When the finite Reynolds number effect disappears, equations (4.22) and (4.23) reduce to $\bar{\epsilon}y/U_\tau^3 = 1/\kappa_\epsilon$ analogous to the classical scaling based on the velocity log law $\bar{\epsilon}y/U_\tau^3 = 1/\kappa$ (see, for example, Townsend 1976). Note that κ_ϵ is identical with κ only if the velocity log law and energy equilibrium conditions are satisfied. Hoyas & Jiménez (2008) found that the magnitudes of all the terms in the budgets of $\overline{u_i u_j}$ and k in the channel decrease almost proportionally to y^{-1} in the region $y^+ = 50$ to $y/h = 0.4$ for $h^+ = 2003$. Figure 8(a) highlights that the largest magnitude of $\bar{\epsilon}y/U_\tau^3$ ($= 2.54$) is attained at $y^+ = 30\text{--}40$. This value is the same for the channel, pipe and boundary layer due to the wall similarity

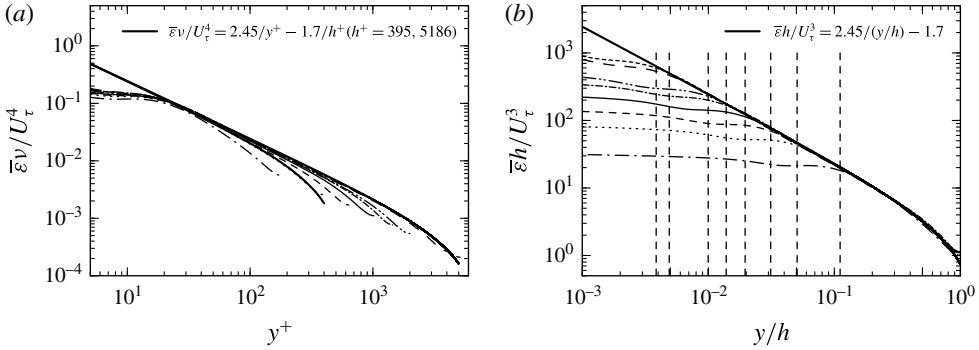


FIGURE 9. Distributions of $\bar{v}U_\tau^4$ and $\bar{\epsilon}h/U_\tau^3$ in a channel flow with log–log coordinates: (a) $\bar{v}U_\tau^4$; (b) $\bar{\epsilon}h/U_\tau^3$. - · - · - ·, $h^+ = 180$; · · · · ·, $h^+ = 395$; - - - - -, $h^+ = 640$; —, $h^+ = 1020$; - · - · - · - ·, $h^+ = 1440$ (Hu *et al.* 2006); — · — · — · — ·, $h^+ = 2003$ (Hoyas & Jiménez 2008); — — —, $h^+ = 4079$ (Bernardini *et al.* 2014); - - - - - , $h^+ = 5186$ (Lee & Moser 2015); — — —, (4.26)–(4.27).

of the constant stress region (Townsend 1976). It depends on the Reynolds number in the channel and pipe, but not in the boundary layer (see figure 8). This finite Reynolds number effect comes from the $d\bar{P}/dx$ effect, which reduces the magnitude of $-\bar{u}\bar{v}$ and hence P_k and $\bar{\epsilon}$ when h^+ is small. On the other hand, this effect is negligible when $h^+ \approx 5000$, which allows us to determine $1/\kappa_\epsilon$ unambiguously. Indeed, $1/\kappa_\epsilon = 2.54$ is identified asymptotically for $h^+ \geq 5000$ in the channel (figure 8a), while this value is obtained for $\delta_{99}^+ \geq 300$ in the zero-pressure-gradient boundary layer due to the absence of the $d\bar{P}/dx$ effect (figure 8b). A fit to the DNS data over $30/\delta^+ \leq y/\delta \leq 0.2$ then yields $c = 2.6, 1.3$ and 0 in the channel, pipe and boundary layer. Indeed, equations (4.22) and (4.23) reproduce the h^+ dependence of the peak magnitude of $\bar{\epsilon}y/U_\tau^3$ successfully for $h^+ \geq 300$ and provide a good fit to the data in the region $30/h^+ \leq y/h \leq 0.2$ (see figure 8c). While the classical overlap argument based on \bar{U} (Millikan 1938) strictly holds only at large h^+ , the overlap region for $\bar{\epsilon}$ is established at small h^+ (≈ 300) (see also figure 8c in which the DNS data for $h^+ = 395$ follow the present overlap scaling very well).

In the outer region ($y/h > 0.2$), there is still a decrease in $\bar{\epsilon}y/U_\tau^3$ towards the centreline (see figure 11b). After the fit to the DNS data in figure 7(d), the decrease is approximated closely by the outer scaling, *viz.*

$$\bar{\epsilon}h/U_\tau^3 = 2.45/(y/h) - d, \tag{4.26}$$

with $d = 1.7$. Figure 9(b) underlines that (4.26) is a good fit in the region $20/h^+ < y/h < 1$ (see the thick lines in figure 9b). Equation (4.26) also applies to the pipe reasonably well albeit with a different value of d . In the boundary layer, it applies only below $y/\delta_{99} \approx 0.4$, with yet another value of d (see figure 12 where $d = 0.9$ and -1.0 for the pipe and boundary layer, respectively). The different magnitudes of d are most likely associated with the different flow characteristics (e.g. effects of the mean pressure gradient in the channel and pipe, curvature in the pipe and the presence of the turbulent/non-turbulent interface in the boundary layer). The present results underline that, as for the mean velocity, there is a discernible departure from similarity in the energy dissipation rate for the channel, pipe and boundary layer.

