



Maximal heat transfer between two parallel plates

Shingo Motoki^{1,†}, Genta Kawahara¹ and Masaki Shimizu¹

¹Graduate School of Engineering Science, Osaka University, 1-3 Machikaneyama, Toyonaka, Osaka 560–8531, Japan

(Received 18 March 2018; revised 7 July 2018; accepted 9 July 2018; first published online 31 July 2018)

The divergence-free time-independent velocity field has been determined so as to maximise heat transfer between two parallel plates with a constant temperature difference under the constraint of fixed total enstrophy. The present variational problem is the same as that first formulated by Hassanzadeh *et al.* (*J. Fluid Mech.*, vol. 751, 2014, pp. 627–662); however, the search range for optimal states has been extended to a three-dimensional velocity field. A scaling of the Nusselt number Nu with the Péclet number Pe (i.e., the square root of the non-dimensionalised enstrophy with thermal diffusion time scale), $Nu \sim Pe^{2/3}$, has been found in the three-dimensional optimal states, corresponding to the asymptotic scaling with the Rayleigh number Ra , $Nu \sim Ra^{1/2}$, expected to appear in an ultimate state, and thus to the Taylor energy dissipation law in high-Reynolds-number turbulence. At $Pe \sim 10^0$, a two-dimensional array of large-scale convection rolls provides maximal heat transfer. A three-dimensional optimal solution emerges from bifurcation on the two-dimensional solution branch at $Pe \sim 10^1$, and the three-dimensional solution branch has been tracked up to $Pe \sim 10^4$ (corresponding to $Ra \approx 2.7 \times 10^6$). At $Pe \gtrsim 10^3$, the optimised velocity fields consist of convection cells with hierarchical self-similar vortical structures, and the temperature fields exhibit a logarithmic-like mean profile near the walls.

Key words: Bénard convection, mixing enhancement, variational methods

1. Introduction

What is a flow maximising heat transfer? We have explored an answer to this naive question. For buoyancy-driven convection, i.e. Rayleigh–Bénard convection, the maximal heat transfer has been discussed for more than half a century (Malkus 1954; Howard 1963; Busse 1969). Kraichnan (1962) has predicted the asymptotic scaling of the Nusselt number Nu with the Rayleigh number Ra as $Nu \sim Ra^{1/2}$ with

† Email address for correspondence: motoki@me.es.osaka-u.ac.jp

a logarithmic correction for very high Ra . In 1990s, a new variational approach called ‘the background method’ was invented by Doering & Constantin (1992), and the method has triggered remarkable advancements in rigorous upper bounds on the Nusselt number Nu (Doering & Constantin 1996; Kerswell 2001; Otero *et al.* 2002; Plasting & Kerswell 2003; Doering, Otto & Reznikoff 2006; Whitehead & Doering 2011, 2012). In these theoretical works, rigorous upper bounds, e.g. $Nu - 1 \leq 0.02634Ra^{1/2}$ (Plasting & Kerswell 2003), have been derived at $Ra \gg 1$. The ‘ultimate’ scaling $Nu \sim Ra^{1/2}$ corresponds to the Taylor law of energy dissipation in high-Reynolds-number turbulence. It has not been demonstrated as yet what flow structure achieves the ultimate scaling $Nu \sim Ra^{1/2}$. Recently, meanwhile, Hassanzadeh, Chini & Doering (2014) have numerically maximised a wall heat flux within a two-dimensional velocity field bounded by two parallel plates with a constant temperature difference. They formulated a variational problem to find a velocity field maximising heat transfer under the constraint of fixed total enstrophy, and found optimal states consisting of an array of large-scale convection rolls for free-slip boundary conditions. The maximal scaling is represented by $Nu \sim Ra^{5/12}$, corresponding to the rigid upper bound derived by the background method for free-slip conditions (Whitehead & Doering 2011, 2012). For no-slip conditions, on the other hand, the velocity fields numerically optimised within a two-dimensional field also exhibit large-scale circulation rolls, and the found scaling is $Nu \sim Ra^{0.37}$ (Souza 2016). Such scalings observed in the two-dimensional optimal states are quite distinct from the ultimate scaling $Nu \sim Ra^{1/2}$. The scalings observed by both Hassanzadeh *et al.* (2014) and Souza (2016) cannot also persist asymptotically at high Péclet number Pe (corresponding to high Ra) because, as Tobiasco & Doering (2017) rigorously proved, the scaling of two-dimensional flow should be given by $Ra^{1/2}$ with logarithmic corrections, and hence their found states cannot be optimal asymptotically.

In this paper, we consider the variational problem first examined by Hassanzadeh *et al.* (2014) for free-slip conditions and then by Souza (2016) for no-slip conditions; however, we extend the search range for optimal states to a three-dimensional velocity field. We report three-dimensional optimal states capable of achieving the ultimate scaling, and discuss the optimised flow structures. In order to satisfy the Navier–Stokes equation the optimised divergence-free vector field needs an external body force which is distinct from buoyancy, but hereafter we refer to it as a ‘velocity’ field.

2. Formulation

Let us consider heat transfer in a three-dimensional, time-independent and incompressible velocity field between two parallel plates, $\mathbf{u}'(x', y', z') = u'e_x + v'e_y + w'e_z$, satisfying the continuity equation

$$\nabla' \cdot \mathbf{u}' = 0, \tag{2.1}$$

where a prime $(\cdot)'$ represents a dimensional variable, and \mathbf{e}_x and \mathbf{e}_y are mutually orthogonal unit vectors in the wall-parallel directions while \mathbf{e}_z is a unit vector in the wall-normal direction. The configuration of the velocity and temperature fields is shown in figure 1. The two parallel plates are positioned at $z' = 0$ and $z' = H$, and the domain of the flow is periodic in the x' - and y' -directions with periods L'_x and L'_y . The upper (or lower) wall surface is held at lower (or higher) constant temperature $T' = 0$

Maximal heat transfer between two parallel plates

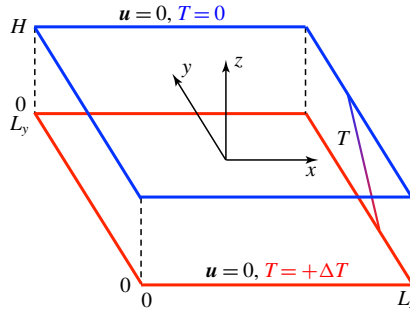


FIGURE 1. Configuration of the velocity and temperature fields.

