

Effective boundary conditions for dynamic contact angle hysteresis on chemically inhomogeneous surfaces

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(Received 17 May 2021; revised 18 November 2021; accepted 23 December 2021)

Recent experiments (Guan *et al.*, *Phys. Rev. Lett.*, vol. 116, issue 6, 2016*a*, p. 066102; Guan *et al.*, *Phys. Rev. E*, vol. 94, issue 4, 2016*b*, p. 042802) showed many interesting phenomena on dynamic contact angle hysteresis while there is still a lack of complete theoretical interpretation. In this work, we study the time averaging of the apparent advancing and receding contact angles on surfaces with periodic chemical patterns. We first derive a new Cox-type boundary condition for the apparent dynamic contact angle on homogeneous surfaces using the Onsager variational principle. Based on this condition, we propose a reduced model for some typical moving contact line problems on chemically inhomogeneous surfaces in two dimensions. Multiscale expansion and averaging techniques are employed to approximate the model for asymptotically small chemical patterns. We obtain a quantitative formula for the averaged dynamic contact angles. It describes explicitly how the advancing and receding contact angles depend on the velocity and the chemical inhomogeneity of the substrate. The formula is a coarse-graining version of the Cox-type boundary condition on inhomogeneous surfaces. Numerical simulations are presented to validate the analytical results. The numerical results also show that the formula characterizes well the complicated behaviour of dynamic contact angle hysteresis observed in the experiments.

Key words: contact lines, wetting and wicking

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1. Introduction

Wetting is a fundamental process in nature and our daily life (de Gennes 1985; Bonn *et al.* 2009). It is of critical importance in many industrial applications, e.g. coating, printing, chemical engineering, oil industry, etc. The wetting property is mainly characterized by the contact angle between the liquid–vapour interface and the solid surface. When a liquid drop is in equilibrium on a homogeneous smooth surface, the contact angle is described by the famous Young’s equation (Young 1805). The equilibrium contact angle, also named Young’s angle, depends on the surface tensions and reflects the material properties of the substrate. However, the real surface is usually neither homogeneous nor smooth and the chemical and geometric inhomogeneity may affect the wetting property dramatically. This makes the wetting phenomena very complicated in real applications, especially for dynamic problems.

For a liquid drop on an inhomogeneous surface, the apparent contact angle is usually different from the microscopic contact angle near the contact line even in equilibrium state. The equilibrium state of a droplet is determined by minimizing the total free energy of the system. When a global minimum is obtained, the apparent contact angle of a liquid can be described either by the Wenzel equation (Wenzel 1936) or by the Cassie–Baxter equation (Cassie & Baxter 1944). In reality, there exist many local minimizers that cannot be described by the two equations (cf. Gao & McCarthy 2007; Marmur & Bittoun 2009). One can observe many equilibrium contact angles in experiments. The largest contact angle is called the advancing contact angle and the smallest one is the receding contact angle. The difference between the advancing and the receding angles is usually referred to the (static) contact angle hysteresis (CAH).

The static CAH has been studied a lot in the literature (see e.g. Johnson & Dettre 1964; Neumann & Good 1972; Cox 1983; Joanny & De Gennes 1984; Schwartz & Garoff 1985; Extrand 2002; Priest, Sedev & Ralston 2007; Whyman, Bormashenko & Stein 2008 among many others). For a two-dimensional problem, the contact line is reduced to a point. When the surface is chemically composed of two or more materials with different Young’s angles, it is found that the advancing contact angle is equal to the largest Young’s angle in the system and the receding contact angle equals the smallest Young’s angle (see Johnson & Dettre 1964; Xu & Wang 2011). For a three-dimensional problem, the situation becomes more complicated. The CAH due to a single defect on a homogeneous solid surface was analysed in Joanny & De Gennes (1984). The analysis can be generalized to surfaces with dilute defects. Recently, some modified Wenzel and Cassie equations have been proposed to characterize quantitatively the local equilibrium contact angle and the CAH in Choi *et al.* (2009), Raj *et al.* (2012), Xu & Wang (2013) and Xu (2016). By these equations, the apparent contact angle can be computed once the position of the contact line is given. However, since the actual position of a contact line usually depends on the dynamic process (see Iliev, Pesheva & Iliev 2018), we need study the dynamic wetting problem for real applications.

Dynamic wetting is much more challenging than the static case due to the motion of the contact line, which is still an unsolved problem in fluid dynamics (see Pismen 2002; Blake 2006; Snoeijer & Andreotti 2013; Sui, Ding & Spelt 2014). The standard no-slip boundary condition may lead to a non-physical non-integrable stress in the vicinity of the contact line (Huh & Scriven 1971; Dussan 1979). To cure this paradox, many models were developed. A natural way is to explicitly adopt the Navier slip boundary condition instead of the no-slip condition (Huh & Scriven 1971; Zhou & Sheng 1990; Haley & Miksis 1991; Spelt 2005; Ren & E 2007) or implicitly impose the slip effect by numerical methods (Renardy, Renardy & Li 2001; Marmottant & Villermaux 2004). Some other

approaches include: to assume a precursor thin film and a disjoining pressure (Schwartz & Eley 1998; Pismen & Pomeau 2000; Eggers 2005); to introduce a new thermodynamics for surfaces (Shikhmurzaev 1993); to treat the moving contact line as a thermally activated process (Blake 2006; Seveno *et al.* 2009; Blake & De Coninck 2011); to use a diffuse interface model for moving contact lines (Gurtin, Polignone & Vinals 1996; Seppelcher 1996; Jacqmin 2000; Qian, Wang & Sheng 2003; Yue & Feng 2011), etc. Most of these models can be regarded as microscopic models for moving contact lines, due to the existence of very small parameters, e.g. the slip length and the diffuse interface thickness, etc. It is very expensive to use them in quantitative numerical simulations for dynamic wetting problems, unless the characteristic size of the problem is very small (Gao & Wang 2012; Sui *et al.* 2014).

To simulate the macroscopic wetting problems efficiently, various effective models have been proposed. One important model is the so-called Cox model developed in Cox (1986) for viscous flows. The relation between the (macroscopic) apparent contact angle and the contact line velocity (characterized by the capillary number) is derived by matched expansions and asymptotic analysis. The model was further validated and developed in Sui & Spelt (2013*b*) and Sibley, Nold & Kalliadasis (2015*a*) and generalized in Ren, Trinh & E (2015) and Zhang & Ren (2019) for distinguished limits in different time regimes. In real simulations, one can use the macroscopic model directly and there is no need to resolve the microscopic slip region in the vicinity of the contact line. This improves significantly the efficiency of the numerical methods and makes it possible to quantitatively simulate some macroscopic moving contact line problems (Sui & Spelt 2013*a*).

To study the dynamic CAH, one needs to consider the moving contact line problems on (either geometrically or chemically) inhomogeneous surfaces. The problem has been studied theoretically in Raphael & de Gennes (1989) and Joanny & Robbins (1990) for the single defect case. For the moving contact line problems with chemically patterned substrates, theoretical study is more difficult. Direct numerical simulations in two dimensions have been done in Wang, Qian & Sheng (2008) and Ren & E (2011). In these simulations, they adopted some standard microscopic moving contact line models where the inhomogeneity of the substrates are described explicitly in the boundary conditions. The stick-slip behaviour of the contact lines was observed. The CAH was also observed when the period of the chemical pattern is small. The main challenge in direct simulations is that the computational complexity is very large in order to resolve the microscopic inhomogeneity. Besides direct simulations, more studies were done by using phenomenological CAH models (Dupont & Legendre 2010; Yue 2020; Zhang & Yue 2020), where the advancing and receding contact angles were given *a priori* and the contact line cannot move unless the dynamic contact angle was beyond the interval bounded by the two angles. The advancing and receding contact angles in these models are effective parameters. In general, it is not clear how the parameters are related to the chemical inhomogeneity of the substrates.

More recently, some experimental results on the dynamic CAH were presented in Guan *et al.* (2016*a,b*). They showed many interesting properties on the dynamic advancing and receding contact angles. Both the advancing and receding contact angles can change with the increase of the contact line velocity. The dependence of the contact angles on the velocity is quite complicated. Sometimes it seems symmetric while it can be very asymmetric in other cases. The asymmetric dependence is partially understood from the distributions of the chemical patterns (see Xu, Zhao & Wang 2019; Xu & Wang 2020). But there is still a lack of complete understanding of all the experimental results.

The motivation of the work is twofold. Firstly, we would like to develop an averaged Cox-type boundary condition for moving contact lines on inhomogeneous surfaces. The boundary condition characterizes quantitatively how the macroscopic advancing and receding angles depend on the microscopic inhomogeneity of the substrates. With this condition, a macroscopic model may be developed for dynamic CAH. Secondly, we would also like to have more theoretical understanding of the complicated phenomena of dynamic CAH in recent experiments in Guan *et al.* (2016*a,b*).

For these purposes, we conduct our study in two steps. First, we derive a simplified Cox-type boundary condition for moving contact lines on general surfaces. The main tool here is to use the Onsager variational principle as an approximation tool. Recent studies showed that it is very useful for approximately modelling many complicated problems in viscous fluids and in soft matter (cf. Doi 2015; Di, Xu & Doi 2016; Man & Doi 2016; Xu, Di & Doi 2016; Zhou & Doi 2018; Doi *et al.* 2019; Guo *et al.* 2019; Xu & Wang 2020). In this paper, we show that the principle can be used to derive a full sharp-interface model and a new simplified Cox-type boundary condition for moving contact lines. Without considering the contact line friction, the boundary condition is a first-order approximation for the original Cox's condition. With the condition, we can construct a reduced model for some interesting moving contact line problems, including the one for the experiments in Guan *et al.* (2016*a,b*). Second, we conduct an asymptotic analysis for the reduced model on chemically inhomogeneous substrates. By multiscale expansions, we derive an averaged dynamics for the contact angle and the contact point. This leads to an explicit formula for the averaged (in time) macroscopic dynamic contact angle on chemically inhomogeneous surfaces. The formula is a coarse-graining boundary condition for dynamic CAH. Our analysis is validated by numerical experiments. Furthermore, numerical examples show that the reduced model and the new boundary conditions can be used to understand the complicated behaviours of the apparent contact angles observed in the experiments in Guan *et al.* (2016*a,b*). All the main phenomena can be captured by the reduced model and described by the averaged formula.

Although the averaging analysis is conducted for a reduced model in the paper, the averaged boundary condition for dynamic CAH is quite general, since it does not depend on the specific set-up of the problem at all. The condition is a form of harmonic average of the simplified Cox-type boundary condition. The main result can also be generalized to the case where the original Cox's boundary condition applies. We expect that the formulae for the averaged macroscopic dynamic contact angles can be used as an effective boundary condition for the two-phase Navier–Stokes equation for moving contact lines on inhomogeneous surfaces. Although the analysis in this paper is restricted to two-dimensional problems, the main results can be used to understand some three-dimensional CAH problems, e.g. on an inhomogeneous surface with dilute defects. Nevertheless, quantitative descriptions for general three-dimensional problems are still challenging and will be left for future study.

The structure of the paper is as follows. In § 2, we introduce the derivations for a Cox-type boundary condition for moving contact lines in a variational approach. A reduced model is presented for some specific problems. In § 3, we do asymptotic analysis for the reduced model to derive the averaged dynamics on chemically inhomogeneous surfaces. Explicit formulae for the apparent dynamic contact angles are derived. In § 4, we discuss the generalization of our result to some other models. In § 5, we validate the asymptotic analysis numerically and make comparisons with experiments. Finally, we give some concluding remarks in § 6.

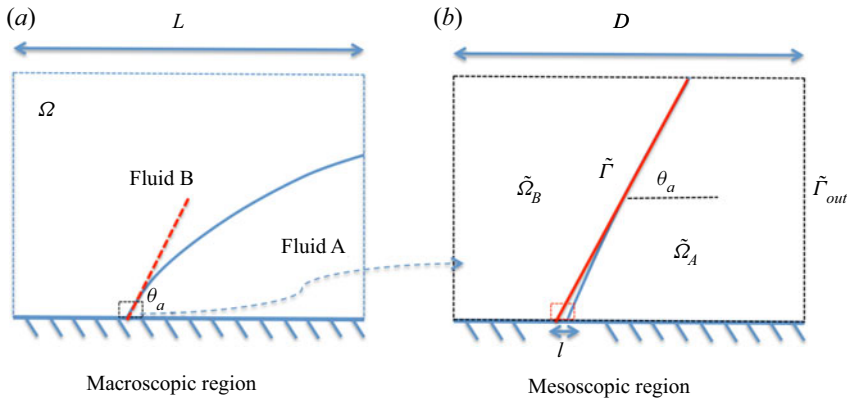


Figure 1. The region near the moving contact point in different scalings ($l \ll D \ll L$).

2. Variational derivation for moving contact line models

In this section, we will derive a Cox-type boundary condition by a variational approach, which describes the dynamics of the apparent contact angle. The Cox-type boundary condition is employed to further reduce the model for two typical problems with moving contact lines. The reduced model acts as a model problem to study the dynamic CAH in the following sections.

2.1. Derivation of a Cox type model for the apparent contact angle

It is known that the two-phase flow has a multiscale property near moving contact lines. In general, the macroscopic contact angle is different from the microscopic one; see for example Cox (1986), where a dynamic boundary condition for the apparent contact angle was derived by matched asymptotic analysis. In the following, we derive a similar boundary condition by using the Onsager principle as an approximation tool. The derivation is much simpler but still captures the essential dynamics of the apparent contact angle. In Appendix A, we show that the variational principle can also be used to derive a full continuum model for moving contact lines.

As shown in figure 1, we separate the domain near the contact line into three different scales. The macroscopic region Ω has a characteristic length L . The microscopic region is of molecular scale with a characteristic length l . In the microscopic scale, the interaction between the liquid molecules and the solid molecules induces a friction of the contact line (Guo *et al.* 2013). The mesoscopic region has a characteristic length $D \ll L$, but still much larger than the molecular scale l . In this region, the no-slip boundary condition is still a good approximation. The contact angle θ_a represents the apparent angle in macroscopic point of view.

We are interested in the contact line dynamics in the mesoscopic region. For this purpose, we analyse the system by using the Onsager principle as an approximation tool. We make the ansatz that the interface between the two fluids in this region can be approximated well by a straight line $\tilde{\Gamma}$ which has a tilting angle equal to the macroscopic contact angle θ_a . With this assumption, we can use the Onsager principle to derive a relation between the apparent contact angle θ_a and the contact line motion as follows.

We first calculate the rate of change in the total free energy of the system. Similar to (A1), the total approximate free energy $\tilde{\mathcal{E}}$ is composed of three surface energies. The changing rate of the total interface energies with respect to the motion of the contact line

is given by

$$\dot{\tilde{\mathcal{E}}} = \gamma (\cos \theta_a - \cos \theta_Y) v_{ct} + \int_{\tilde{\Gamma}} \gamma \kappa v_n ds = \gamma (\cos \theta_a - \cos \theta_Y) v_{ct}. \quad (2.1)$$

Here γ is the fluid–fluid surface tension, v_{ct} is the contact line velocity, θ_Y is the Young’s angle, κ and v_n are respectively the curvature and the normal velocity of the fluid–fluid interface; the second term disappears since the curvature is zero for a straight line. To use the Onsager principle for the open system, we need consider the work to the exterior region on the outer boundary, $\dot{\tilde{\mathcal{E}}}^* = - \int_{\tilde{\Gamma}_{out}} \mathbf{F}_{ext} \cdot \mathbf{v}$, with \mathbf{F}_{ext} being the external force.

This is a higher-order term in comparison with $\dot{\tilde{\mathcal{E}}}$, since it is of order $|\mathbf{F}_{ext}|v_{ct}D$ with $D \ll L = O(1)$. We will ignore this term in the following calculations.

We now compute the energy dissipations in the wedge region as shown in figure 1 (right plot). The total energy dissipation is calculated approximately as

$$\tilde{\Psi} = \xi v_{ct}^2 + \int_{\tilde{\Omega}_A} \frac{\mu_A}{4} |\nabla \mathbf{v} + \nabla \mathbf{v}^T|^2 dx + \int_{\tilde{\Omega}_B} \frac{\mu_B}{4} |\nabla \mathbf{v} + \nabla \mathbf{v}^T|^2 dx, \quad (2.2)$$

In the above formula, $\tilde{\Omega}_A$ and $\tilde{\Omega}_B$ are the domains corresponding to liquids *A* and *B* in the mesoscopic region, μ_A and μ_B are respectively the viscosities of fluids *A* and *B*, and the superscript T stands for the transpose of a matrix. The contact line friction term ξv_{ct}^2 is due to the dissipation in the microscopic region and ξ is the friction coefficient. The velocity \mathbf{v} can be obtained by solving the Stokes equations in wedge regions assuming the interface moving in a steady state. By careful calculations (see Appendix A), we can compute the energy dissipation function approximately

$$\tilde{\Phi} = \frac{1}{2} \tilde{\Psi} \approx \frac{1}{2} \xi v_{ct}^2 + \frac{\mu_A |\ln \zeta|}{2\mathcal{F}(\theta_a, \lambda)} v_{ct}^2, \quad (2.3)$$

where the dimensionless parameter $\zeta = D/l$ is the ratio between the mesoscopic size and the microscopic size, and

$\mathcal{F}(\theta_a, \lambda)$

$$= \frac{\lambda(\theta_a^2 - \sin^2 \theta_a)(\pi - \theta_a + \sin \theta_a \cos \theta_a) + ((\pi - \theta_a)^2 - \sin^2 \theta_a)(\theta_a - \sin \theta_a \cos \theta_a)}{2 \sin^2 \theta_a (\lambda^2(\theta_a^2 - \sin^2 \theta_a) + 2\lambda(\sin^2 \theta_a + \theta_a(\pi - \theta_a)) + ((\pi - \theta_a)^2 - \sin^2 \theta_a))}, \quad (2.4)$$

with $\lambda = \mu_B/\mu_A$. The contact line friction can be understood from the molecular kinetics theory (Blake & Haynes 1969; Blake 2006; Blake & De Coninck 2011). Molecular dynamic simulations have been done in Johansson & Hess (2018) to compute the friction coefficient. For a water–air interface on a clean glass substrate, the coefficient ξ is measured directly in experiments in Guo *et al.* (2013), which is given by $\xi \approx (0.8 \pm 0.2)\mu$. Notice that $\ln \zeta$ is generally chosen as a constant of order 10 (in de Gennes, Brochard-Wyart & Quere (2003), it is chosen as 13.6). Direct computations also show that $1/\mathcal{F}(\theta_a, \lambda) = O(1)$. In this case, ξ can be regarded a small perturbation to the viscous friction coefficient and can be ignored. More detailed discussions on the contact line friction can be found in Duvivier, Blake & De Coninck (2013). It is found that the friction coefficient ξ is proportional to the viscosity of the liquid and exponentially dependent on the strength of solid–liquid interactions. The value of ξ can range over several magnitudes for various systems.