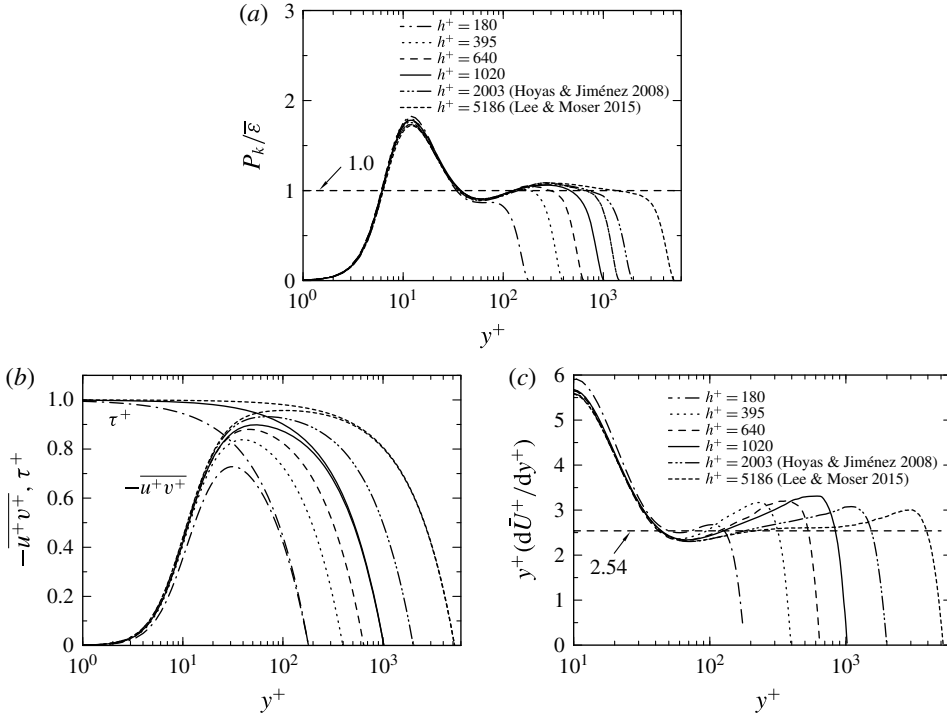


FIGURE 10. Distributions of $P_k/\bar{\varepsilon}$, $-\overline{u^+v^+}$, τ^+ and $y^+(d\bar{U}^+/dy^+)$ in a channel flow: (a) $P_k/\bar{\varepsilon}$; (b) $-\overline{u^+v^+}$ and τ^+ ; (c) $y^+(d\bar{U}^+/dy^+)$. In (b), line patterns are the same as in (a).

The excellent agreement with (4.26) in both the channel and pipe is due to the $d\bar{P}/dx$ effect. This latter effect seems to be responsible for yielding nearly the same slope (i.e. 2.45) as in the overlap scaling (i.e. $1/\kappa_\varepsilon = 2.54$) so that a reasonable collapse on the outer scaling is obtained over a wider range $20/h^+ < y/h < 1$ (see figure 9b) than for the velocity log law, usually between $y^+ \simeq 30$ and $y/h = 0.2$. A nearly identical observation was made for \bar{U} by Monty *et al.* (2007) who noted that the pipe and channel mean velocity profiles lie closer to the log law than in the boundary layer beyond $y/\delta = 0.15$. In the region $20 < y^+ < h^+$, there is satisfactory collapse on inner scaling with the same slope (i.e. 2.45) as for outer scaling, *viz.*

$$\bar{\varepsilon}v/U_\tau^4 = 2.45/y^+ - d/h^+ \tag{4.27}$$

(see figure 9a). Note that since it seems difficult to make a clear distinction between the overlap and outer regions of $\bar{\varepsilon}$ in the channel (see figure 9 where the inner and outer scalings (4.26), (4.27) hold reasonably well in the region $20/h^+ < y/h < 1$), we assume that the upper bound of the overlap region of $\bar{\varepsilon}$ is $y/h = 0.2$, as is normally assumed for the velocity log law. In the present work, the overlap region of $\bar{\varepsilon}$ is thus defined by the region $30/h^+ \leq y/\delta \leq 0.2$, in which (4.22) and (4.23) hold quite well.