(or $T' = \Delta T > 0$). We suppose that the temperature field $T'(x', y', z')$ is determined as a solution to an advection–diffusion equation

$$(\mathbf{u}' \cdot \nabla')T' = \kappa \nabla'^2 T', \quad (2.2)$$

supplemented by the boundary conditions

$$\mathbf{u}'(z' = 0) = \mathbf{u}'(z' = H) = \mathbf{0}; \quad T'(z' = 0) = \Delta T, \quad T'(z' = H) = 0, \quad (2.3a-c)$$

where κ denotes a thermal diffusivity. The strength of the velocity field is measured by the Péclet number Pe , defined, in terms of the total enstrophy (or the averaged square of velocity gradient tensor), as

$$Pe = \frac{\langle |\boldsymbol{\omega}'|^2 \rangle^{1/2} H^2}{\kappa} = \frac{\langle |\nabla' \mathbf{u}'|^2 \rangle^{1/2} H^2}{\kappa}, \quad (2.4)$$

where $\boldsymbol{\omega}' = \nabla' \times \mathbf{u}'$, $|\nabla' \mathbf{u}'|^2 = \nabla' \mathbf{u}' : \nabla' \mathbf{u}'$ and $\langle \cdot \rangle$ is a volume average. The wall-normal convective heat transfer is characterised by the Nusselt number, defined as the ratio of the convective heat flux to the conductive heat flux,

$$Nu = 1 + \frac{\langle w'T' \rangle}{\kappa \Delta T / H}. \quad (2.5)$$

In this study, we explore a three-dimensional velocity field maximising Nu for fixed Pe . The constrained optimisation is relevant to the maximisation of the objective functional

$$\mathcal{F} = \left\langle w\theta - \theta^*(\mathbf{x}) [(\mathbf{u} \cdot \nabla)\theta - \nabla^2\theta - w] + p^*(\mathbf{x}) (\nabla \cdot \mathbf{u}) + \frac{\mu}{2} (Pe^2 - |\nabla \mathbf{u}|^2) \right\rangle \quad (2.6)$$

(see Hassanzadeh *et al.* 2014), where $p^*(\mathbf{x})$, $\theta^*(\mathbf{x})$ and μ are Lagrange multipliers. The variables in (2.6) have been non-dimensionalised as

$$\mathbf{x} = \frac{\mathbf{x}'}{H}, \quad \theta = \frac{\theta'}{\Delta T}, \quad \mathbf{u} = \frac{\mathbf{u}'}{\kappa/H}, \quad p^* = \frac{p'^*}{\rho \kappa^2 / H^2}, \quad \theta^* = \frac{\theta'^*}{\Delta T}, \quad (2.7a-e)$$

where ρ is the constant mass density of the fluid and $\theta = T - (1 - z)$ is a temperature fluctuation about a conductive state. Stationary points of \mathcal{F} are determined by the Euler–Lagrange equations

$$\frac{\delta \mathcal{F}}{\delta \mathbf{u}} \equiv -\nabla p^* + \theta \nabla \theta^* + \mu \nabla^2 \mathbf{u} + (\theta + \theta^*) \mathbf{e}_z = \mathbf{0}, \quad (2.8)$$

$$\frac{\delta \mathcal{F}}{\delta \theta} \equiv (\mathbf{u} \cdot \nabla)\theta^* + \nabla^2\theta^* + w = 0, \tag{2.9}$$

$$\frac{\delta \mathcal{F}}{\delta \theta^*} \equiv -(\mathbf{u} \cdot \nabla)\theta + \nabla^2\theta + w = 0, \tag{2.10}$$

$$\frac{\delta \mathcal{F}}{\delta p^*} \equiv \nabla \cdot \mathbf{u} = 0, \tag{2.11}$$

$$\frac{\partial \mathcal{F}}{\partial \mu} \equiv \frac{1}{2}(Pe^2 - |\nabla \mathbf{u}|^2) = 0. \tag{2.12}$$

3. Numerical optimisation

Solutions to equations (2.8)–(2.11) depend only on μ for fixed periods (L_x, L_y) . For given μ , the solutions correspond to stationary points of the alternative functional

$$\mathcal{G} = \left\langle w\theta - \frac{\mu}{2}|\nabla \mathbf{u}|^2 - \theta^*(\mathbf{x}) [(\mathbf{u} \cdot \nabla)\theta - \nabla^2\theta - w] + p^*(\mathbf{x}) (\nabla \cdot \mathbf{u}) \right\rangle. \tag{3.1}$$

This is because $\mathcal{G} = \mathcal{F} - (\mu/2)Pe^2$ and thus the Euler–Lagrange equations for \mathcal{G} are also given by (2.8)–(2.11). In our previous work on a different functional in a different configuration (Motoki, Kawahara & Shimizu 2018), we have developed a numerical approach to find local maxima of a functional kindred to \mathcal{G} by a combination of the steepest ascent method and the Newton–Krylov method. Using the same procedures, we obtain an optimal state $(\mathbf{u}_{opt}, \theta_{opt}, \theta_{opt}^*, p_{opt}^*)$ maximising \mathcal{G} for given μ . Since \mathcal{F} has the gradients common to \mathcal{G} , the optimal state gives the maximum of \mathcal{F} at $Pe = \langle |\nabla \mathbf{u}_{opt}|^2 \rangle^{1/2}$. Thus the optimal states of \mathcal{F} can be obtained without fixing Pe in the process of the optimisation.

Only when we fix Pe , maximal points for a specific value of Pe (say, Pe_0) are calculated by updating μ as

$$\mu_{new} = \mu + \epsilon(\langle |\nabla \mathbf{u}_{opt}|^2 \rangle - Pe_0^2), \tag{3.2}$$

taking account of the fact that the decrease (or increase) in μ corresponds to the increase (or decrease) in Pe , where ϵ is a small positive constant to be taken as $\epsilon \sim 10^{-5}$. Equations (2.8)–(2.11) are discretised by employing the spectral Galerkin method based on Fourier–Chebyshev expansions (for more details, see § 3 and appendix A in Motoki *et al.* 2018).

In this paper, we present the optimal states in the square wall-parallel domain of $(L_x, L_y, L_z) = (\pi/2, \pi/2, 1)$. By increasing or decreasing the wall-parallel domain size to $(L_x, L_y, L_z) = (2, 2, 1)$ or $(\pi/(2\sqrt{2}), \pi/(2\sqrt{2}), 1)$, we have confirmed that the effects of the domain size are insignificant on the scaling of Nu with Pe at $Pe \gtrsim 10^3$ as well as the spatial structures in the optimal states, which will be described in the following sections. The numerical computations are carried out on 64^3 grid points for $Pe \leq 500$ and 128^3 grid points for $Pe > 500$. It has been validated in comparison with 256^3 grid points that the results presented in this paper are independent of the spatial resolution. The dependence on domain size and spatial resolution is shown in appendix A.