By using the Onsager principle, we minimize the Rayleighian $\mathcal{R} = \tilde{\Phi} + \dot{\tilde{\mathcal{E}}}$ with respect to v_{ct} . This leads to an equation for v_{ct}

$$\left(\xi + \frac{\mu_A |\ln \zeta|}{\mathcal{F}(\theta_a, \lambda)} \right) v_{ct} = -\gamma (\cos \theta_a - \cos \theta_Y). \tag{2.5}$$

This equation basically means that the local dissipative force (due to the contact line friction and the viscous dissipation) is balanced by the effective unbalanced Young’s force, which is the dominant term in the driving force in the mesoscopic region. It gives a relation between the contact line velocity and the apparent contact angle θ_a . The relation (2.5) can be rewritten in a dimensionless form

$$\left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}(\theta_a, \lambda)} \right) Ca = -(\cos \theta_a - \cos \theta_Y), \tag{2.6}$$

where $\alpha = \xi/\mu_A$ and $Ca = \mu_A v_{ct}/\gamma$ is the capillary number. The equation takes into account both the viscous friction in the mesoscopic region and the microscopic friction in the vicinity of the contact line.

When the contact line friction is less important than the viscous dissipation, the first term in (2.6) can be ignored. Then the equation is reduced to

$$|\ln \zeta| Ca = -\mathcal{F}(\theta_a, \lambda) (\cos \theta_a - \cos \theta_Y). \tag{2.7}$$

This is a Cox-type formula for the apparent contact angle and the capillary number of the contact line. Equation (2.7) is consistent with Cox’s formula at leading order when Ca is small. This will be discussed as follows. We recall Cox’s formula for small Ca

$$|\ln \zeta| Ca = \mathcal{K}(\theta_a, \lambda) - \mathcal{K}(\theta_Y, \lambda). \tag{2.8}$$

where

$$\begin{aligned} \mathcal{K}(\theta, \lambda) &= \int_0^\theta \frac{\lambda(\beta^2 - \sin^2 \beta)(\pi - \beta + \sin \beta \cos \beta) + ((\pi - \beta)^2 - \sin^2 \beta)(\beta - \sin \beta \cos \beta)}{2 \sin \beta (\lambda^2(\beta^2 - \sin^2 \beta) + 2\lambda(\sin^2 \beta + \beta(\pi - \beta) + (\pi - \beta)^2 - \sin^2 \beta))} d\beta, \\ &= \int_0^\theta \mathcal{F}(\beta, \lambda) \sin \beta d\beta. \end{aligned} \tag{2.9}$$

A first-order approximation of Cox’s formula leads to

$$\begin{aligned} |\ln \zeta| Ca &= \int_{\theta_Y}^{\theta_a} \mathcal{F}(\beta, \lambda) \sin \beta d\beta \\ &\approx -\mathcal{F}(\theta_a, \lambda) (\cos \theta_a - \cos \theta_Y) + O((\theta_a - \theta_Y)^2). \end{aligned} \tag{2.10}$$

This implies that Cox’s formula is consistent with our analysis by using the Onsager principle to leading order. The difference between the two formulae is illustrated in figure 2. We can see that their difference is small for the small capillary number case (e.g. $Ca \leq 0.01$). When Ca is large, the linear approximation of the interface in the mesoscopic region is not very accurate anymore. Then there is a larger difference between (2.7) and Cox’s formula.

Equation (2.6) can be regarded as a coarse-graining boundary condition for the two-phase Navier–Stokes equation in the macroscopic region Ω . It gives a relation

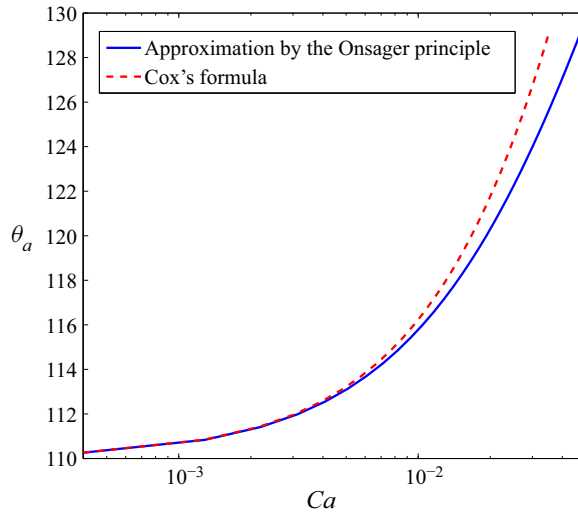


Figure 2. Comparison between Cox's formula and (2.7). Here, we choose $\lambda = 0$ and $\theta_Y = 110^\circ$. Their difference is small for small capillary number ($Ca \sim O(10^{-2})$).

between the apparent contact angle and the contact line velocity. The results are similar to that in de Gennes *et al.* (2003). One can use (2.6) instead of the microscopic boundary conditions (e.g. (A14)) to avoid resolving the mesoscopic region by very fine meshes in numerical simulations.

2.2. Model problems

In some problems with small characteristic size, the energy dissipation in the mesoscopic region may dominate. Then one can derive a reduced model for such problems. One typical example is the spreading of a small droplet on hydrophilic surfaces which gives the so-called Tanner's law (Tanner 1979). Other examples can be found in de Gennes *et al.* (2003), Chan, Yang & Carlson (2020) and Xu & Wang (2020). In the following, we will introduce two typical examples. Then we show that they can be described by a unified reduced model, which will be used to study the dynamic CAH in the next section.

EXAMPLE 2.1. A moving contact line problem in a micro-channel.

In the example, we consider a contact line problem in microfluidics, which is similar to that considered in Joanny & De Gennes (1984). As shown in figure 3, suppose that the two walls of a channel are moving at a velocity u_{wall} . There is a bar on the left-hand side of the channel to keep the liquid from moving out. Suppose that the height h_0 of the channel is smaller than the capillary length. Then we could assume that the interface remains almost circular if the velocity u_{wall} is small. Then, the position of the contact point is fully determined by the dynamic contact angle since the volume of the liquid is conserved.

Suppose the volume of the liquid is V_0 . We suppose the left boundary of the liquid domain is $x = 0$ and the x -coordinate of the contact point is x_{ct} . Suppose the apparent

Dynamical contact angle hysteresis

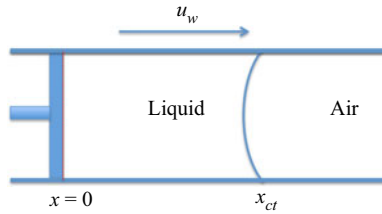


Figure 3. Contact point motion in a micro-channel.

contact angle is θ_a . Then the volume of liquid is calculated by

$$\begin{aligned} V_0 &= h_0 x_{ct} + \frac{h_0^2}{4} \frac{\theta_a - \pi/2 - \sin(\theta_a - \pi/2) \cos(\theta_a - \pi/2)}{\sin^2(\theta_a - \pi/2)} \\ &= h_0 x_{ct} + \frac{h_0^2}{8} \frac{(2\theta_a - \pi + \sin(2\theta_a))}{\cos^2 \theta_a}. \end{aligned} \quad (2.11)$$

This equation gives a relation between x_{ct} and the apparent contact angle θ_a . We do time derivative for the above equation and notice that $\dot{V}_0 = 0$. Then we have

$$\dot{x}_{ct} = -\frac{h_0}{2} \frac{\cos \theta_a + \left(\theta_a - \frac{\pi}{2}\right) \sin \theta_a}{\cos^3 \theta_a} \dot{\theta}_a. \quad (2.12)$$

On the other hand, since the relative velocity of the contact line with respect to the two walls is $\dot{x}_{ct} - u_{wall}$, (2.6) implies

$$\left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)}\right) \frac{\mu}{\gamma} (\dot{x}_{ct} - u_{wall}) = -(\cos \theta_a - \cos \theta_Y), \quad (2.13)$$

where

$$\mathcal{F}_1(\theta_a) = \mathcal{F}(\theta_a, 0) = \frac{(\theta_a - \sin \theta_a \cos \theta_a)}{2 \sin^2 \theta_a}. \quad (2.14)$$

Equations (2.12) and (2.13) compose a complete system of ordinary differential equations (ODEs) for the apparent contact angle and the contact point position. Denote

$$\mathcal{G}_1(\theta) = -\frac{\cos^3 \theta_a}{\cos \theta_a + \left(\theta_a - \frac{\pi}{2}\right) \sin \theta_a}, \quad (2.15)$$

then the ODE system is written as

$$\left. \begin{aligned} \dot{\theta}_a &= \frac{2\mathcal{G}_1(\theta)}{h_0} \left(-\left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)}\right)^{-1} \frac{\gamma}{\mu} (\cos \theta_a - \cos \theta_Y) + u_{wall} \right), \\ \dot{x}_{ct} &= -\left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)}\right)^{-1} \frac{\gamma}{\mu} (\cos \theta_a - \cos \theta_Y) + u_{wall}. \end{aligned} \right\} \quad (2.16)$$

EXAMPLE 2.2. A capillary problem along a moving thin fibre.

Motivated by the recent experiments in Guan *et al.* (2016a), we consider a capillary problem along a moving fibre. As shown in figure 4, we suppose a fibre is inserted in

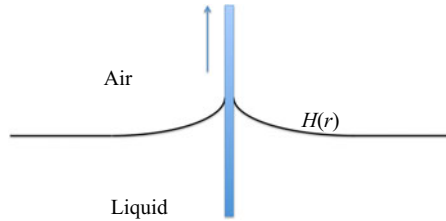


Figure 4. Contact line motion on a moving fibre.

a liquid. When the fibre moves up and down, the contact line will recede and advance accordingly. We assume that the radius r_0 of the fibre is much smaller than the capillary length l_c . By the Young–Laplace equation, the radially symmetric liquid–vapour interface can be described by the following equation (see de Gennes *et al.* 2003):

$$x = H(r) = h - r_0 \cos \theta_a \ln \frac{r + \sqrt{r^2 - r_0^2 \cos^2 \theta_a}}{r_0 \cos \theta_a}, \quad r \geq r_0. \quad (2.17)$$

Here, we assume the upper direction is the positive x -direction. There are two parameters, h and θ_a , in this equation. By the definition of the capillary length, we can assume that the interface intersects with the horizontal surface $x = 0$ at $r = l_c$. Then we have

$$H(l_c) = 0. \quad (2.18)$$

This gives a relation between θ_a and h , which is

$$h = r_0 \cos \theta_a \ln \frac{l_c + \sqrt{l_c^2 - r_0^2 \cos^2 \theta_a}}{r_0 \cos \theta_a}. \quad (2.19)$$

Notice that the x -coordinate of the contact line is given by

$$x_{ct} := H(r_0) = h - r_0 \cos \theta_a \ln \frac{1 + \sin \theta_a}{\cos \theta_a} = r_0 \cos \theta_a \ln \frac{l_c + \sqrt{l_c^2 - r_0^2 \cos^2 \theta_a}}{r_0(1 + \sin \theta_a)}. \quad (2.20)$$

Direct calculation gives

$$\dot{x}_{ct} = r_0 \mathcal{G}_2^{-1}(\theta_a) \dot{\theta}_a, \quad (2.21)$$

where

$$\mathcal{G}_2^{-1}(\theta_a) = r_0^{-1} \frac{\partial x_{ct}}{\partial \theta_a} \approx - \left(\sin \theta_a \ln \frac{2l_c}{r_0(1 + \cos \theta_a)} + 1 - \sin \theta_a \right). \quad (2.22)$$

Equation (2.21) gives a relation between the time derivative of the contact line position and that of the dynamic contact angle.

Applying the boundary condition (2.6) to the relative velocity of the contact line $\dot{x}_{ct} - u_{wall}$, we obtain

$$\left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)}\right) \frac{\mu}{\gamma} (\dot{x}_{ct} - u_{wall}) = -(\cos \theta_a - \cos \theta_Y). \quad (2.23)$$

The two equations compose a complete system for the capillary rising problem. They can be rewritten as

$$\left. \begin{aligned} \dot{\theta}_a &= \frac{\mathcal{G}_2(\theta)}{r_0} \left(- \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1} \frac{\gamma}{\mu} (\cos \theta_a - \cos \theta_Y) + u_{wall} \right), \\ \dot{x}_{ct} &= - \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1} \frac{\gamma}{\mu} (\cos \theta_a - \cos \theta_Y) + u_{wall}. \end{aligned} \right\} \quad (2.24)$$

This generalizes the formula given in Xu & Wang (2020). We would like to remark that for this problem we actually need to solve a three-dimensional two-phase Stokes system in a region around the fibre when we calculate the total viscous dissipation in the system. This may lead to a correction for the three-dimensional effect in the function $\mathcal{F}_1(\theta)$. Hereinafter, we ignore this effect for simplicity.

We can see that the ordinary differential systems (2.16) and (2.24) in the two examples have the same structure. They can be written as a unified form as follows:

$$\left. \begin{aligned} \dot{\theta}_a &= \frac{\mathcal{G}(\theta_a)}{l_0} \left(- \frac{\gamma}{\mu} \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1} (\cos \theta_a - \cos \theta_Y) + u_{wall} \right), \\ \dot{x}_{ct} &= - \frac{\gamma}{\mu} \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1} (\cos \theta_a - \cos \theta_Y) + u_{wall}. \end{aligned} \right\} \quad (2.25)$$

The second equation of (2.25) is due to the condition (2.7) where $\mathcal{F}_1(\theta_a)$ is given in (2.14). Since $\mathcal{F}_1(\theta_a) = \mathcal{F}(\theta_a, 0)$, it corresponds to the case when $\mu_B/\mu_A = 0$ (see (2.4)), i.e. a liquid–vapour system. In the first equation of (2.25), l_0 is a characteristic length and the function $\mathcal{G}(\theta_a)$ comes from the geometric set-up of a problem. Both l_0 and $\mathcal{G}(\theta_a)$ may change for different problems. Hereinafter, we will use (2.25) as a model problem to study the CAH for a liquid–vapour system on a chemically patterned surface.

3. Averaging for dynamic contact angles on inhomogeneous surfaces

In this section, we consider the case when the solid surface is chemically inhomogeneous. This implies that the Young’s angle θ_Y is not a constant but a function of the position on the solid substrate. For example, we can assume that $\theta_Y = \hat{\theta}_Y(x)$, where x is the position on the solid surface. Then the system (2.25) can be rewritten as

$$\left. \begin{aligned} \dot{\theta}_a &= \frac{\mathcal{G}(\theta_a)}{l_0} \left(- \frac{\gamma}{\mu} \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1} (\cos \theta_a - \cos \hat{\theta}_Y(\hat{x}_{ct})) + u_{wall} \right), \\ \dot{\hat{x}}_{ct} &= - \frac{\gamma}{\mu} \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1} (\cos \theta_a - \cos \hat{\theta}_Y(\hat{x}_{ct})), \end{aligned} \right\} \quad (3.1)$$

where \hat{x}_{ct} is the actual position of the contact line on the solid surface satisfying $\dot{\hat{x}}_{ct} = \dot{x}_{ct} - u_{wall}$.

The system (3.1) can be made dimensionless using the capillary length l_c and the characteristic time scale l_c/U^* , where $U^* = \gamma/\mu$. Using a change of variables $\hat{x}_{ct}/l_c \rightarrow \hat{x}_{ct}$ and $t/l_c/U^* \rightarrow t$ (we still use \hat{x}_{ct} and t for the dimensionless variables for simplicity in notation), the dimensionless system for (3.1) is given by

$$\left. \begin{aligned} \dot{\theta}_a &= g(\theta_a) \left(f(\theta_a) (\cos \hat{\theta}_Y(\hat{x}_{ct}) - \cos \theta_a) + v \right), \\ \dot{\hat{x}}_{ct} &= f(\theta_a) (\cos \hat{\theta}_Y(\hat{x}_{ct}) - \cos \theta_a), \end{aligned} \right\} \quad (3.2)$$

where we have denoted

$$f(\theta) = \left(\alpha + \frac{|\ln \zeta|}{\mathcal{F}_1(\theta_a)} \right)^{-1}, \quad g(\theta) = \frac{l_c \mathcal{G}(\theta)}{l_0}, \quad \text{and} \quad v = \frac{u_{wall}}{U^*} \quad (3.3a-c)$$

for simplicity in notation. We call the function $f(\theta)$ the dynamic factor, as $f(\theta)$ arises from the force balance equation (2.7). We call the function $g(\theta)$ the geometric factor, which describes the geometric relation between the apparent contact angle and contact line velocity. We will see later that $f(\theta)$ plays a very important role in both the dynamic process and the final steady state, while $g(\theta)$ only affects the dynamic process before the steady state is achieved.

3.1. Time averaging of the ODE system

We first introduce some properties satisfied by the dynamic factor f and g

$$f(\theta) \geq 0, f(0) = 0; \quad -M \leq g(\theta) \leq -m, \quad (3.4a,b)$$

for some positive numbers m and M . In addition, we also assume that f is monotonically increasing in the interval $[0, \pi]$. These conditions are quite general and are satisfied by the two examples in the previous section.

We assume that the substrate has periodic chemical patterns with period ε so that Young's angle at the position x satisfies $\hat{\theta}_Y(x) = \varphi(x/\varepsilon)$, where φ is a periodic continuously differentiable function with period 1. The minimum and maximum of φ are θ_A and θ_B , respectively, with $0 < \theta_A < \theta_B < \pi$. One example of such functions is

$$\varphi(z) = \frac{\theta_A + \theta_B}{2} + \frac{\theta_B - \theta_A}{2} \sin(2\pi z). \quad (3.5)$$

In the following, we will use the method of averaging to derive the effective dynamics of the contact angle and contact line position. This method has been studied in detail (e.g. in Pavliotis & Stuart 2008; E 2011) and has been widely used in obtaining the effective boundary conditions (e.g. Miskis & Davis 1994).

