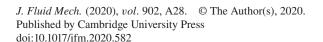
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Collision-induced breakage of agglomerates in homogenous isotropic turbulence laden with adhesive particles

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We carry out direct numerical simulation combined with adhesive discrete element calculations to investigate collision-induced breakage of agglomerates in homogeneous isotropic turbulence. The adopted method tracks the dynamics of individual particles while they are travelling alone through the fluid and while they are colliding with other particles. Based on extensive simulation runs, an adhesion parameter Ad_n is constructed to quantify the possibility of occurrence of sticking, rebound and breakage events. The collision-induced breakage rate is then formulated based on the Smoluchowski equation and a breakage fraction. The breakage fraction, defined as the fraction of collisions that result in breakage, is then analytically estimated by a convolution of the probability distribution of collision velocity and a universal transfer function. It is shown that the breakage rate decreases exponentially as the adhesion parameter Ad_n increases for doublets and scales as linear functions of the agglomerate size, with the slope controlled by Ad_n . These results allow one to estimate the breakage rate for early stage agglomerates of arbitrary size. Moreover, the role of the flow structure on the collision-induced breakage is also examined. Violent collisions and breakages are more likely caused by particles ejected rapidly from strong vortices and happen in straining sheets. Our results extend the findings of shear-induced fragmentation, forming a more complete picture of breakage of agglomerates in turbulent flows.

Key words: particle/fluid flow, breakup/coalescence

1. Introduction

For solid micron particles immersed in turbulence, various complicated particle-scale interactions, such as van der Waals attraction (Israelachvili 2011; Chen, Li & Marshall 2019a), capillary force (Royer *et al.* 2009) and electrostatic forces (Jones 2005; Steinpilz *et al.* 2020), lead to the formation of agglomerates. On the other hand, breakage of agglomerates also happens due to the flow stress (Higashitani, Iimura & Sanda 2001; Bäbler, Morbidelli & Bałdyga 2008) and collisions of other particles (Liu & Hrenya 2018).

Both the formation and the breakage of agglomerates find broad applications in industry, ranging from particulate matter control (Chang *et al.* 2017; Jaworek *et al.* 2018; Wei *et al.* 2019), drug delivery (Voss & Finlay 2002), agglomerate dispersion in gas phase (Iimura *et al.* 2009) to water treatment (Renault *et al.* 2009). However, to predict if and how fast agglomeration and deagglomeration occur in turbulence is highly challenging because of the multiscale characteristics associated with both turbulent flows and the interacting modes between particles (Marshall 2009; Li *et al.* 2011; Marshall & Li 2014).

The mechanisms of agglomeration have been extensively studied. It is generally accepted that the turbulent flow first brings two initially separate particles to a sufficiently close distance, and microphysical mechanisms (collisional dissipation, hydrodynamic interactions, surface effects) then determine whether the two approaching particles can form an agglomerate. Collision kernels, expressed as the product of the mean relative radial velocity and the radial distribution function, have been proposed to predict the rate at which the flow brings separate particles into contact (Saffman & Turner 1956; Wang, Wexler & Zhou 2000). The kernel functions are further extended to reflect the influence of particle inertia, identifying the effect of preferential concentration (Squires & Eaton 1991; Saw et al. 2008; Balachandar & Eaton 2010; Tagawa et al. 2012) leading to an inhomogeneous particle distribution and sling or caustic effects (Falkovich, Fouxon & Stepanov 2002; Wilkinson, Mehlig & Bezuglyy 2006; Pumir & Wilkinson 2016) which cause inertial particles to collide with large velocity differences. Recent studies also suggest that complicated interparticle interactions, including elastic repulsion (Bec, Musacchio & Ray 2013; Voßkuhle et al. 2013), electrostatic interactions (Lu et al. 2010; Lu & Shaw 2015) and van der Waals adhesion (Kellogg et al. 2017; Chen et al. 2019a), give rise to non-trivial collision phenomenon that cannot be predicted from the ghost collision approximation, where particles can pass through each other without any modification to their trajectories.

The breakage of agglomerates, in contrast, is still far from clear. Previous studies mainly focus on shear-induced breakage. Discrete particle approach, which provides information at the particle level, has been employed to better understand the relationship between flow strain rate and the internal stress of agglomerates. For isostatic agglomerates exposed to the flow, the forces and torques on each elementary particle can be calculated assuming force and torque balances on all particles (Seto, Botet & Briesen 2011; Vanni & Gastaldi 2011; Fellay & Vanni 2012). The bond between particles instantly breaks up if the interparticle force reaches a critical value (bond strength), leading to the breakage of the isostatic agglomerate (De Bona, Lanotte & Vanni 2014; Bäbler et al. 2015). To simulate the breakage of hyperstatic agglomerates with a dense structure, soft-sphere discrete element method (DEM) is usually regarded as a powerful tool. In DEM, translational and rotational motions of all particles in an agglomerate are integrated with a sufficiently small time step so that the deformations at the contact region are resolved. Based on DEM simulations, a criterion for shear-induced breakage of hyperstatic agglomerates has been proposed, which is valid across a wide range of shear stress and interparticle adhesion values (Ruan, Chen & Li 2020).

Turbulent flows are usually considered to enhance the clustering and agglomeration of particles. However, recent work has revealed that a stronger clustering effect gives rise to a higher collision velocity, which increases the breakage rate of agglomerates (Liu & Hrenya 2018). The collision-induced breakage is important for gas—solid systems containing small but heavy particles (with high Stokes numbers). Such systems exist in the electrostatic agglomerators for the removal of fly ash particles from flue gas (Jaworek *et al.* 2018), high temperature gas-cooled nuclear reactors containing graphite aerosols in the primary loop (Wei *et al.* 2019) and fluidized beds with Geldart Group A particles (Gu, Ozel &

Sundaresan 2016). The competition between clustering and deagglomeration provides an explanation for the saturation of agglomeration levels in these gas—solid systems. To predict the kernel function for collision-induced breakage in turbulence requires one to know (i) the statistics of particle collision velocity; (ii) the particle-scale interactions (e.g. adhesions, elastic repulsions and frictions), which determine whether two colliding agglomerates will either merge into a large one, rebound from each other or break up into fragments (Dizaji, Marshall & Grant 2019). However, to our knowledge, the formulation of the breakage rate that can reflect both these two aspects is still far from perfect. Besides, it has been suggested that flow structure significantly affect the collisions of non-interacting particles (Bec *et al.* 2016; Picardo *et al.* 2019; Xiong *et al.* 2019). It is not clear how to correlate the collision-induced breakage to the structure of flows.

In this paper, we try to address the issues above by investigating the collision-induced deagglomeration of solid adhesive particles in homogeneous isotropic turbulence. An adhesive DEM is employed to fully resolve the translational and rotational motions of all particles. We first introduce how to identify various events, including sticking, rebound, collision-induced breakage and shear-induced breakage of agglomerates, in simulations. The collision-induced breakage rate is then formulated based on the Smoluchowski equations and a breakage fraction function. A universal transfer function is proposed to predict the breakage fraction function from the probability distribution of collision velocity. We also demonstrate how intense vorticity and strain contribute to the breakage of agglomerates and show how the breakage rate scales with particle size, particle number density and agglomerate size.

2. Methods

2.1. Fluid phase calculation

To investigate the collision-induced breakage of agglomerates, we consider non-Brownian solid particles suspended in an incompressible isotropic turbulent flow, which is calculated by direct numerical simulation (DNS) on a cubic, triply periodic domain with 128³ grid points. A pseudospectral method with second-order Adams–Bashforth time stepping is applied to solve the continuity and momentum equations

$$\nabla \cdot \boldsymbol{u} = 0, \tag{2.1a}$$

$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla)\mathbf{u} = -\frac{1}{\rho_f} \nabla p + \nu \nabla^2 \mathbf{u} + \mathbf{f}_F + \mathbf{f}_P. \tag{2.1b}$$

Here, \boldsymbol{u} is the fluid velocity, p is the pressure, ρ_f is the fluid density and ν is the fluid kinematic viscosity. The small wavenumber forcing term \boldsymbol{f}_F is used to maintain the turbulence with an approximately constant kinetic energy. The particle body force \boldsymbol{f}_P is calculated at each Cartesian grid node i using $\boldsymbol{f}_p(\boldsymbol{x}_i) = -\sum_{n=1}^N F_n^F \delta_h(\boldsymbol{x}_i - \boldsymbol{X}_{p,n})$. Here, \boldsymbol{x}_i is the location of grid node i, \boldsymbol{F}_n^F is the fluid force on particle n located at $\boldsymbol{X}_{p,n}$ and $\delta_h(\boldsymbol{x}_i - \boldsymbol{X}_{p,n})$ is a regularized delta function, which is given by

$$\delta_h\left(\mathbf{x}_i - X_{p,n}\right) = \begin{cases} \frac{n_{bi}}{N_g N_b}, & \text{if } \mathbf{x}_i \in \mathcal{N}^B, \\ 0, & \text{if } \mathbf{x}_i \notin \mathcal{N}^B. \end{cases}$$
(2.2)

Here, \mathcal{N}^B is the set consisting of $N_b=27$ adjoining grid cells (three in each directions) and each cell has $N_g=8$ grid nodes. The cell containing the particle locates in the centre

of the 27 cells. For a given grid node x_i , the number of cells in the set \mathcal{N}^B that contain this specific node is recorded as n_{bi} . For the nodes defining the centre cell in \mathcal{N}^B (i.e. the cell containing the particle), each of the nodes is shared by eight different cells in \mathcal{N}^B , therefore, $n_{bi} = 8$. It indicates that the eight nodes receive the same load. The summation of δ_h over all grid nodes is unity, i.e. $\sum_{x_i} \delta_h(x_i - X_{p,n}) = 1$, indicating that the choice of delta function is conservative in force.