4.5. Fractional contributions to $\langle \bar{\varepsilon} \rangle / U_\tau^3$

It is of importance to clarify if the integral of $\bar{\varepsilon}$ over the overlap region yields the logarithmic h^+ dependence of $\langle \bar{\varepsilon} \rangle / U_\tau^3$. In the present study, we follow the same

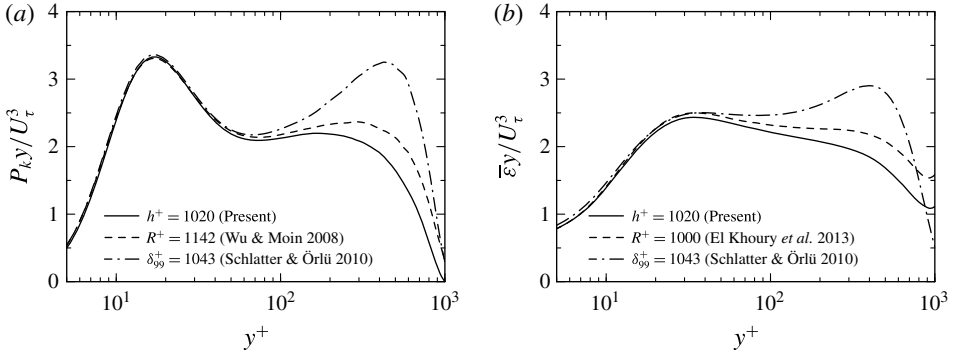


FIGURE 11. Distributions of P_{ky}/U_{τ}^3 and $\bar{\epsilon}y/U_{\tau}^3$ in a channel, pipe and boundary layer at $\delta^+ \approx 1000$: (a) P_{ky}/U_{τ}^3 ; (b) $\bar{\epsilon}y/U_{\tau}^3$.

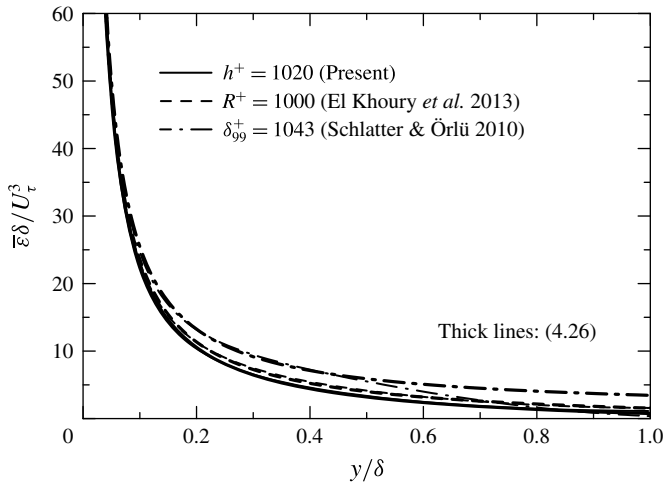


FIGURE 12. Distributions of $\bar{\epsilon}\delta/U_{\tau}^3$ in a channel, pipe and boundary layer at $\delta^+ \approx 1000$.

approach as in Sreenivasan (1995), viz.

$$\frac{\langle \bar{\epsilon} \rangle}{U_{\tau}^3} = \underbrace{\int_0^{30} \bar{\epsilon}^+ dy^+}_{C_i} + \underbrace{\int_{30\nu/U_{\tau}}^{0.2h} \frac{\bar{\epsilon}}{U_{\tau}^3} dy}_{C_{log}} + \underbrace{\int_{0.2}^1 \frac{\bar{\epsilon}h}{U_{\tau}^3} d\left(\frac{y}{h}\right)}_{C_o}, \tag{4.28}$$

where the limits for the second integral in (4.28) correspond to the extent of the overlap region of $\bar{\epsilon}$, i.e. $y^+ \simeq 30$ and $y/h = 0.2$. Values of C_i , C_{log} and C_o obtained from the DNS data in the channel are shown in figure 13 and are compared with the corresponding values in the pipe and boundary layer. Clearly, there is a $\ln(h^+)$ dependence for C_{log} (figure 13b). This dependence is obtained by integrating (4.22) or (4.23), viz.

$$C_{log} \simeq \int_{30\nu/U_{\tau}}^{0.2h} \left(\frac{1}{\kappa_{\epsilon}y} - \frac{c}{h} \right) dy = 2.54(\ln(h^+) + \ln(0.2) - \ln(30)) - 2.6(0.2 - 30/h^+), \tag{4.29}$$

in which the last term of (4.29), the finite Reynolds number effect or the $d\bar{P}/dx$ effect, cannot be dismissed when h^+ is small. On the other hand, the last term of (4.29) is negligible in the zero-pressure-gradient boundary layer due to the absence of the $d\bar{P}/dx$ effect (see figure 13b). Given that C_o is essentially constant ($\sim 1/\kappa_\varepsilon$) (figure 13c) but the magnitude of C_i increases slowly with h^+ (figure 13a), we integrate $\bar{\varepsilon}$ from $y=0$ to $0.2h$ (viz. $C_i + C_{log}$) (figure 13b). The resulting integral is described adequately by

$$C_{in} + C_{log} = \int_0^{0.2h} \frac{\bar{\varepsilon}}{U_\tau^3} dy = 2.54 \ln(h^+) - C_2 \tag{4.30}$$