We introduce the fast spatial variable $y = \hat{x}_{ct}/\varepsilon$ and fast temporal variable $\tau = t/\varepsilon$. Consider the multiple scale asymptotic expansions

$$\theta_a = \theta_0(t, \tau) + \varepsilon \theta_1(t, \tau) + \dots, \quad y = y_0(t, \tau) + \varepsilon y_1(t, \tau) + \dots. \quad (3.6a,b)$$

Then the system of (3.2) can be rewritten as

$$\begin{aligned} \frac{1}{\varepsilon} \frac{\partial \theta_0}{\partial \tau} + \left(\frac{\partial \theta_0}{\partial t} + \frac{\partial \theta_1}{\partial \tau} \right) + \varepsilon \left(\frac{\partial \theta_1}{\partial t} + \frac{\partial \theta_2}{\partial \tau} \right) + \dots \\ = g(\theta_0 + \varepsilon \theta_1 + \dots) (f(\theta_0 + \varepsilon \theta_1 + \dots) (\cos \varphi(y_0 + \varepsilon y_1 + \dots) \\ - \cos(\theta_0 + \varepsilon \theta_1 + \dots)) + v), \end{aligned} \tag{3.7a}$$

$$\begin{aligned} \frac{1}{\varepsilon} \frac{\partial y_0}{\partial \tau} + \left(\frac{\partial y_0}{\partial t} + \frac{\partial y_1}{\partial \tau} \right) + \varepsilon \left(\frac{\partial y_1}{\partial t} + \frac{\partial y_2}{\partial \tau} \right) + \dots \\ = \frac{1}{\varepsilon} f(\theta_0 + \varepsilon \theta_1 + \dots) (\cos \varphi(y_0 + \varepsilon y_1 + \dots) - \cos(\theta_0 + \varepsilon \theta_1 + \dots)). \end{aligned} \tag{3.7b}$$

First-order equations in $O(1/\varepsilon)$. We have the two equations in the fast time scale

$$\frac{\partial \theta_0}{\partial \tau} = 0, \tag{3.8}$$

$$\frac{\partial y_0}{\partial \tau} = f(\theta_0) (\cos \varphi(y_0) - \cos \theta_0). \tag{3.9}$$

The first equation implies that $\theta_0 = \theta_0(t)$ is indeed a slow variable that does not depend on the fast time scale τ . Then, for given θ_0 , the second equation is a simple ODE for y_0 with respect to τ , that can be easily solved. We discuss its solution in two different cases for the parameter θ_0 .

In the first case when $\theta_0 \in [\theta_A, \theta_B]$, for any given initial value for y_0 , the solution of (3.9) approaches some equilibrium value $y_{0,\infty}$, which satisfies $\varphi(y_{0,\infty}) = \theta_0$. By the phase plane analysis (see figure 5), we know that there are three types of equilibrium points: $y_{0,\infty}$ is asymptotically stable, semi-stable or unstable if $\varphi'(y_{0,\infty}) > 0$, $\varphi'(y_{0,\infty}) = 0$ or $\varphi'(y_{0,\infty}) < 0$, respectively. Every solution path must be attracted to either an asymptotically stable point or a semi-stable point, regardless of the initial value of y_0 . For instance, if the initial value y_0^{init} satisfies $\varphi(y_0^{init}) < \theta_0$, then y_0 increases monotonically with τ until it reaches the nearest equilibrium point $y_{0,\infty}$ which is larger than y_0^{init} . This equilibrium point must satisfy $\varphi'(y_{0,\infty}) \geq 0$ and thus becomes asymptotically stable or semi-stable. If the initial value y_0^{init} satisfies $\varphi(y_0^{init}) > \theta_0$, then y_0 decreases monotonically with τ until it reaches the nearest equilibrium point $y_{0,\infty}$ that is smaller than y_0^{init} . This equilibrium point must also satisfy $\varphi'(y_{0,\infty}) \geq 0$ and thus becomes asymptotically stable or semi-stable.

In the second case that $\theta_0 > \theta_B$ or $\theta_0 < \theta_A$, $\cos \varphi(y_0) - \cos \theta_0$ is either always positive or always negative. As a result, y_0 is monotonic in τ and diverges to $\pm\infty$ either increasingly or decreasingly. Moreover, using the method of separable variables, y_0 can be solved and represented implicitly as

$$Q(y_0(t, \tau), \theta_0) = Q(y_0(t, 0), \theta_0) + \tau, \tag{3.10}$$

where

$$Q(z, \phi) = \int \frac{dz}{f(\phi)(\cos \varphi(z) - \cos \phi)} \tag{3.11}$$

is monotonically increasing or decreasing in z and thus can be inverted to give $y_0(t, \tau)$.

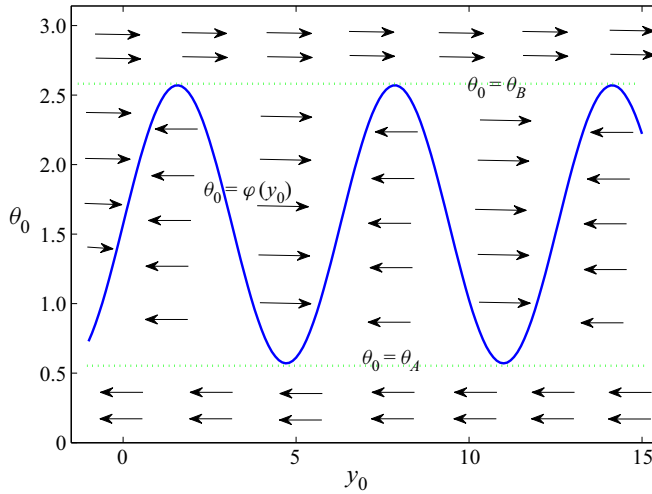


Figure 5. Sketch of phase plane analysis for the ODEs (3.8) and (3.9). Here, θ_0 is independent of τ ; y_0 increases when $\theta_0 > \varphi(y_0)$ and y_0 decreases when $\theta_0 < \varphi(y_0)$.

Second-order equations in $O(1)$. We consider the $O(1)$ equation for θ , which is given by

$$\frac{\partial \theta_0}{\partial t} + \frac{\partial \theta_1}{\partial \tau} = g(\theta_0) (f(\theta_0)(\cos \varphi(y_0) - \cos \theta_0) + v). \tag{3.12}$$

We can assume that θ_1 is of sublinear growth in τ , i.e. there exists a constant $\alpha \in [0, 1)$ such that $|\theta_1(t, \tau)| \leq C|\tau|^\alpha$ for some constant C (see also E 2011). Define the time averaging operator $\langle \cdot \rangle_\tau$ as

$$\langle F \rangle_\tau = \lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T F(\tau) \, d\tau. \tag{3.13}$$

Then, applying this time averaging operator to (3.12) gives rise to

$$\frac{\partial \theta_0}{\partial t} = g(\theta_0) (\langle f(\theta_0)(\cos \varphi(y_0) - \cos \theta_0) \rangle_\tau + v), \tag{3.14}$$

where we have used the sublinearity of θ_1 to eliminate $\langle \partial \theta_1 / \partial \tau \rangle_\tau$.

From the previous analysis for the leading-order equations, y_0 is monotonic in τ . Thus we can simplify the averaged term by using (3.9),

$$\langle f(\theta_0)(\cos \varphi(y_0) - \cos \theta_0) \rangle_\tau = \lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T \frac{\partial y_0}{\partial \tau} \, d\tau = \lim_{T \rightarrow \infty} \frac{y_0(t, T) - y_0(t, 0)}{T}. \tag{3.15}$$

We discuss the limit on the right-hand side for different cases on θ_0 . In the first case that $\theta_0 \in [\theta_A, \theta_B]$, this limit is zero since every solution path $y(t, \cdot)$ converges to an asymptotically stable or semi-stable equilibrium point (by the analysis for the leading-order equations). In the second case that $\theta_0 > \theta_B$ or $\theta_0 < \theta_A$, we shall show that this limit is

$$\left(\int_0^1 \frac{dz}{f(\theta_0)(\cos \varphi(z) - \cos \theta_0)} \right)^{-1}, \tag{3.16}$$

the harmonic average of $f(\theta_0)(\cos \varphi(z) - \cos \theta_0)$ over $z \in [0, 1]$.

Dynamical contact angle hysteresis

The argument for the second case is as follows. Let

$$b = \int_0^1 \frac{dz}{f(\theta_0)(\cos \varphi(z) - \cos \theta_0)} = \frac{1}{f(\theta_0)} \int_0^1 \frac{dz}{(\cos \varphi(z) - \cos \theta_0)}. \quad (3.17)$$

From (3.10) we know that if $\tau = nb$ for any integer n , then

$$y_0(t, \tau) - y_0(t, 0) = n. \quad (3.18)$$

Writing $T = nb + a$ with $n = \lfloor T/b \rfloor$ (the largest integer no greater than T/b) and $0 \leq a < b$, and letting $n \rightarrow \infty$, we have

$$\lim_{T \rightarrow \infty} \frac{y_0(t, T) - y_0(t, 0)}{T} = b^{-1}. \quad (3.19)$$

This implies that $\langle f(\theta_0)(\cos \varphi(y_0) - \cos \theta_0) \rangle_\tau$ is exactly equal to the harmonic average of $f(\theta_0)(\cos \varphi(z) - \cos \theta_0)$ over a period $[0, 1]$.

By the above calculations, (3.14) is reduced to

$$\frac{d\theta_0}{dt} = \begin{cases} g(\theta_0)v, & \theta_0 \in [\theta_A, \theta_B]; \\ g(\theta_0)(b^{-1} + v), & \theta_0 > \theta_B \text{ or } \theta_0 < \theta_A. \end{cases} \quad (3.20)$$

By this equation, we can discuss the dynamics for the slow variable \hat{x}_{ct} . As $\varepsilon \rightarrow 0$ we have

$$\begin{aligned} \frac{d\hat{x}_{ct}}{dt} &= \frac{\partial y_0}{\partial \tau} + \varepsilon \left(\frac{\partial y_0}{\partial t} + \frac{\partial y_1}{\partial \tau} \right) + O(\varepsilon^2) \\ &\sim f(\theta_0)(\cos \varphi(y_0) - \cos \theta_0) + O(\varepsilon). \end{aligned} \quad (3.21)$$

On application of the time averaging operator $\langle \cdot \rangle_\tau$, the leading order of \hat{x}_{ct} satisfies

$$\frac{d\langle \hat{x}_{ct,0} \rangle_\tau}{dt} = \langle f(\theta_0)(\cos \varphi(y_0) - \cos \theta_0) \rangle_\tau = \begin{cases} 0, & \theta_0 \in [\theta_A, \theta_B], \\ b^{-1}, & \theta_0 > \theta_B \text{ or } \theta_0 < \theta_A. \end{cases} \quad (3.22)$$

We introduce the average of the contact angle and the contact point position such that

$$\Theta_a := \langle \theta_0 \rangle_\tau = \theta_0, \quad \text{and} \quad \hat{X}_{ct} := \langle \hat{x}_{ct,0} \rangle_\tau. \quad (3.23a,b)$$

The above analysis can be summarized as follows. In the first case that $\theta_A \leq \Theta_a \leq \theta_B$, the averaged equations are

$$\dot{\Theta}_a = g(\Theta_a)v, \quad (3.24a)$$

$$\dot{\hat{X}}_{ct} = 0. \quad (3.24b)$$

In the second case that $\Theta_a > \theta_B$ or $\Theta_a < \theta_A$, the averaged equations are

$$\dot{\Theta}_a = g(\Theta_a) \left(f(\Theta_a) \left(\int_0^1 \frac{dz}{\cos \varphi(z) - \cos \Theta_a} \right)^{-1} + v \right), \quad (3.25a)$$

$$\dot{\hat{X}}_{ct} = f(\Theta_a) \left(\int_0^1 \frac{dz}{\cos \varphi(z) - \cos \Theta_a} \right)^{-1}. \quad (3.25b)$$

3.2. The effective contact angles

Based on the above analysis, we can make a prediction for the averaged apparent contact angle Θ_a and the averaged contact line motion \hat{X}_{ct} . This will lead to the formula for the effective advancing and receding contact angles when the contact line moves on a chemically patterned surface.

First consider the case $v > 0$, i.e. the wall moves in the positive direction. This corresponds to a receding contact line, since the fluid moves to the negative direction relative to the substrate. We discuss three possible stages while leaving the details to [Appendix C](#):

- (i) When the initial value of the contact angle Θ_a lies in the regime $(\theta_B, \pi]$, the averaged contact line dynamics follows (3.25). In this stage, the effective contact angle Θ_a decreases towards θ_B exponentially fast. Moreover, the effective contact line position \hat{X}_{ct} moves in the positive direction. This first stage is indeed a transient stage.
- (ii) When the contact angle Θ_a reaches θ_B , the averaged dynamics switches to (3.24). The effective contact angle Θ_a continues decreasing until it reaches θ_A . However, the effective contact line position \hat{X}_{ct} remains unchanged.
- (iii) When the contact angle Θ_a attains θ_A , the averaged dynamics switches back to (3.25). In this situation, the effective contact angle Θ_a decreases until it eventually arrives at a stable steady state $\Theta^* < \theta_A$. The steady state Θ^* satisfies

$$f(\Theta^*) \left(\int_0^1 \frac{dz}{\cos \varphi(z) - \cos \Theta^*} \right)^{-1} + v = 0. \quad (3.26)$$

When Θ_a attains Θ^* , the effective contact line position \hat{X}_{ct} moves in the negative direction at a constant velocity equal to $-v$.

If the initial contact angle lies in the regime $[\theta_A, \theta_B]$ or $[0, \theta_A)$, the above three-stage dynamics may be reduced to a two-stage process or only one stage. In all these situations, Θ_a always reaches the equilibrium contact angle Θ^* . Meanwhile, the average contact line position \hat{X}_{ct} finally moves with a constant negative velocity $-v$. Notice that it is the actual contact line position on the solid wall. The equilibrium contact angle Θ^* is actually the effective receding contact angle, which is denoted by $\Theta^* = \Theta^*(v)$ as a function of $v > 0$.

In the case of $v < 0$, a similar analysis can be made to predict the dynamics of the effective advancing contact angle, with the corresponding velocities of opposite signs. The effective contact angle Θ_a eventually arrives at a steady state Θ^* , which also satisfies (3.26); and the actual contact line position \hat{X}_{ct} moves with a constant positive velocity $-v$. The final steady state Θ^* is called the effective advancing contact angle, which is also denoted by $\Theta^* = \Theta^*(v)$ for $v < 0$.

As an interesting but important fact, we remark that: the effective advancing contact angle $\Theta^*(v) > \theta_B$ with $v < 0$, and it approaches θ_B as v increases to zero; the effective receding contact angle $\Theta^*(v) < \theta_A$ with $v > 0$, and it approaches θ_A as v decreases to zero. When $v = 0$, the contact line can be pinned for any contact angle between θ_A and θ_B . Similar ideas have been investigated in many phenomenological moving contact line models in the study of CAH (Prabhala, Panchagnula & Vedantam 2013; Yue 2020).

In summary, depending on the initial value of the contact angle, the averaged dynamics of the contact line and the contact angle can be characterized by a process with at most three stages as described above. In any cases, one approaches to a steady state where the effective advancing angle or receding angle does not change any more. The effective

contact angles are given by the (3.26). It is worth noting that the final effective advancing and receding contact angles only depend on the dynamic factor $f(\theta_a)$ and the dragging velocity v . The geometric factor $g(\theta_a)$ only affects the dynamic process that how Θ_a approaches the effective advancing and receding contact angles. The above results are numerically validated in § 5.

4. Discussions on the main results

4.1. The averaged models for a Cox-type boundary condition

The main result of the above analysis is that we obtain (3.26) for the effective advancing and receding contact angles on chemically patterned surfaces. It is easy to see that the dimensionless wall velocity $v = u_{wall}/U^*$ is opposite to the effective capillary number Ca for the contact line motion. We replace v by $-Ca$, and (3.26) can be rewritten as

$$Ca = -f(\Theta^*) \left(\int_0^1 \frac{dz}{\cos \Theta^* - \cos \varphi(z)} \right)^{-1}. \tag{4.1}$$

For simplicity, we ignore the contact line friction (i.e. $\alpha = 0$) in the following discussions and the general cases with non-zero α can be analysed similarly. The effective condition (4.1) is then simplified to

$$|\ln \zeta| Ca = -\mathcal{F}_1(\Theta^*) \left(\int_0^1 \frac{dz}{\cos \Theta^* - \cos \varphi(z)} \right)^{-1}, \tag{4.2}$$

where $\mathcal{F}_1(\theta) = \mathcal{F}(\theta, 0)$ is defined in (2.14). We can see that the equation is quite similar to the Cox-type boundary condition (2.7). The only difference is that the term $\cos \theta - \cos \theta_Y$ is replaced by its harmonic average on a chemically inhomogeneous surface (with contact angle pattern $\varphi(z)$). When $\varphi(z) \equiv \theta_Y$, (4.2) will reduce to (2.7) (with $\lambda = 0$). In general cases, it is a complicated nonlinear equation for the dynamic contact angle Θ^* with the given parameter Ca and the chemical pattern function φ . We will discuss its properties below.

Equation (4.2) can be solved simply by numerical methods. We show some results to see how the effective contact angles depends on the wall velocity and the chemical patterns. To show the effect of the chemical inhomogeneity and the velocity on the effective contact angles, we consider a simple chemically patterned surface. In this case, the pattern is described by

$$\varphi_\chi(z) = \begin{cases} \theta_A, & z \in [0, \chi], \\ \theta_B, & z \in (\chi, 1]. \end{cases} \tag{4.3}$$

Here, χ is the fraction of the solid surface occupied by material A.