All the parameters in our simulation have been non-dimensionalized by typical length, velocity and mass scales that are relevant to the agglomeration of microparticles. Specifically, the typical length scale is $L_0=100r_p=0.001$ m, where $r_p=10$ μ m is the particle radius. The box size for the simulation is set as $2\pi L_0$. The velocity scale is set as $U_0=10$ m s⁻¹ which is the typical value for the gas flow in a turbulent-mixing agglomerate (Jaworek *et al.* 2018). The typical mass is $M_0=\rho_f L_0^3=10^{-9}$ kg, where $\rho_f=1$ kg m⁻³ is the fluid density. The typical time scale is given by $T_0=L_0/U_0=10^{-4}$ s. Other dimensional input parameters are the fluid viscosity $\mu=1.0\times10^{-5}$ Pa s, the particle density $\rho_p=10-320$ kg m⁻³ and the particle surface energy $\gamma=0.01-5$ J m⁻². Hereinafter, all the variables appear in their dimensionless form and, for simplicity, the same notations as the dimensional variables are used. One could obtain 'physical' values of dimensionless variables by multiplying the dimensionless values with the typical scales.

2.2. Equations of motion and particle-particle interactions

A soft-sphere DEM is employed to track the dynamics of every individual particle. We integrate the linear and angular momentum equations of particles

$$m_i \dot{\boldsymbol{v}}_i = \boldsymbol{F}_i^F + \boldsymbol{F}_i^C, \tag{2.3a}$$

$$I_i \dot{\boldsymbol{\Omega}}_i = \boldsymbol{M}_i^F + \boldsymbol{M}_i^C, \tag{2.3b}$$

where m_i and I_i are mass and moment of inertia of particle i, and v_i and Ω_i are the translational velocity and the rotation rate of the particle. The forces and torques are induced by both the fluid flow $(F_i^F \text{ and } M_i^F)$ and the interparticle contact $(F_i^C \text{ and } M_i^C)$. In this work, the dominant fluid force/torque is the Stokes drag given by $F^{drag} = -3\pi\mu d_p(v-u)f$ and $M^{drag} = -\pi\mu d_p^3(\Omega-\omega/2)$, where u and ω are velocity and vorticity of the fluid, μ is the fluid viscosity and d_p is the particle diameter. Each particle in the flow is surrounded by other particles, the presence of surrounding particles will influence the drag force for any given particle. The friction factor f, given by Di Felice (1994), is used to correct for the crowding of particles. It plays a similar role as the mobility matrix used in Stokesian dynamics for calculating the hydrodynamic drag experienced by a particle inside an agglomerate (Seto et al. 2011; Vanni & Gastaldi 2011; De Bona et al. 2014). For particle Reynolds number in the range 0.01 to 10^4 , f can be written as

$$f = (1 - \phi)^{1 - \zeta}, \quad \zeta = 3.7 - 0.65 \exp\left[-\frac{1}{2} \left(1.5 - \ln Re_p\right)^2\right].$$
 (2.4)

Here, ϕ is the local particle volume fraction which is determined by the concentration blob method (Marshall & Sala 2013; Marshall & Li 2014) and Re_p is the particle Reynolds number, which is defined as $Re_p = d_p |\mathbf{v} - \mathbf{u}|/\nu$. In addition to the Stokes drag, we also include the Saffman and Magnus lift forces in F_i^F (Rubinow & Keller 1961; Saffman 1965). Added mass force is neglected here, since the current work considers small and heavy particles.

Two approaching particles interact with each other through the fluid squeeze film between them. Such near contact interaction significantly reduces the approach velocity and further influences the collision and agglomeration process. In this work, a viscous damping force derived from the classical lubrication theory is included, given by

$$F_l = -\frac{3\pi\mu r_p^2}{2h}\frac{\mathrm{d}h}{\mathrm{d}t}.$$
 (2.5)

Here, F_l is initiated at a surface separation distance $h = h_{max} = 0.01 r_p$ and a minimum value of h, $h_{min} = 2 \times 10^{-4} r_p$, is set at the instant of particle contact according to experiments (Yang & Hunt 2006; Marshall 2011). The maximum value $h_{max} = 0.01 r_p$ is selected such that the particles are close enough that the lubrication theory is valid. The value of h_{max} is assigned according to previous work on particle—wall collision (Davis, Serayssol & Hinch 1986; Marshall 2011), in which simulation results yield a good fit to the experimental data for restitution coefficient. The minimum separation distance h_{min} is set to avoid singularity. It is normally accepted that the fluid density and viscosity can increase significantly at small value of h, making the fluid within the contact region behave in a more 'solid-like' manner and limiting the value of h. Surface roughness will also impose a lower limit on the value of h (Barnocky & Davis 1988). The contact mechanics are then activated when $h < h_{min}$. Setting a small gap between contacting particles has been widely adopted in contact theories (see Israelachvili (2011) and references therein). The hydrodynamic force is then neglected when the two particles are in contact with each other since the contacting forces are normally much larger than the hydrodynamic force.

When two particles i and j are in contact at t_0 , the normal force F^N , the sliding friction F^S , the twisting torque M^T and the rolling torque M^R acting on particle i from particle j are expressed as

$$F_{ij}^{N} = F_{ij}^{NE} + F_{ij}^{ND} = -4F_{C} \left(\hat{a}_{ij}^{3} - \hat{a}_{ij}^{3/2} \right) - \eta_{N} \mathbf{v}_{ij} \cdot \mathbf{n}_{ij}, \tag{2.6a}$$

$$F_{ij}^{S} = -\min \left[k_T \int_{t_0}^{t} \boldsymbol{v}_{ij}(\tau) \cdot \boldsymbol{\xi}_{S} d\tau + \eta_T \boldsymbol{v}_{ij} \cdot \boldsymbol{\xi}_{S}, F_{ij,crit}^{S} \right], \tag{2.6b}$$

$$M_{ij}^{T} = -\min \left[\frac{k_{T}a^{2}}{2} \int_{t_{0}}^{t} \boldsymbol{\Omega}_{ij}^{T}(\tau) \cdot \boldsymbol{n}_{ij} d\tau + \frac{\eta_{T}a^{2}}{2} \boldsymbol{\Omega}_{ij}^{T} \cdot \boldsymbol{n}_{ij}, M_{ij,crit}^{T} \right], \qquad (2.6c)$$

$$M_{ij}^{R} = -\min \left[4F_{C} \hat{a}_{ij}^{3/2} \int_{t_{0}}^{t} \mathbf{v}_{ij}^{L}(\tau) \cdot \mathbf{t}_{R} \, d\tau + \eta_{R} \mathbf{v}_{ij}^{L} \cdot \mathbf{t}_{R}, \, M_{ij,crit}^{R} \right].$$
 (2.6*d*)

The normal force F_{ij}^N contains an elastic term F_{ij}^{NE} derived from the Johnson–Kendall–Roberts (Johnson, Kendall & Roberts 1971) contact theory and a damping term F_{ij}^{ND} , which is proportional to the rate of deformation. Here, F^{NE} combines the effects of van der Waals attraction and the elastic deformation and its scale is set by the critical pull-off force, $F_C = 3\pi R_{ij}\gamma$, where $R_{ij} = \left(r_{p,i}^{-1} + r_{p,j}^{-1}\right)^{-1}$ is the reduced particle radius and γ is the surface energy density of the particle. The surface energy density γ is defined as half the work required to separate two contacting surfaces per unit area.

The normal dissipation coefficient η_N in (2.6a) is given as $\eta_N = \alpha \sqrt{m^* k_N}$, where the coefficient α is a function of a prescribed value of coefficient of restitution e_0 (see Marshall 2009), $m^* = (m_i^{-1} + m_j^{-1})^{-1}$ is the effective mass of the two colliding particles and the normal elastic stiffness k_N is expressed as $k_N = (4/3)E_{ij}a_{ij}$. The tangential stiffness k_T is

expressed as $k_T = 8G_{ij}a_{ij}$ and the effective elastic modulus E_{ij} and shear modulus G_{ij} are functions of particle's Young's modulus E_i and Poisson ratio σ_i ,

$$\frac{1}{E_{ij}} = \frac{1 - \sigma_i^2}{E_i} + \frac{1 - \sigma_j^2}{E_j}, \quad \frac{1}{G_{ij}} = \frac{2 - \sigma_i}{G_i} + \frac{2 - \sigma_j}{G_j}, \tag{2.7a,b}$$

where $G_i = E_i/(2(1+\sigma_i))$ is the particle's shear modulus. The radius of contact area a_{ij} is related to the value at the zero-load equilibrium state $a_{ij,0}$ through $a_{ij} = \hat{a}_{ij}a_{ij,0}$, where $a_{ij,0}$ is given as $a_{ij,0} = (9\pi\gamma R_{ij}^2/E_{ij})^{1/3}$ and \hat{a}_{ij} is calculated inversely from the particle overlap, δ , through (Johnson *et al.* 1971; Chokshi, Tielens & Hollenbach 1993; Marshall 2009)

$$\frac{\delta}{\delta_C} = 6^{1/3} \left[2(\hat{a}_{ij})^2 - \frac{4}{3} (\hat{a}_{ij})^{1/2} \right], \tag{2.8}$$

where δ_C is the critical overlap and is given by $\delta_C = a_{ij,0}^2/(2(6)^{1/3}R_{ij})$. The contact between the particles is built up when the overlap $\delta > 0$ and is broken when $\delta < -\delta_C$. For the tangential dissipation coefficient η_T in (2.6b) and (2.6c), we simply set $\eta_T = \eta_N$ (Tsuji, Tanaka & Ishida 1992). The rolling viscous damping coefficient η_R in (2.6d) is a function of coefficient of restitution e_0 , normal elastic force F_{ij}^{NE} and the effective mass of the two colliding particles m^* , for details see Marshall (2009).