4. Ultimate scaling

Figure 2(a) shows the maximal Nu as a function of Pe . At large Pe ($\gtrsim 10^3$), we observe the scaling of Nu with Pe , $Nu - 1 \approx 0.082Pe^{2/3}$. The scaling $Nu \sim Pe^{2/3}$

Maximal heat transfer between two parallel plates

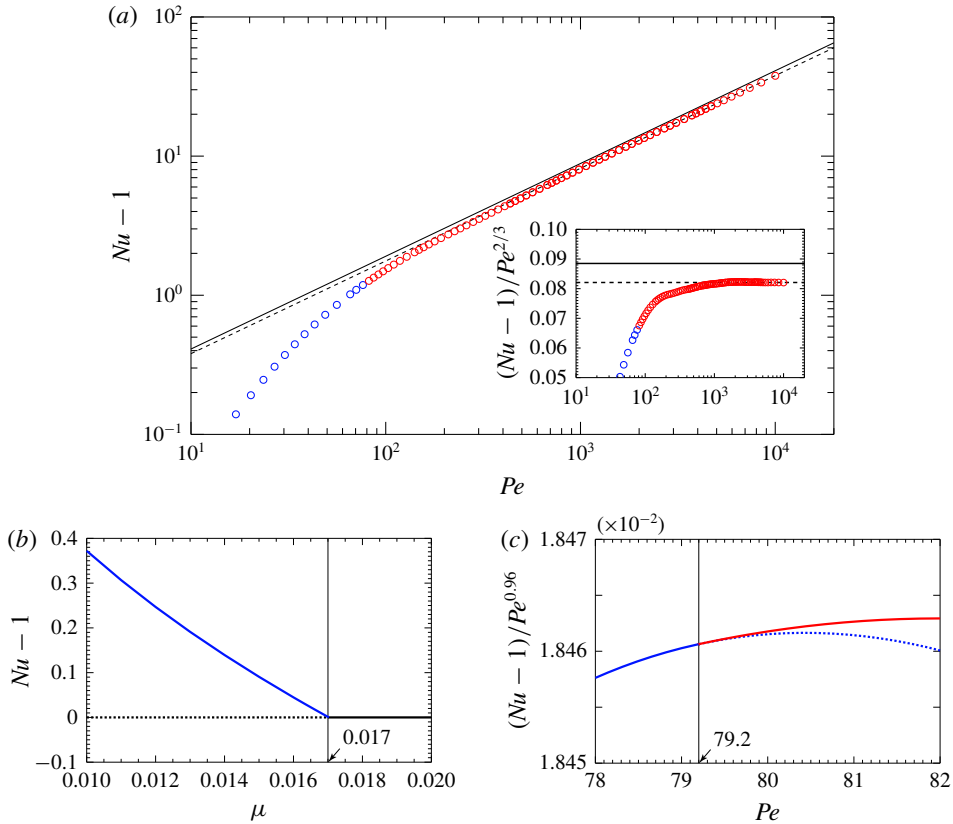


FIGURE 2. (a) Nusselt number Nu as a function of Péclet number Pe in the optimal states. The blue and red circles denote two-dimensional and three-dimensional optimal states, respectively. The dashed line indicates the power fit $Nu - 1 = 0.0821Pe^{2/3}$ determined in the range $5 \times 10^3 < Pe < 10^4$. The solid line represents the scaling $Nu - 1 = 0.0885Pe^{2/3}$ evaluated from the rigorous upper bound $Nu - 1 = 0.02634Ra^{1/2}$ (Plasting & Kerswell 2003) assuming the identity $Pe^2 = Ra(Nu - 1)$ (Hassanzadeh *et al.* 2014). The inset shows the compensated Nu . (b,c) Nu as a function of (b) much larger μ (much smaller Pe) and (c) larger μ (smaller Pe). The blue and red curves respectively show the two-dimensional and three-dimensional solutions, and the black line is a conductive solution. The solid (or dashed) line denotes an optimal (or saddle) solution.

corresponds to the ultimate scaling $Nu \sim Ra^{1/2}$ in the Rayleigh–Bénard problem, provided that the total energy budget is given by the Boussinesq equation, that is $Pe^2 = Ra(Nu - 1)$ (Hassanzadeh *et al.* 2014), where $Ra = g\beta\Delta TH^3/(\nu\kappa)$ is the Rayleigh number, g , β and ν being the acceleration due to gravity, the thermal expansion coefficient of the fluid and the kinematic viscosity, respectively. The thick solid line indicates the rigorous upper bound derived by using the background method (Plasting & Kerswell 2003). The obtained maximal scaling is close to the upper bound, but the prefactor is approximately 7.2% less than that of the bound. We have confirmed that the optimal states in the different domains, $(L_x, L_y, L_z) = (2, 2, 1)$ and $(\pi/(2\sqrt{2}), \pi/(2\sqrt{2}), 1)$, exhibit consistent scaling $Nu - 1 \approx 0.082Pe^{2/3}$ at $Pe \gtrsim 10^3$ (as can be seen in figure 8 in appendix A).

Supposing that $Nu \sim Pe^{2/3}$ and choosing the reference velocity as $U = (g\beta\Delta TH)^{1/2}$, we have the scaling with respect to the energy dissipation as

$$\frac{\nu \langle |\nabla' \mathbf{u}'|^2 \rangle}{U^3/H} \sim Pr^{-1/2}, \quad (4.1)$$

where Pr is the Prandtl number. Thus the scaling $Nu \sim Pe^{2/3}$ means that the energy dissipation normalised by U^3/H is independent of the Reynolds number, in accord with the Taylor's scaling view for turbulent energy dissipation. Although the Taylor dissipation law does not hold in turbulent shear flows over a smooth-wall surface, the Reynolds-number-independent skin-friction coefficient can be observed in high-Reynolds-number rough-wall turbulence, implying the emergence of the Taylor law. The ultimate scaling $Nu \sim Ra^{1/2}$ has not also been observed in turbulent Rayleigh–Bénard convection between smooth horizontal plates, i.e. the same boundary conditions as in the present study. For homogeneous turbulent convection without thermal and velocity boundary layers, e.g. in three-dimensional periodic boundary box with the vertical mean temperature gradient (Lohse & Toschi 2003), the ultimate scaling $Nu \sim Ra^{1/2}$ has been observed. However, it is still an open question whether or not the ultimate scaling can be found in high- Ra convective turbulence between two parallel plates with surface roughness (Roche *et al.* 2001; Zhu *et al.* 2017).