for $h^+ \geq 300$ with $C_2 = 9.28$. Note that the sum of (4.30) and C_o (≈ 2.6) is identical to (4.3). This implies that the more appropriate expression for the logarithmic dependence of $\langle \bar{\varepsilon} \rangle / U_\tau^3$ for the channel requires integration from $y=0$ to $0.2h$, viz. the contribution of C_i (h^+) cannot be ignored. The same trend is observed for the pipe. The slightly different magnitude of the integral from $y=0$ to 0.2δ (viz. $C_i + C_{log}$) between the three flows is attributed to the finite Reynolds number effect or the $d\bar{P}/dx$ effect, represented well by the terms $-c(y^+/h^+)$ and $-c(y/h)$ in (4.22) and (4.23). This effect however does not affect the $\ln(\delta^+)$ dependence of $C_i + C_{log}$ (see figure 13b where the $2.54 \ln(\delta^+)$ dependence is valid for the three flows when $\delta^+ \geq 300$). The present results highlight that the slope of 2.54 in (4.30) can be identified with $1/\kappa_\varepsilon$ as inferred from the overlap scaling of $\bar{\varepsilon}$, and that $1/\kappa_\varepsilon$ is identical with the slope for the $\ln(h^+)$ dependence of U_b^+ .

The Reynolds number dependence of C_i is more significant for the channel/pipe than for the boundary layer (figure 13a) owing to the finite Reynolds number effect (viz. the $d\bar{P}/dx$ effect) in the former two flows. Schlatter & Örlü (2010) observed a difference in $\tau_{1rms}^+ = (\partial u^+ / \partial y^+)_w$, τ_{1rms}^{+2} being one of the major contributors to $\bar{\varepsilon}^+$ at the wall, between the channel and boundary layer at low Reynolds numbers and attributed it to the presence of $d\bar{P}/dx$ in the channel. On the other hand, C_o differs significantly between the three flows (figure 13c) due to the different external flow characteristics (see figure 12 which shows distributions of $\bar{\varepsilon}\delta/U_\tau^3$ in the three flows). The constancy of C_o for the channel and pipe is associated with the excellent outer scaling we observe for these two flows, viz. integrating (4.26) from $y=0.2\delta$ to δ yields 2.58 and 1.53 for the channel and pipe, respectively, these two values being reasonable estimates of C_o (see figure 13c).

The dependence on δ^+ of C_i tends to become small in all three flows as the Reynolds number increases (see figure 13a), implying a decreasing contribution of C_i to the $2.54 \ln(h^+)$ dependence as h^+ increases. When $h^+ \rightarrow \infty$, the overlap region should contribute exclusively to the $2.54 \ln(h^+)$ dependence of the integrated turbulent energy dissipation rate. The present logarithmic h^+ dependence of U_b^+ is essentially linked to the excellent overlap region we observe for $\bar{\varepsilon}$ even at small h^+ . Note that $\kappa_\varepsilon = 0.39$ defined in (4.22) and (4.23) is not identical with κ obtained from the velocity log law (1.6) for the Reynolds numbers examined (see figures 8a and 10c). This is because the constancy of $1/\kappa \equiv y^+(d\bar{U}^+/dy^+)$ is apparent only above $h^+ = 5000$ due to the non-negligible viscous effect on \bar{U} (figure 10c). Also, there is a discernible departure from unity of $P_k/\bar{\varepsilon}$ in the region normally referred to as the velocity log law (figure 10a). The universality of κ obtained from the velocity log law has been questioned (see the review of Smits, McKeon & Marusic (2011)); its magnitude increases slowly with increasing h^+ in the channel ($\kappa = 0.37$ at $h^+ = 2000$ by Zanoun *et al.* (2003); $\kappa = 0.38$ at $h^+ = 5200$ by Lee & Moser (2015);