The sliding friction F^S , twisting torque M^T and rolling torque M^R ((2.6*b*)–(2.6*d*)) are all calculated based on spring–dashpot–slider models, where $v_{ij} \cdot \xi_S$, Ω^T_{ij} and v^L_{ij} are the relative sliding, twisting and rolling velocities. When these resistances reach their critical limits, namely $F^S_{ij,crit}$, $M^T_{ij,crit}$ and $M^R_{ij,crit}$, irreversible relative sliding, twisting and rolling motions will take place between a particle and its neighbouring particle. The critical limits are expressed as (Marshall 2009)

$$F_{ij,crit}^{S} = \mu_{S} F_{C} \left| 4 \left(\hat{a}_{ij}^{3} - \hat{a}_{ij}^{3/2} \right) + 2 \right|, \tag{2.9a}$$

$$M_{ij,crit}^{T} = \frac{3\pi a_{ij} F_{ij,crit}^{S}}{16},$$
(2.9b)

$$M_{ii\,crit}^R = 4F_C \hat{a}_{ii}^{3/2} \theta_{crit} R_{ij}. \tag{2.9c}$$

Here $\mu_S(=0.3)$ is the friction coefficient and $\theta_{crit}(=0.01)$ is the critical rolling angle. We set these values according to experimental measurements (Sümer & Sitti 2008). The soft-sphere DEM for adhesive particles has been successfully applied to simulations of various systems, including particle–wall collisions (Chen, Liu & Li 2019b) and deposition of particles on a fibre (Yang, Li & Yao 2013) or on a plane (Liu *et al.* 2015), and agglomeration of particles in a pressure-driven duct flow (Liu & Wu 2020), with a series of experimental and theoretical validations.

2.3. Simulation conditions

Monodisperse particles are randomly seeded into the domain after the turbulence reaching the statistically stationary state. The statistical properties of the turbulent flow is fixed. Dimensionless flow parameters include the Taylor–Reynolds number $Re_{\lambda} = 93.0$, the fluctuating velocity u' = 0.28, the dissipation rate $\epsilon = 0.0105$, the kinematic viscosity $\nu = 0.001$, the Kolmogorov length $\eta = 0.0175$, the Kolmogorov time $\tau_k = 0.31$ and the large-eddy turnover time $T_e = 7.4$. These parameters together with typical scales and particle properties are listed in table 1 in both dimensional and dimensionless forms.

Parameters	Physical value	Dimensionless value
	Typical scales	
Length, L_0	0.001 m	1
Velocity, U_0	$10 \; {\rm m s^{-1}}$	1
Time, T_0	10^{-4} s	1
Mass, M_0	10^{-9} kg	1
	Fluid properties	
Dynamic viscosity, μ	10^{-5} Pa s	_
Kinematic viscosity, v	$10^{-5} \text{ m}^2 \text{ s}^{-1}$	0.001
Taylor–Reynolds number, Re_{λ}	<u>—</u>	93.0
Fluctuating velocity, u'	$2.8 \; \mathrm{m s^{-1}}$	0.28
Dissipation rate, ϵ	$1.05 \times 10^4 \text{ m}^2 \text{ s}^{-3}$	0.0105
Kolmogorov length, η	$1.75 \times 10^{-5} \text{ m}$	0.0175
Kolmogorov time, τ_k	$3.1 \times 10^{-5} \text{ s}$	0.31
Large-eddy turnover time, T_e	$7.4 \times 10^{-4} \text{ s}$	7.4
Integral length , l_0	$1.03 \times 10^{-3} \text{ m}$	1.03
	Particle properties	
Particle number, N	4×10^{4}	_
Particle radius, r_P	$5.0-12.5 \mu m$	0.005-0.0125
Average particle volume fraction, $\bar{\phi}$	$8.4 \times 10^{-5} - 1.3 \times 10^{-3}$	_
Particle density, ρ_P	$10-320 \text{ kg m}^{-3}$	10-32
Surface energy, γ	$0.01-5 \mathrm{J}\mathrm{m}^{-2}$	0.1-50

TABLE 1. Physical and dimensionless values of the parameters in the simulation.

The solid particles are assumed to be of micrometre scale so that the interparticle adhesion due to van der Waals attraction is expected to be the dominant force. Gravity is thus neglected here. One of the most important parameters governing the clustering of particles is the Kolmogorov scale Stokes number, $St = \tau_p/\tau_k$, where $\tau_p = m/(6\pi r_p \mu)$ is the particle response time and $\tau_k = (\nu/\epsilon)^{1/2}$ is the Kolmogorov time. In the classical theory of turbulent collision of non-adhesive particles, St significantly influences the value of the collision kernel.

The turbulent flow brings separate particles together to form agglomerates in the presence of adhesion. A sufficiently high collisional impact velocity between particles, on the other hand, gives rise to the breakage of agglomerates (collision-induced breakage, see figure 1a). The adhesion parameter $Ad = \gamma/(\rho_p u^2 r_p)$, defined as the ratio of interparticle adhesion to particle's kinetic energy, is normally used to quantify the adhesion effect (Li & Marshall 2007; Marshall & Li 2014). The surface energy density γ is determined according to experimental measurements (Sümer & Sitti 2008; Krijt et al. 2013) or calculated from the Hamaker coefficients of the materials (Marshall & Li 2014). For two colliding particles, a modified adhesion number $Ad_n = \gamma/(\rho_p v_n^2 r_p)$, which is defined based on normal impact velocity v_n , is often used to predict the post-collision behaviour. The determination of Ad_n requires the information of the normal impact velocity v_n , which is usually obtained from the post-processing of the simulations. One can also adopt analytical expressions to model v_n (see Ayala, Rosa & Wang 2008; Pan & Padoan 2010) so that the value of Ad_n can be estimated before the simulations. The parameter Ad (Ad_n) has been successfully used to estimate the critical sticking velocity of two colliding particles (Chen,

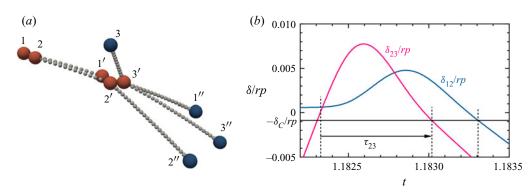


FIGURE 1. (a) Trajectories of an agglomerate (doublet) and a particle from DNS–DEM simulation. Here, 1, 2 and 3 are initial positions of the particles; 1', 2' and 3' are corresponding particles at the collision moment; 1", 2" and 3" are corresponding particles at the end of trajectories. Here, 82 000 collision time steps are used to resolve the process in panel (a), and the position of the particles at each 2000 time steps is presented by a grey sphere. (b) Evolution of the interparticle overlap, where the contacting bond between particle 2 and 3 are formed at $\delta_{23} = 0$ (indicated by the vertical dashed line on the left-hand side) and the bonds between particle 2 and 3 and particle 1 and 2 break at $\delta_{23} = -\delta_C$ and $\delta_{12} = -\delta_C$, indicated by the vertical dashed lines in the middle and on the right-hand side, respectively.

Li & Yang 2015), agglomeration efficiency of particles in turbulence (Chen *et al.* 2019*a*), the aerosol capture efficiency during fibre filtrations (Yang *et al.* 2013; Chen, Liu & Li 2016) and the packing structure of adhesive particles (Liu *et al.* 2015, 2017). In this work we systematically vary Ad (Ad_n) to show the effect of adhesion on the collision-induced breakage.

2.4. Identification of collision, rebound and breakage events

The DNS–DEM computational framework is designed with multiple-time steps (Li & Marshall 2007; Marshall 2009). The flow field is updated with a dimensionless fluid time step $\mathrm{d}t_F = 0.005$, which ensures a sufficiently small Courant number. A dimensionless particle convective time step $\mathrm{d}t_P = 2.5 \times 10^{-4}$ is adopted to update the force, velocity and position of particles that do not collide with other particles. Such a small $\mathrm{d}t_p$ ensures that the distance each particle travels during a time step is only a small fraction of the particle radius so that any possible collision events can be captured. Once a particle collides with other particles during the particle time step, we then recover its information (i.e. its force, velocity and position) to the start of the current particle time step and instead advect it with a dimensionless collision time step $\mathrm{d}t_C = 6.25 \times 10^{-6}$. The value of $\mathrm{d}t_C$ is small enough to resolve the rapid variation of the deformation within the contact region between touching particles (see figure 1b) (Marshall 2009). All processes, including particle agglomeration, breakage and rearrangement of agglomerates, therefore are automatically accounted for.

Figure 1(a) presents a typical collision-induced breakage event from the DNS-DEM simulation, where a doublet containing particles 1 (P1) and 2 (P2) collides with a third particle (P3) and then breaks into two singlets. The evolutions of interparticle overlap (scaled by the particle radius r_p) between P1 and P2 and that between P2 and P3 are shown in figure 1(b). The vertical dashed lines, from left to right, mark the moment when the contact between P2 and P3 is formed, the bond between P2 and P3 and that between

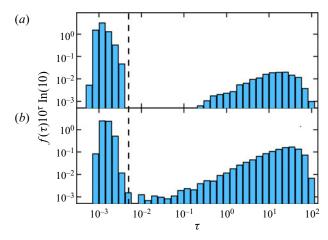


FIGURE 2. Scaled probability distribution of the contact duration τ for the interparticle bonds in two typical cases with St = 5.8 and (a) Ad = 0.64 and (b) Ad = 6.4. The vertical dashed line indicates the critical value $\tau = \tau_C = 0.005$, which separates the rebound events ($\tau < \tau_C$) and the breakage events ($\tau > \tau_C$).

P1 and P2 break. The contact duration τ of each bond thus can be calculated. For instance, τ_{23} in figure 1(*b*) indicates the contact duration between P2 and P3.

To accurately interpret the breakage mechanism and formulate the breakage rate of agglomerates in turbulence, it is of crucial importance to identify various events in the simulation, including sticking of particles upon collision, rebound, collision-induced breakage and shear-induced breakage of agglomerates. We determine all these events according to the following criteria.

- (a) If the contact duration τ between two colliding particles is smaller than a critical value τ_C , we regard it as a rebound event. In this case, there is no agglomerate formed by these two colliding particles. A rebound event normally happens when the collisional velocity is large (Dong *et al.* 2018; Fang *et al.* 2019).
- (b) If the bond between two colliding particles does not break within τ_C , we regard it as a sticking collision. An agglomerate is then formed (or grows in size) upon the collision.
- (c) When a breakage of a certain bond, whose contact duration is larger than τ_C , leads to the fragmentation of an agglomerate, we regard it as a breakage event. For each breakage case, two different breakage mechanisms are further identified: if the broken agglomerate collideds with other particles right before its breakage, we consider the breakage event as a collision-induced breakage, otherwise, the breakage event is regarded as shear-induced breakage.