5. Appearance of three-dimensional solution

At large μ (small Pe), a two-dimensional array of convection rolls gives maximal heat transfer. The solution arises from supercritical pitchfork bifurcation on a conductive solution at $\mu \approx 1.703 \times 10^{-2}$ ($Pe \equiv 0$) (figure 2*b*), and it satisfies the reflection symmetry

$$[u, v, w, \theta](x, y, z) = [-u, v, w, \theta](-x, y, z) \quad (5.1)$$

and the shift-and-reflection symmetry

$$[u, v, w, \theta](x, y, z) = [u, v, -w, -\theta](x + L_x/2, y, 1 - z) \quad (5.2)$$

(see figure 3*a*). Figure 3(*a,b*) visualise isosurfaces of the temperature field T and of the second invariant of the velocity gradient tensor

$$Q = -\frac{1}{2} \frac{\partial u_i}{\partial x_j} \frac{\partial u_j}{\partial x_i}. \quad (5.3)$$

As μ decreases further, the second pitchfork bifurcation occurs on the two-dimensional solution branch at $\mu \approx 3.028 \times 10^{-3}$ ($Pe \approx 79.2$, corresponding to $Ra \approx 5.11 \times 10^3$ via $Pe^2 = Ra(Nu - 1)$) (figure 2*c*). Subsequently, the two-dimensional solution becomes a saddle solution, and a three-dimensional optimal solution with the shift-and-reflection symmetry

$$[u, v, w, \theta](x, y, z) = [u, v, -w, -\theta](x + L_x/2, y + L_y/2, 1 - z) \quad (5.4)$$

appears (see figure 3*b*). In order to identify a qualitative change in the velocity field through the second bifurcation, we introduce the one-dimensional energy spectra E_w of the wall-normal velocity w defined as

$$E_w(k_x, z) = \sum_{k_y=-K}^K |\tilde{w}(k_x, k_y, z)|^2, \quad E_w(k_y, z) = \sum_{k_x=-K}^K |\tilde{w}(k_x, k_y, z)|^2, \quad (5.5a,b)$$

Maximal heat transfer between two parallel plates

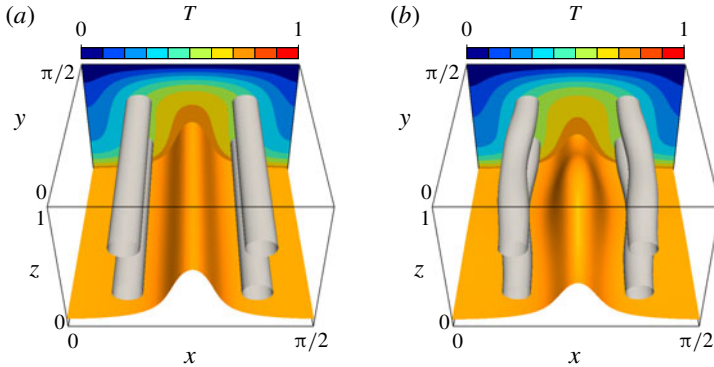


FIGURE 3. (a) Two-dimensional saddle and (b) three-dimensional optimal solutions at $Pe = 80.0$. The orange objects show the isosurfaces of the temperature, $T = 0.75$, and the light grey tube-like objects are the vortex structures visualised by the positive second invariant of the velocity gradient tensor, $Q = 2560$. The contours represent the temperature field in the plane $y = \pi/2$.

where K is a positive integer representing the truncation, and \tilde{w} is the Fourier coefficient such that

$$w(x, y, z) \approx \sum_{k_x=-K}^K \sum_{k_y=-K}^K \tilde{w}(k_x, k_y, z) \exp \left[i \left\{ \frac{2\pi k_x}{L_x} x + \frac{2\pi k_y}{L_y} y \right\} \right]. \quad (5.6)$$

Figure 4(a–d) show the premultiplied energy spectra $k_x E_w(k_x, z)$ (or $k_y E_w(k_y, z)$) at the Péclet number $Pe = 79.2$, just after the onset of the three-dimensional solution, as a function of the distance to the wall, z and the x - (or y -) component of the ‘wavenumber’ vector, k_x (or k_y). In the optimised velocity field (figure 4a) within a two-dimensional field, there exist only the modes for odd k_x representing a pair of counterrotating large-scale rolls around $z = 1/2$ fully extending to the periodic box in the x -direction (see figure 3a for the rolls at higher Pe). It is also the case even at higher Péclet number $Pe \sim 10^3$. Figure 4(b) shows the spectrum as a function of the other component k_y for the three-dimensional velocity field at $Pe = 79.2$. In the spectra $k_y E_w$, the only fundamental mode for $k_y = 1$ is dominant, since the solution has been obtained just after the bifurcation point (the onset of the three-dimensional solution). In $k_x E_w$, the modes for even k_x also appear as a result of the emergence of smaller-scale three-dimensional structures in addition to the large-scale rolls (figure 4c). In order to extract the deviation from the original two-dimensional velocity field, the spectrum of the velocity difference between the two solutions at $Pe = 79.2$ is shown in figure 4(d). The leading mode is at $k_x = 2$, and the spectral component has a peak at $z = 1/4$ (half the distance between one of the two walls and the midplane). That is to say, the smaller-scale vortical structures for $k_x = 2$, half the size of the large-scale rolls, emerge at $z = 1/4$, closer to the wall. In figure 4(e), the relevant structures are visualised by the difference in the y -component of vorticity, $\omega_y^{3D} - \omega_y^{2D}$. The extracted structure is characterised in terms of a three-dimensional mode $(k_x, k_y) = (2, 1)$, and exhibits an array of vortices arranged in a wall-parallel plane around $z = 1/4$ (and $3/4$). The onset of the smaller three-dimensional vortical structures near the walls brings about the bending of the original larger two-dimensional rolls and associated vortex tubes (figure 3b), enhancing heat transfer.