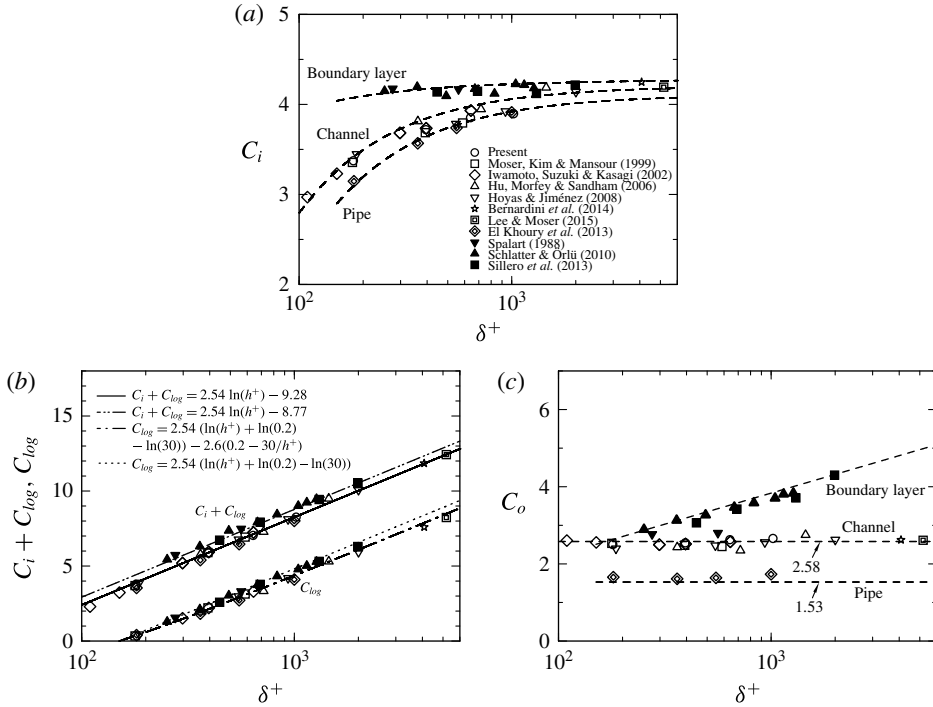


FIGURE 13. Distributions of piecewise contributions to $\langle \bar{\epsilon} \rangle / U_\tau^3$ in a channel, pipe and boundary layer as a function of δ^+ : (a) from $y^+ = 0$ to 30 (C_i); (b) from $y^+ = 30$ to $y/\delta = 0.2$ (C_{log}) and from $y/\delta = 0$ to 0.2 ($C_i + C_{log}$); (c) from $y/\delta = 0.2$ to 1 (C_o).

see also figure 10c). Marusic *et al.* (2013) also reported that experiments support a universal logarithmic behaviour of the mean velocity and streamwise turbulence intensities in the region $3\delta^{+1/2} < y^+ < 0.15\delta^+$ of the laboratory boundary layer, pipe and atmospheric surface layer with $\kappa = 0.39$ at extremely large Reynolds number ($2 \times 10^4 < \delta^+ < 6 \times 10^5$). The present value of κ_ϵ may be reconcilable with the value of κ (obtained at very large h^+) if one recognizes that the outer layer similarity of $\bar{\epsilon}$ is established at a much smaller h^+ than for \bar{U}^+ . Indeed, this appears to be adequately supported by the available DNS data (see figure 7).

5. Conclusions

In the present study, we have examined the functional dependence on the Kármán number h^+ of the energy dissipation function (*viz.* (1.7), (1.8)) in a fully developed turbulent channel flow. The present DNS data for $h^+ = 180, 395, 640$ and 1020 together with other DNS and experimental data extending to $h^+ = 10^4$ have been used to clarify this dependence. After establishing that the streamwise extent of the computational domain is sufficient to allow reliable estimates of the integrals across the channel half-width of the mean and turbulent energy dissipation rates, an unambiguous relation for U_b^+ with respect to h^+ is obtained on the basis of the energy balances for both mean and turbulent kinetic energy. The scaling behaviour of the turbulent energy dissipation rate has also been carefully examined in order to confirm the logarithmic dependence of U_b^+ on h^+ . The main conclusions are as follows.

In a channel flow, after normalizing by U_τ^3 , the energy dissipation function, or sum of the integrals of the mean and turbulent energy dissipation rates, is equal to U_b^+ (i.e. (2.7)). For $h^+ \geq 300$, the integral of the mean energy dissipation rate associated with the mean velocity gradient, i.e. $\langle \nu(d\bar{U}/dy)^2 \rangle$, normalized by U_τ^3 , is essentially constant, whereas $\langle \bar{\varepsilon} \rangle / U_\tau^3$ increases logarithmically with increasing h^+ . Viscosity affects $\langle \bar{\varepsilon} \rangle$ and $\langle \nu(d\bar{U}/dy)^2 \rangle$ significantly for $h^+ < 300$ since there is no clear separation between inner and outer regions. The logarithmic h^+ dependence of $\langle \bar{\varepsilon} \rangle / U_\tau^3$ for $h^+ \geq 300$ is hence linked to that of U_b^+ . The resulting logarithmic friction relation (4.6) is supported convincingly by DNS and experimental data over the range $300 \leq h^+ \leq 10^4$.

Support for the logarithmic h^+ dependence of $\langle \bar{\varepsilon} \rangle / U_\tau^3$ is provided by the scaling behaviour of the mean turbulent energy dissipation rate. The inner layer scaling, i.e. $\bar{\varepsilon} \nu / U_\tau^4 = f(y^+)$, does not hold for $y^+ \leq 20$. On the other hand, $\bar{\varepsilon}$ collapses almost perfectly with U_τ^3 and h in the region $20/h^+ < y/h < 1$. Unlike the mean velocity, the turbulent energy dissipation rate is not affected significantly by viscosity for $y^+ > 20$. Whereas the classical overlap argument based on \bar{U} (Millikan 1938) strictly holds only at large h^+ , the overlap region for $\bar{\varepsilon}$ is established at small h^+ (≈ 300) independently of the existence of a velocity log law. It does however require the Reynolds number to be large enough ($h^+ \approx 300$) to allow an overlap region where the relevant length scale is y . In this region ($30/h^+ \leq y/h \leq 0.2$), $\bar{\varepsilon} y / U_\tau^3$ approaches a constant ($\kappa_\varepsilon^{-1} = 2.54$), allowing for a finite Reynolds number correction, equations (4.22) and (4.23), for $h^+ \geq 300$. When h^+ is sufficiently large (≥ 5000) for the velocity log law to be established over a region where $P_k \simeq \bar{\varepsilon}$ and $-\bar{u}v \simeq \text{const.}$, the Kármán constant κ can be identified with κ_ε . The present logarithmic h^+ dependence of U_b^+ follows from the overlap argument based entirely on the behaviour of $\bar{\varepsilon}$ in the inner and outer regions. We stress that the outer layer similarity of $\bar{\varepsilon}$ is more convincing than that of \bar{U} and is established at a smaller value of h^+ (see figure 7). This is the reason why the present U_b^+ relation (4.6) is validated over a wide range of h^+ and is established at a lower Reynolds number than that the velocity log law. The present logarithmic Reynolds number dependence of U_b^+ also applies to the pipe due to the excellent similarity of the overlap scaling for $\bar{\varepsilon}$ in internal flows.