Figure 6 shows the effective advancing and receding contact angles computed by (3.26) (or (4.2) equivalently). Here, we choose $|\ln \zeta| = 1$ for simplicity. We could see that the effective contact angle depends on the two contact angles θ_A and θ_B , the wall velocity v and also the fraction χ . Firstly, for given chemical patterns where θ_A , θ_B and χ are fixed, the advancing contact angle increases when the absolute value of the velocity (i.e. $-v$) increases. Meanwhile the receding contact angle decreases when the velocity v increases. The dependence of the effective contact angles on the velocity is affected by both the chemical properties θ_A , θ_B and their arrangement (represented by χ). For given chemical

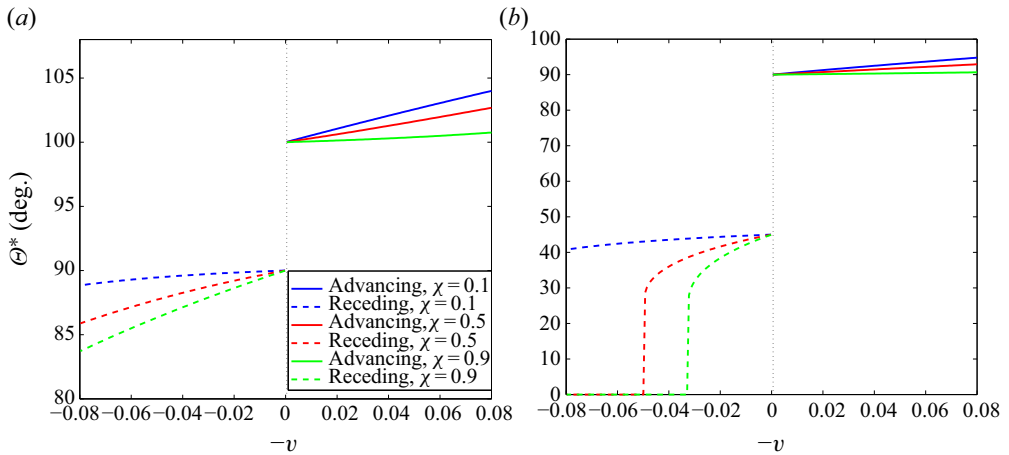


Figure 6. The effective contact angles on chemically patterned surfaces; (a) $\theta_A = 90^\circ$, $\theta_B = 100^\circ$. (b) $\theta_A = 45^\circ$, $\theta_B = 90^\circ$.

properties θ_A and θ_B , the dependence of the contact angles on the velocity seems more asymmetric for larger χ , which means that the receding contact angle changes more dramatically than the advancing contact angle when the absolute value of the velocity increases. For a given arrangement (i.e. χ is fixed), the dependence seems more symmetric when both θ_A and θ_B are close to 90° . These dependences may lead to very complicated experimental observations (Guan *et al.* 2016a,b). We will make numerical comparisons in the next section.

From (4.1), we could see that in steady and viscous dominant states the effective apparent contact angle depends on the contact line velocity, the contact line friction coefficient α , the viscous friction factor \mathcal{F}_1 and the chemical pattern $\varphi(z)$ of the substrate. We notice that the geometric factor g , which is determined by the specific set-up of a problem, does not appear in the equation. The same formula holds for both a capillary problem in a tube or the forced wetting problem around a fibre. The averaged formula (4.1) is an effective formula for the advancing contact angle and receding contact angle on an inhomogeneous surface. It gives the explicit relation of how the advancing and receding contact angles depend on the chemical inhomogeneity of the solid surface. Thus, we expect that the formula (4.2) can be used as a boundary condition for the two-phase Navier–Stokes equations.

The analysis also indicates that our theoretical results may be used to design substrates for certain purposes (e.g. the directed motion), since it characterizes quantitatively the dependence of the advancing and receding contact angles on the contact line velocity. For example, for a substrate composed of two materials with Young’s angles θ_A and θ_B ($\theta_A < \theta_B$), the rupture forces in the advancing and receding cases are respectively $\Delta F_a = \gamma |\cos \theta_{adv} - \cos \theta_B|$ and $\Delta F_r = \gamma |\cos \theta_{rec} - \cos \theta_A|$ (Guan *et al.* 2016b), where θ_{adv} and θ_{rec} are the effective advancing and receding contact angles given by (3.26). We can design substrates with asymmetric dependence of the rupture forces on the contact line velocity so that the contact line moves easier in one direction where the rupture force is smaller.

In the above analysis, we mainly consider the wetting problem of a liquid–gas system. The approach can be easily generalized to the liquid–liquid system. In this case, the

function \mathcal{F}_1 in (4.2) should be replaced by $\mathcal{F}(\theta_a, \lambda)$ defined in (2.4). We get an equation

$$|\ln \zeta|Ca = -\mathcal{F}(\Theta^*, \lambda) \left(\int_0^1 \frac{dz}{\cos \Theta^* - \cos \varphi(z)} \right)^{-1} \quad (4.4)$$

for two-phase flow with viscous ratio λ . It is an averaged boundary condition for the apparent contact angle on a chemically inhomogeneous surface, corresponding to the Cox-type boundary condition (2.7) on homogeneous surfaces.

The averaging technique also works if we choose Cox's boundary condition (2.8) (instead of the simplified version (2.7)), but the analysis should be much more complicated. In this case, the effective boundary condition will be

$$|\ln \zeta|Ca = \left(\int_0^1 \frac{dz}{\mathcal{K}(\Theta^*, \lambda) - \mathcal{K}(\varphi(z), \lambda)} \right)^{-1}. \quad (4.5)$$

It is a harmonic average of the force term in Cox's formula. Once again, it reduces to Cox's formula (2.8) when $\varphi(z) \equiv \theta_Y$. This boundary condition is the averaged version of Cox's formula on an inhomogeneous surface. It can be used as a coarse-graining boundary for moving contact line problems on chemically inhomogeneous surfaces. As mentioned in § 2.2, the formulae (4.4) and (4.8) are quite close when the capillary number Ca is small. In addition, the same analysis can also be done for other similar boundary conditions (Voinov 1976).

4.2. *The inertial effect*

In general, Cox's boundary condition works well only when the inertial effect is negligible in the mesoscopic region (Cox 1986). Define the Reynolds number as $Re = \rho UD/\eta$, where U is the velocity of the contact line and D is the characteristic length of the mesoscopic region. Notice that the slip velocity can be bounded by a quantity $(\gamma/\xi)|\cos \theta_A - \cos \theta_B|$ on a chemically patterned surface with Young's angles θ_A and θ_B . If the length scale D is small or the contact line friction ξ is large, it is possible that Re is still small even when the contact line slips on the substrate. For example, in the experiments of Guan *et al.* (2016b), the Reynolds numbers Re are in the range $[0, 0.14]$. In this case, the inertial effect is not important and the system can be well approximated by Stokes flows. The previous averaged formulae are good approximations to the apparent contact angles. In the following, we will discuss briefly more general cases when the inertial effect cannot be ignored.

When the Reynolds number is not small but in an intermediate regime ($1 \leq Re \leq D/l$), R. G. Cox also derives a boundary condition such that (Cox 1998)

$$Ca \ln \left(\frac{\zeta}{Re} \right) = \mathcal{K}(\vartheta(\theta_a)) - \mathcal{K}(\theta_Y). \quad (4.6)$$

Here, ϑ is a function of θ_a such that

$$\vartheta(\theta_a) = g_{iv}^{-1}(g_{iv}(\theta_a) - Ca \ln Re), \quad (4.7)$$

with $g_{iv}(\theta) = 1.53(\theta - \sin \theta)$. By definition, the Reynolds number Re can be written as $Re = Ca/Oh^2$, where $Oh = \mu_A/\sqrt{\rho_A \gamma D}$ is the Ohnesorge number. Then, the condition (4.6) gives a complicated nonlinear relation between the capillary number Ca and the apparent contact angle θ_a . When Oh is small, the Reynolds number can be large and the inertial effect is not negligible. The condition is verified qualitatively for the moderate

inertia case in Stoev, Ramé & Garoff (1999). This condition is slightly modified and validated in Sui & Spelt (2013*b*). We can use the model to describe the inertial effect on the apparent contact angle.

In this case, the two-phase interface in outer regions cannot be approximated well by a quasi-static profile. The geometric equation in the previous section (the first equation in (3.2)) does not hold. Instead, we need to solve a full two-phase Navier–Stokes system coupled with (4.6). Nevertheless, we can assume that the stick-slip motion of the contact line occurs in a much smaller time scale than that of the bulk motion, and the apparent contact angle oscillates around a value. In this case, it is possible to do similar multiple scale analysis for the coupled system as in the previous section and conduct more detailed estimates. This may lead to a condition for the averaged contact angle on chemically inhomogeneous surfaces as follows:

$$Ca \ln \left(\frac{\zeta}{Re} \right) = \left(\int_0^1 \frac{dz}{\mathcal{K}(\vartheta(\Theta^*)) - \mathcal{K}(\varphi(z))} \right)^{-1}. \quad (4.8)$$

Notice that the above formula is a nonlinear equation with respect to the averaged capillary number Ca and the averaged apparent contact angle Θ^* . We could solve it numerically. The comparisons of this equation with (4.2) and (4.4) are given in figure 7. Here, we consider chemically patterned surfaces as described by (4.3). We choose the two Young's angles $\theta_A = 80^\circ$, $\theta_B = 100^\circ$ and the ratio $\chi = 0.5$ for simplicity. In calculations, we set $\ln \zeta = 10$, $\lambda = 0$ and $Oh = 0.01$. In figure 7, we show the advancing contact angles for simplicity. It can be seen that the inertial effect on the averaged apparent contact angle is quite small when the averaged capillary number Ca is small (less than 0.01). The observations can be understood as follows. Firstly, on the chemically patterned surfaces, the slip velocity is still bounded due to the friction of the contact line. Previous molecular dynamics simulations and those based on continuum models show that the maximal slip velocity is a few times larger than that in steady state (Wang *et al.* 2008; Wu *et al.* 2010; Ren & E 2011). In this case, the difference between the original Cox's formula (2.8) and the modified formula (4.6) with inertial effects may not be very large. Secondly, since the slip occurs for a very short time in comparison with the slow motion of the contact line in the stick regions, the averaged behaviours are determined mainly by the slow motion of the contact line when the period of the patterns is small. Notice that, in the stick regions, the inertial effect is even smaller so that the difference between (2.8) and (4.6) is very small. Therefore, after time averaging, the formulae (4.8) and (4.4) (also (4.2)) will behave similarly when the averaged capillary number is small. In addition, if the averaged capillary number is large, the inertial effect will not be negligible and one should use (4.8) instead of the other two formulae.

4.3. Other theoretical models

In the last part of this section, we will discuss some other models which have been widely studied in the literature.

The first is the diffuse interface model where the interface of two fluids is not sharp. The interface is described by a phase-field function ϕ which is defined in the whole domain. In general, ϕ satisfies a Cahn–Hilliard equation. There are several types of boundary conditions for the model to describe the moving contact line. One is to impose the no-slip boundary condition for the velocity \mathbf{v} and constrain the dynamic contact angle to the Young's angle effectively (Jacqmin 2000; Yue, Zhou & Feng 2010). The other is the generalized Navier slip boundary condition where the microscopic contact angle will relax

Dynamical contact angle hysteresis

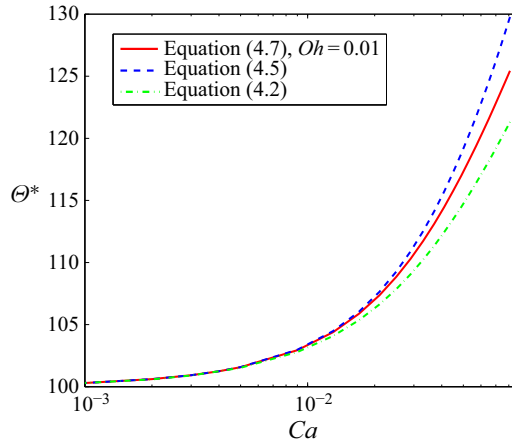


Figure 7. Comparisons of the averaged formulae by different models.

to the Young's angle due to the unbalanced Young's force (Qian *et al.* 2003). The boundary condition reads

$$\partial_t \phi + v_s \partial_s \phi = Cn \partial_n \phi + \partial_\phi L(x, \phi), \quad (4.9)$$

where $\partial_s \phi$ and $\partial_n \phi$ are respectively the derivatives of ϕ in the tangential and normal directions,

$$L(x, \phi) = \frac{\gamma_{SL} + \gamma_{SV}}{2} + \frac{\gamma_{SL} - \gamma_{SV}}{4} (3\phi - \phi^3) \quad (4.10)$$

characterizes the solid–fluid interface energies (Xu & Wang 2011). By Young's equation, $\partial_\phi L = -(3\gamma_{LV}/4) \cos \theta_Y(x) (1 - \phi^2)$, where $\theta_Y(x)$ depends on the location when the substrate is inhomogeneous.

In the phase-field model, the Cahn number Cn is a small parameter to describe the interface thickness. When we do averaging of the model on chemically patterned substrates, we must consider the size of the chemical inhomogeneity relative to Cn . When the pattern size is much smaller than Cn , we may not observe the CAH and obtain only a Cassie equation for the apparent contact angle (Xu & Wang 2010). When the pattern size is much larger than Cn , which is the case we are more interested in, we may first consider the sharp-interface limit (Sibley *et al.* 2013; Xu, Di & Yu 2018) and then do averaging. The results would be similar to those in this paper but in a different form.

Similar discussions can be made for some other contact line models, such as the model with a precursor thin film (Sharma 1993; Schwartz & Eley 1998; Pismen & Pomeau 2000) and the model from density functional theory (Nold *et al.* 2014; Yatsyshin, Savva & Kalliadasis 2015). In these models, the long range interaction between the substrate and the liquid molecules plays an important role. The contact angle is no longer defined microscopically in the vicinity of the contact line. For example, there exists a liquid thin film even on a partial wetting regime in the precursor film model (Eggers 2005). Then the inhomogeneity of the substrate makes the disjoining pressure and the thickness of the precursor film dependent on location. Although our analysis does not apply to this model directly, the main results might still be applicable if one considers the apparent contact angle in a larger mesoscopic region where the microscopic details are not very relevant and an effective slip model is a good approximation (Savva & Kalliadasis 2011).

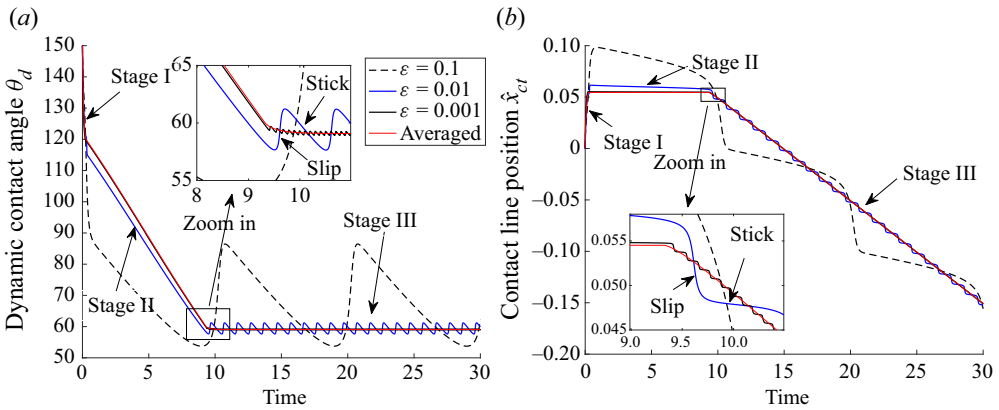


Figure 8. Receding dynamics for $\varepsilon = 0.1, 0.01, 0.001$ and $v = 0.01$ given $\theta_A = 60^\circ$ and $\theta_B = 120^\circ$. (a) Dynamical contact angle starting from $\theta_{init} = 150^\circ$. (b) The contact line position starting from $\hat{x}_{ct} = 0$.

5. Numerical experiments

In this section, we numerically solve the system (3.2), and its averaged system (3.24)–(3.25). From the numerical comparisons of the dynamics of θ_a and \hat{x}_{ct} with their averaged dynamics of Θ_a and \hat{X}_{ct} , we can verify our analytical results in the previous section. We apply the forward Euler scheme to numerically solve the system (3.2) and its averaged system (3.24)–(3.25).

5.1. Verification of the analysis

We first consider the case of a two-dimensional microscopic channel where the geometric factor is given by $g(\theta) = 4\mathcal{G}_1(\theta)$ and the dynamic factor is given by $f(\theta_a) = \mathcal{F}_1(\theta_a)/|\ln \zeta|$. We neglect the contact line friction ($\alpha = 0$) for simplicity. We use the sine pattern for $\varphi(y)$ with the two extrema being $\theta_A = 60^\circ$ and $\theta_B = 120^\circ$. The cutoff parameter is set to be $\zeta = 100$.

Figure 8 shows the evolutionary behaviour of the dynamic contact angle θ_a and the contact line position \hat{x}_{ct} modelled by (3.2) with different periods $\varepsilon = 10^{-1}, 10^{-2}$ and 10^{-3} . The dimensionless velocity is $v = 0.01$, and the initial contact angle is $\theta_{init} = 150^\circ$. It shows a clear three-stage process.

- (i) In the first stage, since the initial contact angle is greater than $\theta_B = 120^\circ$ and the wall velocity is positive, the averaged dynamics (3.25) predicts that the contact line \hat{x}_{ct} moves to the positive direction and the contact angle θ_a decreases towards θ_B . This is consistent with the numerical results of the original dynamics (3.2) (shown by red curves), in particular for small ε as depicted by the solid blue and black curves. Moreover, this stage is very short and thus is transient.
- (ii) When θ_a is around $\theta_B = 120^\circ$, the second-stage dynamics emerges. The contact line moves very slowly as if it stays almost unchanged, but the contact angle continues to recede. This behaviour is consistent with the prediction by the averaged dynamics (3.24).
- (iii) As the receding angle achieves some value around $\theta_A = 60^\circ$, the dynamical process goes into the third stage. The contact angle oscillates around the effective receding contact angle given by (3.26). There are also oscillations for the contact line

Dynamical contact angle hysteresis

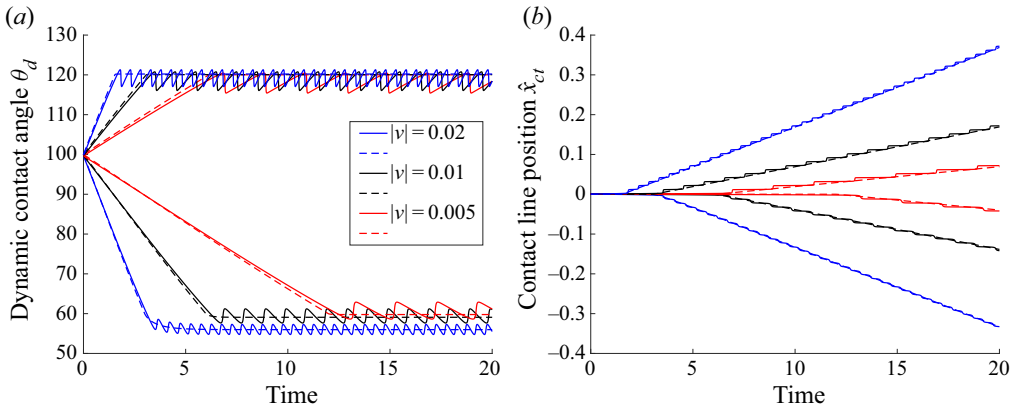


Figure 9. Advancing and receding dynamics for $\varepsilon = 0.01$ and $v = \pm 0.02, \pm 0.01, \pm 0.005$ given $\theta_A = 60^\circ$ and $\theta_B = 120^\circ$. (a) Dynamical contact angle starting from $\theta_{init} = 100^\circ$. (b) The contact line position starting from 0. From top to bottom, the solid curves represent the contact angle and contact line motion in the original dynamics. The dashed curves are the corresponding averaged dynamics.

position \hat{x}_{ct} . However, the averaged position of the contact line increases linearly with respect to the time.