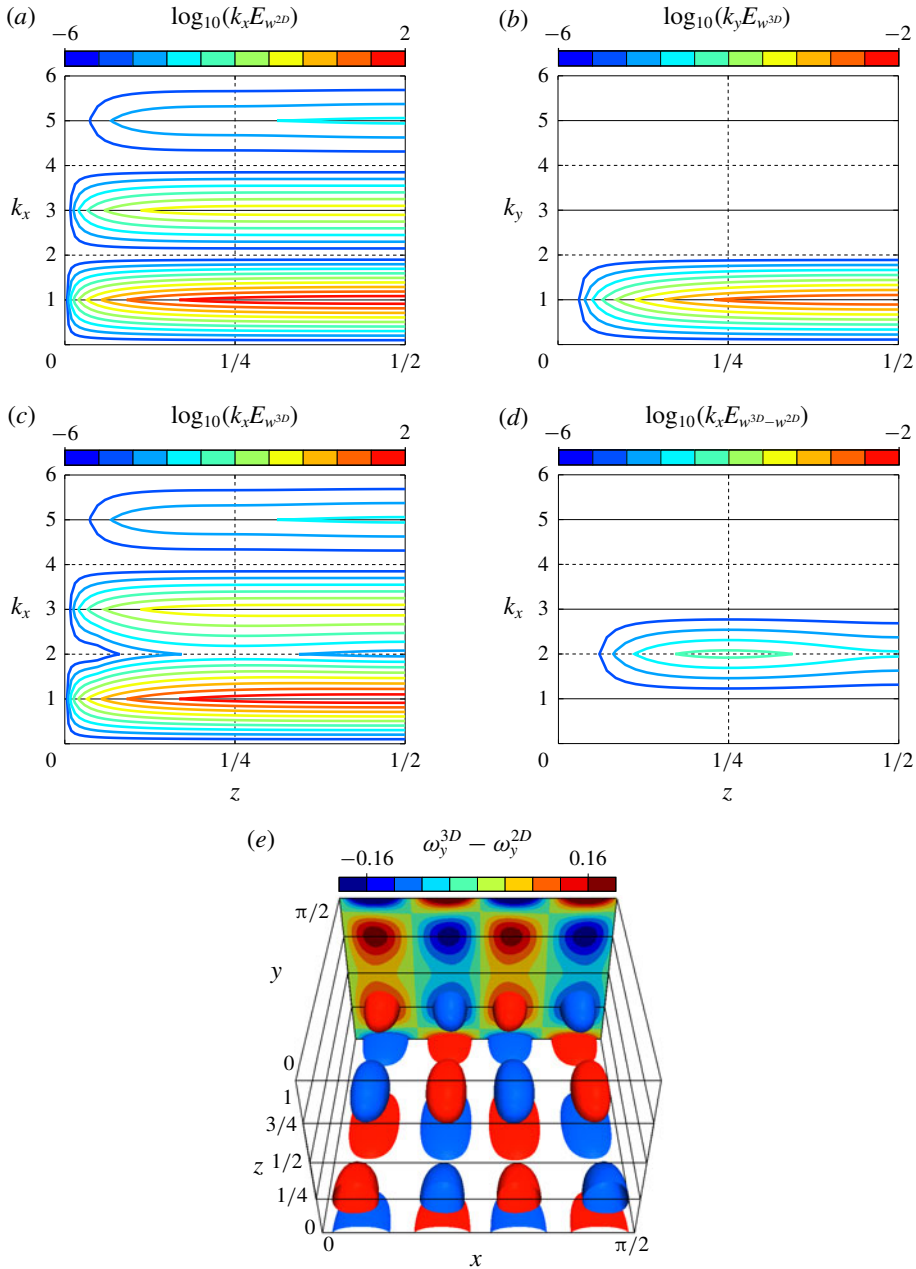


FIGURE 4. (a–d) One-dimensional premultiplied energy spectra of the wall-normal velocity w , $k_x E_w(k_x, z)$ and $k_y E_w(k_y, z)$, at $Pe = 79.2$. The spectrum of (a) the two-dimensional solution w^{2D} , (b,c) the three-dimensional solution w^{3D} , and (d) their difference $w^{3D} - w^{2D}$. The lateral axis denotes the distance to the wall z , and the longitudinal axis is the wavenumber component (a,c,d) k_x in the x -direction and (b) k_y in the y -direction. (e) Spatial distribution of the difference in the y -component of vorticity ω_y between the three- and two-dimensional solutions, $\omega_y^{3D} - \omega_y^{2D}$ at $Pe = 79.2$. The red/blue objects respectively show the isosurfaces of $\omega_y^{3D} - \omega_y^{2D} = \pm 0.12$. The contours represent $\omega_y^{3D} - \omega_y^{2D}$ in the plane $y = \pi/2$.

Maximal heat transfer between two parallel plates

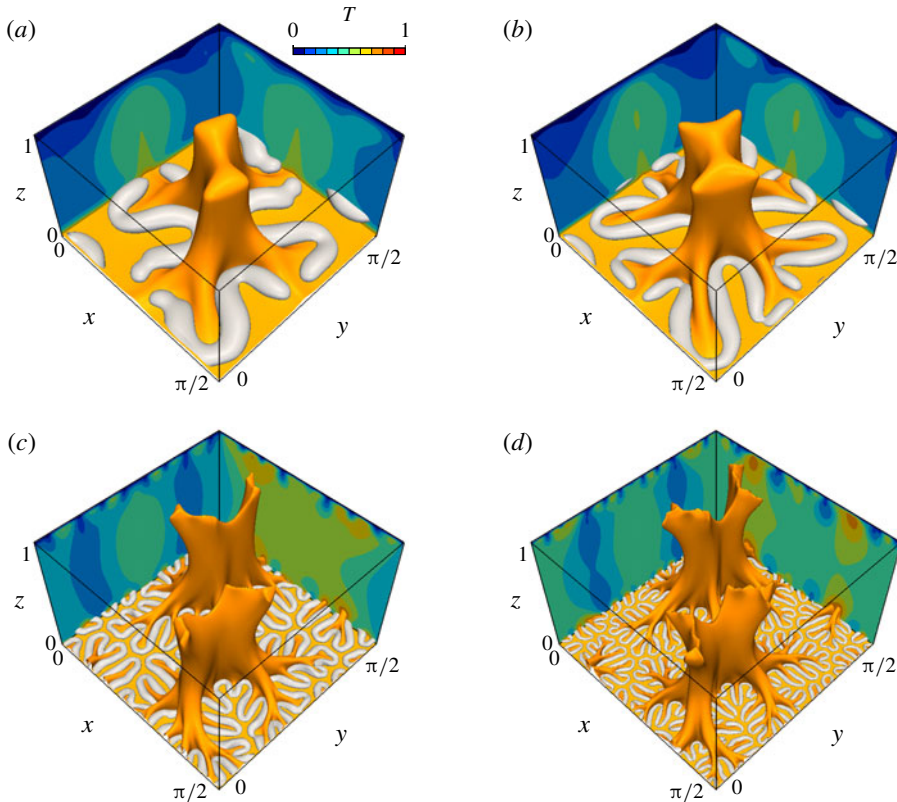


FIGURE 5. Optimal states at Péclet number (a) $Pe = 508$, (b) $Pe = 1006$, (c) $Pe = 5041$ and (d) $Pe = 10009$. The orange objects show the isosurfaces of $T = 0.75$. The light grey tube-like structures are the isosurfaces of (a) $Q = 8.0 \times 10^4$, (b) $Q = 4.8 \times 10^5$, (c) $Q = 1.6 \times 10^7$ and (d) $Q = 1.6 \times 10^8$ (note that only those in the lower half of the domain are shown for visualisation of the near-wall structures). The contours represent temperature field in the planes $x = 0$ and $y = \pi/2$.