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REFERENCES

- ABE, H., ANTONIA, R. A. & KAWAMURA, H. 2009 Correlation between small-scale velocity and scalar fluctuations in a turbulent channel flow. *J. Fluid Mech.* **627**, 1–32.
- ABE, H. & ANTONIA, R. A. 2011 Scaling of normalized mean energy and scalar dissipation rates in a turbulent channel flow. *Phys. Fluids* **23**, 055104.
- ABE, H., KAWAMURA, H. & MATSUO, Y. 2001 Direct numerical simulation of a fully developed turbulent channel flow with respect to the Reynolds number dependence. *Trans. ASME J. Fluids Engng* **123**, 382–393.
- ABE, H., KAWAMURA, H. & MATSUO, Y. 2004a Surface heat-flux fluctuations in a turbulent channel flow up to $Re_\tau = 1020$ with $Pr = 0.025$ and 0.71 . *Intl J. Heat Fluid Flow* **25**, 404–419.

- ABE, H., KAWAMURA, H. & CHOI, H. 2004*b* Very large-scale structures and their effects on the wall shear-stress fluctuations in a turbulent channel flow up to $Re_\tau = 640$. *Trans. ASME J. Fluids Engng* **126**, 835–843.
- ABE, H., KAWAMURA, H., TOH, S. & ITANO, T. 2007 Effects of the streamwise computational domain size on DNS of a turbulent channel flow at high Reynolds number. In *Advances in Turbulence XI, Proceedings of the 11th EUROMECH European Turbulence Conference, Porto, Portugal, June 25–28, 2007* (ed. J. M. L. M. Palma & A. S. Lopes), pp. 233–235. Springer.
- AHN, J., LEE, J. H., JANG, S. J. & SUNG, H. J. 2013 Direct numerical simulations of fully developed turbulent pipe flows for $Re_\tau = 180$, 544 and 934. *Intl J. Heat Fluid Flow* **44**, 222–228.
- AHN, J., LEE, J. H., LEE, J. L., KANG, J.-H. & SUNG, H. J. 2015 Direct numerical simulation of a 30R long turbulent pipe flow at $Re_\tau = 3008$. *Phys. Fluids* **27**, 065110.
- DEL ÁLAMO, J. C., JIMÉNEZ, J., ZANDONADE, P. & MOSER, R. D. 2004 Scaling of the energy spectra of turbulent channels. *J. Fluid Mech.* **500**, 135–144.
- ANTONIA, R. A., ABE, H. & KAWAMURA, H. 2009 Analogy between velocity and scalar fields in a turbulent channel flow. *J. Fluid Mech.* **628**, 241–268.
- ANTONIA, R. A., KIM, J. & BROWNE, L. W. B. 1991 Some characteristics of small-scale turbulence in a turbulent duct flow. *J. Fluid Mech.* **233**, 369–388.
- ANTONIA, R. A., TEITEL, M., KIM, J. & BROWNE, L. W. B. 1992 Low-Reynolds-number effects in a fully developed turbulent channel flow. *J. Fluid Mech.* **236**, 579–605.
- AFZAL, N. 1976 Millikan's argument at moderately large Reynolds number. *Phys. Fluids* **19**, 600–602.
- BAKKEN, O. M., KROGSTAD, P., ASHRAFIAN, A. & ANDERSSON, H. I. 2005 Reynolds number effects in the outer layer of the turbulent flow in a channel with rough walls. *Phys. Fluids* **17**, 065101.
- BALAKUMAR, B. J. & ADRIAN, R. J. 2007 Large- and very-large-scale motions in channel and boundary-layer flows. *Phil. Trans. R. Soc. Lond. A* **365**, 665–681.
- BERNARDINI, M., PIROZZOLI, S. & ORLANDI, P. 2014 Velocity statistics in turbulent channel flow up to $Re_\tau = 4000$. *J. Fluid Mech.* **742**, 171–191.
- BRADSHAW, B. 1967 'Inactive' motion and pressure fluctuations in turbulent boundary layers. *J. Fluid Mech.* **30**, 241–258.
- CHIN, C., MONTY, J. P. & OOI, A. 2014 Reynolds number effects in DNS of pipe flow and comparison with channels and boundary layers. *Intl J. Heat Fluid Flow* **45**, 33–40.
- COMTE-BELLOT, G. 1963 Contribution à l'étude de la turbulence de conduite. PhD thesis, University of Grenoble (trans. P. Bradshaw ARC 31 609 FM 4102, 1969).
- DEAN, R. B. 1978 Reynolds number dependence of skin friction and other bulk flow variables in two-dimensional rectangular duct flow. *Trans. ASME J. Fluids Engng* **100**, 215–223.
- DEGRAAFF, D. B. & EATON, J. K. 2000 Reynolds-number scaling of the flat-plate turbulent boundary layer. *J. Fluid Mech.* **422**, 319–346.
- DURST, F., FISCHER, M., JOVANOVIĆ, J. & KIMURA, H. 1998 Methods to set up and investigate low Reynolds number, fully developed turbulent plane channel flows. *Trans. ASME J. Fluids Engng* **120**, 496–503.
- EGGELS, J. G. M., UNGER, F., WEISS, M. R., WESTERWEEL, J., ADRIAN, R. J., FRIEDRICH, R. & NIEUWSTADT, F. T. M. 1994 Fully developed turbulent pipe flow: a comparison between direct numerical simulation and experiment. *J. Fluid Mech.* **268**, 175–209.
- EL KHOURY, G. K., SCHLATTER, P., NOORANI, A., FISCHER, P. F., BRETHERWATER, G. & JOHANSSON, A. V. 2013 Direct numerical simulation of turbulent pipe flow at moderately high Reynolds numbers. *Flow Turbul. Combust.* **91**, 475–495.
- FISCHER, M., JOVANOVIĆ, J. & DURST, F. 2001 Reynolds number effects in the near-wall region of turbulent channel flows. *Phys. Fluids* **13**, 1755–1767.
- FLORES, O. & JIMÉNEZ, J. 2010 Hierarchy of minimal flow units in the logarithmic layer. *Phys. Fluids* **22**, 071704.
- FURUICHI, N., TERAOKA, Y., WADA, Y. & TSUJII, Y. 2015 Friction factor and mean velocity profile for pipe flow at high Reynolds number. *Phys. Fluids* **27**, 095108.
- HOYAS, S. & JIMÉNEZ, J. 2008 Reynolds number effects on the Reynolds-stress budgets in turbulent channels. *Phys. Fluids* **20**, 101511.