In the third stage, the contact line moves to the negative direction relative to the wall with a stick-slip effect. Take the $\varepsilon = 0.01$ case for example (in the zoom-in plot). As the contact angle achieves approximately 57.5° , the contact line starts to move fast (e.g. the zoom-in plot of the $\varepsilon = 0.01$ curve when $t = 9.5$). This fast movement of \hat{x}_{ct} in turn leads to a fast increase of θ_a until θ_a arrives at approximately 62° . This is the slip behaviour of the contact line. When θ_a is around 62° , the deviation of θ_a from $\varphi(\hat{x}_{ct})$ is small so that the contact line moves very slowly as if it sticks there (e.g. $\hat{x}_{ct} \approx 0.047$ in the zoom-in plot of the $\varepsilon = 0.01$ curve). The angle θ_a decreases slowly towards 57.5° and another stick-slip period follows. Both the oscillation of the contact angle and the stick-slip of the contact line position share the same period proportional to ε . The stick-slip motion has also been discussed in detail in Xu & Wang (2020).

Figure 8 also shows that the dynamics of the contact angle and the contact line position converges to the averaged dynamics (red curves) modelled by (3.24) and (3.25) as the period ε decreases. When $\varepsilon = 10^{-3}$, the differences between the original dynamics and the averaged dynamics is quite small.

When v is negative, the situation is similar to that shown in figure 8. In this case, one will observe the effective advancing contact angle in the third stage instead (also see the plots in figure 9). For the other choices of θ_A, θ_B and initial angle θ_{init} , the numerical results are also similar except that the three-stage behaviour may be replaced by a two-stage process or a one-stage process depending on whether θ_{init} is inside or outside $[\theta_A, \theta_B]$.

Figure 9 shows the effect of velocity v on the dynamics. In these experiments, we fix $\varepsilon = 0.01$, $\theta_{init} = 100^\circ$ and vary the dimensionless velocity v from 0.02 to -0.02. As shown by the bottom three groups of curves in figure 9, when $v > 0$, the contact angle θ_a decreases towards the receding angle and the contact line position \hat{x}_{ct} moves to the negative direction. In the stick-slip stage, the effective contact line velocity in the averaged dynamics is exactly equal to the wall velocity v . The effective receding angle also depends on v . As $|v|$ becomes smaller, the effective receding angle is closer to $\theta_A = 60^\circ$ from below. In the case $v < 0$, the advancing dynamics is observed and θ_a increases until it starts

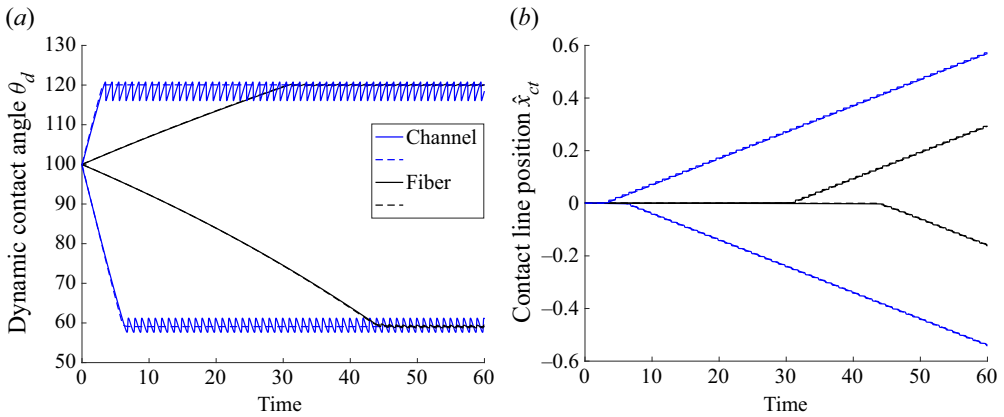


Figure 10. Advancing and receding dynamics for $\varepsilon = 0.01$ and $v = \pm 0.01$ given $\theta_A = 60^\circ$ and $\theta_B = 120^\circ$. (a) Dynamical contact angle starting from $\theta_{init} = 100^\circ$. (b) The contact line position starting from 0. From top to bottom, the solid curves represent the contact angle and contact line dynamics with respect to $v = -0.01$ and $v = 0.01$. Black curves show the dynamics in the case of a fibre while blue curves show the dynamics in the case of a microscopic channel. The dashed curves are the corresponding averaged dynamics.

to oscillate around the effect advancing angle. Then, \hat{x}_{ct} moves to the positive direction with an averaged velocity equal to v . As $|v|$ becomes smaller, the effective advancing angle is closer to $\theta_B = 120^\circ$ from above. This validates our analysis in § 3.1. Moreover, the sensitivities of the effective receding and advancing contact angles to $|v|$ are different and asymmetric in this case.

Finally, we will study the effect of the geometric factor $g(\theta_a)$. We solve the problem (3.2) for two different choices of g , which correspond to the moving contact line problems in a microscopic channel ($g = 4\mathcal{G}_1$) and on a moving fibre ($g = 4\mathcal{G}_2$). Figure 10 shows the dynamics of the advancing and receding angles. It is clear that the geometric factor affects the dynamic process, especially the first two stages. The contact angle approaches its equilibrium value in the micro-channel case much faster than it does in the moving fibre case. However, the effective advancing and receding angles are the same in the two cases and they only depend on the dynamic factor $f(\theta_a)$, as shown by (3.26).

5.2. Comparison with experimental results

In this subsection, we will use our model and analysis to explain the experimental results of Guan *et al.* (2016a,b). There, the dynamic CAH is observed by careful design of physical experiments. A very thin glass fibre with an inhomogeneous surface is inserted into a liquid reservoir. The fibre moves up and down so that a contact line moves on its surface. The capillary forces on the fibre are measured by atomic force microscopy (AFM) and the effective contact angles are computed. Several liquids with different surface tensions, viscosities and equilibrium angles are tested in their experiments. Many interesting phenomena are observed in the experiments. It is found that the dependence of the advancing and receding contact angles on the fibre velocity is not unified (see figure 6 in Guan *et al.* 2016b). In some cases (e.g. the water–air system), the dependence of the advancing and receding contact angles on the velocity is very asymmetric. In some cases (e.g. the octanol–air system), this dependence seems symmetric. In some other cases (e.g. the FC77–air system), the advancing and receding contact angles are all very small and close to each other.

To compare with the experiments, we use the reduced model (2.24) which is an approximation for the problem in Guan *et al.* (2016b). The radius of the fibre is $r_0 = 1.1 \mu\text{m}$ which is consistent with the experiment. We suppose the surface of the fibre is composed of two different materials *A* and *B* with different Young's angles θ_A and θ_B . On the surface, the pattern of the Young's angle $\varphi(z)$ is a piecewise constant periodic function with $\varphi_\chi(z) = \theta_A$ if $0 \leq z < \chi$ and $\varphi_\chi(z) = \theta_B$ if $\chi \leq z < 1$, where χ is the percentage of material *A* in a period. For the convenience in numerical computations, we smooth this discontinuous pattern by a hyperbolic tangent function

$$\varphi_\chi^\delta(z) = \frac{\theta_A + \theta_B}{2} + \frac{\theta_B - \theta_A}{2} \tanh\left(\frac{\sin(2\pi z) - \sin(\chi - 1/2)\pi}{\delta}\right), \tag{5.1}$$

where $\delta \ll 1$ is chosen to control the thickness of the smooth transition between two patterns. We use φ_χ^δ in our simulations. Here, θ_A and θ_B can be chosen approximately according to the receding and advancing contact angles in the experiments with the smallest moving speed. We choose the fraction χ and the dimensionless friction coefficient α as fitting parameters. The dimensionless wall velocity is represented by $v = \mu u_{\text{wall}}/\gamma$, where the fibre speed $|u_{\text{wall}}|$ is suggested by the experiments as $2 \mu\text{m s}^{-1}$, $5 \mu\text{m s}^{-1}$, $20 \mu\text{m s}^{-1}$ and $50 \mu\text{m s}^{-1}$. We refer to table 1 of Guan *et al.* (2016b) for the material properties, especially the surface tension γ and the viscosity μ . Since the capillary lengths of the materials under consideration have the range 0.86–2.71 mm, we choose it to be $l_c = 1\text{mm}$. The logarithm of the cutoff parameter is fixed at $\ln \zeta = 10$. As we observe in the numerical experiments, the variation of $\ln \zeta$ in its reasonable regime (of order $O(10)$) does not affect the results too much.

The numerical results are given in figure 11. We could see that the dependence of the CAH on the capillary number is not unified. For all the four cases, the advancing and receding contact angles and their dependence on the wall velocity are similar to those in the experiments in Guan *et al.* (2016a,b). The numerical results also agree with the discussions in § 4.1 based on the formula (3.26) of the effective contact angle. This also indicates that the experimental observations may be understood from our theoretical analysis in § 3, especially (3.26) on the effective contact angles. There we show that effective advancing and receding contact angles depend on the capillary number, the friction coefficient, the Young's angles of the inhomogeneous substrate and also the spatial distributions of the patterns. All these parameters have important impacts and the interplay among them gives rise to very complicated experimental phenomena.

In real experiments, there are always thermal noises which affect the dynamics of the contact line. To make the numerical results more comparable to the experiments, we add a stochastic force in (2.7) to model other non-deterministic effects, e.g. thermal noises. The resulting stochastic system for the apparent contact angle θ_d and contact line position \hat{x}_{ct} reads

$$\left. \begin{aligned} \dot{\theta}_d &= g(\theta_d)(f(\theta_d)(\cos \hat{\theta}_Y(\hat{x}_{ct}) - \cos \theta_d + \sigma \dot{W}) + v), \\ \dot{\hat{x}}_{ct} &= f(\theta_d)(\cos \hat{\theta}_Y(\hat{x}_{ct}) - \cos \theta_d + \sigma \dot{W}). \end{aligned} \right\} \tag{5.2}$$

This system of equations should be understood in the Itô sense. Since the contact angle and the contact line position are linked by the kinematic constraint (e.g. (2.12) and (2.21)) through the geometric factor $g(\theta_d)$, they are driven by the same Brownian motion $W(t)$. We choose the noise level to be small so that it does not affect the dynamics too much. We then numerically solve (5.2) for one sample path using the Euler–Maruyama scheme. Numerical results by solving the stochastic equation (5.2) are shown in figure 12. We could see a similar velocity dependence of the CAH as that in figure 11 in the deterministic case.

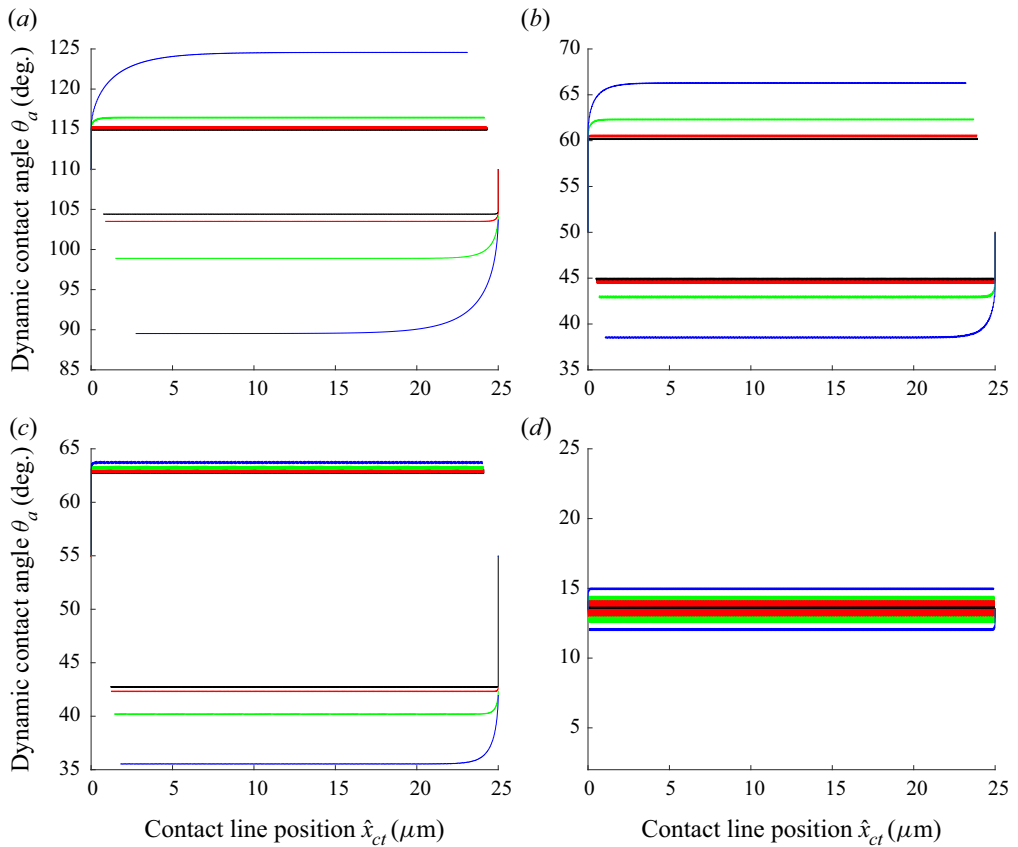


Figure 11. Dependence of CAH on different wall speeds. The dimensional period of the chemical pattern is set to be $\varepsilon = 0.05 \mu\text{m}$. (a) Water–air, $\theta_A = 105^\circ$, $\theta_B = 115^\circ$, $\alpha = 4 \times 10^5$ and $\chi = 0.9$. (b) Octanol–air, $\theta_A = 45^\circ$, $\theta_B = 60^\circ$, $\alpha = 1 \times 10^4$ and $\chi = 0.4$. (c) Decane–air, $\theta_A = 43^\circ$, $\theta_B = 63^\circ$, $\alpha = 5 \times 10^4$ and $\chi = 0.9$. (d) FC77–air, $\theta_A = 13^\circ$, $\theta_B = 14^\circ$, $\alpha = 1 \times 10^3$ and $\chi = 0.4$. The black, red, green and blue curves represent the results with fibre speeds of $|u_{wall}| = 2 \mu\text{m/s}$, $5 \mu\text{m/s}$, $20 \mu\text{m/s}$ and $50 \mu\text{m/s}$, respectively.

Moreover, the dynamic behaviours fit well with the experiments for all the four cases, i.e. the water–air, octanol–air, decane–air and FC77–air systems (Guan *et al.* 2016b).

In the end, we would like to remark that the previous comparisons with experiments are almost quantitative, since the fibre velocities are chosen to be the same as in the experiments. Here, we choose the fraction χ of the chemical pattern as a fitting parameter. The reason can be understood as follows. In our simplified model, we assume that the contact line on the fibre is circular and the liquid–air interface is axisymmetric. This assumption does not hold in real experiments, where the chemical inhomogeneity is very complex on the fibre surface. The relaxation behaviour of the contact line is much more complicated than that in our model. Although it is possible to use a circular curve to approximate the contact line on such surfaces by homogenization (Joanny & De Gennes 1984; Xu 2016), the effective pattern in the axial direction might be different for different liquids even on the same substrate. This is due to the fact that the correlation length of the oscillating contact line can be very different (Golestanian & Raphaël 2003; Golestanian 2004). Actually, this can be seen from the experiments in

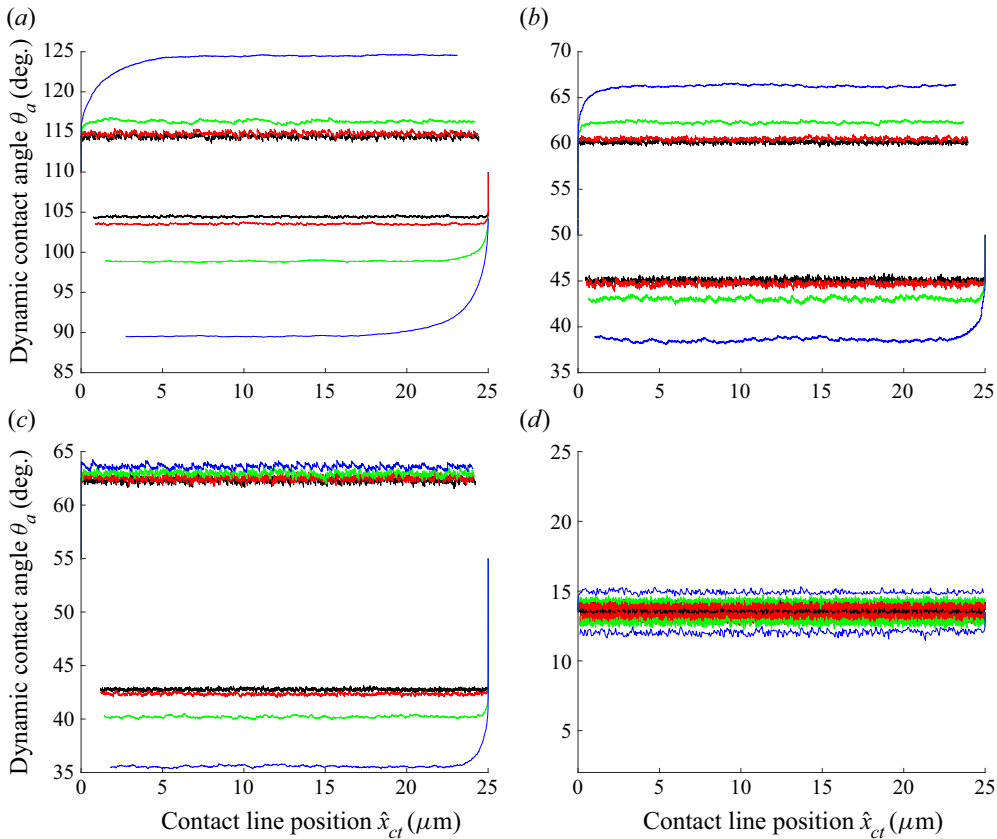


Figure 12. Dependence of CAH on different wall speeds in the presence of noise. The dimensional period of the chemical pattern is set to $\varepsilon = 0.05 \mu\text{m}$. The noise level σ is chosen case by case without affecting the effective advancing and receding angles. (a) Water–air, $\theta_A = 105^\circ$, $\theta_B = 115^\circ$, $\alpha = 4 \times 10^5$, $\chi = 0.9$ and $\sigma = 0.1$. (b) Octanol–air, $\theta_A = 45^\circ$, $\theta_B = 60^\circ$, $\alpha = 1 \times 10^4$, $\chi = 0.4$ and $\sigma = 0.02$. (c) Decane–air, $\theta_A = 43^\circ$, $\theta_B = 63^\circ$, $\alpha = 5 \times 10^4$, $\chi = 0.9$ and $\sigma = 0.03$. (d) FC77–air, $\theta_A = 13^\circ$, $\theta_B = 14^\circ$, $\alpha = 1 \times 10^3$, $\chi = 0.4$ and $\sigma = 0.002$. The black, red, green and blue curves represent the results with fibre speeds at $|u_{wall}| = 2 \mu\text{m}$, $5 \mu\text{m}$, $20 \mu\text{m}$ and $50 \mu\text{m}$, respectively.