To determine the value of τ_C , we plot the probability distribution of the contact duration τ for the interparticle bonds in two typical cases in double logarithmic coordinates (see figure 2). There is an obvious scale separation between the contact duration in rebound events and breakage events. In the current work, the critical value $\tau_C = 0.005$ (indicated by the vertical dashed line) was chosen to separate the rebound events ($\tau < \tau_C$) and the breakage events ($\tau > \tau_C$). The following quantities thus can be recorded in each simulation run: the number of collisions N_C ; the number of sticking events N_S ; rebound events N_R ; and breakage events N_B .

3. Results

3.1. Effect of adhesion on breakage

In figure 3(a-c), we show the temporal evolution of the number of overall collisions N_C , the number of sticking collisions N_S , rebound events N_R and breakage events N_B for St = 5.8 and three different values of adhesion parameter Ad_n , which is defined as

$$Ad_n = \frac{\gamma}{\rho_p \bar{v}_n^2 r_p},\tag{3.1}$$

where $\bar{v}_n = \sqrt{\langle v_n^2 \rangle}$ is the square root of the average value of v_n^2 over all collision events. The particles are considered to have collided at the minimum separation distance h = $h_{min} = 2 \times 10^{-4} r_p$ and the impact velocity v_n is calculated for each collision event at this moment. The values of v_n are different for different collision events and \bar{v}_n here can be regarded as an effective value to measure the kinetic energy of colliding particles. When the adhesion is extremely weak ($Ad_n = 0.73$), N_C increases linearly with time. It indicates that the collision kernel Γ almost keeps as a constant, which is consistent with previous DNS results for non-adhesive particles (Wang et al. 2000). Here, N_R is close to N_C and both N_S and N_B are nearly zero. Agglomerates therefore can barely be formed given such a weak adhesion. For the case with a relatively stronger adhesion $(Ad_n = 7.3)$, agglomeration between colliding particles can be clearly observed. However, the agglomeration at this Ad_n value is still quite limited, since the sticking probability is small (\sim 0.4). When Ad_n further increases to 70, adhesion plays a dominant role. As illustrated in figure 3(c), $N_S \approx N_C$, implying that almost all collisions lead to the agglomeration of colliding particles. Moreover, N_C no longer increases linearly with time in this case, which confirms previous results that intense agglomeration will push the system away from statistical equilibrium.

Another interesting result observed in figure 3 is that the breakage of agglomerates is not obvious when the adhesion is either too weak or too strong. When $Ad_n = 0.73$, the breakage is limited by the small number of bonds that can be formed upon collisions. In contrast, the contacting bond formed at $Ad_n = 70$ is too strong to be broken by the fluid stress or the impact of a third particle. A considerable number of breakage events can only be observed at a moderate value of Ad_n .

We normalize the number of sticking collisions N_S , rebound collisions N_R and breakage events N_B with the total number of collisions N_C and plot them against Ad_n in figure 4. Three different regimes can be identified: a rebound regime with $\hat{N}_R > 95\%$; a sticking regime with $\hat{N}_S > 95\%$; and a transient regime between the above two regimes. The critical Ad_n values dividing the three regimes are approximately 1.5 and 35. Simulation results for different St collapse, implying that the possibility of occurrence of sticking, rebound and breakage events can be well quantified by the dimensionless adhesion number Ad_n .

3.2. Formulation of breakage rate

In the current subsection, we focus on the formulation of the rate of collision-induced breakage of agglomerates. In turbulent flow laden with particles, the growth or collision-induced breakage of agglomerates results from two successive processes. First, the turbulent flow brings two initially separate agglomerates (or particles) close enough to initiate collisions. Second, the two colliding agglomerates will either merge into a large one, rebound from each other or break up into fragments.

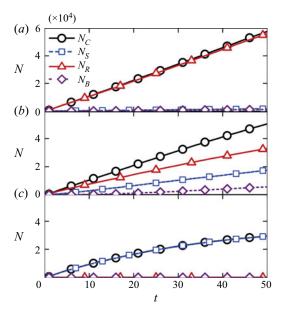


FIGURE 3. Temporal evolution of the number of collisions N_C , the number of sticking collisions N_S and rebound collisions N_R , and the number of breakage events N_B for St = 5.8 and (a) $Ad_n = 0.73$, (b) $Ad_n = 7.3$ and (c) $Ad_n = 70$.

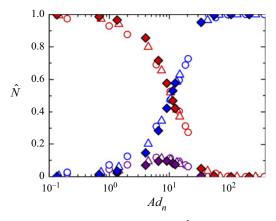


FIGURE 4. Normalized number of sticking collisions \hat{N}_S (blue), rebound collisions \hat{N}_R (red) and breakage events \hat{N}_B (purple) over the entire simulation as functions of Ad_n . Results for three different Stokes numbers are shown: circles, St = 2.9; triangles, St = 5.8; and diamonds, St = 12.

For the first step (i.e. collision), we introduce the classic statistical model of the collision rate in particle-laden turbulence. The collision rate for agglomerates of size i, $\dot{n}_C(i)$, can be expressed as

$$\dot{n}_C(i) = \sum_{j=1}^{\infty} \Gamma(i,j) n(j) n(i), \tag{3.2}$$

where $\Gamma(i,j)$ is the collision kernel between agglomerates of size i and agglomerates of size j and n(i) is the average number concentration of size group i. For homogenous isotropic turbulence, the collision kernel $\Gamma(i,j)$ has been modelled by (Zhou, Wexler & Wang 2001)

$$\Gamma(i,j) = 2\pi R_{ij}^2 \langle |w_r| \rangle g\left(R_{ij}\right), \tag{3.3}$$

The breakage rate due to the collisions with other particles or agglomerates can be expressed as the product of the collision rate $\dot{n}_C(i)$ and the fraction of collision events resulting in breakage Ψ (Kellogg *et al.* 2017) as follows:

$$f_{br}(i) = \frac{\Psi \dot{n}_C(i)}{n(i)} = \Psi \sum_{i=1}^{\infty} \Gamma(i, j) n(j).$$
 (3.4)

Here, the fraction of breakage events Ψ is defined as the ratio of the breakage number to the overall collision number and should include the influence of both turbulent transport and particle scale interactions. In prior work, a critical breakage velocity $v_{b,crit}$ was introduced, assuming that agglomerate breaks when the magnitude of the normal relative velocity v_n satisfies $v_n > v_{b,crit}$. The fraction of breakage events Ψ , therefore, can be calculated as $\Psi = \int_{v_{b,crit}}^{\infty} P_C(v_n) \, \mathrm{d}v_n$, with $P_C(v_n)$ being the probability density function (p.d.f.) of normal impact velocity (Kellogg *et al.* 2017; Liu & Hrenya 2018). Here, we introduce a new statistical framework to calculate Ψ in terms of well known impact velocity distributions $P_C(v_n)$. This formulation is expected to be more general than the previous model based on the critical breakage velocity. For collision events with impact velocity v_n , the fine-grained probability of breakage is recorded as $\psi(v_n)$. Thus, the distribution of velocity for a breakage event is given by

$$P_B(v_n) = \frac{P_C(v_n)\psi(v_n)}{\int_0^\infty P_C(v)\psi(v) \, dv},$$
(3.5)

where the denominator is the normalization coefficient. Here, $\psi(v)$ can be regarded as a transfer function, which relates the probability distribution of breakage to the impact velocity distribution.

For particles with a given adhesion value, $\psi(v_n)$ is expected to be zero as v_n tends to zero (sticking regime), and rises to unity as v_n increases, given that all colliding agglomerates

will break when the impact velocity is sufficiently large. Knowing the value of $\psi(v_n)$, one can directly obtain the fraction of breakage Ψ through

$$\Psi = \int_0^\infty P_C(v_n)\psi(v_n) \, \mathrm{d}v_n. \tag{3.6}$$

Substituting (3.6) into (3.4) further gives the breakage rate.

To validate the statistical framework above and to give a specification of the transfer function $\psi(v_n)$, we obtain the statistics of doublet breakage from DNS-DEM simulation and compare them with the theoretical descriptions in (3.4). The breakage of doublets has been widely adopted as the prototype of agglomerates that break into two fragments. For doublets, the breakage rate in (3.4) reduces to

$$f_{br}(2) = \frac{\Psi \dot{n}_C(2)}{n(2)} = \Psi \sum_{j=1}^{\infty} \Gamma(2, j) n(j).$$
 (3.7)

At the early stage of agglomeration most particles remain as singlets (Liu & Hrenya 2018; Chen *et al.* 2019*a*) and the equation above can be further simplified as

$$f_{br}(2) \approx \Psi \Gamma(1, 2) n(1) = n(1) S_{12} \Psi \Gamma(1, 1).$$
 (3.8)

On the right-hand side of the equation, we relate the singlet–doublet collision kernel $\Gamma(1,2)$ to the singlet–singlet kernel through $\Gamma(1,2) = S_{12}\Gamma(1,1)$, where the constant S_{12} is the correction for collisional cross-sectional areas for singlet–doublet collisions. Here, $\Gamma(1,1)$ for particles with different St values has been well modelled from the ghost particle approach. Although the expression in (3.8) only gives low-order statistics for the breakage of doublets, it provides valuable insights: the breakage rate scale linearly to the number concentration and the effect of turbulent transport are included in both $\Gamma(1,1)$ and the breakage fraction Ψ ; contacting interactions affects the breakage rate by changing Ψ through the transfer function $\psi(v_n)$ in (3.6).

In order to obtain the transfer function $\psi(v_n)$, we track all the collision events in the simulation and record whether the collision leads to the breakage of the agglomerate according to the criterion in § 2.4. The p.d.f. of the impact velocity $P_C(v_n)$ for singlet–doublet collision events are then measured at different St and St values (as shown in figure St and the number of singlet–doublet collision events that can be observed within a large-eddy turnover time is quite limited. We thus run three simulations with different initial random positions of particles to obtain more collision events. It ensures a good statistic on the collision velocity for singlet–doublet collision events and breakage events. For a given value of St, varying St does not obviously affect St can be observed. For collisions that result in the breakage of a doublet, we also plot the corresponding p.d.f. of the impact velocity, St in figure St can be observed. One can easily find a strong correlation between St of the impact velocity, St and St are more likely to happen with a higher impact velocity.