- HU, Z. W., MORFEY, C. L. & SANDHAM, N. D. 2006 Wall pressure and shear stress spectra from direct numerical simulations of channel flow. *AIAA J.* **44** (7), 1541–1549.
- HULTMARK, M., VALLIKIVI, M., BAILEY, S. C. C. & SMITS, A. J. 2013 Logarithmic scaling of turbulence in smooth- and rough-wall pipe flow. *J. Fluid Mech.* **728**, 376–395.
- HUSSAIN, A. K. M. F. & REYNOLDS, W. C. 1975 Measurements in fully developed turbulent channel flow. *Trans. ASME J. Fluids Engng* **97**, 568–580.
- IWAMOTO, K., SUZUKI, Y. & KASAGI, N. 2002 Reynolds number effect on wall turbulence: toward effective feedback control. *Intl J. Heat Fluid Flow* **23**, 678–689.
- JIMÉNEZ, J. & MOIN, P. 1991 The minimal flow unit in near-wall turbulence. *J. Fluid Mech.* **225**, 213–240.
- JIMÉNEZ, J. & MOSER, R. D. 2007 What are we learning from simulating wall turbulence? *Phil. Trans. R. Soc. Lond. A* **365**, 715–732.
- KIM, J., MOIN, P. & MOSER, R. 1987 Turbulence statistics in fully developed channel flow at low Reynolds number. *J. Fluid Mech.* **177**, 133–166.
- KLEBANOFF, P. S. 1954 Characteristics of turbulence in a boundary layer with zero pressure gradient. *NACA Tech. Rep.* TN 3178.
- LAADHARI, F. 2007 Reynolds number effect on the dissipation function in wall-bounded flows. *Phys. Fluids* **19**, 038101.
- LAUFER, J. 1951 Investigation of turbulent flow in a two-dimensional channel. *NACA Rept.* 1053.
- LEE, M. & MOSER, R. D. 2015 Direct numerical simulation of turbulent channel flow up to $Re_\tau \approx 5200$. *J. Fluid Mech.* **774**, 395–415.
- LOZANO-DURÁN, A. & JIMÉNEZ, J. 2014 Effect of the computational domain on direct simulations of turbulent channels up to $Re_\tau = 4200$. *Phys. Fluids* **26**, 011702.
- MARUSIC, I., MONTY, J. P., HULTMARK, M. & SMITS, A. J. 2013 On the logarithmic region in wall turbulence. *J. Fluid Mech.* **716**, R3.
- MCKEON, B. J. & MORRISON, J. F. 2007 Asymptotic scaling in turbulent pipe flow. *Phil. Trans. R. Soc. Lond. A* **365**, 771–787.
- MCKEON, B. J., SWANSON, C. J., ZAGAROLA, M. V., DONNELLY, R. J. & SMITS, A. J. 2004 Friction factors for smooth pipe flow. *J. Fluid Mech.* **511**, 41–44.
- MILLIKAN, C. M. 1938 A critical discussion of turbulent flows in channels and circular tubes. In *Proceedings of the 5th Int. Congr. Appl. Mech., New York*, pp. 386–392. Wiley.
- MONTY, J. P. 2005 Developments in smooth wall turbulent duct flows. PhD thesis, University of Melbourne, Australia.
- MONTY, J. P., HUTCHINS, N., NG, H. C. H., MARUSIC, I. & CHONG, M. S. 2009 A comparison of turbulent pipe, channel and boundary layer flows. *J. Fluid Mech.* **632**, 431–442.
- MONTY, J. P., STEWART, J. A., WILLIAMS, R. C. & CHONG, M. S. 2007 Large-scale features in turbulent pipe and channel flows. *J. Fluid Mech.* **589**, 147–156.
- MORRISON, J. F., MCKEON, B. J., JIANG, W. & SMITS, A. J. 2004 Scaling of the streamwise velocity component in turbulent pipe flow. *J. Fluid Mech.* **508**, 99–131.
- MOSER, R. D., KIM, J. & MANSOUR, N. N. 1999 Direct numerical simulation of turbulent channel flow up to $Re_\tau = 590$. *Phys. Fluids* **11**, 943–945.
- NIKURADSE, J. 1932 Laws of turbulent flow in smooth pipes (English translation). NASA TT F-10 (1966).
- PATEL, V. C. & HEAD, M. R. 1969 Some observations on skin friction and velocity profiles in fully developed pipe and channel flows. *J. Fluid Mech.* **38**, 181–201.
- ROTTA, J. C. 1962 Turbulent boundary layers in incompressible flow. *Prog. Aeronaut. Sci.* **2**, 1–219.
- SCHLATTER, P. & ÖRLÜ, R. 2010 Assessment of direct numerical simulation data of turbulent boundary layers. *J. Fluid Mech.* **659**, 116–126.
- SCHLICHTING, H. 1979 *Boundary Layer Theory*, 7th edn. McGraw-Hill.
- SCHULTZ, M. P. & FLACK, K. A. 2013 Reynolds-number scaling of turbulent channel flow. *Phys. Fluids* **25** (2), 025104.
- SHAH, D. A. 1988 Scaling of the ‘bursting’ and ‘pulse’ periods in wall bounded turbulent flows. PhD thesis, University of Newcastle.