Guan *et al.* (2016b), where the periods of the effective patterns seem very different for different fluids. The characterization of dynamic CAH on general surfaces with chemical and geometrical roughness in three dimensions is very interesting and will be left for future work.

6. Conclusion

In this paper, we derive a formula (4.1) for the apparent contact angles on chemically inhomogeneous surfaces. It can be regarded as a Cox-type boundary condition for the time averaged apparent contact angle on these surfaces. The formula characterizes quantitatively how the averaged advancing and receding contact angles depend on the velocity, the Young’s angles and the distributions of the chemical inhomogeneities. It can be used to understand the complicated behaviours for the dynamic CAH observed in experiments.

The derivation of the above formula is based on a reduced model for the macroscopic contact angle for moving contact line problems. Without considering the contact line

friction, the model is a leading-order approximation for the famous Cox's formula for small capillary number and is easier to analyse in cases with inhomogeneous surfaces. The reduced model is derived by using the Onsager principle as an approximation tool, which is much simpler than the standard asymptotic matching methods used in Cox (1986).

Although the main result is obtained by averaging the reduced model for a liquid–vapour system with small size, it can be generalized to other two-phase flow systems using the same averaging technique. In particular, it is straightforward to do averaging for the Cox's boundary condition and derive a similar formula (4.8). These formulae can be used coupled with the standard two-phase Navier–Stokes equation. This will lead to a coarse-graining model for two-phase flow systems on chemically inhomogeneous surfaces. The dynamic CAH is given by these formulae and one does not need to resolve the microscopic inhomogeneity of the solid surfaces as in Yue (2020).

We mainly focus on the two-dimensional problem in the paper. But the results are useful for three-dimensional problems when the inhomogeneity is simple. For example, when the defect is dilute, the static advancing and receding contact angles have been derived by Joanny & De Gennes (1984). Then it is possible to reduce the three-dimensional problem to a two-dimensional one by symmetry assumptions. Thus, one can apply the results in this paper to these problems. Some other problems may be handled in a similar way by combining our analysis with the modified Cassie–Baxter equation for static CAH in Choi *et al.* (2009), Xu & Wang (2013) and Xu (2016).

For more general three-dimensional problems with rough or chemically inhomogeneous surfaces, the relaxation dynamics of the contact line is very complicated. The CAH may also depend on the depinning processes of a contact line even in quasi-static processes (Choi *et al.* 2009; Iliev *et al.* 2018). For dynamical problems, the correlations and roughening processes of the contact line make the problem even more complicated (Golestanian & Raphaël 2003; Golestanian 2004). Both the time averaging and the spatial homogenization need to be considered simultaneously. The analysis for these problems will be left for future work.

Finally, we would like to remark that we mainly discussed Cox-type boundary conditions in this paper. However, these conditions might fail to predict the experimental observations when the flow field is very complex near the contact line (Blake, Bracke & Shikhmurzaev 1999; Clarke & Stattersfield 2006; Davis & Davis 2013; Mohammad Karim, Davis & Kavehpour 2016). This fact has been highlighted in a recent work (Shikhmurzaev 2020). There, the author presents some examples as a 'litmus test' for the mathematical models for moving contact lines and concludes that the standard models like the Cox's boundary condition cannot explain the contact line motion in all situations. The apparent contact angle cannot be described by a single function of the contact line velocity in those examples. A model that might pass the test is the interface formation model (Shikhmurzaev 1993, 2007). In this model, wetting of a substrate is induced by formation of a new liquid–solid interface and the process is described by some complicated partial differential equations. The contact angle is still given by Young's equation while the surface tensions are not constants. Although there are some controversies on this model (Eggers & Evans 2004; Shikhmurzaev & Blake 2004; Lindner-Silvester & Schneider 2005; Shikhmurzaev 2006), its equivalence to the standard slip model has been recently shown in certain parameter regimes (Sibley, Savva & Kalliadasis 2012; Sibley *et al.* 2015*b*). It would be very interesting to study the homogenization of the interface formation model on inhomogeneous or rough substrates (see discussions in e.g. Shikhmurzaev 2020). This is outside of the scope of this paper.

Funding. The work of Z.Z. was partially supported by the NSFC grant (No. 11731006, No. 12071207), the Guangdong Provincial Key Laboratory of Computational Science and Material Design (No. 2019B030301001) and the Guangdong Basic and Applied Basic Research Foundation (2021A1515010359). The work of X.X. partially supported by the NSFC grant (No. 11971469) and by the National Key R&D Program of China under Grant 2018YFB0704304 and Grant 2018YFB0704300.

Declaration of interests. The authors report no conflict of interest.

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Appendix A. Derivation for a continuum model for moving contact lines by the Onsager principle

Consider a region Ω near the contact line as in figure 13. For simplicity, we suppose Ω is a two-dimensional domain. The boundary of Ω is composed of two parts, the lower solid boundary Γ_S and the outer boundary Γ_O . On Γ_S , there exists a moving contact line, which is an intersection point between the solid boundary and the two-phase flow interface Γ . Then Ω represents an open system near the contact point. In the following, we will derive a sharp interface continuum model for moving contact lines. We adopt the Onsager principle to derive the model. The method has been used to develop the generalized Navier slip boundary condition for a diffuse interface model in Qian, Wang & Sheng (2006). In the derivation, we ignore the gravitational force and the inertial effect, which can be added simply if needed.

To use the Onsager principle, we first compute the rate of change of the total energy in the system. The total free energy consists of three interface energies

$$\mathcal{E} = \int_{\Gamma_{SA}} \gamma_{SA} ds + \int_{\Gamma_{SB}} \gamma_{SB} ds + \int_{\Gamma} \gamma ds, \tag{A1}$$

where Γ_{SA} and Γ_{SB} are respectively the parts of solid boundary in contact with the fluid A and fluid B, γ_{SA} and γ_{SB} are corresponding surface tensions and γ is the surface tension of the two-phase flow interface. Direct calculations give

$$\dot{\mathcal{E}} = \gamma (\cos \theta_d - \cos \theta_Y) v_{ct} + \gamma \int_{\Gamma} v_n \kappa ds. \tag{A2}$$

Here, θ_d is the dynamic contact angle with respect to the fluid A, θ_Y is Young’s angle, v_{ct} is the velocity of the contact line, $v_n = \mathbf{v} \cdot \mathbf{n}$ is the normal velocity and κ is the curvature of the interface. In the derivation, we have also used Young’s equation $\gamma \cos \theta_Y = \gamma_{SB} - \gamma_{SA}$.

The energy dissipation function, which is defined as half of the total energy dissipation rate in the system, can be written as

$$\begin{aligned} \Phi = & \int_{\Omega_A} \frac{\mu_A}{4} |\nabla \mathbf{v} + \nabla \mathbf{v}^T|^2 dx + \int_{\Omega_B} \frac{\mu_B}{4} |\nabla \mathbf{v} + \nabla \mathbf{v}^T|^2 dx + \int_{\Gamma_{SA}} \frac{\beta_A}{2} v_{\tau}^2 dx \\ & + \int_{\Gamma_{SB}} \frac{\beta_B}{2} v_{\tau}^2 dx + \frac{\xi}{2} v_{ct}^2, \end{aligned} \tag{A3}$$

where Ω_A and Ω_B are the regions in Ω occupied by fluid A and fluid B, respectively, \mathbf{v} is the corresponding velocity field, v_{τ} is the slip velocity on the solid boundary, μ_A and μ_B are viscosity parameters, β_A and β_B are phenomenological slip coefficients and ξ is

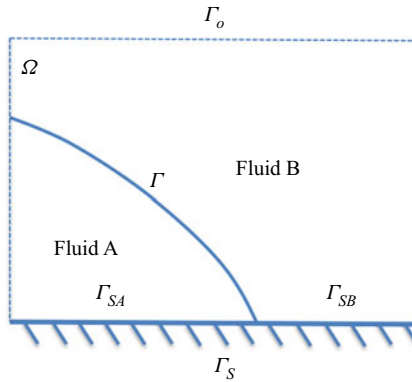


Figure 13. A domain of two-phase flow with a moving contact line.

the friction coefficient of the contact line. The normal velocity on the solid boundary Γ_S is zero.

Since the system is an open system, we need also to consider the work to the outer fluids at the boundary Γ_O . It is given by

$$\dot{\mathcal{E}}^* = - \int_{\Gamma_O} \mathbf{F}_{ext} \cdot \mathbf{v} \, ds = - \int_{\Gamma_{OA}} \mathbf{F}_{ext} \cdot \mathbf{v}_A \, ds - \int_{\Gamma_{OB}} \mathbf{F}_{ext} \cdot \mathbf{v}_B \, ds, \quad (\text{A4})$$

where Γ_{OA} and Γ_{OB} are the respective open boundaries in contact with fluid A and fluid B.

With the above definitions, the Onsager principle states that (Doi 2013) the dynamical equation of the system is given by minimizing the Onsager–Machlup action defined as follows:

$$O = \dot{\mathcal{E}} + \dot{\mathcal{E}}^* + \Phi, \quad (\text{A5})$$

under the constraint of incompressibility condition

$$\nabla \cdot \mathbf{v} = 0. \quad (\text{A6})$$

Introduce a Lagrangian multiplier $p(x)$ in Ω . We minimize the following modified functional with respect to the velocity:

$$\mathcal{R}_\lambda = \dot{\mathcal{E}} + \dot{\mathcal{E}}^* + \Phi - \int_{\Omega_A \cup \Omega_B} p \nabla \cdot \mathbf{v} \, dx. \quad (\text{A7})$$

Direct calculation for the first variation of \mathcal{R}_λ gives

$$\begin{aligned} \delta \mathcal{R}_\lambda = & \int_{\Gamma} \gamma \kappa \delta v_n \, ds + \gamma (\cos \theta_a - \cos \theta_b) \delta v_{ct} - \int_{\Gamma_O} \mathbf{F}_{ext} \cdot \delta \mathbf{v} \, ds \\ & + \int_{\Omega_A} \frac{\mu_A}{2} (\nabla \mathbf{v} + \nabla \mathbf{v}^T) : (\nabla \delta \mathbf{v} + \nabla \delta \mathbf{v}^T) \, dx + \int_{\Omega_B} \frac{\mu_B}{2} (\nabla \mathbf{v} + \nabla \mathbf{v}^T) : (\nabla \delta \mathbf{v} + \nabla \delta \mathbf{v}^T) \, dx \\ & + \int_{\Gamma_{SA}} \beta_A v_\tau \delta v_\tau \, ds + \int_{\Gamma_{SB}} \beta_B v_\tau \delta v_\tau \, ds + \xi v_{ct} \delta v_{ct} - \int_{\Omega_A \cup \Omega_B} p \nabla \cdot \delta \mathbf{v} \, dx. \end{aligned} \quad (\text{A8})$$

Integration by parts gives

$$\begin{aligned} & \int_{\Omega_A} \frac{\mu_A}{2} (\nabla \mathbf{v} + \nabla \mathbf{v}^T) : (\nabla \delta \mathbf{v} + \nabla \delta \mathbf{v}^T) \, dx \\ &= \int_{\partial \Omega_A} \mu_A (\nabla \mathbf{v} + \nabla \mathbf{v}^T) \mathbf{n} \cdot \delta \mathbf{v} \, dx - \int_{\Omega_A} \nabla \cdot (\mu_A (\nabla \mathbf{v} + \nabla \mathbf{v}^T)) \cdot \delta \mathbf{v} \, dx, \end{aligned} \quad (\text{A9})$$

and

$$- \int_{\Omega_A} p \nabla \cdot \delta \mathbf{v} \, dx = - \int_{\partial \Omega_A} p \mathbf{n} \cdot \delta \mathbf{v} \, dx + \int_{\Omega_A} \nabla p \cdot \delta \mathbf{v} \, dx. \quad (\text{A10})$$

Similar calculations can be done in Ω_B . Combing all these calculations, we immediately derive the corresponding Euler–Lagrange equation for (A7)

$$\left. \begin{aligned} -\nabla \cdot (\mu (\nabla \mathbf{v} + \nabla \mathbf{v}^T)) + \nabla p &= 0 \\ \nabla \cdot \mathbf{v} &= 0 \end{aligned} \right\} \text{ in } \Omega, \quad (\text{A11})$$

coupled with the interface condition on Γ

$$[\mathbf{v}] = 0, \quad [\mu (\nabla \mathbf{v} + \nabla \mathbf{v}^T) - p \mathbf{I}] \mathbf{n} = \gamma \kappa \mathbf{n} \quad \text{on } \Gamma, \quad (\text{A12})$$

the Navier slip boundary condition on Γ_S

$$v_n = 0, \quad \beta(x) v_\tau = -\mu \frac{\partial v_\tau}{\partial n} \quad \text{on } \Gamma_S \quad (\text{A13})$$

and the condition for the moving contact line

$$\xi v_{ct} = -\gamma (\cos \theta_d - \cos \theta_Y). \quad (\text{A14})$$

Here

$$\mu(x) = \begin{cases} \mu_A, & \text{if } x \in \Omega_A; \\ \mu_B, & \text{if } x \in \Omega_B; \end{cases} \quad \text{and} \quad \beta(x) = \begin{cases} \beta_A, & \text{if } x \in \Gamma_{SA}; \\ \beta_B, & \text{if } x \in \Gamma_{SB}. \end{cases} \quad (\text{A15a,b})$$

On the outer boundary Γ_O , we also have a relation for the external force such that

$$\mathbf{F}_{ext} = (\mu (\nabla \mathbf{v} + \nabla \mathbf{v}^T) - p \mathbf{I}) \mathbf{n}. \quad (\text{A16})$$

The boundary condition (A14) for moving contact lines is exactly the model derived in Ren & E (2007). Specifically, when $\xi = 0$, the condition is reduced to

$$\theta_d = \theta_Y. \quad (\text{A17})$$

This implies that the microscopic dynamic contact angle is equal to the Young’s angle. Together with the Navier slip boundary condition (A13), this is the model used in the asymptotic analysis in Cox (1986).

Therefore, the above analysis indicates that some well-known continuum models for moving contact lines can be derived in a variational framework of the Onsager principle.

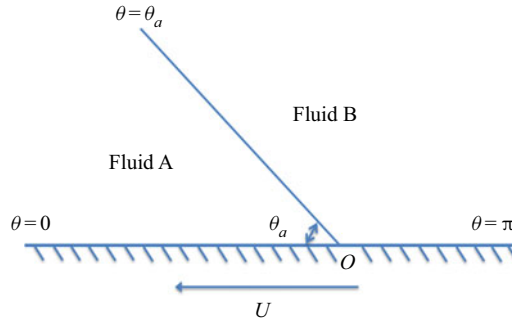


Figure 14. The wedge region near the moving contact point.

Appendix B. Calculate the energy dissipation in a wedge region

Since we assume the region is in steady state, Φ_{vis} can be computed by solving the Stokes equation in the region. For simplicity, we can change variables and consider the problem as shown in figure 14. We choose a polar coordinate system (r, ϕ) near the contact point. Let the contact point locate at the origin O . The polar axis is in the right direction. In this system, the solid boundary will have a velocity $U = -v_{ct}$, as shown in figure 14. The viscous energy dissipation in the wedge region can be computed by solving the Stokes equations

$$\left. \begin{aligned} -\mu_A \Delta v_A + \nabla p_A &= 0, \\ \text{div} v_A &= 0, \end{aligned} \right\} \text{ in Region A;} \tag{B1}$$

and

$$\left. \begin{aligned} -\mu_B \Delta v_B + \nabla p_B &= 0, \\ \text{div} v_B &= 0, \end{aligned} \right\} \text{ in Region B.} \tag{B2}$$

We use no slip boundary condition on Γ_S . The two-phase flow interface is assumed unchanged with time. Then the Stokes equation can be solved by the biharmonic equation.

We now calculate the dissipation in the wedge. To solve the problem, we apply the computations in Cox (1986). Introduce two streamfunctions ψ_A and ψ_B . We have

$$(v_A)_r = \frac{1}{r} \frac{\partial \psi_A}{\partial \phi}, \quad (v_A)_\phi = -\frac{\partial \psi_A}{\partial r}. \tag{B3a,b}$$

Here, $(v_A)_r$ is the velocity in the radial direction, and $(v_A)_\phi$ is the velocity in the angular direction. Similar formulae hold for v_B . Then we have

$$\Delta^2 \psi_A = 0, \quad \Delta^2 \psi_B = 0. \tag{B4a,b}$$

The equations should satisfy the boundary conditions on the solid surface. We choose the no-slip boundary condition for the velocity except in the vicinity of the contact line when $r < l$ with the microscopic length l is a cutoff parameter. When $r > l$, we have

$$\psi_A = 0, \quad \frac{\partial \psi_A}{\partial \phi} = Ur, \quad \text{on } \phi = 0; \tag{B5}$$

$$\psi_B = 0, \quad \frac{\partial \psi_B}{\partial \phi} = -Ur, \quad \text{on } \phi = \pi. \tag{B6}$$

On the interface $\phi = \theta_a$, we have

$$\left. \begin{aligned} \frac{\partial \psi_A}{\partial r} = \frac{\partial \phi_B}{\partial r} = 0, \\ \frac{\partial \psi_A}{\partial \phi} = \frac{\partial \psi_B}{\partial \phi}, \\ \frac{1}{r^2} \frac{\partial^2 \psi_A}{\partial \phi^2} - \frac{\partial^2 \psi_A}{\partial r^2} + \frac{1}{r} \frac{\partial \psi_A}{\partial r} = \lambda \left(\frac{1}{r^2} \frac{\partial^2 \psi_B}{\partial \phi^2} - \frac{\partial^2 \psi_B}{\partial r^2} + \frac{1}{r} \frac{\partial \psi_B}{\partial r} \right), \end{aligned} \right\} \quad (B7)$$

where $\lambda = \mu_A/\mu_B$.