In the velocity field optimised within a two-dimensional field, such smaller-scale structures closer to the walls have not been found even at higher Pe . In the three-dimensional optimal velocity field, on the other hand, the three-dimensional smaller-scale structures with the higher wavenumber emerge closer to the walls, as mentioned above. This is a crucial difference between the two- and three-dimensional optimal fields.

6. Hierarchical self-similar structures

Tree-like structures of isotherms are observed in the optimal states at small μ (large Pe), shown in figure 5. The orange objects show isosurfaces of $T = 0.75$, and a 'trunk' of the 'tree' represents a hot 'plume' where the positive wall-normal velocity has been found to be dominant. As Pe increases, the tree 'roots' grow deeper while maintaining the large-scale trunk. The light grey objects show smallest-scale vortex structures visualised by the positive isosurfaces of Q in the near-wall region of the lower half of the domain (similar vortical structures exist on the upper wall). The smaller and stronger vortices appear closer to the walls with increasing enstrophy,

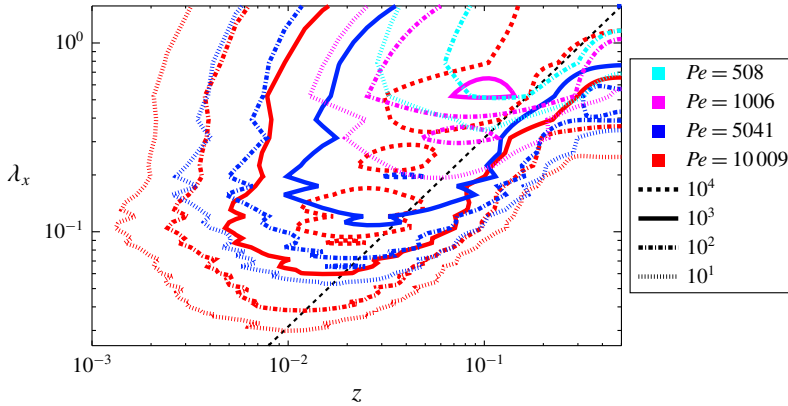


FIGURE 6. Energy spectra of the wall-normal velocity w , $k_x E_w(k_x, z)$, as a function of the distance to the wall, z and the wavelength in the x -direction, λ_x . The dashed diagonal indicates $\lambda_x = L_x z$.

i.e. Pe . The roots are seen to be generated as a consequence of upward fluid motion induced between the roughly antiparallel nearest segments of the winding tube-like vortices. As seen in the bifurcation of the three-dimensional solution from the two-dimensional solution, the local folding of the larger vortices stems from the onset of the smaller vortical structures closer to the wall.

Figure 6 shows the energy spectra of the wall-normal velocity w as a function of the distance to the wall, z , and the wavelength in the x -direction, $\lambda_x = L_x/k_x$, relevant to the size of the vortical structures. It can be seen that smaller-scale structures are generated closer to the wall as Pe is increased. At $Pe = 10\,009$ several spectral peaks are observed along the ‘ridge’ represented by the dashed diagonal $\lambda_x = L_x z$, implying that the optimal velocity fields possess hierarchical self-similarity. As shown in figure 7(a), the energy spectra scale with the conduction length $\lambda_\theta = (2Nu)^{-1}$ in the close vicinity of the wall. The hierarchical structures exist down to $z/\lambda_\theta \approx 1$, where the size of the structures is $\lambda_x \approx 5Nu^{-1}$. Since Nu scales with $Pe^{2/3}$ at large Pe , the smallest scale is estimated as $\lambda_x \sim Pe^{-2/3}$, much smaller than the optimal aspect ratio, $L/H \sim Pe^{-0.371}$, in the two-dimensional field (Souza 2016). Figure 7(b) shows the mean temperature profile \bar{T} as a function of z/λ_θ . $1 - \bar{T} = z/\lambda_\theta$ holds at $z/\lambda_\theta \ll 1$, where the thermal conduction dominates over the convection. As the distance to the wall, z increases, the hierarchical vortex structures promote the convective heat transfer. In the region $1 \lesssim z/\lambda_\theta \lesssim 10$ where the self-similarity appears, the logarithmic-like temperature profiles are observed at $Pe = 1008, 5041$ and $10\,009$. The dashed line indicates the logarithmic fit $1 - \bar{T} = 0.0358 \ln(z/\lambda_\theta) + 0.423$ determined in the range $2 < z/\lambda_\theta < 4$ at $Pe = 10\,009$. Recently, the logarithmic temperature profiles have also been observed numerically and experimentally in turbulent Rayleigh–Bénard convection (Ahlers *et al.* 2012; Ahlers, Bodenschatz & He 2014). In the region far from the wall, $10\lambda_\theta \lesssim z \lesssim 1/2$, mixing by the large-scale convection cells is dominant, and thus the temperature profile is flattened.

7. Summary and conclusions

We have found the three-dimensional optimal states which lead to the scaling $Nu \sim Pe^{2/3}$ consistent with the ultimate scaling $Nu \sim Ra^{1/2}$ in Rayleigh–Bénard