- SILLERO, J. A., JIMENEZ, J. & MOSER, R. D. 2013 One-point statistics for turbulent wall-bounded flows at Reynolds numbers up to $\delta^+ \approx 2000$. *Phys. Fluids* **25**, 105102.
- SMITS, A. J., MCKEON, B. J. & MARUSIC, I. 2011 High-Reynolds number wall turbulence. *Annu. Rev. Fluid Mech.* **43**, 353–375.
- SPALART, P. R. 1988 Direct simulation of a turbulent boundary layer up to $R_\theta = 1410$. *J. Fluid Mech.* **187**, 61–98.
- SREENIVASAN, K. R. 1995 The energy dissipation in turbulent shear flows. In *Symposium on Developments in Fluid Dynamics and Aerospace Engineering* (ed. S. M. Deshpande, A. Prabhu, K. R. Sreenivasan & P. R. Viswanath), pp. 159–190. Interline Publishers.
- SWANSON, C. J., JULIAN, B., IHAS, G. G. & DONNELLY, R. J. 2002 Pipe flow measurements over a wide range of Reynolds numbers using liquid helium and various gases. *J. Fluid Mech.* **461**, 51–60.
- TANAHASHI, M., KANG, S.-J., MIYAMOTO, T., SHIOKAWA, S. & MIYAUCHI, T. 2004 Scaling law of fine scale eddies in turbulent channel flows up to $Re_\tau = 800$. *Intl J. Heat Fluid Flow* **25**, 331–340.
- TAYLOR, G. I. 1935 Statistical theory of turbulence. III. Distribution of dissipation of energy in a pipe over its cross-section. *Proc. R. Soc. Lond. A* **151**, 455–464.
- TOWNSEND, A. A. 1961 Equilibrium layers and wall turbulence. *J. Fluid Mech.* **11**, 97–120.
- TOWNSEND, A. A. 1976 *The Structure of Turbulent Shear Flow*. vol. 2. Cambridge University Press.
- TSUKAHARA, T., SEKI, Y., KAWAMURA, H. & TOCHIO, D. 2005 DNS of turbulent channel flow at very low Reynolds numbers. In *Proceedings of the Fourth Int. Symp. on Turbulence and Shear Flow Phenomena, Williamsburg, USA*, pp. 935–940.
- VREMAN, A. W. & KUERTEN, J. G. M. 2014 Statistics of spatial derivatives of velocity and pressure in turbulent channel flow. *Phys. Fluids* **26**, 085103.
- WU, X. & MOIN, P. 2008 A direct numerical simulation study on the mean velocity characteristics in turbulent pipe flow. *J. Fluid Mech.* **608**, 81–112.
- ZANOUN, E.-S., DURST, F. & NAGIB, H. 2003 Evaluating the law of the wall in two-dimensional fully developed turbulent channel flows. *Phys. Fluids* **15**, 3079–3089.
- ZANOUN, E.-S., NAGIB, H. & DURST, F. 2009 Refined C_f relation for turbulent channels and consequences for high Re experiments. *Fluid Dyn. Res.* **41**, 1–12.