The biharmonic equations in the wedge domains can be solved combining the above boundary and interface conditions. This leads to

$$\psi_A = Ur ((C_A\phi + D_A) \cos \phi + (E_A\phi + F_A) \sin \phi); \quad (B8)$$

$$\psi_B = Ur ((C_B\phi + D_B) \cos \phi + (E_B\phi + F_B) \sin \phi). \quad (B9)$$

Here, the two groups of coefficients are given by

$$C_A = \sin \theta_a \left(-\lambda(\pi \sin \theta_a + \sin^2 \theta_a \cos \theta_a + \theta_a(\pi - \theta_a) \cos \theta_a) + \cos \theta_a(\sin^2 \theta_a - (\pi - \theta_a)^2) \right) / \delta; \quad (B10)$$

$$D_A = 0; \quad (B11)$$

$$E_A = \sin^2 \theta_a \left(-\lambda(\sin^2 \theta_a + \theta_a(\pi - \theta_a)) + \sin^2 \theta_a - (\pi - \theta_a)^2 \right) / \delta; \quad (B12)$$

$$F_A = \theta_a \left(\lambda(\sin^2 \theta_a + \theta_a(\pi - \theta_a) + \pi \sin \theta_a \cos \theta_a) + (-\sin^2 \theta_a + (\pi - \theta_a)^2) \right) / \delta; \quad (B13)$$

and

$$C_B = \frac{-D_B}{\pi} = \sin \theta_a \left(\lambda \cos \theta_a (\theta_a^2 - \sin^2 \theta_a) - \pi \sin \theta_a + \sin^2 \theta_a \cos \theta_a + \theta_a(\pi - \theta_a) \cos \theta_a \right) / \delta; \quad (B14)$$

$$E_B = \sin^2 \theta_a \left(\lambda(\theta_a^2 - \sin^2 \theta_a) + (\sin^2 \theta_a + \theta_a(\pi - \theta_a)) \right) / \delta; \quad (B15)$$

$$F_B = \left(\lambda(\sin^2 \theta_a - \theta_a^2)(\theta_a - \pi \cos^2 \theta_a) - \pi(\pi - \theta_a) \sin \theta_a \cos \theta_a - \theta_a \sin^2 \theta_a \right) / \delta; \quad (B1)$$

$$+ \pi \sin^2 \theta_a \cos^2 \theta_a + \pi(\pi - \theta_a)\theta_a \cos^2 \theta_a - (\pi - \theta_a)\theta_a^2) / \delta. \quad (B16)$$

Here

$$\delta = \lambda(\theta_a^2 - \sin^2 \theta_a)(\pi - \theta_a + \sin \theta_a \cos \theta_a) + \left((\pi - \theta_a)^2 - \sin^2 \theta_a \right) (\theta_a - \sin \theta_a \cos \theta_a). \quad (B17)$$

With the formula for ψ_A and ψ_B , we can compute the velocities in the two regions. For liquid A, we have

$$(v_A)_r = U ((C_A + F_A) \cos \phi + (E_A - D_A) \sin \phi - C_A\phi \sin \phi + E_A\phi \cos \phi), \quad (B18)$$

$$(v_A)_\phi = -U ((C_A\phi + D_A) \cos \phi + (E_A\phi + F_A) \sin \phi). \quad (B19)$$

Then we have

$$v_A = (v_A)_r \mathbf{r} + (v_A)_\phi \boldsymbol{\tau}, \tag{B20}$$

where \mathbf{r} and $\boldsymbol{\tau}$ are the unit vectors in the radial and angular directions, respectively. We have similar representations for v_B . The gradient of the velocity gives

$$\nabla v_A = \frac{2U}{r} (-C_A \sin \phi + E_A \cos \phi) \boldsymbol{\tau} \otimes \mathbf{r}. \tag{B21}$$

Similarly,

$$\nabla v_B = \frac{2U}{r} (-C_B \sin \phi + E_B \cos \phi) \boldsymbol{\tau} \otimes \mathbf{r}. \tag{B22}$$

Then the viscous energy dissipations in the wedge regions can be computed by

$$\begin{aligned} \Psi &= \int_{l_s}^R \int_0^{\theta_a} \frac{\mu_A}{2} |\nabla v_A + (\nabla v_A)^T|^2 r \, d\phi \, dr + \int_{l_s}^R \int_{\theta_a}^\pi \frac{\mu_B}{2} |\nabla v_B + (\nabla v_B)^T|^2 r \, d\phi \, dr \\ &= 2\mu_A |\ln \zeta| U^2 \left(C_A^2 (\theta_a - \sin \theta_a \cos \theta_a) + C_A E_A (\cos 2\theta_a - 1) + E_A^2 (\theta_a + \sin \theta_a \cos \theta_a) \right. \\ &\quad \left. + \lambda \left(C_B^2 (\theta_a - \sin \theta_a \cos \theta_a) + C_B E_B (\cos 2\theta_a - 1) + E_B^2 (\theta_a + \sin \theta_a \cos \theta_a) \right) \right). \end{aligned} \tag{B23}$$

Here, $\zeta = D/l$ is the cutoff parameter with D being the characteristic size of the mesoscopic region and l being the microscopic size. Direct calculations lead to

$$\begin{aligned} \Psi &= 2\mu_A |\ln \zeta| U^2 \\ &\quad \times \frac{\sin^2 \theta_a (\lambda^2 (\theta_a^2 - \sin^2 \theta_a) + 2\lambda (\sin^2 \theta_a + \theta_a (\pi - \theta_a)) + ((\pi - \theta_a)^2 - \sin^2 \theta_a))}{\lambda (\theta_a^2 - \sin^2 \theta_a) (\pi - \theta_a + \sin \theta_a \cos \theta_a) + ((\pi - \theta_a)^2 - \sin^2 \theta_a) (\theta_a - \sin \theta_a \cos \theta_a)}. \end{aligned} \tag{B24}$$

Appendix C. Properties of the averaged dynamics

In this section, we study the properties of the averaged dynamics (3.24) and (3.25). Without loss of generality, we assume $v > 0$. We also recall that f is a non-negative function satisfying $f(0) = 0$ and $f'(\theta) > 0$ for $\theta \in [0, \pi]$, g is a negative function bounded by $-M$ and $-m$. We consider the behaviour of the dynamic system for different regimes of Θ_a starting at $\Theta_a(0) > \theta_B$:

- (i) When $\Theta_a > \theta_B = \max_{0 \leq y \leq 1} \varphi(y)$, the averaged dynamics (3.25) is a good approximation. It yields the following properties:

- (a) Θ_a monotonically decreases at a speed of at least mv until it arrives at θ_B .

This is because the harmonic average

$$C(\Theta_a) = \left(\int_0^1 \frac{dz}{\cos \varphi(z) - \cos \Theta_a} \right)^{-1} \tag{C1}$$

is positive when $\Theta_a > \theta_B$. As a result, we have

$$\dot{\Theta}_a = g(\Theta_a) \left(f(\Theta_a) \left(\int_0^1 \frac{dz}{\cos \varphi(z) - \cos \Theta_a} \right)^{-1} + v \right) \leq -mv < 0. \tag{C2}$$

(b) \hat{X}_{ct} moves in the positive direction with a diminishing velocity.

In fact $C(\Theta_a) > 0$ for $\Theta_a > \theta_B$, and $C(\Theta_a) \rightarrow 0$ as $\Theta_a \rightarrow \theta_B$ from the right. This can be shown in a similar way to that in the classical Laplace's method in asymptotic analysis of integral. By expanding $\varphi(z)$ around its local maximizer z_0 (which is a local minimizer of $\cos \varphi(z)$), we have

$$\begin{aligned} & \int_0^1 \frac{dz}{\cos \varphi(z) - \cos \Theta_a} \\ & \geq \int_{z_0}^{z_0+\eta} \frac{dz}{\cos \theta_B + (z - z_0)^2 (\cos \varphi)''(z_0) + O((z - z_0)^3) - \cos \Theta_a} \\ & \sim \frac{\frac{\pi}{2}}{\sqrt{(\cos \varphi)''(z_0)(\cos \theta_B - \cos \Theta_a)}} \rightarrow +\infty \quad \text{as } \Theta_a \rightarrow \theta_B, \end{aligned} \quad (C3)$$

where η is a small positive number. As a result, $C(\Theta_a)^{-1}$ diverges to $+\infty$ as $\Theta_a \rightarrow \theta_B$ from the right.

(c) Θ_a approaches θ_B exponentially fast.

In fact, multiplying $\sin \Theta_a$ on both sides of (3.25a), we have

$$\begin{aligned} & \frac{d}{dt}(\cos \theta_B - \cos \Theta_a) \\ & = g(\Theta_a) \sin \Theta_a \left[f(\Theta_a) \left(\int_0^1 \frac{dz}{\cos \varphi(y) - \cos \theta_B + \cos \theta_B - \cos \Theta_a} \right)^{-1} + v \right] \\ & \leq -m\beta(f(\theta_B)(\cos \theta_B - \cos \Theta_a) + v), \end{aligned} \quad (C4)$$

where $\beta = \min\{\sin \Theta_a(0), \sin \theta_B\}$ and we have used the relation $\Theta_a \geq \theta_B = \max_{0 \leq y \leq 1} \varphi(y)$. An application of Gronwall's inequality implies that

$$\begin{aligned} \cos \theta_B - \cos \Theta_a & \leq (\cos \theta_B - \cos \Theta_a(0)) \exp(-m\beta f(\theta_B)t) \\ & \quad - \frac{v}{f(\theta_B)} (1 - \exp(-m\beta f(\theta_B)t)). \end{aligned} \quad (C5)$$

It can be seen that Θ_a decreases exponentially fast and arrives at θ_B at some finite time t_1^* . Moreover, it is easily estimated that

$$t_1^* \leq \frac{1}{m\beta f(\theta_B)} \ln \left(1 + \frac{(\cos \theta_B - \cos \Theta_a(0))f(\theta_B)}{v} \right). \quad (C6)$$

The time period $[0, t_1^*]$ is a transient period for the dynamics of Θ_a and \hat{X}_{ct} .

(ii) When $\Theta_a \in [\theta_A, \theta_B]$, the effective dynamics follows (3.24) which yields the following properties:

(a) The effective apparent contact angle $\Theta_a(t)$ decreases monotonically.

In fact, it is straightforward to show that $(d/dt)\Theta_a \leq -vm$ and $\Theta_a(t) \leq -vm(t - t_1^*) + \theta_B$. Therefore, $\Theta_a(t)$ must arrive at θ_A at some finite time t_2^* with $t_2^* \leq t_1^* + (\theta_B - \theta_A)/vm$.

(b) The effective contact line position \hat{X}_{ct} remains unchanged.

(iii) When $\Theta_a < \theta_A = \min_{0 \leq y \leq 1} \varphi(y)$, the dynamics of the effective contact angle and contact point position are given by (3.25a) and (3.25b). This dynamic system has the

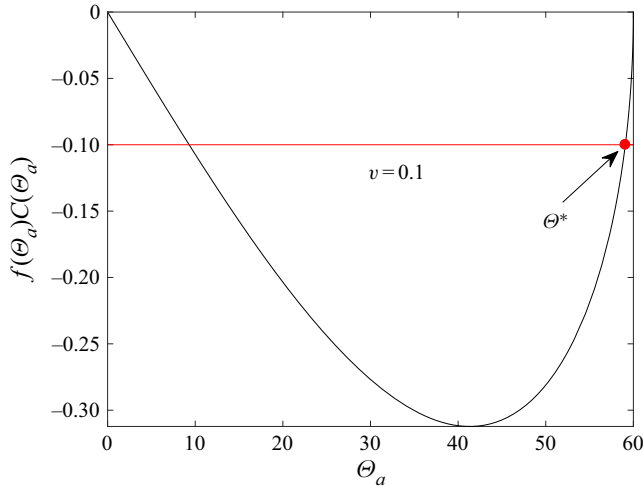


Figure 15. Sketch of the function $f(\Theta_a)C(\Theta_a)$ in the case that $v = 0.1$, f is given by \mathcal{F}_1 in (2.14) and φ is given by (3.5) with $\theta_A = 60^\circ$ and $\theta_B = 120^\circ$. The red point represents the steady apparent contact angle Θ^* closest to θ_A . It is clear that $f(\Theta_a)C(\Theta_a)$ is non-decreasing at Θ^* .

following properties:

- (a) Θ_a eventually arrives at a stable steady state $\Theta^* \in (0, \theta_A)$ satisfying $f(\Theta^*)C(\Theta^*) = -v$.

In fact, $f(\Theta_a) > 0$ and $C(\Theta_a) < 0$ for $0 < \Theta_a < \theta_A$. Since $C(\Theta_a) \rightarrow 0$ as $\Theta_a \rightarrow \theta_A$ from the left (similar to the proof in case (i)(b)), we also have $f(\Theta_a)C(\Theta_a) = 0$ when $\Theta_a = 0$ or θ_A . Then the equation $f(\Theta_a)C(\Theta_a) + v = 0$ has at least two roots in $(0, \theta_A)$ for small $v > 0$. As a result, the dynamics (3.25a) admits at least two steady states. As Θ_a starts from θ_A in this regime, we are interested in the steady state closest to θ_A . We denote this state as Θ^* .

We have that Θ^* is asymptotically stable or semi-stable if the right-hand side of (3.25a) has a non-positive derivative at $\Theta_a = \Theta^*$. Since $g(\Theta_a) < 0$, direct calculation shows that this is equivalent to verifying the derivative of $f(\Theta_a)C(\Theta_a)$ is non-negative at $\Theta_a = \Theta^*$ (see figure 15). This can also be proved by contradiction: suppose the derivative of $f(\Theta_a)C(\Theta_a)$ is negative at $\Theta_a = \Theta^*$, then $f(\Theta_a)C(\Theta_a)$ is decreasing nearby $\Theta_a = \Theta^*$, and we can find $\Theta^{**} \in (\Theta^*, \theta_A)$ such that $f(\Theta^{**})C(\Theta^{**}) < -v$; but this implies that there must be another root of $f(\Theta_a)C(\Theta_a) + v = 0$ in the interval (Θ^{**}, θ_A) by intermediate value theorem, which contradicts the assumption that Θ^* is the closest root to θ_A . Therefore, Θ^* is a stable steady state.

- (b) Before achieving the steady state Θ^* , Θ_a continues decreasing due to the non-positiveness of the right-hand side of (3.25a). Moreover, the effective contact line position \hat{X}_{ct} moves to the negative direction since $-v < f(\Theta_a)C(\Theta_a) < 0$.
- (c) When Θ_a arrives at the steady state Θ^* , \hat{X}_{ct} keeps on moving in the negative direction at a constant velocity $d\hat{X}_{ct}/dt = -v$.

Similar results hold in the case of $v < 0$. We can write the stable steady effective contact angle as a function of the drag velocity v , i.e. $\Theta^* = \Theta^*(v)$. This function has the following

properties:

- (i) The steady effective contact angle $\Theta^*(v)$ must be outside the range of the chemical pattern $[\theta_A, \theta_B]$: if $v > 0$, $\Theta^*(v) < \theta_A$ and is not far from θ_A , this is called a receding contact angle; if $v < 0$, $\Theta^*(v) > \theta_B$ and is not far from θ_B , this is called an advancing contact angle.
- (ii) $\Theta^*(v) \rightarrow \theta_A$ as $v \rightarrow 0^+$, while $\Theta^*(v) \rightarrow \theta_B$ as $v \rightarrow 0^-$. In other words, depending on different directions of the quasi-static motion, the steady effective contact angle approaches the lower bound θ_A or the upper bound θ_B of the chemical pattern. This is a consequence of implicit function theorem and the smoothness of the function $f(\Theta_a)C(\Theta_a)$ (see also [figure 6](#) for a sketch).
- (iii) In the extreme case $v = 0$, $\Theta^*(0)$ can be any value on the interval $[\theta_A, \theta_B]$. This can be seen from the averaged dynamics (3.24a) and (3.25a) in three different cases: if the initial contact angle is larger than θ_B , then (C5) with $v = 0$ shows that the apparent contact angle decays exponentially to θ_B ; if the initial contact angle is smaller than θ_A , similar results hold that the apparent contact angle increases exponentially to θ_A ; if the initial contact angle is between θ_A and θ_B , then (3.24a) with $v = 0$ implies that it is already in equilibrium.

From these discussions, we can define the equilibrium apparent contact angle to be any value in the range $[\theta_A, \theta_B]$ when there is chemical roughness on the substrate. The contact line pins when $\Theta_a \in [\theta_A, \theta_B]$; the contact line advances if $\Theta_a > \theta_B$, while the contact line recedes if $\Theta_a < \theta_A$.