We then calculate the transfer function $\psi(v_n)$ inversely from $P_C(v_n)$ and $P_B(v_n)$ according to (3.5). As shown in figure 6(a), despite the inconsistency in $P_C(v_n)$, $\psi(v_n)$ for different St collapses nicely. In contrast, the adhesion strongly affects $\psi(v_n)$. Although, there is considerable scatter in the data at large v_n due to the limited sample size of the

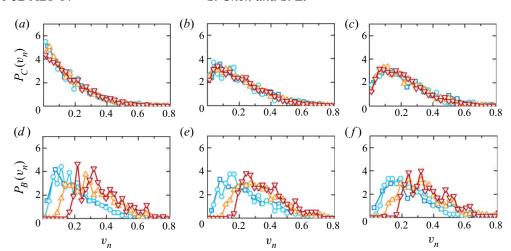


FIGURE 5. Probability density functions of the collision velocity (normal component) v_n for singlet–doublet collision events (a-c) and collision-induced breakage events (d-f). Statistics are made over approximately a large-eddy turnover time $t \in [15, 25]$. Different columns are results for different Stokes numbers: $St = 2.9 \ (a,d)$; $St = 5.8 \ (b,e)$; and $St = 12 \ (c,f)$. For each Stokes number, we show results from different Ad values: Ad = 0.64 (squares); Ad = 1.3 (circles); Ad = 6.4 (upward triangles); and Ad = 12 (downward triangles).

energetic collision events, the transfer function $\psi(v_n)$ at a given Ad value is roughly linear to the collision velocity v_n . The results in figure 6(a) suggest that the transfer function may only depend on the short-range contacting interactions, whereas the effects of turbulent transport and hydrodynamic interactions are included in the p.d.f. of the impact velocity $P_C(v_n)$. To validate the argument above, we run simulations with different particle radius (ranging from 0.0075 to 0.0125) and with/without the hydrodynamic damping force (2.5) at a fixed St value. As seen in figure 6(a), the measured transfer function $\psi(v_n)$ does not show obvious dependence on the particle size and the hydrodynamic interaction, confirming that the transformation function $\psi(v_n)$ is determined by the short-range contacting interactions.

According to the results in figure 6(a), we propose a linear relationship between ψ and v_n as follows:

$$\psi(v_n) = \begin{cases} 0, & \text{for } v_n < v_{C1}, \\ \frac{1}{v_{C2} - v_{C1}} (v_n - v_{C1}), & \text{for } v_{C1} \le v_n \le v_{C2}, \\ 1, & \text{for } v_n > v_{C2}. \end{cases}$$
(3.9)

Two typical values of collision velocity v_{C1} and v_{C2} are indicated by (3.9). Breakage does not happen when the collision velocity between two agglomerates, v_n , is smaller than v_{C1} . On the other hand, if $v_n > v_{C2}$, the colliding doublets always break. We then fit the measured values of the transfer function $\psi(v_n)$ (linear part) using (3.9) for all the cases presented in figure 6(a) and plot the fitting parameters v_{C1} and the slope $(v_{C2} - v_{C1})^{-1}$ as a function of Ad. It is seen that the fitted values of the slope for different cases centre around

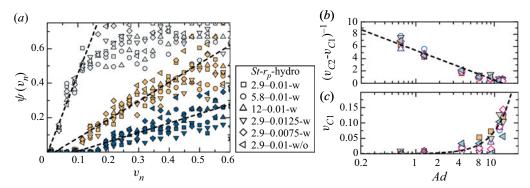


FIGURE 6. (a) Transfer function $\psi(v_n)$ versus collision velocity v_n for different Stokes numbers: St = 2.9 (squares); 5.8 (circles); and 12 (triangles). Also for different Ad values: Ad = 1.3 (light blue); 6.4 (yellow); and 12 (dark blue). Results with different particle radius (ranging from 0.0075 to 0.0125) and with/without the hydrodynamic damping force (2.5) at St = 2.9 are also included. Scatters are results calculated from p.d.f. in figure 5, and dashed lines are linear fittings from (3.9). (b and c) Fitting parameters $(v_{C2} - v_{C1})^{-1}$ and v_{C1} as functions of Ad. Legends are the same as in panel (a).

a logarithmic curve (figure 6b), which reads

$$(v_{C2} - v_{C1})^{-1} = -2.1 \ln \left(\frac{Ad}{13}\right). \tag{3.10}$$

Several interesting features are indicated by (3.10). First, the slope diverges in the small adhesion limit ($Ad \rightarrow 0$), indicating that there is a critical collision velocity separating the breakage and non-breakage collisions. This is in accordance with the theoretical model proposed by Liu & Hrenya (2018), in which a Heaviside function $H(v-v_{b,crit})$ is proposed to transform the p.d.f. of normal impact velocity $P_C(v_n)$ into the p.d.f. of impact velocity for breakage events $P_B(v_n)$. We show here that such a transfer function is reasonable only when the adhesive interaction is extremely weak. As Ad increases, the slope of $\psi(v_n)$ considerably decreases and there is no sharp transition between breakage and non-breakage collision velocities. Although the data points for the minimum breakage velocity v_{C1} are relatively dispersed when plotted as a function of Ad, a quadratic curve, $v_{C1} = aAd^2$ with $a = 7.4 \times 10^{-4}$, can roughly describe the variation of v_{C1} (see figure 6c). At large adhesion limit v_{C1} diverges, implying that all collisions give rise to the growth of agglomerates when the adhesion is sufficiently strong.

To further validate the model of the transfer function, we present an example of the model prediction for cases with St=2.9 in figure 7(a). First, the p.d.f. of the normal collision velocity $P_C(v_n)$ is measured from the simulation with small Ad value (1.3). The breakage fraction Ψ is then calculated by substituting (3.9) and the measured $P_C(v_n)$ into (3.6). One can also adopt models of $P_C(v_n)$ obtained from simulations with non-interacting particles to estimate the breakage fraction Ψ (Salazar & Collins 2012; Saw *et al.* 2014; Bhatnagar, Gustavsson & Mitra 2018). Such approximation does not bring large errors since $P_C(v_n)$ is almost independent of adhesive interactions (see figure 5). The result generated from the model together with predictions for St=1.4, 5.8 and 11.5 is plotted as a dashed line in figure 7(b). We see that the model predictions are in accordance with DNS-DEM simulations.

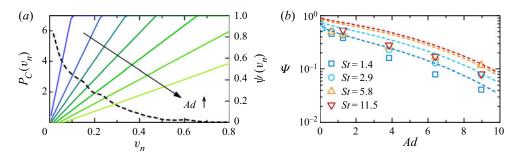


FIGURE 7. (a) Probability density functions $P_C(v_n)$ of the normal collision velocity for St=2.9 and Ad=1.3 (left-hand axis) and the transfer function $\psi(v_n)$ modelled by (3.9) (right-hand axis). Colour code spans from blue to yellow with increasing Ad (from 0.1 to 10). (b) Fraction of collision-induced breakage of doublets Ψ at different Ad values. Points are DNS-DEM results and dashed lines are results calculated from $P_C(v_n)$ and the modelled $\psi(v_n)$ (3.9).

The deviation between the model and the simulations in figure 7(b) may result from the linear assumption of the transfer function $\psi(v_n)$ (3.9), in which a sharp transition is assumed between the linear part $((v_n - v_{C1})/(v_{C2} - v_{C1}))$ and unity. The simulation data in figure 6(a), in contrast, shows a much slower approach to unity, indicating that the model in (3.9) overestimates $\psi(v_n)$ when $v_n \to v_{C2}$. Despite this deviation, our simplified model well captures the variation of breakage fraction Ψ with adhesion Ad. Moreover, the Stokes number dependence of Ψ can be observed in figure 7(b). Since the breakage fraction Ψ here is calculated from a universal transfer function, the St number dependence of Ψ originates from the difference in $P_C(v_n)$: the hydrodynamic damping force significantly reduces the relative approaching velocity of colliding particles with small St.

The collision-induced breakage rate of the doublets $f_{br}(2)$ is calculated from (3.8) and compared with DNS-DEM results in figure 8(a). Quantitative agreement is observed, indicating that the analytical model well captures the effects of the particle inertia and the adhesive interaction on the breakage. Since the adhesion parameter Ad does not include the effect of particle inertia, there is considerable distinction in results for different St at the same Ad. We stress again that particle inertia affects the breakage rate through its influence on the statistics of the collision velocity. One simple way to include both effects of particle inertia and the adhesion is to use the modified adhesion parameter Ad_n (see (3.1)), which scales the adhesion using St-dependent average velocity $\bar{v}_n = \sqrt{(v_n^2)}$. The normalized breakage rate, when plotted as a function of Ad_n , collapses nicely onto the exponential curve (see figure 8b)

$$\frac{f_{br}\tau_k}{r_p^3n(1)} = 86\exp(-0.12Ad_n). \tag{3.11}$$

The result indicates that $\bar{v}_n = \sqrt{\langle v_n^2 \rangle}$ is an appropriate choice to scale the effect of adhesion and the collision-induced breakage rate can be well estimated once Ad_n is known.

It should be noted that the model in (3.8) is valid only for early stage agglomeration, since the transfer function is derived for singlet–doublet collisions. Both agglomerate size and structure may affect the formulation of the transfer function. Predicting the breakage rate for agglomerates with arbitrary size and structures through first principles is practically impossible. It is thus normally accepted to describe the breakage rate using an exponential or a power-law function, in which the parameters are related to agglomerate

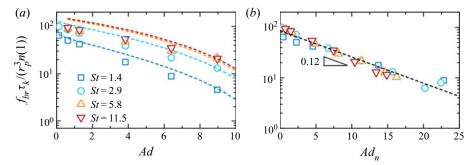


FIGURE 8. (a) Normalized breakage rate $f_{br}\tau_k/(r_p^3n(1))$ for doublets as a function of Ad. The scatters are DNS–DEM results and the dashed lines are predictions from (3.8), in which the breakage fraction Ψ is calculated from the p.d.f. of normal collision velocity through $\Psi = \int_0^\infty P_C(v_n)\psi(v_n)\,\mathrm{d}v$ (see (3.6)) and the transfer function $\psi(v_n)$ is modelled by (3.9). (b) Normalized breakage rate as a function of Ad_n . The dashed line is exponential fittings using (3.11).

size and particle–particle interactions. Agglomerate size dependence of the breakage rate will be discussed in § 3.3.