Maximal heat transfer between two parallel plates

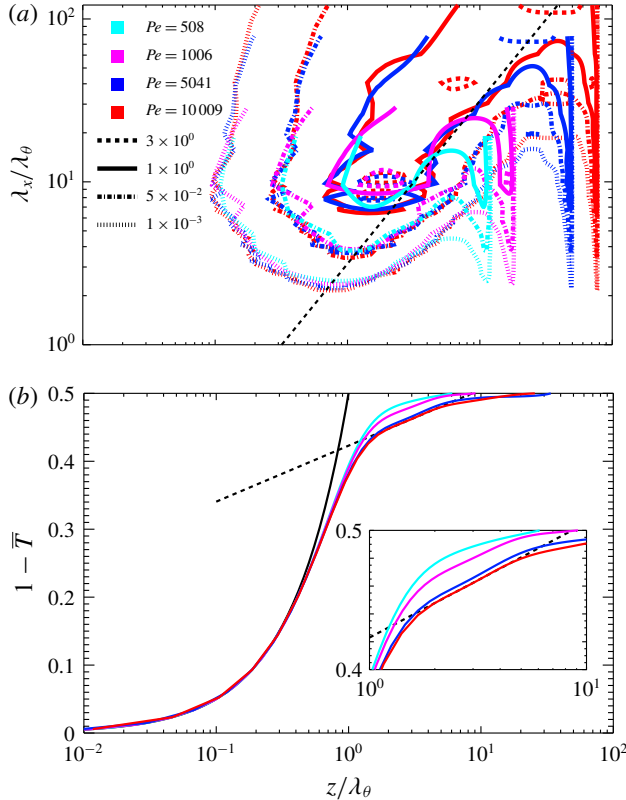


FIGURE 7. (a) Energy spectra $k_x E_w(k_x, z)$ as a function of z and λ_x . The energy spectra $k_x E_w$, the distance to the wall, z and the wavelength in the x -direction, λ_x are normalised by $\lambda_\theta = (2Nu)^{-1}$. The dashed diagonal indicates $\lambda_x = L_x z$. (b) Mean temperature profile \bar{T} as a function of z/λ_θ . The black solid line indicates $1 - \bar{T} = z/\lambda_\theta$, and the dashed line represents the logarithmic fit $1 - \bar{T} = 0.0358 \ln(z/\lambda_\theta) + 0.423$ determined in the range $2 < z/\lambda_\theta < 4$ at $Pe = 10009$.

convection. The optimal heat transfer is achieved by three-dimensional convection cells with smaller-scale vortices attached on the walls. At large Pe , the optimal velocity field exhibits hierarchical self-similarity. The large-scale cells mix up the temperature almost completely around the midplane between the two walls. Near the walls, meanwhile, self-similar vortical structures locally enhance heat transfer, and yield a logarithmic-like mean temperature distribution. Our earlier optimisation for heat transfer in plane Couette flow (Motoki *et al.* 2018) provided the optimal velocity fields in which we observed hierarchical structure consisting of a number of streamwise vortex tubes. The logarithmic-like mean temperature profiles as well as the ultimate scaling $Nu \sim Ra^{1/2}$ were also found in the optimal fields. It has recently been rigorously proved that the ultimate scaling $Nu \sim Ra^{1/2}$ with logarithmic corrections can be achieved by some velocity field which is two-dimensional but exhibits hierarchical self-similarity (Tobasco & Doering 2017). These results suggest that self-similar hierarchy of a velocity field would be a necessary condition for the emergence of the ultimate scaling and logarithmic-like mean temperature profile between two parallel no-slip plates.

In order for the optimal state achieving maximal heat transfer to fulfil the Navier–Stokes equation we need external body force

$$\mathbf{f} \equiv -(\mathbf{u} \cdot \nabla)\mathbf{u} - \nabla p + Pr\nabla^2\mathbf{u} + PrRa(1 - z + \theta)\mathbf{e}_z, \quad (7.1)$$

which is different from the buoyant force in the Boussinesq equation, where (\mathbf{u}, θ) is an optimal solution to the Euler–Lagrange equations (2.8)–(2.12) and p is pressure determined by the Poisson equation stemming from the Boussinesq equations. Our preliminary study, however, demonstrates that by using homotopy from the body force to the buoyancy the optimal state can be continuously connected to a steady solution to the Boussinesq equation. Although the connected solution is not stable, it reproduces the mean and root-mean-squared velocities and temperature as well as thermal plumes in turbulent Rayleigh–Bénard convection. This steady solution to the Boussinesq equation exhibits the usually observed scaling $Nu \sim Ra^{1/3}$ rather than the ultimate scaling $Nu \sim Ra^{1/2}$. It can be stated that the optimal state identified for maximal heat transfer in this work is relevant to convective turbulence in the sense that its connected solution to the Boussinesq equation represents well the structure and statistics in a turbulent state. The authors are currently working on investigating the steady solutions in the Rayleigh–Bénard convection case and establishing a relation between solutions of the Euler–Lagrange equations and the Boussinesq equations. The results will be presented in a separate paper.

Acknowledgements

We are grateful to Professor C. R. Doering at University of Michigan for useful discussions and suggestions. This work was partially supported by a Grant-in-Aid Scientific Research (grant nos 25249014, 26630055) from the Japanese Society for Promotion of Science 665 (JSPS). S.M. is supported by JSPS Grant-in-Aid for JSPS Fellows grant no. 666 16J00685.

Appendix A. Dependence of optimal states on domain size and spatial resolution

Figure 8 shows the Nusselt number compensated by $Pe^{2/3}$ as a function of Pe in the optimal states for different domain sizes. The green, red and blue symbols represent the domains $(L_x, L_y, L_z) = (2, 2, 1)$, $(\pi/2, \pi/2, 1) \approx (1.57, 1.57, 1)$ and $(\pi/(2\sqrt{2}), \pi/(2\sqrt{2}), 1) \approx (1.11, 1.11, 1)$, respectively. In any domains, the appearance of three-dimensional optimal states and the scaling $Nu - 1 \approx 0.082Pe^{2/3}$ at $Pe \gtrsim 10^3$ can be observed. For the present optimisation problem, it is expected that there exists a velocity field with the domain size which leads to the global optimal. However, we predict that the improvement in prefactor by optimising the domain size would not be significant, since it is considered that the emergence of the hierarchical small-scale structures near the walls, which are robustly observed in different domain sizes (figure 9), plays a key role in the heat transfer enhancement.

In figure 8, the symbols +, ● and × respectively show the results obtained on different grid points of 64^3 , 128^3 and 256^3 , and the effects of the spatial resolutions on the Nusselt number and the Péclet number (i.e., the enstrophy) are minor. For the domain $(L_x, L_y, L_z) = (\pi/2, \pi/2, 1)$, a spatial resolution of 128^3 grid points is enough to evaluate the characteristics of the optimal states at $Pe \lesssim 10^4$; 64^3 grid points are sufficient at $Pe \lesssim 10^3$.