REFERENCES

- BLAKE, T.D. 2006 The physics of moving wetting lines. *J. Colloid Interface Sci.* **299** (1), 1–13.
- BLAKE, T.D., BRACKE, M. & SHIKHMURZAEV, Y.D. 1999 Experimental evidence of nonlocal hydrodynamic influence on the dynamic contact angle. *Phys. Fluids* **11** (8), 1995–2007.
- BLAKE, T.D. & DE CONINCK, J. 2011 Dynamics of wetting and Kramers's theory. *Eur. Phys. J. Spec. Top.* **197** (1), 249–264.
- BLAKE, T.D. & HAYNES, J.M. 1969 Kinetics of liquid/liquid displacement. *J. Colloid Interface Sci.* **30** (3), 421–423.
- BONN, D., EGGERS, J., INDEKEU, J., MEUNIER, J. & ROLLEY, E. 2009 Wetting and spreading. *Rev. Mod. Phys.* **81** (2), 739–805.
- CASSIE, A. & BAXTER, S. 1944 Wettability of porous surfaces. *Trans. Faraday Soc.* **40**, 546–551.
- CHAN, T.S., YANG, F. & CARLSON, A. 2020 Directional spreading of a viscous droplet on a conical fibre. *J. Fluid Mech.* **894**, A26.
- CHOI, W., TUTEJA, A., MABRY, J.M., COHEN, R.E. & MCKINLEY, G.H. 2009 A modified Cassie–Baxter relationship to explain contact angle hysteresis and anisotropy on non-wetting textured surfaces. *J. Colloid Interface Sci.* **339**, 208–216.
- CLARKE, A. & STATTERSFIELD, E. 2006 Direct evidence supporting nonlocal hydrodynamic influence on the dynamic contact angle. *Phys. Fluids* **18** (4), 048106.
- COX, R.G. 1983 The spreading of a liquid on a rough solid surface. *J. Fluid Mech.* **131**, 1–26.
- COX, R. 1986 The dynamics of the spreading of liquids on a solid surface. Part 1. Viscous flow. *J. Fluid Mech.* **168**, 169–194.
- COX, R.G. 1998 Inertial and viscous effects on dynamic contact angles. *J. Fluid Mech.* **357**, 249–278.
- DAVIS, M.J. & DAVIS, S.H. 2013 Droplet spreading: theory and experiments. *C.R. Phys.* **14** (7), 629–635.
- DI, Y., XU, X. & DOI, M. 2016 Theoretical analysis for meniscus rise of a liquid contained between a flexible film and a solid wall. *Europhys. Lett.* **113** (3), 36001.
- DOI, M. 2013 *Soft Matter Physics*. Oxford University Press.
- DOI, M. 2015 Onsager principle as a tool for approximation. *Chin. Phys. B* **24**, 020505.
- DOI, M., ZHOU, J., DI, Y. & XU, X. 2019 Application of the Onsager–Machlup integral in solving dynamic equations in nonequilibrium systems. *Phys. Rev. E* **99** (6), 063303.

- DUPONT, J.-B. & LEGENDRE, D. 2010 Numerical simulation of static and sliding drop with contact angle hysteresis. *J. Comput. Phys.* **229** (7), 2453–2478.
- DUSSAN, E.B. 1979 On the spreading of liquids on solid surfaces: static and dynamic contact lines. *Annu. Rev. Fluid Mech.* **11** (1), 371–400.
- DUVIVIER, D., BLAKE, T.D. & DE CONINCK, J. 2013 Toward a predictive theory of wetting dynamics. *Langmuir* **29** (32), 10132–10140.
- EGGERS, J. 2005 Contact line motion for partially wetting fluids. *Phys. Rev. E* **72** (6), 061605.
- EGGERS, J. & EVANS, R. 2004 Comment on “Dynamic wetting by liquids of different viscosity,” by T.D. Blake and Y.D. Shikhmurzaev. *J. Colloid Interface Sci.* **280** (2), 537–538.
- EXTRAND, C.W. 2002 Model for contact angles and hysteresis on rough and ultraphobic surfaces. *Langmuir* **18**, 7991–7999.
- GAO, L. & MCCARTHY, T.J. 2007 How Wenzel and Cassie were wrong. *Langmuir* **23**, 3762–3765.
- GAO, M. & WANG, X.-P. 2012 A gradient stable scheme for a phase field model for the moving contact line problem. *J. Comput. Phys.* **231** (4), 1372–1386.
- DE GENNES, P.-G. 1985 Wetting: statics and dynamics. *Rev. Mod. Phys.* **57** (3), 827–863.
- DE GENNES, P.G., BROCHARD-WYART, F. & QUERE, D. 2003 *Capillarity and Wetting Phenomena*. Springer.
- GOLESTANIAN, R. 2004 Moving contact lines on heterogeneous substrates. *Phil. Trans. R. Soc. Lond. A* **362** (1821), 1613–1623.
- GOLESTANIAN, R. & RAPHAËL, E. 2003 Roughening transition in a moving contact line. *Phys. Rev. E* **67** (3), 031603.
- GUAN, D., WANG, Y., CHARLAIX, E. & TONG, P. 2016a Asymmetric and speed-dependent capillary force hysteresis and relaxation of a suddenly stopped moving contact line. *Phys. Rev. Lett.* **116** (6), 066102.
- GUAN, D., WANG, Y., CHARLAIX, E. & TONG, P. 2016b Simultaneous observation of asymmetric speed-dependent capillary force hysteresis and slow relaxation of a suddenly stopped moving contact line. *Phys. Rev. E* **94** (4), 042802.
- GUO, S., GAO, M., XIONG, X., WANG, Y.J., WANG, X., SHENG, P. & TONG, P. 2013 Direct measurement of friction of a fluctuating contact line. *Phys. Rev. Lett.* **111** (2), 026101.
- GUO, S., XU, X., QIAN, T., DI, Y., DOI, M. & TONG, P. 2019 Onset of thin film meniscus along a fibre. *J. Fluid Mech.* **865**, 650–680.
- GURTIN, M.E., POLIGNONE, D. & VINALS, J. 1996 Two-phase binary fluids and immiscible fluids described by an order parameter. *Math. Models Meth. Appl. Sci.* **6** (06), 815–831.
- HALEY, P.J. & MIKSI, M.J. 1991 The effect of the contact line on droplet spreading. *J. Fluid Mech.* **223**, 57–81.
- HUH, C. & SCRIVEN, L.E. 1971 Hydrodynamic model of steady movement of a solid/liquid/fluid contact line. *J. Colloid Interface Sci.* **35** (1), 85–101.
- ILIEV, S., PESHEVA, N. & ILIEV, P. 2018 Contact angle hysteresis on doubly periodic smooth rough surfaces in Wenzel’s regime: the role of the contact line depinning mechanism. *Phys. Rev. E* **97** (4), 042801.
- JACQMIN, D. 2000 Contact-line dynamics of a diffuse fluid interface. *J. Fluid Mech.* **402**, 57–88.
- JOANNY, J.F. & DE GENNES, P.-G. 1984 A model for contact angle hysteresis. *J. Chem. Phys.* **81** (1), 552–562.
- JOANNY, J. & ROBBINS, M. 1990 Motion of a contact line on a heterogeneous surface. *J. Chem. Phys.* **92** (2), 32063212.
- JOHANSSON, P. & HESS, B. 2018 Molecular origin of contact line friction in dynamic wetting. *Phys. Rev. Fluids* **3** (7), 074201.
- JOHNSON, R.E. JR. & DETTRE, R.H. 1964 Contact angle hysteresis. III. Study of an idealized heterogeneous surfaces. *J. Phys. Chem.* **68**, 1744–1750.
- LINDNER-SILWESTER, T. & SCHNEIDER, W. 2005 The moving contact line with weak viscosity effects—an application and evaluation of Shikhmurzaev’s model. *Acta Mech.* **176** (3), 245–258.
- MAN, X. & DOI, M. 2016 Ring to mountain transition in deposition pattern of drying droplets. *Phys. Rev. Lett.* **116** (6), 066101.
- MARMOTTANT, P. & VILLERMAUX, E. 2004 On spray formation. *J. Fluid Mech.* **498**, 73–111.
- MARMUR, A. & BITTOUN, E. 2009 When Wenzel and Cassie are right: reconciling local and global considerations. *Langmuir* **25**, 1277–1281.
- MISKIS, M.J. & DAVIS, S.H. 1994 Slip over rough and coated surfaces. *J. Fluid Mech.* **273**, 125–139.
- MOHAMMAD KARIM, A., DAVIS, S.H. & KAVEHPOUR, H.P. 2016 Forced versus spontaneous spreading of liquids. *Langmuir* **32** (40), 10153–10158.
- NEUMANN, A.W. & GOOD, R.J. 1972 Thermodynamics of contact angles: I. Heterogeneous solid surfaces. *J. Colloid Interface Sci.* **38**, 341–358.

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- NOLD, A., SIBLEY, D.N., GODDARD, B.D. & KALLIADASIS, S. 2014 Fluid structure in the immediate vicinity of an equilibrium three-phase contact line and assessment of disjoining pressure models using density functional theory. *Phys. Fluids* **26** (7), 072001.
- PAVLIOTIS, G.A. & STUART, A.M. 2008 *Multiscale Methods: Averaging and Homogenization*. Springer.
- PISMEN, L.M. 2002 Mesoscopic hydrodynamics of contact line motion. *Colloids Surf. A* **206** (1), 11–30.
- PISMEN, L.M. & POMEAU, Y. 2000 Disjoining potential and spreading of thin liquid layers in the diffuse-interface model coupled to hydrodynamics. *Phys. Rev. E* **62** (2), 2480–2492.
- PRABHALA, B., PANCHAGNULA, M.V. & VEDANTAM, S. 2013 Three-dimensional equilibrium shapes of drops on hysteretic surfaces. *Colloid Polym. Sci.* **291**, 279–289.
- PRIEST, C., SEDEV, R. & RALSTON, J. 2007 Asymmetric wetting hysteresis on chemical defects. *Phys. Rev. Lett.* **99** (2), 026103.
- QIAN, T., WANG, X.P. & SHENG, P. 2003 Molecular scale contact line hydrodynamics of immiscible flows. *Phys. Rev. E* **68**, 016306.
- QIAN, T., WANG, X.P. & SHENG, P. 2006 A variational approach to moving contact line hydrodynamics. *J. Fluid Mech.* **564**, 333–360.
- RAJ, R., ENRIGHT, R., ZHU, Y., ADERA, S. & WANG, E.N. 2012 Unified model for contact angle hysteresis on heterogeneous and superhydrophobic surfaces. *Langmuir* **28**, 15777–15788.
- RAPHAEL, E. & DE GENNES, P.-G. 1989 Dynamics of wetting with nonideal surfaces. The single defect problem. *J. Chem. Phys.* **90** (12), 7577–7584.
- REN, W., TRINH, P.H. & E, W. 2015 On the distinguished limits of the Navier slip model of the moving contact line problem. *J. Fluid Mech.* **772**, 107–126.
- REN, W. & E, W. 2007 Boundary conditions for the moving contact line problem. *Phys. Fluids* **19** (2), 022101.
- REN, W. & E, W. 2011 Contact line dynamics on heterogeneous surfaces. *Phys. Fluids* **23**, 072103.
- RENARDY, M., RENARDY, Y. & LI, J. 2001 Numerical simulation of moving contact line problems using a volume-of-fluid method. *J. Comput. Phys.* **171** (1), 243–263.
- SAVVA, N. & KALLIADASIS, S. 2011 Dynamics of moving contact lines: a comparison between slip and precursor film models. *Europhys. Lett.* **94** (6), 64004.
- SCHWARTZ, L.W. & ELEY, R. 1998 Simulation of droplet motion on low-energy and heterogeneous surfaces. *J. Colloid Interface Sci.* **202** (1), 173–188.
- SCHWARTZ, L.W. & GAROFF, S. 1985 Contact angle hysteresis on heterogeneous surfaces. *Langmuir* **1**, 219–230.
- SEPPECHER, P. 1996 Moving contact lines in the Cahn–Hilliard theory. *Intl J. Engng Sci.* **34** (9), 977–992.
- SEVENO, D., VAILLANT, A., RIOBOO, R., ADAO, H., CONTI, J. & DE CONINCK, J. 2009 Dynamics of wetting revisited. *Langmuir* **25** (22), 13034–13044.
- SHARMA, A. 1993 Relationship of thin film stability and morphology to macroscopic parameters of wetting in the apolar and polar systems. *Langmuir* **9** (3), 861–869.
- SHIKHMURZAEV, Y.D. 1993 The moving contact line on a smooth solid surface. *Intl J. Multiphase Flow* **19** (4), 589–610.
- SHIKHMURZAEV, Y.D. 2006 Remark on the moving contact line with weak viscosity effects—an application and evaluation of Shikhmurzaev’s model by T. Lindner-Silwester and W. Schneider (Acta Mech. 176, 245–258, 2005). *Acta Mech.* **182** (1), 141–143.
- SHIKHMURZAEV, Y.D. 2007 *Capillary Flows with Forming Interfaces*. Chapman and Hall/CRC.
- SHIKHMURZAEV, Y.D. 2020 Moving contact lines and dynamic contact angles: a litmus test for mathematical models, accomplishments and new challenges. *Eur. Phys. J. Spec. Top.* **229** (10), 1945–1977.
- SHIKHMURZAEV, Y.D. & BLAKE, T.D. 2004 Response to the comment on [J. Colloid Interface Sci. 253 (2002) 196] by J. Eggers and R. Evans. *J. Colloid Interface Sci.* **280** (2), 539–541.
- SIBLEY, D.N., NOLD, A. & KALLIADASIS, S. 2015a The asymptotics of the moving contact line: cracking an old nut. *J. Fluid Mech.* **764**, 445–462.
- SIBLEY, D.N., NOLD, A., SAVVA, N. & KALLIADASIS, S. 2013 The contact line behaviour of solid–liquid–gas diffuse-interface models. *Phys. Fluids* **25** (9), 092111.
- SIBLEY, D.N., NOLD, A., SAVVA, N. & KALLIADASIS, S. 2015b A comparison of slip, disjoining pressure, and interface formation models for contact line motion through asymptotic analysis of thin two-dimensional droplet spreading. *J. Engng Maths* **94** (1), 19–41.
- SIBLEY, D.N., SAVVA, N. & KALLIADASIS, S. 2012 Slip or not slip? A methodical examination of the interface formation model using two-dimensional droplet spreading on a horizontal planar substrate as a prototype system. *Phys. Fluids* **24** (8), 082105.
- SNOEIJER, J.H. & ANDREOTTI, B. 2013 Moving contact lines: scales, regimes, and dynamical transitions. *Annu. Rev. Fluid Mech.* **45**, 269–292.

- SPELT, P.D.M. 2005 A level-set approach for simulations of flows with multiple moving contact lines with hysteresis. *J. Comput. Phys.* **207** (2), 389–404.
- STOEV, K., RAMÉ, E. & GAROFF, S. 1999 Effects of inertia on the hydrodynamics near moving contact lines. *Phys. Fluids* **11** (11), 3209–3216.
- SUI, Y., DING, H. & SPELT, P. 2014 Numerical simulations of flows with moving contact lines. *Annu. Rev. Fluid Mech.* **46**, 97–119.
- SUI, Y. & SPELT, P.D.M. 2013a An efficient computational model for macroscale simulations of moving contact lines. *J. Comput. Phys.* **242**, 37–52.
- SUI, Y. & SPELT, P.D.M. 2013b Validation and modification of asymptotic analysis of slow and rapid droplet spreading by numerical simulation. *J. Fluid Mech.* **715**, 283–313.
- TANNER, L.H. 1979 The spreading of silicone oil drops on horizontal surfaces. *J. Phys. D: Appl. Phys.* **12** (9), 1473.
- VOINOV, O.V. 1976 Hydrodynamics of wetting. *Fluid Dyn.* **11** (5), 714–721.
- WANG, X.P., QIAN, T. & SHENG, P. 2008 Moving contact line on chemically patterned surfaces. *J. Fluid Mech.* **605**, 59–78.
- E, W. 2011 *Principle of Multiscale Modeling*. Cambridge University Press.
- WENZEL, R.N. 1936 Resistance of solid surfaces to wetting by water. *Ind. Engng Chem.* **28**, 988–994.
- WHYMAN, G., BORMASHENKO, E. & STEIN, T. 2008 The rigorous derivative of Young, Cassie–Baxter and Wenzel equations and the analysis of the contact angle hysteresis phenomenon. *Chem. Phys. Lett.* **450**, 355–359.
- WU, C., LEI, S., QIAN, T. & WANG, X. 2010 Stick-slip motion of moving contact line on chemically patterned surfaces. *Commun. Comput. Phys.* **7** (3), 403–422.
- XU, X. 2016 Modified Wenzel and Cassie equations for wetting on rough surfaces. *SIAM J. Appl. Maths* **76** (6), 2353–2374.
- XU, X., DI, Y. & DOI, M. 2016 Variational method for contact line problems in sliding liquids. *Phys. Fluids* **28**, 087101.
- XU, X., DI, Y. & YU, H. 2018 Sharp-interface limits of a phase-field model with a generalized Navier slip boundary condition for moving contact lines. *J. Fluid Mech.* **849**, 805–833.
- XU, X. & WANG, X.P. 2010 Derivation of the Wenzel and Cassie equations from a phase field model for two phase flow on rough surface. *SIAM J. Appl. Maths* **70**, 2929–2941.
- XU, X. & WANG, X.P. 2011 Analysis of wetting and contact angle hysteresis on chemically patterned surfaces. *SIAM J. Appl. Maths* **71**, 1753–1779.
- XU, X. & WANG, X.P. 2013 The modified Cassie’s equation and contact angle hysteresis. *Colloid Polym. Sci.* **291**, 299–306.
- XU, X. & WANG, X.-P. 2020 Theoretical analysis for dynamic contact angle hysteresis on chemically patterned surfaces. *Phys. Fluids* **32** (11), 112102.
- XU, X., ZHAO, Y. & WANG, X.-P. 2019 Analysis for contact angle hysteresis on rough surfaces by a phase field model with a relaxed boundary condition. *SIAM J. Appl. Maths* **79**, 2551–2568.
- YATSYSHIN, P., SAVVA, N. & KALLIADASIS, S. 2015 Wetting of prototypical one-and two-dimensional systems: thermodynamics and density functional theory. *J. Chem. Phys.* **142** (3), 034708.
- YOUNG, T. 1805 An essay on the cohesion of fluids. *Phil. Trans. R. Soc. Lond.* **95**, 65–87.
- YUE, P. 2020 Thermodynamically consistent phase-field modelling of contact angle hysteresis. *J. Fluid Mech.* **899**, A15.
- YUE, P. & FENG, J.J. 2011 Can diffuse-interface models quantitatively describe moving contact lines? *Eur. Phys. J. Spec. Top.* **197** (1), 37–46.
- YUE, P., ZHOU, C. & FENG, J.J. 2010 Sharp-interface limit of the Cahn–Hilliard model for moving contact lines. *J. Fluid Mech.* **645**, 279–294.
- ZHANG, Z. & REN, W. 2019 Distinguished limits of the Navier slip model for moving contact lines in stokes flow. *SIAM J. Appl. Maths* **79**, 1654–1674.
- ZHANG, J. & YUE, P. 2020 A level-set method for moving contact lines with contact angle hysteresis. *J. Comput. Phys.* **418**, 109636.
- ZHOU, J. & DOI, M. 2018 Dynamics of viscoelastic filaments based on Onsager principle. *Phys. Rev. Fluids* **3** (8), 084004.
- ZHOU, M.-Y. & SHENG, P. 1990 Dynamics of immiscible-fluid displacement in a capillary tube. *Phys. Rev. Lett.* **64** (8), 882–885.