It is of great importance to know how the breakage rate scales with particle size r_p and particle number density n. We measure the doublet breakage at different particle sizes ($r_p = 0.005$ –0.015) and particle numbers (N = 19600–40000) for typical St and Ad values (shown in figure 9). The results are plotted in a scaled form: $\hat{f}_{br} = f_{br}(r_p)/f_{br}(r_{p,0})$, $\hat{r}_p = r_p/r_{p,0}$ in figure 9(a) and $\hat{f}_{br} = f_{br}(n(1))/f_{br}(n_m(1))$, $\hat{n}(1) = n(1)/n_m(1)$ in figure 9(a). Here, $f_{br}(r_{p,0})$ is the doublet breakage rate for the case with $r_{p,0} = 0.01$ and $f_{br}(n_m(1))$ is the breakage rate for the case with the maximum value of singlet number density $n_m(1)$. As displayed in figure 9, DNS–DEM results follow the power laws $\hat{f}_{br} \propto \hat{r}_p^2$ and $\hat{f}_{br} \propto \hat{n}^1(1)$ when particle size and singlet number density are varied.

The n(1) dependence is easy to understand from (3.8). The \hat{r}_p^2 scaling originates from the r_p dependence of the collision kernel $\Gamma(1,1)$ in (3.8). For inertial particles ($St \gg 1$), the approaching velocity of colliding particles is decorrelated from the local fluid gradient, thus is not affected by the particle size. The \hat{r}_p^2 scaling enters $\Gamma(1,1)$ through the effective collision area. We note that the size scaling here is valid for particles that are smaller than or comparable to the Kolmogorov scale. It may not hold for particles that are considerably larger than the Kolmogorov scale. In the latter case, particle-resolved simulations would be needed to precisely calculate the flow around and forces on particles (Ernst, Dietzel & Sommerfeld 2013; Liu & Wu 2019; Peng, Ayala & Wang 2019; Wang et al. 2019).

3.3. Agglomerate size dependence of the breakage rate

The breakage rate of agglomerates with size *A* are calculated from DNS–DEM simulations according to

$$f_{br}(A) = \frac{N_{br}(A)}{N(A)\Delta t},\tag{3.12}$$

where N(A) is the number of agglomerates of size A averaged over the time range $t \in [30, 40]$, $N_{br}(A)$ is the breakage number of agglomerates with size A and $\Delta t = 10$. As shown in figure 10(a), a stronger adhesion promotes the formation of larger agglomerates.

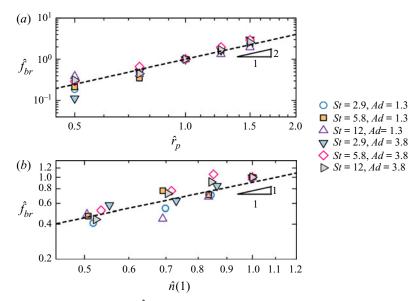


FIGURE 9. Scaled breakage rate \hat{f}_{br} as a function of (a) scaled particle size \hat{r}_p and (b) scaled number density of singlet $\hat{n}(1)$ at St = 2.9, 5.8 12 and Ad = 1.3, 3.8. Dashed lines in (a and b) indicate power law functions with exponents 2 and 1, respectively.

In contrast, the number of breakages decreases with Ad (see figure 10b). To provide meaningful statistics, we only calculate $f_{br}(A)$ when $N_{br}(A)$ is larger than 20. The results are normalized by the mean shear rate G and plotted as a function of size A in figure 10(c). It is seen that the breakage rate depends linearly on the agglomerate size with the slope being a function of Ad_n . Fitting the data at different Ad_n and St according to

$$\frac{f_{br}(A)}{G} = \zeta(St, Ad_n)A + \chi \tag{3.13}$$

gives us the values of the slope $\zeta(St, Ad_n)$. As shown in figure 10(d), when plotted as a function of Ad_n , ζ for different St centres around a universal curve, which is analogous to the f_{br} dependence in figure 8(b). The universal curve has an power-law form: $\zeta = 0.012Ad_n^{-0.81}$. These results once again confirm that the modified adhesion parameter Ad_n is an appropriate choice to reflect both effects of the particle inertia and adhesive interactions on the breakage.

3.4. Role of flow structure

In this subsection, we quantify the correlation between structures of turbulence and the breakage of agglomerates with different St and Ad values. We identify the flow structures based on the second invariant of the velocity gradient tensor $Q = (\mathcal{R}^2 - \mathcal{S}^2)/2$, where the strain rate tenor $\mathcal{S} = (\mathcal{A} + \mathcal{A}^T)/2$ and the rotation rate tensor $\mathcal{R} = (\mathcal{A} - \mathcal{A}^T)/2$ are symmetric and antisymmetric parts of the velocity gradient tensor $\mathcal{A} = \tau_k \nabla u$ (normalized by the Kolmogorov time τ_k), respectively. Figure 11(a) presents the countour plots of Q, showing the vortex tubes with $Q > 3.3\sqrt{\langle Q^2 \rangle}$ and straining sheets with $Q < -2.5\sqrt{\langle Q^2 \rangle}$, and the corresponding two-dimensional slice at y = 0. One can clearly see the red vortex

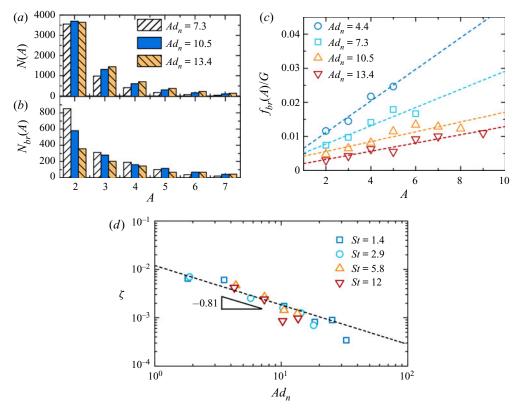


FIGURE 10. (a) Number of agglomerates of size A averaged over the time range $t \in [30, 40]$. (b) Number of breakages of agglomerates of size A measured within $t \in [30, 40]$ for St = 5.8. (c) Breakage rate, normalized by the shear rate G, as a function of agglomerate size A. The dashed lines are linear fittings from (3.13). (d) The fitting values of the slope ζ for the linear relationship between f_{br}/G and A at different Ad_n and St values. The dashed line indicates the power function $\zeta = 0.012Ad_n^{-0.81}$.

tubes surrounded by blue straining sheets (vortex-strain worm-rolls), which implies that intense structures typically occur near each other (Picardo *et al.* 2019).

We calculate the average Q, sampled by singlet–doublet collisions, at different St and Ad values in figure 11(b). The results for non-interacting particles based on ghost collision approximations are also included (Picardo $et\ al.\ 2019$) (only data at St>0.5 are shown here). One can notice that as St increases from 0.5 to 20, Q increases from a negative value to zero, implying that finite-inertia particles ($St\sim1$) tend to collide in the straining zone whereas particles with large inertia collide uniformly. According to Picardo $et\ al.\ (2019)$, decreasing St also leads to the approach to zero of Q and the largest absolute value of Q occurs at $St\approx0.3$. Such flow structure dependence is due to two aspects. First, particles with finite inertia ($St\approx1$) tend to accumulate in straining regions outside vortices due to the centrifugal effect (known as preferential concentration). Moreover, particle inertia also increases the relative approaching velocity between particles. Such an effect also prevails in straining zones (Picardo $et\ al.\ 2019$). Here, we show that varying particle–particle contacting interactions (Ad) does not obviously affect the structure dependence of collisions.

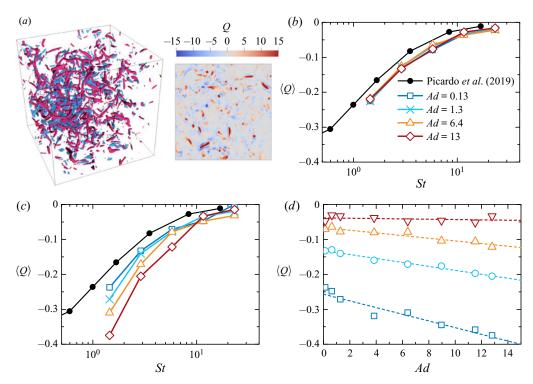


FIGURE 11. (a) Countour plot of Q and the two-dimensional slice at y=0. Vortex tubes with $Q>3.3\sqrt{\langle Q^2\rangle}$ are coloured in red and straining sheets with $Q<-2.5\sqrt{\langle Q^2\rangle}$ are coloured in blue. (b) Average Q, sampled by singlet-doublet collision events and (c) average Q sampled by doublet breakage events as functions of St. (d) Average Q for breakage events as a function of Ad at different St values: St=1.4 (squares); St=2.9 (circles); St=5.8 (upward triangles); and St=12 (downward triangles). The straight dashed lines are linear fittings.

The average Q, sampled by singlet–doublet collision-induced breakage events, shows a strong dependence on Ad (figure 11c). Doublets with larger Ad value are more difficult to break thus needing higher impact velocities. For particles with moderate inertia ($St \approx 1$), violent collisions are more likely caused by particles ejected rapidly from strong vortices and happen in straining sheets (with smaller negative Q) that envelope the vortices. As St increases, the relative velocity between colliding particles becomes less sensitive to the underlying flow, both collision events and breakage events distribute more uniformly in the flow. As shown in figure 11(d), the relationship between Q and Ad at given St can be well described by linear functions.

4. Discussion and conclusions

By means of DNS and multiple time scale DEM, we are able to resolve all the collision, rebound and breakage events for adhesive particles in turbulence. We have shown that the collision-induced breakage rate of agglomerates can be modelled based on the statistics of the collision rate and a breakage fraction function Ψ . A scaling relationship of the breakage rate for doublets at the early stage is proposed, which includes the effects of particle size, turbulent transport and particle number concentration. The fraction function Ψ is further expressed as a function of the well known distributions of impact velocity and

a universal transfer function $\psi(v_n)$, which are shown to rely on particle—particle contacting interactions and are independent of particle inertia St, particle size and hydrodynamic interactions. Based on a large number of simulations, we propose an exponential function of adhesion parameter Ad_n for the breakage rate of doublets and show that the breakage rate increases linearly as the agglomerate size increases. The framework allows one to estimate the breakage rate for early stage agglomerates of arbitrary size.