Maximal heat transfer between two parallel plates

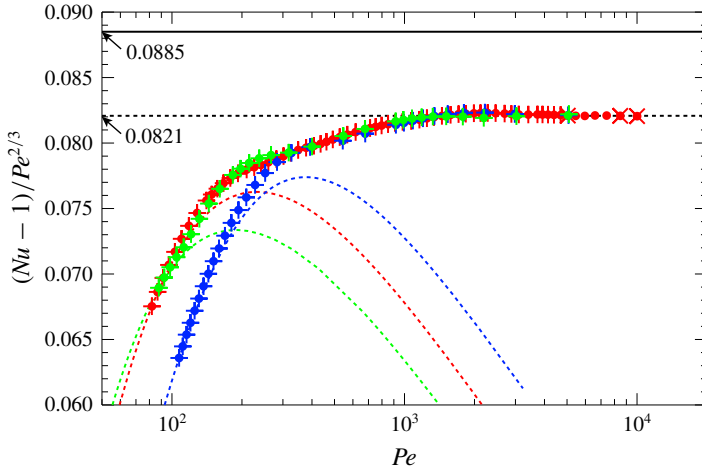


FIGURE 8. Nusselt number Nu compensated by $Pe^{2/3}$ as a function of the Péclet number Pe in the optimal states for different domains. The green, red and blue symbols (or dashed curves) respectively show the domains $(L_x, L_y, L_z) = (2, 2, 1)$, $(\pi/2, \pi/2, 1)$ and $(\pi/(2\sqrt{2}), \pi/(2\sqrt{2}), 1)$ (or the two-dimensional domains $(L_x, L_z) = (2, 1)$, $(\pi/2, 1)$ and $(\pi/(2\sqrt{2}), 1)$). The three-dimensional (or two-dimensional) solutions are obtained on grid points of $+$, 64^3 ; \bullet , 128^3 ; \times , 256^3 (or 256^2). The solid and dashed lines represent the scaling $Nu - 1 = 0.0885Pe^{2/3}$ (evaluated from the rigorous upper bound by Plasting & Kerswell 2003) and $Nu - 1 = 0.0821Pe^{2/3}$ (determined from the power fit at $Pe > 5 \times 10^3$), respectively.

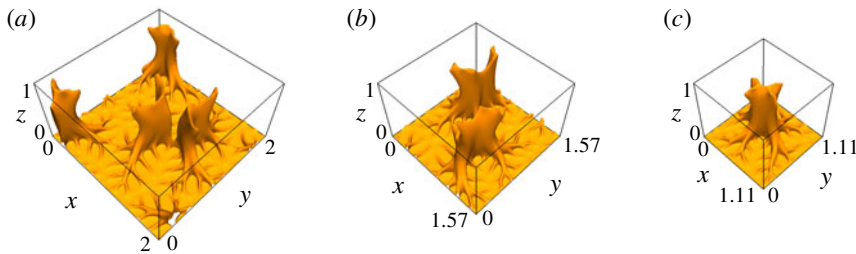


FIGURE 9. Optimal states in the domain of (a) $(L_x, L_y, L_z) = (2, 2, 1)$, (b) $(L_x, L_y, L_z) = (\pi/2, \pi/2, 1)$ and (c) $(L_x, L_y, L_z) = (\pi/(2\sqrt{2}), \pi/(2\sqrt{2}), 1)$. The orange objects show the isosurfaces of the temperature $T = 0.75$. The Péclet number is (a) $Pe = 5051$, (b) $Pe = 5041$, (c) $Pe = 5074$.

References

- AHLERS, G., BODENSCHATZ, E., FUNFSCHILLING, D., GROSSMANN, S., HE, X., LOHSE, D., STEVENS, R. J. A. M. & VERZICCO, R. 2012 Logarithmic temperature profiles in turbulent Rayleigh–Bénard convection. *Phys. Rev. Lett.* **109**, 114501.
- AHLERS, G., BODENSCHATZ, E. & HE, X. 2014 Logarithmic temperature profiles of turbulent Rayleigh–Bénard convection in the classical and ultimate state for a Prandtl number of 0.8. *J. Fluid Mech.* **758**, 436–467.
- BUSSE, F. H. 1969 On Howard’s upper bound for heat transport by turbulent convection. *J. Fluid Mech.* **37**, 457–477.

- DOERING, C. R. & CONSTANTIN, P. 1992 Energy dissipation in shear driven turbulence. *Phys. Rev. Lett.* **69**, 1648–1651.
- DOERING, C. R. & CONSTANTIN, P. 1996 Variational bounds on energy dissipation in incompressible flows. III. Convection. *Phys. Rev. E* **53** (6), 5957–5981.
- DOERING, C. R., OTTO, F. & REZNIKOFF, M. G. 2006 Bounds on vertical heat transport for infinite-Prandtl-number Rayleigh–Bénard convection. *J. Fluid Mech.* **560**, 229–241.
- HASSANZADEH, P., CHINI, G. P. & DOERING, C. R. 2014 Wall to wall optimal transport. *J. Fluid Mech.* **751**, 627–662.
- HOWARD, L. N. 1963 Heat transport by turbulent convection. *J. Fluid Mech.* **17**, 405–432.
- KERSWELL, R. R. 2001 New results in the variational approach to turbulent Boussinesq convection. *Phys. Fluids* **13**, 192–209.
- KRAICHNAN, R. H. 1962 Turbulent thermal convection at arbitrary Prandtl number. *Phys. Fluids* **5** (11), 1374–1389.
- LOHSE, D. & TOSCHI, F. 2003 Ultimate state of thermal convection. *Phys. Rev. Lett.* **90**, 034502.
- MALKUS, W. V. R. 1954 The heat transport and spectrum of thermal turbulence. *Proc. R. Soc. Lond. A* **225**, 196–212.
- MOTOKI, S., KAWAHARA, G. & SHIMIZU, M. 2018 Optimal heat transfer enhancement in plane Couette flow. *J. Fluid Mech.* **835**, 1157–1198.
- OTERO, J., WITTENBERG, R. W., WORTHING, R. A. & DOERING, C. R. 2002 Bounds on Rayleigh–Bénard convection with an imposed heat flux. *J. Fluid Mech.* **473**, 191–199.
- PLASTING, S. C. & KERSWELL, R. R. 2003 Improved upper bound on the energy dissipation rate in plane Couette flow: the full solution to Busse’s problem and the Constantin–Doering–Hopf problem with one-dimensional background field. *J. Fluid Mech.* **477**, 363–379.
- ROCHE, P. E., CASTAING, B., CHABAUD, B. & HÉBRAL, B. 2001 Observation of the 1/2 power law in Rayleigh–Bénard convection. *Phys. Rev. E* **63**, 045303(R).
- SOUZA, A. N. 2016 An optimal control approach to bounding transport properties of thermal convection. PhD thesis, University of Michigan.
- TOBASCO, I. & DOERING, C. R. 2017 Optimal wall-to-wall transport by incompressible flows. *Phys. Rev. Lett.* **118**, 264502.
- WHITEHEAD, J. P. & DOERING, C. R. 2011 Ultimate state of two-dimensional Rayleigh–Bénard convection between free-slip fixed-temperature boundaries. *Phys. Rev. Lett.* **106**, 244501.
- WHITEHEAD, J. P. & DOERING, C. R. 2012 Rigid bounds on heat transport by a fluid between slippery boundaries. *J. Fluid Mech.* **707**, 241–259.
- ZHU, X., STEVENS, R. J. A. M., VERZICCO, R. & LOHSE, D. 2017 Roughness-facilitated local 1/2 scaling does not imply the onset of the ultimate regime of thermal convection. *Phys. Rev. Lett.* **119**, 154501.