It is of great interest to compare our results with shear-induced breakage of agglomerates, which has been extensively investigated for both isostatic loose agglomerates (De Bona *et al.* 2014) and dense ones. The shear-induced breakup rate for doublets scales exponentially with a dimensionless parameter, \mathcal{N} (De Bona *et al.* 2014),

$$f_{br}^{sh} = \frac{k_f}{\tau_k} \exp(-\alpha \mathcal{N}), \tag{4.1}$$

where $\mathcal{N}=F_C/(6\pi\mu r_p^2G_{eff})$, F_C is the strength of the bond and $6\pi\mu r_p^2G_{eff}$ estimates the largest tensile stress acting on the bond by the flow field with an effective shear rate G_{eff} . Here, k_f is a prefactor of order unity and α is fitted to be 4.8 for $\mathcal{N}<0.5$ and 1.8 for $\mathcal{N}>1.5$. According to (3.11) and (4.1), the ratio between collision-induced breakage rate f_{br}^{co} and shear-induced breakage rate f_{br}^{sh} can be estimated as

$$\frac{f_{br}^{sh}}{f_{br}^{co}} \sim \phi^{-1} \frac{\exp\left(-0.25\alpha\gamma r_p^{-1}\mu^{-1}G_{eff}^{-1}\right)}{\exp(-0.12Ad_n)} = \phi^{-1} \frac{\exp\left(-0.25\alpha Ad_{sh}\right)}{\exp(-0.12Ad_n)},\tag{4.2}$$

where ϕ is the volume fraction of particles. The numerator in (4.2) is rearranged to form an adhesion parameter Ad_{sh} , which measures the relative importance of adhesion and the shear stress. The parameter Ad_{sh} has been successfully used to predict whether an agglomerate exposed to the simple shear flow will break or not (Ruan *et al.* 2020). Given the parameters in our simulation conditions, we have $f_{br}^{sh}/f_{br}^{co} \ll 1$, indicating that shear-induced breakage can be neglected in the current work. However, increasing the effective shear rate (G_{eff}) and decreasing the volume fraction (ϕ) of the particles can both magnify the relative importance of shear-induced breakage. Given (4.2), it is straightforward to determine the dominant breakage mechanism. Our results extend those of Seto *et al.* (2011), Vanni & Gastaldi (2011), Fellay & Vanni (2012), De Bona *et al.* (2014) and Bäbler *et al.* (2015), which focus on the breakage of agglomerates due to hydrodynamic stresses, forming a more complete picture of breakage in turbulent flows.

In the present work, we have also shown that for adhesive particles with moderate inertia ($St \approx 1$), the breakage events are more likely caused by particles ejected from strong vortices and happen in strain regions. It should be noted that the Reynolds number Re_{λ} currently used in the DNS-DEM simulation is fixed as 93, which is a modest value. Higher Re_{λ} results in stronger intermittency and more intense vortex and strain structures, which give rise to extremely high impact velocities. Such intense structures, however, occupy smaller volumes as Re_{λ} increases (Picardo et al. 2019). These competing effects would cause a non-monotonic variation of the breakage rate. For heavy particles with $St \ge 10$, the radial relative velocity increases with Re_{λ} since the particles carry a memory of more energetic motions as Re_{λ} increases. Such an effect is expected to increase the collision-induced breakage rate according to (3.8). Other effects, including the correlated and extreme collision events (Bec et al. 2016; Saw et al. 2016) and multifractal statistics of velocities differences (Saw et al. 2014), appear in high-Reynolds-number flows may also contribute to the breakage rate. A complete picture of agglomeration and breakage, therefore, should include the role of both the turbulent transport and particle-level interactions, which will be systematically investigated in future studies.

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Declaration of interests

The authors report no conflict of interest.

REFERENCES

- AYALA, O., ROSA, B. & WANG, L.-P. 2008 Effects of turbulence on the geometric collision rate of sedimenting droplets. Part 2. Theory and parameterization. *New J. Phys.* **10** (7), 075016.
- BÄBLER, M. U., BIFERALE, L., BRANDT, L., FEUDEL, U., GUSEVA, K., LANOTTE, A. S., MARCHIOLI, C., PICANO, F., SARDINA, G., SOLDATI, A., et al. 2015 Numerical simulations of aggregate breakup in bounded and unbounded turbulent flows. *J. Fluid Mech.* **766**, 104–128.
- BÄBLER, M. U., MORBIDELLI, M. & BAŁDYGA, J. 2008 Modelling the breakup of solid aggregates in turbulent flows. *J. Fluid Mech.* **612**, 261–289.
- BALACHANDAR, S. & EATON, J. K. 2010 Turbulent dispersed multiphase flow. *Annu. Rev. Fluid Mech.* 42, 111–133.
- BARNOCKY, G. & DAVIS, R. H. 1988 Elastohydrodynamic collision and rebound of spheres: experimental verification. *Phys. Fluids* **31** (6), 1324–1329.
- BEC, J., MUSACCHIO, S. & RAY, S. S. 2013 Sticky elastic collisions. Phys. Rev. E 87 (6), 063013.
- BEC, J., RAY, S. S., SAW, E. W. & HOMANN, H. 2016 Abrupt growth of large aggregates by correlated coalescences in turbulent flow. *Phys. Rev.* E **93** (3), 031102.
- BHATNAGAR, A., GUSTAVSSON, K. & MITRA, D. 2018 Statistics of the relative velocity of particles in turbulent flows: monodisperse particles. *Phys. Rev.* E **97** (2), 023105.
- CHANG, Q., ZHENG, C., YANG, Z., FANG, M., GAO, X., LUO, Z. & CEN, K. 2017 Electric agglomeration modes of coal-fired fly-ash particles with water droplet humidification. *Fuel* 200, 134–145.
- CHEN, S., LI, S. Q. & MARSHALL, J. S. 2019a Exponential scaling in early-stage agglomeration of adhesive particles in turbulence. Phys. Rev. Fluids 4 (2), 024304.
- CHEN, S., LI, S. Q. & YANG, M. 2015 Sticking/rebound criterion for collisions of small adhesive particles: effects of impact parameter and particle size. *Powder Technol.* **274**, 431–440.
- CHEN, S., LIU, W. & LI, S. Q. 2016 Effect of long-range electrostatic repulsion on pore clogging during microfiltration. *Phys. Rev.* E 94 (6), 063108.
- CHEN, S., LIU, W. & LI, S. 2019b A fast adhesive discrete element method for random packings of fine particles. Chem. Engng Sci. 193, 336–345.
- CHOKSHI, A., TIELENS, A. G. G. M. & HOLLENBACH, D. 1993 Dust coagulation. Astrophys. J. 407, 806–819.
- DAVIS, R. H., SERAYSSOL, J.-M. & HINCH, E. J. 1986 The elastohydrodynamic collision of two spheres. *J. Fluid Mech.* 163, 479–497.
- DE BONA, J., LANOTTE, A. S. & VANNI, M. 2014 Internal stresses and breakup of rigid isostatic aggregates in homogeneous and isotropic turbulence. *J. Fluid Mech.* **755**, 365–396.
- DI FELICE, R. 1994 The voidage function for fluid-particle interaction systems. *Intl J. Multiphase Flow* **20** (1), 153–159.
- DIZAJI, F. F., MARSHALL, J. S. & GRANT, J. R. 2019 Collision and breakup of fractal particle agglomerates in a shear flow. *J. Fluid Mech.* **862**, 592–623.
- Dong, M., Mei, Y., Li, X., Shang, Y. & Li, S. 2018 Experimental measurement of the normal coefficient of restitution of micro-particles impacting on plate surface in different humidity. *Powder Technol.* 335, 250–257.

- ERNST, M., DIETZEL, M. & SOMMERFELD, M. 2013 A lattice Boltzmann method for simulating transport and agglomeration of resolved particles. *Acta Mech.* 224 (10), 2425–2449.
- FALKOVICH, G., FOUXON, A. & STEPANOV, M. G. 2002 Acceleration of rain initiation by cloud turbulence. *Nature* **419** (6903), 151–154.
- FANG, Z., WANG, H., ZHANG, Y., WEI, M., WU, X. & SUN, L. 2019 A finite element method (FEM) study on adhesive particle-wall normal collision. *J. Aerosol Sci.* 134, 80–94.
- FELLAY, L. S. & VANNI, M. 2012 The effect of flow configuration on hydrodynamic stresses and dispersion of low density rigid aggregates. *J. Colloid Interface Sci.* 388 (1), 47–55.
- FLESCH, J. C., SPICER, P. T. & PRATSINIS, S. E. 1999 Laminar and turbulent shear-induced flocculation of fractal aggregates. *AIChE J.* **45** (5), 1114–1124.
- Gu, Y., Ozel, A. & Sundaresan, S. 2016 A modified cohesion model for CFD-DEM simulations of fluidization. *Powder Technol.* **296**, 17–28.
- HIGASHITANI, K., IIMURA, K. & SANDA, H. 2001 Simulation of deformation and breakup of large aggregates in flows of viscous fluids. *Chem. Engng Sci.* **56** (9), 2927–2938.
- IIMURA, K., SUZUKI, M., HIROTA, M. & HIGASHITANI, K. 2009 Simulation of dispersion of agglomerates in gas phase–acceleration field and impact on cylindrical obstacle. Adv. Powder Technol. 20 (2), 210–215.
- ISRAELACHVILI, J. N. 2011 Intermolecular and Surface Forces. Academic press.
- JAWOREK, A., MARCHEWICZ, A., SOBCZYK, A. T., KRUPA, A. & CZECH, T. 2018 Two-stage electrostatic precipitators for the reduction of PM2.5 particle emission. *Prog. Energy Combust. Sci.* 67, 206–233.
- JIANG, Q. & LOGAN, B. E. 1991 Fractal dimensions of aggregates determined from steady-state size distributions. Environ. Sci. Technol. 25 (12), 2031–2038.
- JOHNSON, K. L., KENDALL, K. & ROBERTS, A. D. 1971 Surface energy and the contact of elastic solids. *Proc. R. Soc. Lond.* A **324** (1558), 301–313.
- JONES, T. B. 2005 Electromechanics of Particles. Cambridge University Press.
- Kellogg, K. M., Liu, P., Lamarche, C. Q. & Hrenya, C. M. 2017 Continuum theory for rapid cohesive-particle flows: general balance equations and discrete-element-method-based closure of cohesion-specific quantities. *J. Fluid Mech.* 832, 345–382.
- KRIJT, S., GÜTTLER, C., HEISSELMANN, D., DOMINIK, C. & TIELENS, A. G. G. M. 2013 Energy dissipation in head-on collisions of spheres. *J. Phys. D: Appl. Phys.* 46 (43), 435303.
- LI, S. Q. & MARSHALL, J. S. 2007 Discrete element simulation of micro-particle deposition on a cylindrical fiber in an array. *J. Aerosol Sci.* 38 (10), 1031–1046.
- LI, S. Q., MARSHALL, J. S., LIU, G. & YAO, Q. 2011 Adhesive particulate flow: the discrete-element method and its application in energy and environmental engineering. *Prog. Energy Combust. Sci.* 37 (6), 633–668.
- LIU, P. & HRENYA, C. M. 2018 Cluster-induced deagglomeration in dilute gravity-driven gas—solid flows of cohesive grains. *Phys. Rev. Lett.* **121** (23), 238001.
- LIU, W., JIN, Y., CHEN, S., MAKSE, H. A. & LI, S. Q. 2017 Equation of state for random sphere packings with arbitrary adhesion and friction. *Soft Matt.* 13 (2), 421–427.
- LIU, W., LI, S. Q., BAULE, A. & MAKSE, H. A. 2015 Adhesive loose packings of small dry particles. Soft Matt. 11 (32), 6492–6498.
- LIU, W. & WU, C. Y. 2019 Analysis of inertial migration of neutrally buoyant particle suspensions in a planar Poiseuille flow with a coupled lattice Boltzmann method-discrete element method. *Phys. Fluids* 31 (6), 063301.
- LIU, W. & WU, C.-Y. 2020 Migration and agglomeration of adhesive micro-particle suspensions in a pressure-driven duct flow. *AIChE J.* **66** (6), e16974.
- LU, J., NORDSIEK, H., SAW, E. W. & SHAW, R. A. 2010 Clustering of charged inertial particles in turbulence. *Phys. Rev. Lett.* **104** (18), 184505.
- LU, J. & SHAW, R. A. 2015 Charged particle dynamics in turbulence: theory and direct numerical simulations. *Phys. Fluids* **27** (6), 065111.
- MARSHALL, J. S. 2009 Discrete-element modeling of particulate aerosol flows. *J. Comput. Phys.* **228** (5), 1541–1561.

- MARSHALL, J. S. 2011 Viscous damping force during head-on collision of two spherical particles. *Phys. Fluids* **23** (1), 013305.
- MARSHALL, J. S. & LI, S. Q. 2014 Adhesive Particle Flow. Cambridge University Press.
- MARSHALL, J. S. & SALA, K. 2013 Comparison of methods for computing the concentration field of a particulate flow. *Intl J. Multiphase Flow* **56**, 4–14.
- PAN, L. & PADOAN, P. 2010 Relative velocity of inertial particles in turbulent flows. *J. Fluid Mech.* **661**, 73–107.
- PENG, C., AYALA, O. M. & WANG, L. P. 2019 A direct numerical investigation of two-way interactions in a particle-laden turbulent channel flow. *J. Fluid Mech.* 875, 1096–1144.
- PICARDO, J. R., AGASTHYA, L., GOVINDARAJAN, R. & RAY, S. S. 2019 Flow structures govern particle collisions in turbulence. *Phys. Rev. Fluids* 4 (3), 032601.
- PUMIR, A. & WILKINSON, M. 2016 Collisional aggregation due to turbulence. *Annu. Rev. Condens. Matter Phys.* 7, 141–170.
- RENAULT, F., SANCEY, B., CHARLES, J., MORIN-CRINI, N., BADOT, P. M., WINTERTON, P. & CRINI, G. 2009 Chitosan flocculation of cardboard-mill secondary biological wastewater. *Chem. Engng J.* **155** (3), 775–783.
- ROYER, J. R., EVANS, D. J., OYARTE, L., GUO, Q., KAPIT, E., MÖBIUS, M. E., WAITUKAITIS, S. R. & JAEGER, H. M. 2009 High-speed tracking of rupture and clustering in freely falling granular streams. *Nature* **459** (7250), 1110–1113.
- RUAN, X., CHEN, S. & LI, S. Q. 2020 Structural evolution and breakage of dense agglomerates in shear flow and Taylor–Green vortex. *Chem. Engng Sci.* 211, 115261.
- RUBINOW, S. I. & KELLER, J. B. 1961 The transverse force on a spinning sphere moving in a viscous fluid. *J. Fluid Mech.* 11 (3), 447–459.
- SAFFMAN, P. G. 1965 The lift on a small sphere in a slow shear flow. J. Fluid Mech. 22 (2), 385-400.
- SAFFMAN, P. G. & TURNER, J. S. 1956 On the collision of drops in turbulent clouds. *J. Fluid Mech.* 1 (1), 16–30.
- SALAZAR, J. P. L. C. & COLLINS, L. R. 2012 Inertial particle relative velocity statistics in homogeneous isotropic turbulence. *J. Fluid Mech.* **696**, 45–66.
- SAW, E. W., BEWLEY, G. P., BODENSCHATZ, E., RAY, S. S. & BEC, J. 2014 Extreme fluctuations of the relative velocities between droplets in turbulent airflow. *Phys. Fluids* **26** (11), 111702.
- SAW, E. W., KUZZAY, D., FARANDA, D., GUITTONNEAU, A., DAVIAUD, F., WIERTEL-GASQUET, C., PADILLA, V. & DUBRULLE, B. 2016 Experimental characterization of extreme events of inertial dissipation in a turbulent swirling flow. *Nat. Commun.* 7, 12466.
- SAW, E. W., SHAW, R. A., AYYALASOMAYAJULA, S., CHUANG, P. Y. & GYLFASON, A. 2008 Inertial clustering of particles in high-Reynolds-number turbulence. *Phys. Rev. Lett.* **100** (21), 214501.
- SETO, R., BOTET, R. & BRIESEN, H. 2011 Hydrodynamic stress on small colloidal aggregates in shear flow using Stokesian dynamics. *Phys. Rev.* E **84** (4), 041405.
- SQUIRES, K. D. & EATON, J. K. 1991 Preferential concentration of particles by turbulence. *Phys. Fluids A: Fluid Dyn.* **3** (5), 1169–1178.
- STEINPILZ, T., JOERIS, K., JUNGMANN, F., WOLF, D., BRENDEL, L., TEISER, J., SHINBROT, T. & WURM, G. 2020 Electrical charging overcomes the bouncing barrier in planet formation. *Nat. Phys.* **16**, 225–229.
- SÜMER, B. & SITTI, M. 2008 Rolling and spinning friction characterization of fine particles using lateral force microscopy based contact pushing. *J. Adhes. Sci. Technol.* **22** (5–6), 481–506.
- SUNDARAM, S. & COLLINS, L. R. 1997 Collision statistics in an isotropic particle-laden turbulent suspension. Part 1. Direct numerical simulations. *J. Fluid Mech.* **335**, 75–109.
- TAGAWA, Y., MERCADO, J. M., PRAKASH, V. N., CALZAVARINI, E., SUN, C. & LOHSE, D. 2012 Three-dimensional Lagrangian Voronoï analysis for clustering of particles and bubbles in turbulence. *J. Fluid Mech.* **693**, 201–215.
- TSUJI, Y., TANAKA, T. & ISHIDA, T. 1992 Lagrangian numerical simulation of plug flow of cohesionless particles in a horizontal pipe. *Powder Technol.* 71 (3), 239–250.
- VANNI, M. & GASTALDI, A. 2011 Hydrodynamic forces and critical stresses in low-density aggregates under shear flow. *Langmuir* 27 (21), 12822–12833.

- VOSSKUHLE, M., LÉVÊQUE, E., WILKINSON, M. & PUMIR, A. 2013 Multiple collisions in turbulent flows. *Phys. Rev.* E **88** (6), 063008.
- Voss, A. & Finlay, W. H. 2002 Deagglomeration of dry powder pharmaceutical aerosols. *Intl J. Pharm.* **248** (1–2), 39–50.
- WANG, G., WAN, D., PENG, C., LIU, K. & WANG, L. P. 2019 LBM study of aggregation of monosized spherical particles in homogeneous isotropic turbulence. *Chem. Engng Sci.* 201, 201–211.
- WANG, L. P., WEXLER, A. S. & ZHOU, Y. 2000 Statistical mechanical description and modelling of turbulent collision of inertial particles. *J. Fluid Mech.* 415, 117–153.
- WEI, M., ZHANG, Y., FANG, Z., WU, X. & SUN, L. 2019 Graphite aerosol release to the containment in a water ingress accident of high temperature gas-cooled reactor (HTGR). *Nucl. Engng Des.* 342, 170–175.
- WILKINSON, M., MEHLIG, B. & BEZUGLYY, V. 2006 Caustic activation of rain showers. *Phys. Rev. Lett.* **97** (4), 048501.
- XIONG, Y., LI, J., FEI, F., LIU, Z. & LUO, W. 2019 Influence of coherent vortex structures in subgrid scale motions on particle statistics in homogeneous isotropic turbulence. *Intl J. Multiphase Flow* 113, 358–370.
- YANG, F. L. & HUNT, M. L. 2006 Dynamics of particle–particle collisions in a viscous liquid. *Phys. Fluids* **18** (12), 121506.
- YANG, M., LI, S. Q. & YAO, Q. 2013 Mechanistic studies of initial deposition of fine adhesive particles on a fiber using discrete-element methods. *Powder Technol.* **248**, 44–53.
- ZHOU, Y., WEXLER, A. S. & WANG, L. P. 2001 Modelling turbulent collision of bidisperse inertial particles. *J. Fluid Mech.* **433**, 77–104.